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Additional Information

1 **±±Development of a Diesel Surrogate Fuel Library**

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6 **Abstract**

7 Diesel fuel is composed of a complex mixture of hundreds of hydrocarbons that vary globally depending on
8 crude oil sources, refining processes, legislative requirements and other factors. In order to simplify the
9 study of this fuel, researchers create surrogate fuels to mimic the physical and chemical properties of Diesel
10 fuels. This work employed the commercial software Reaction Workbench - Surrogate Blend Optimizer
11 (SBO) to develop a Surrogate Fuel Library containing 18 fuels. Within the fuel library, the cetane number
12 ranges from 35 to 60 (in increments of 5) at threshold soot index (TSI) levels representative of low, baseline
13 and high sooting tendency fuels (TSI = 17, 31 and 48, respectively). The Surrogate Fuel Library provides
14 the component blend ratios and predicted properties for cetane number, threshold soot index, lower
15 heating value, density, kinematic viscosity, molar hydrogen-to-carbon ratio and distillation curve
16 temperatures from T₁₀ to T₉₀. A market petroleum Diesel fuel with a cetane number of 50 and a threshold
17 soot index of 31 was selected as the Baseline Diesel Fuel. The combustion, physical and chemical properties
18 of the Baseline Diesel Fuel were precisely matched by the Baseline Surrogate Fuel. To validate the SBO
19 predicted fuel properties, a set of five surrogate fuels, deviating in cetane number and threshold soot index,
20 were blended and examined with ASTM tests. Good agreement was obtained between the SBO predicted
21 and ASTM measured fuel properties. To further validate the Surrogate Fuel Library, key properties that
22 were effected by altering the component blend ratios to control cetane number and TSI were compared to
23 a set of five market Diesel fuels with good results. These properties included density, viscosity, energy

24 density and the T_{10} and T_{90} distillation temperatures. The Surrogate Fuel Library provided by this work
25 supplies Diesel engine researchers and designers the ability to analytically and experimentally vary fuel
26 cetane number and threshold soot index with fully-representative surrogate fuels. This new capability to
27 independently vary cetane number and threshold soot index provides a means to further enhance the
28 understanding of Diesel combustion and design future combustion systems that improve efficiency and
29 emissions.

30 **Key Words**

31 Diesel fuel, surrogate fuel, Surrogate Fuel Library, fuel properties, cetane number, threshold soot index

32

33 **1. Introduction**

34 The internal combustion Diesel engine is a highly-versatile power plant for industrial applications and
35 personal mobility. Diesel engines enjoy advantages in efficiency, specific torque, durability, scalability and
36 fuel adaptability. As a result of its importance to society, researchers continue to gain understanding and
37 explore novel combustion systems while engine development engineers work to introduce new Diesel
38 combustion technologies into production [1-5]. The continuous improvement of Diesel engine
39 performance, fuel economy, and emissions is required to achieve the complex needs of society.

40 Diesel fuel is composed of hundreds of hydrocarbon species that are not well-characterized. Research has
41 shown that Diesel fuel is primarily composed of four hydrocarbon classes: normal-alkanes, iso-alkanes,
42 cyclo-alkanes and aromatics [6-8]. The aromatic hydrocarbons are classified by the number benzene rings
43 in the molecule. Mono-aromatics have a single benzene ring and polycyclic aromatic hydrocarbons (PAH)
44 contain two or more benzene rings. As a result of this complex and undefined composition, researchers
45 create Diesel surrogate fuels for computational and experimental investigations [9-16]. A surrogate fuel is
46 a simple analog created from a small set of well-defined hydrocarbon species. Often surrogate fuels are
47 designed to mimic a subset of Diesel fuel properties. A fully-representative surrogate fuel is designed to
48 replicate numerous physical, chemical and combustion properties of a full-range petroleum Diesel fuel.
49 Such fuel properties include cetane number, threshold soot index, lower heating value, density, kinematic
50 viscosity, surface tension, distillation temperatures and aromatic content.

51 Surrogate fuels have many applications including spray characterization, chemical kinetic modeling and
52 combustion simulation [17-20]. The application of single-component surrogate fuels, such as n-heptane for
53 Diesel combustion kinetics [21-23] and n-dodecane for Diesel fuel physical properties [24-26], are well-
54 understood, highly utilized and greatly valued. Through combustion simulation or experimental work,
55 single-component surrogates have played a significant role to expand the fundamental understanding of
56 Diesel combustion. As engineering tools, single-component surrogates have guided the development of

57 conventional and novel Diesel combustion systems. However, single-component surrogates cannot fully
58 represent the physical, chemical and combustion properties of Diesel fuels.

59 Recent work has increased the number of well-characterized hydrocarbons that are representative of Diesel
60 fuel and potentially useful as surrogate fuel components [8, 18, 27-31]. These efforts have enabled the
61 development of multi-component surrogate fuels that can more closely replicate the properties of Diesel
62 fuel [32-40]. However, as researchers strive to match the combustion and physical properties of Diesel fuel,
63 the complexity of multi-component surrogate fuels has greatly increased. Surrogates assembled with
64 numerous components exceedingly raise the expense of analytical and experimental implementation. For
65 successful industrialization, the tradeoffs between surrogate complexities and predictive combustion
66 simulation accuracy must be understood, rationalized and optimized for the intended application.

67 Additional forces driving researchers include the understanding that fuel supplies and standards vary
68 regionally and that future Diesel fuels may be considerably different from current fuels. Today, Diesel
69 engine manufacturers encounter a broad range of fuel properties that may influence engine design and the
70 introduction of new technologies. For example, in the United States ASTM D975-16a established a minimum
71 cetane number requirement of 40 [41] whereas in Europe EN 590:2009 required a minimum cetane
72 number of 51 [42]. As a result of variations in fuel properties, Diesel combustion researchers and design
73 engineers require surrogate fuels that provide the capability to independently control two key fuel
74 properties: cetane number and threshold soot index [43]. While doing so other essential Diesel fuel
75 properties such as density, viscosity, heating value and distillation curve temperatures must be reasonably
76 controlled within the range of market fuels. It is believed that the systematic application of multi-
77 component surrogate fuels with independent control of fuel cetane number and threshold soot index will
78 enhance the fundamental understanding of combustion, efficiency and emissions. At the same time,
79 improved surrogates may provide a means for future improvements in Diesel spray modeling, combustion
80 simulation, and predictive NO_x, CO, HC, soot and exhaust particle emissions.

81 This investigation creates a library of fully-representative multi-component surrogate Diesel fuels that are
82 appropriate for both exploratory combustion research and direct application to the engine combustion
83 system design process. The effort balanced complexity and accuracy with usefulness and the ability to
84 industrialize the findings.

85 **2. Objective and Requirements**

86 The objective of this research was to bring multi-component surrogate fuels closer to routine use by the
87 automotive industry. To this end, the following requirements were placed on the surrogate fuels developed
88 through this investigation:

- 89 • The Surrogate Fuel Library must contain a Baseline Surrogate Fuel that closely matches the
90 combustion, physical and chemical properties of a Baseline Petroleum Fuel (market fuel.)
- 91 • The Surrogate Fuel Library must contain surrogate fuels with cetane number ranging from 35 to
92 60 (in increments of 5). In doing so, the library covers potential next-generation fuels which may
93 extend the cetane number range as low as 35 for naphtha-like fuels [44][45] or as high as 60 for
94 synthetic fuels [46][47].
- 95 • The library must contain threshold soot index levels representative of low, baseline, and high
96 sooting fuels. Three TSI levels are required to reproduce potential fuel variations and support
97 future investigations that enhance the understanding of soot and particle emissions.
- 98 • The combustion and physical properties of the surrogate fuels, namely lower heating value, density,
99 viscosity, surface tension, and distillation curve temperatures, must be representative of market
100 Diesel fuels.
- 101 • The number of surrogate fuel components must be kept to a minimum to manage increased
102 complexity, kinetic mechanism size, computational and experimental expenses.

- 103 • To support spray and combustion simulation, the combustion, physical, chemical and temperature-
104 dependent properties of the surrogate components must be available along with validated, detailed
105 kinetic mechanisms.
- 106 • To support experimental work, the surrogate components must be available with high-purity, in
107 large quantities, and must meet safety guidelines for storage, blending and handling.

108 **3. Methodology**

109 *3.1. Master Kinetic Mechanism*

110 As mentioned above, there has been and continues to be substantial progress in the development of detailed
111 kinetic mechanisms for surrogate fuel components. This work employed the ANSYS 2015 Model Fuel
112 Library and the accompanying Diesel Fuel Master Kinetic Mechanism [48]. The kinetic mechanism
113 consisted of 55 fuel components, 5,155 chemical species and 31,084 chemical reactions. The mechanism
114 was accompanied by physical, chemical and thermodynamic properties for the fuel components. The fuel
115 component information was utilized to predict surrogate fuel properties and the kinetic mechanism was
116 used for closed-homogenous gas-phase reactor simulations.

117 *3.2. Surrogate Blend Modeling and Fuel Property Predictions*

118 A review of the literature revealed several methods to formulate surrogate fuels [9, 49-58]. In this work,
119 the Reaction Workbench - Surrogate Blend Optimizer (SBO) was employed to model surrogate fuel
120 properties, understand the impact of various compounds on the surrogate properties, determine the blend
121 mixtures needed to achieve the objectives and predict the surrogate properties [56][59]. The SBO utilized
122 a genetic optimization procedure that minimized the differences between user specified fuel properties and
123 their computed values. Upon iteration and convergence, the SBO delivered the surrogate composition that
124 best matched the properties of the target Diesel fuel. To formulate the surrogate fuel the user selects the
125 surrogate fuel components from the available library. Then target values are assigned to the following

126 surrogate fuel parameters: Cetane Number (CN), Threshold Soot Index (TSI), Lower Heating Value (LHV),
127 density, viscosity, molar hydrogen-to-carbon ratio (molar H/C), and distillation curve temperatures from
128 T₁₀ to T₉₀. Weighting factors may be applied to prioritize the role of each parameter in determining the
129 surrogate blend composition. The SBO performs the optimization then reports the user specified target
130 value and the SBO predicted value for each of the parameters listed above. The component fuel property
131 data, surrogate blend optimization methods and property blend models were provided by the Model Fuel
132 Library [48] and the Reaction Workbench Software and User Manual [59].

133 3.3. *Gas Phase Reactor Simulation*

134 The ignition process was examined for several pure surrogate fuel components and multi-component
135 surrogate fuel formulations developed with the SBO. This was accomplished with 0-dimensional, transient,
136 closed-homogeneous gas-phase reactor simulations using Chemkin-Pro. The reactor volume was constant
137 and the mass was evenly distributed. The reactor was configured without heat loss and the oxidizer was
138 air (nitrogen and oxygen). The matrix of reactor initial conditions were representative of in-cylinder engine
139 conditions for moderate engine speeds and loads.

140 3.4. *Fuel Property Measurements*

141 Market Diesel fuels and surrogate fuels were characterized with the ASTM tests given in **Table 1**. At a
142 nominal 50 cetane number, ASTM D6890 provided a CN reproducibility of 2.618. ASTM D1322 provided a
143 smoke point reproducibility of 3 mm. Threshold Soot Index (TSI) was calculated from the smoke point
144 measurements using the method defined by Calcote and Manos [60].

145 **Table 1.** Measured fuel properties and ASTM procedures.

| Fuel Property | ASTM |
|---------------------------|-------|
| Cetane Number | D6890 |
| Smoke Point | D1322 |
| LHV | D240N |
| Density | D4052 |
| Viscosity | D445 |
| Lubricity | D6079 |
| Hydrogen and Carbon | D5291 |
| Sulfur | D7039 |
| Distillation Temperatures | D86 |
| Hydrocarbon Classes | D1319 |
| Aromatic Content | D5186 |
| Surface Tension | D3825 |

146 *3.5. Surrogate Fuel Development*

147 A baseline Diesel fuel was selected to provide target fuel properties for the development of a baseline
148 surrogate fuel. Then a Diesel surrogate palette containing 13 hydrocarbon species was selected from 55
149 potential surrogate fuel components. A methodology which included the Reaction Workbench – Surrogate
150 Blend Optimizer was developed to determine the surrogate fuel components and the blend formulations to
151 achieve the objective and requirements in Section 2. Given the surrogate components and the fuel property
152 target values, a baseline surrogate fuel was formulated to closely match the properties of the baseline Diesel
153 fuel. A set of blending rules were developed to guide the formulation of the remaining surrogate fuels. The
154 methodology and predicted fuel properties were validated. A set of surrogate fuels were blended and
155 analyzed using ASTM fuel property tests and the measured properties were compared to the predicted fuel
156 properties.

157 *3.5.1. Baseline Diesel Fuel*

158 In this work the baseline Diesel fuel was defined as an available market fuel which could be used for engine
159 and vehicle testing. Several market fuel samples from the USA, Europe and Canada were evaluated. Upon

160 review, a market fuel with a cetane number of 50 and a TSI value of 31 was selected as the baseline Diesel
161 fuel. Fuel properties for the baseline and several market Diesel fuels are summarized in **Table 2**.

162 **Table 2.** Measured properties of the baseline Diesel fuel and several market Diesel fuels.

| Property | Baseline Fuel | Market Fuel #1 | Market Fuel #2 | Market Fuel #3 | Market Fuel #4 | Market Fuel #5 |
|----------------------|---------------|----------------|----------------|----------------|----------------|----------------|
| Cetane Number | 50.9 | 47.6 | 45.0 | 50.4 | 55.8 | 44.2 |
| LHV (MJ/kg) | 43.00 | 42.97 | 43.04 | 43.19 | 43.50 | 43.08 |
| Density (g/ml) | 0.849 | 0.855 | 0.839 | 0.836 | 0.809 | 0.839 |
| Kin. Viscosity (cSt) | 3.063 | 3.094 | 2.266 | 2.631 | 1.821 | 2.257 |
| T ₁₀ (°C) | 227 | 223 | 204 | 187 | 197 | 200 |
| T ₉₀ (°C) | 312 | 314 | 312 | 326 | 269 | 303 |
| Alkanes (%v/v) | 76.0 | 65.2 | 72.3 | 81.9 | 92.4 | 80.7 |
| Alkenes (%v/v) | 7.5 | 14.0 | 6.8 | 5.0 | 4.1 | 3.0 |
| Aromatics (%v/v) | 16.5 | 20.8 | 20.9 | 13.1 | 3.5 | 16.3 |

163

164 3.5.2. Diesel Surrogate Palette

165 The complete list of 55 surrogate components in the 2015 Model Fuel Library were studied. Fuel properties
166 such as cetane number, TSI, LHV, density, viscosity, and boiling point were analyzed. The first task was to
167 reduce the list of 55 components to manageable number. The following guidelines were applied to remove
168 fuel species from consideration:

- 169 • Remove hydrocarbon classes that were not typically present in Diesel fuel in substantial volume
170 (<10%v/v). For example, alcohols, ethers, hydrogen, hydrogen sulfide.
- 171 • Remove species that had boiling points that were well beyond the distillation temperature range
172 of the target Diesel fuel. For example, most alkenes have low boiling points.
- 173 • Remove species that were problematic for blending and conducting experimental investigations.
174 For example, eicosane and naphthalene have high melting points.

- 175 • Use a single species to represent a group of species with similar properties. For example, m-xylene
 176 was used to represent several aromatics including benzene, ethylbenzene, o-xylene, p-xylene and
 177 n-propylbenzene.

178 This process of analysis and species removal resulted in a Diesel surrogate palette with 13 hydrocarbon
 179 species distributed between four hydrocarbon classes. The surrogate palette and key fuel properties are
 180 given in **Table 3**.

181 **Table 3.** Hydrocarbon classes and species selected for the surrogate palette.

| | Cetane Number | TSI | LHV (MJ/kg) | Density (g/ml) | Boiling Point (°C) |
|------------------------|---------------|-----|-------------|----------------|--------------------|
| <i>n-Alkanes</i> | | | | | |
| n-Hexadecane | 100 | 6 | 45.23 | 0.773 | 287 |
| n-Dodecane | 83.8 | 6 | 44.23 | 0.750 | 216 |
| n-Decane | 76.7 | 4.5 | 44.56 | 0.730 | 174 |
| n-Heptane | 54.4 | 2.7 | 44.56 | 0.683 | 98 |
| <i>iso-Alkanes</i> | | | | | |
| Heptamethylnonane | 15 | 21 | 44.38 | 0.793 | 240 |
| iso-Octane | 14 | 6.8 | 44.65 | 0.692 | 99 |
| <i>cyclo-Alkanes</i> | | | | | |
| Decahydronaphthalene | 44 | 20 | 43.02 | 0.896 | 187 |
| Methylcyclohexane | 22.5 | 5 | 43.72 | 0.770 | 101 |
| Cyclohexane | 18.5 | 3.5 | 43.98 | 0.779 | 81 |
| <i>Aromatics</i> | | | | | |
| 1-Methylnaphthalene | 0 | 100 | 40.27 | 1.001 | 245 |
| 1,2,4-Trimethylbenzene | 8.9 | 51 | 41.64 | 0.876 | 169 |
| m-Xylene | 2.6 | 51 | 40.81 | 0.864 | 139 |
| Toluene | 2.6 | 40 | 40.72 | 0.865 | 111 |

182 **3.5.3. Surrogate Components and Blend Formulation**

183 A detailed investigation was conducted to identify the surrogate components from **Table 3** that could best
 184 achieve the requirements set forth in Section 2 and create a baseline surrogate fuel that closely matched
 185 properties of the baseline Diesel fuel given in **Table 2**. The Surrogate Blend Optimizer was used to generate
 186 numerous multi-component surrogate fuels. The number of components from the surrogate palette ranged

187 from 2 through 8. The target value for CN was 50 and TSI was 31. The weighting factors for these targets
188 were set at 10.0 because matching the CN and TSI were given the highest priority. The measured values for
189 the baseline Diesel fuel were used as the target values for LHV, density, viscosity, molar H/C, and T₁₀ to T₉₀.
190 A weighting factor of 1.0 was used for these targets. Sensitivity studies were conducted to identify the
191 surrogate palette components that had small effects on matching the baseline Diesel fuel properties. The
192 influences could have been considered small due to the impact of the component properties or a lesser
193 component volume fraction determined by the optimizer (<5%v/v).

194 The investigation concluded that a four-component surrogate best achieved the requirements given in
195 Section 2. The four components included n-hexadecane to represent the n-alkane class, 2,2,4,4,6,8,8-
196 heptamethylnonane to represent the iso-alkane class, decahydronaphthalene to represent the cyclo-alkane
197 class, and the aromatics were represented by 1-methylnaphthalene. General information and properties
198 for the four surrogate components are provided in **Table 4**. The volume fractions for the baseline surrogate
199 fuel components were: n-hexadecane=0.37, heptamethylnonane=0.33, decahydronaphthalene=0.18 and 1-
200 methylnaphthalene=0.12. The SBO predicted properties for the baseline surrogate fuel closely matched the
201 ASTM measured properties for the baseline Diesel fuel. The results are provided in **Table 5** and discussed
202 in Section 4.1.

203 **Table 4.** The four hydrocarbon species used to formulate the surrogate fuels.

| Parameter | n-Hexadecane | Heptamethyl- nonane | Decahydro- naphthalene | 1-Methyl- naphthalene |
|---------------------------|---------------------------------|---------------------------------|---------------------------------|---------------------------------|
| Hydrocarbon Class | n-Alkane | iso-Alkane | cyclo-Alkane | Aromatic |
| Chemical Formula | C ₁₆ H ₃₄ | C ₁₆ H ₃₄ | C ₁₀ H ₁₈ | C ₁₁ H ₁₀ |
| Molecular Weight (g/mol) | 226.45 | 226.45 | 138.25 | 142.2 |
| CAS Number | 544-76-3 | 4390-04-9 | 91-17-8 | 90-12-0 |
| Purity (%) | 99 | 87 | 99 | 97 |
| Cetane Number | 100 | 15 | 44 | 0 |
| Threshold Soot Index | 6 | 21 | 20 | 100 |
| LHV (MJ/kg) | 45.23 | 44.38 | 43.02 | 40.27 |
| Density (g/ml) | 0.773 | 0.793 | 0.896 | 1.001 |
| Kinematic Viscosity (cSt) | 3.975 | 4.293 | 2.254 | 2.861 |
| Boiling Point (°C) | 287 | 240 | 187 | 242 |

204 Following the development of baseline surrogate fuel, blending rules were created to guide the formulation
 205 of the remaining surrogates. First, the volume fractions of n-hexadecane and heptamethylnonane would be
 206 tuned to control cetane number while the sum of the volume fractions for these two components should be
 207 held close to 0.7. Second, the volume fractions of decahydronaphthalene and 1-methylnaphthalene would
 208 be adjusted to control TSI while the sum of the volume fractions for these two components should be held
 209 near to 0.3. And finally, while formulating the surrogate fuels a general tolerance of ± 1 was established for
 210 cetane number and TSI. This tolerance was set within the ASTM measurement reproducibility for these
 211 properties. The application of these blending rules moderated the fuel properties to reasonable and
 212 consistent values as the blend formulations were adjusted to independently control fuel cetane number and
 213 TSI.

214 The blending rules and the Surrogate Blend Optimizer were then used to formulate the fuels for the
 215 Surrogate Fuel Library. For this exercise, the SBO input target values were the four surrogate component
 216 volume fractions instead of the fuel properties. As a result, the SBO simply calculated the fuel properties
 217 for the input formulation (there was no optimization). With this technique, the blending rules were easily
 218 applied and formulations were developed for each surrogate fuel. The volume fractions of n-hexadecane

219 and heptamethylnonane were adjusted to achieve the target CN values and the volume fractions of
220 decahydronaphthalene and 1-methylnaphthalene were adjusted to achieve the target TSI values.
221 Throughout the process, the remaining predicted properties (LHV, density, etc.) were monitored. To create
222 surrogate fuels with the lowest possible sooting tendency, a set of fuels were formulated without 1-
223 methylnaphthalene. Hence, these surrogates contained three components that were all saturated
224 hydrocarbon compounds (no carbon-carbon double bonds or benzene rings).

225 A naming convention was created to identify the surrogate fuels. The convention used the prefix CN
226 followed the target cetane number, an underscore, then the prefix TSI followed by the target threshold soot
227 index value. Thus, baseline surrogate fuel that had a target CN of 50 and a target TSI of 31 was named
228 CN50_TSI31.

229 **4. Results**

230 *4.1. Baseline Diesel and Baseline Surrogate Fuel Property Comparison*

231 ASTM fuel property test results for the baseline Diesel fuel and the baseline surrogate fuel CN50_TSI31 are
232 provided in **Table 5**. While formulating CN50_TSI31, matching the target cetane number and target TSI
233 were given the highest priority (weighting factor = 10) followed by density, heating value and viscosity.
234 There was less flexibility towards matching the distillation curve. This was a result of the decision to limit
235 the surrogate to four components coupled with difficulties handling hydrocarbons with high melting points.
236 A lubricity improver was added to the surrogate fuel at a concentration of 100ppm to achieve the lubricity
237 of the market Diesel fuel.

238 **Table 5.** ASTM measured properties of the baseline Diesel fuel compared with the ASTM measured and
 239 SBO predicted properties of the baseline surrogate fuel CN50_TSI31.

| Fuel Property | Units | Baseline Diesel Fuel (Measured) | Baseline Surrogate Fuel (Measured) | Baseline Surrogate Fuel (Predicted) |
|--------------------------------|-------|---------------------------------|------------------------------------|-------------------------------------|
| Cetane Number | | 50.9 | 50.1 | 49.9 |
| Smoke Point | mm | 19.0 | 18.8 | |
| Threshold Soot Index | | 31.0 | 33.7 | 31.5 |
| Lower Heating Value | MJ/kg | 43.004 | 42.857 | 43.81 |
| Density at 15°C | g/ml | 0.849 | 0.831 | 0.821 |
| Kinematic Viscosity at 40°C | cSt | 3.06 | 2.41 | 2.728 |
| Kinematic Viscosity at 120°C | cSt | 0.99 | 0.89 | |
| Surface Tension | N/m | 0.0312 | 0.0273 | |
| Lubricity – Wear Scar Diameter | µm | 489 | 440 | |
| T ₁₀ | °C | 226.8 | 220.6 | 229.2 |
| T ₉₀ | °C | 311.7 | 272.4 | 277.7 |
| Alkane Hydrocarbons | %v/v | 76.0 | 82.7 | 88.0 |
| Alkene Hydrocarbons | %v/v | 7.5 | 4.9 | 0.0 |
| Aromatic Hydrocarbons | %v/v | 16.5 | 12.4 | 12.0 |
| Total Aromatics | %m/m | 16.4 | 16.4 | |
| Mono-Cyclic Aromatics | %m/m | 16.2 | 0.4 | |
| Polycyclic Aromatics | %m/m | 0.2 | 16.0 | |
| Carbon Content | %m/m | 86.38 | 86.07 | |
| Hydrogen Content | %m/m | 13.42 | 13.51 | |
| Sulfur Content | ppm | 9.4 | 1405 | |
| H/C Molar Ratio | molR | 1.85 | 1.87 | 1.87 |
| Stoichiometric A/F Ratio | | 14.58 | 14.60 | |

240

241 The baseline Diesel fuel had a measured cetane number of 50.9 compared to 50.1 for CN50_TSI31. At a
 242 nominal 50 cetane number, ASTM D6890 provided a CN reproducibility of 2.618 [61]. The ASTM
 243 measurements suggest the baseline Diesel fuel and surrogate CN50_TSI31 match cetane number within the
 244 reproducibility of the test procedure.

245 ASTM D1322 provided a smoke point reproducibility of 3 mm [62]. The fuels test result show a smoke point
 246 of 19 mm for the baseline Diesel and 18.8 mm for CN50_TSI31. A match within the measurement
 247 reproducibility. The TSI for the baseline Diesel fuel was 31.0 compared to 33.7 for the surrogate
 248 CN50_TSI31.

249 The baseline Diesel LHV was 43.004 MJ/kg while surrogate CN50_TSI31 was 42.857 MJ/kg. The difference
250 between the Diesel and surrogate fuels was only 0.3%. ASTM D240N provided a reproducibility of 0.4
251 MJ/kg [63]. With an absolute difference of only 0.147 MJ/kg between the two fuels, it was concluded that
252 CN50_TSI31 matched the lower heating value of the baseline Diesel fuel within the reproducibility of the
253 measurements.

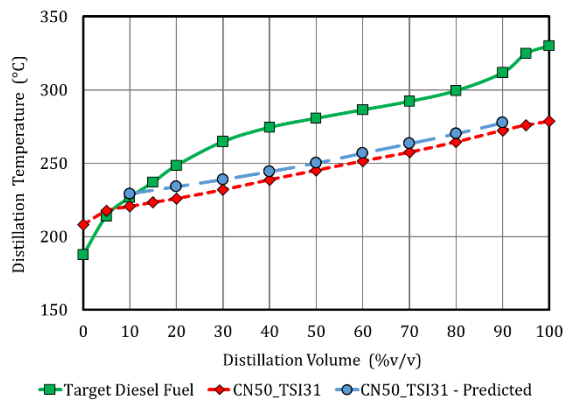
254 ASTM tests reported densities of 0.849 g/ml for the baseline Diesel and 0.831 g/ml for CN50_TSI31; a
255 difference of only 2.1%. Typical Diesel fuel has a nominal density of 0.85 g/ml and ranges between 0.82
256 and 0.88 g/ml [6]. At 15°C, the reproducibility of ASTM D4052 is reported at 0.0052 g/ml [64].

257 At 40°C, the kinematic viscosity of the baseline Diesel fuel was 3.06 cSt compared to 2.41 cSt for surrogate
258 CN50_TSI31. ASTM D975 established a viscosity requirement of 1.9-4.1 cSt for No.2-D Diesel fuel [41].
259 Diesel fuel viscosity drops rapidly as temperature increases. At 120°C, the baseline Diesel value dropped to
260 0.99 cSt and the surrogate fuel dropped to 0.89 cSt. Under fully-warmed-up engine operating conditions,
261 this small difference in viscosity is considered to be negligible.

262 The surface tension of the baseline Diesel was measured at 0.0312 N/m while the CN50_TSI31 surrogate
263 was 0.0273 N/m; a 12% difference. In other works, Wang, et al. reported a Diesel fuel surface tension of
264 0.028 N/m which was very close to surrogate CN50_TSI31 [65]. Ra, et al. investigated the effects of fuel
265 properties with Diesel and Biodiesel surrogates and reported approximately 0.026 N/m for a Diesel
266 surrogate fuel [66]. At 25°C, the DIPPR correlation calculates the surface tension of n-dodecane to be 0.025
267 N/m [67]. The surface tension of CN50_TSI31 is well within the range of previously reported values.

268 The distillation curves for the baseline Diesel and surrogate fuels are presented in **Figure 1**. Test results
269 showed reasonable agreement over the entire distillation temperature range. Surrogate CN50_TSI31 had a
270 T₁₀ distillation temperature that was only 6°C less than the baseline Diesel fuel. In the mid-range from T₃₀
271 to T₈₀ the surrogate was 35°C lower. At the final boiling point, CN50_TSI31 was 51°C lower than the baseline

272 Diesel fuel. The lower distillation temperatures for CN50_TSI31 resulted from the decision to limit the
273 number of surrogate components to four and exclude n-alkanes larger than n-hexadecane. The SBO
274 predicted distillation temperatures for surrogate CN50_TSI31 were slightly higher than the ASTM measured
275 values for the surrogate fuel.



276

277 **Figure 1.** Distillation curves for the baseline Diesel fuel and surrogate CN50_TSI31.

278 The surrogate and baseline Diesel fuels were characterized by two ASTM test methods that provided a
279 simplified view of the hydrocarbon classes. On a volume basis, CN50_TSI31 had slightly more alkanes than
280 the baseline Diesel fuel. The surrogate was precisely blended to contain 88% alkanes while the test results
281 showed 82.7% for the surrogate and 76% for the baseline Diesel fuel. ASTM D1319 test showed that the
282 baseline Diesel fuel contained 7.5% alkenes. The surrogate was formulated without alkenes. However, test
283 results showed the surrogate fuel contained 4.9% alkenes. This may have resulted from detection errors.
284 There is also the possibility that some alkenes were present as impurities in the surrogate components. If
285 alkenes were present in the surrogate fuel, the concentrations were small and can be neglected for the
286 purposes of this work.

287 On a volume basis, CN50_TSI31 contained slightly less aromatics than the baseline Diesel fuel. CN50_TSI31
288 was precisely blended to contain 12%v/v aromatics which is in very good agreement with the ASTM result.

289 On a mass basis, the total aromatics were the same for both fuels. This was an expected result because the
290 baseline Diesel fuel contained mono-cyclic aromatics which generally have lower densities than polycyclic
291 aromatics. CN50_TSI31 was formulated with 1-methylnaphthalene; a polycyclic aromatic with a density
292 that is roughly 15% higher than many mono-cyclic aromatics.

293 The fuel carbon and hydrogen content matched very well with less than 1% difference. The Diesel fuel had
294 9.4 ppm sulfur while the surrogate fuel contained 1405 ppm. Testing revealed that 1-methylnaphthalene
295 was the source of the sulfur. While present, the sulfur concentration was considered too low to have a
296 significant impact on the spray, combustion and emission performance of the surrogate fuels.

297 *4.2. Surrogate Fuel Library*

298 The surrogate fuel names and several predicted properties are given in **Table 6**. The blend formulations
299 and a complete list of the predicted fuel properties are given in the Appendix. The surrogates are grouped
300 by the TSI value and sorted in order of increasing CN.

301 **Table 6.** The Surrogate Fuel Library containing the SBO predicted fuel properties for 18 fuels with varying
 302 CN and TSI. Fuel CN50_TSI31 was developed to match the baseline Diesel fuel.

| Fuel | CN | TSI | LHV (MJ/kg) | Density (g/ml) | Viscosity (cSt) | Molar H/C | T ₁₀ (°C) | T ₉₀ (°C) |
|------------|------|------|----------------|-------------------|--------------------|--------------|-------------------------|-------------------------|
| CN35_TSI17 | 34.8 | 19.0 | 44.04 | 0.806 | 2.737 | 2.017 | 215 | 262 |
| CN40_TSI17 | 40.7 | 18.2 | 44.09 | 0.805 | 2.724 | 2.017 | 216 | 269 |
| CN45_TSI17 | 45.0 | 17.6 | 44.13 | 0.804 | 2.714 | 2.017 | 217 | 273 |
| CN50_TSI17 | 53.5 | 16.6 | 44.16 | 0.806 | 2.654 | 2.016 | 216 | 278 |
| CN55_TSI17 | 55.2 | 16.2 | 44.23 | 0.803 | 2.692 | 2.016 | 219 | 280 |
| CN60_TSI17 | 60.3 | 15.5 | 44.28 | 0.802 | 2.680 | 2.016 | 221 | 281 |
| CN35_TSI31 | 35.5 | 31.1 | 43.74 | 0.820 | 2.756 | 1.897 | 224 | 266 |
| CN40_TSI31 | 40.5 | 32.8 | 43.73 | 0.822 | 2.749 | 1.873 | 227 | 272 |
| CN45_TSI31 | 45.2 | 30.9 | 43.80 | 0.820 | 2.736 | 1.884 | 227 | 275 |
| CN50_TSI31 | 49.9 | 31.5 | 43.81 | 0.821 | 2.728 | 1.872 | 229 | 278 |
| CN55_TSI31 | 55.0 | 30.8 | 43.86 | 0.820 | 2.716 | 1.872 | 231 | 280 |
| CN60_TSI31 | 59.2 | 30.3 | 43.90 | 0.819 | 2.707 | 1.871 | 232 | 282 |
| CN35_TSI48 | 34.8 | 48.8 | 43.290 | 0.842 | 2.788 | 1.725 | 239 | 268 |
| CN40_TSI48 | 39.9 | 48.1 | 43.340 | 0.841 | 2.776 | 1.724 | 240 | 272 |
| CN45_TSI48 | 45.0 | 47.5 | 43.380 | 0.840 | 2.765 | 1.724 | 242 | 276 |
| CN50_TSI48 | 48.4 | 48.9 | 43.310 | 0.845 | 2.720 | 1.693 | 242 | 278 |
| CN55_TSI48 | 55.2 | 46.2 | 43.470 | 0.839 | 2.742 | 1.723 | 245 | 280 |
| CN60_TSI48 | 59.9 | 46.8 | 43.490 | 0.839 | 2.734 | 1.711 | 248 | 282 |

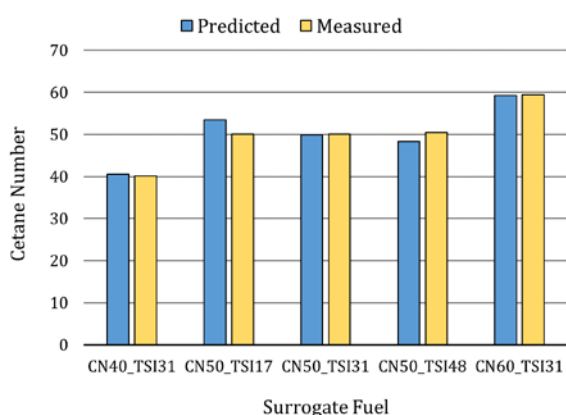
303 For a given TSI value (e.g., TSI=17), as the CN increased from 35 to 60 the other fuel properties remained
 304 nearly constant. Since the properties of n-hexadecane (CN=100) and heptamethylnonane (CN=15) were
 305 very similar, adjusting their volume fractions to control the CN had little impact on the other properties.
 306 However, the distillation temperatures slightly increased since n-hexadecane had a higher boiling point.

307 For a given CN, as TSI values increased, the LHV and molar H/C decreased while the density and distillation
 308 temperatures increased. This was primarily due to the impact of increasing the volume fraction of 1-
 309 methylnaphthalene and decreasing the decahydronaphthalene to control the TSI value.

310 4.3. Predicted and Measured Property Comparison

311 The Surrogate Blend Optimizer provided property predictions for each surrogate fuel. It was crucially
312 important to validate predicted fuel properties. To that end, five surrogate fuels were precision blended
313 and characterized with ASTM fuel property tests. The surrogates included the baseline surrogate
314 CN50_TSI31. Fuels CN40_TSI31 and CN60_TSI31 were selected to independently vary the cetane number
315 and fuels CN50_TSI17 and CN50_TSI48 were chosen to independently vary the TSI values. The measured
316 fuel properties were compared to the values predicted by the Surrogate Blend Optimizer.

317 **Figure 2** compares the predicted and measured cetane numbers. As the cetane increased for fuels
318 CN40_TSI31, CN50_TSI31 and CN60_TSI31 the predicted values were precisely matched by the measured
319 results. The differences were within the reproducibility of the ASTM D6890 procedure. For the second
320 comparison, fuels CN50_TSI17, CN50_TSI31 and CN50_TSI48 showed some cetane number variation. Fuel
321 CN50_TSI17 had a predicted cetane number of 53.5 compared to a measured value of 50.1. In the case of
322 fuel CN50_TSI48, the predicted cetane number was 48.4 compared to the measured value of 50.5. For these
323 five fuels, the average difference between the predicted and measured cetane numbers was only 1.3 and the
324 maximum observed difference between a predicted and measured cetane number was 3.4.

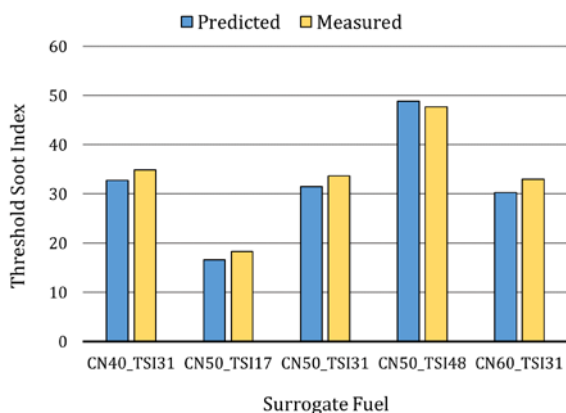


325

326 **Figure 2.** A comparison of predicted and measured cetane numbers for five surrogate fuels.

327 *4.3.1. Threshold Soot Index*

328 The TSI results are given in **Figure 3.** For the first comparison, as cetane number was increased for fuels
329 CN40_TSI31, CN50_TSI31 and CN60_TSI31, the measured TSI values were slightly greater than the
330 predicted values. For the second comparison, as TSI values were increased from 17 to 48 (fuels
331 CN50_TSI17, CN50_TSI31 and CN50_TSI48) the predicted and measured values were in good agreement.
332 For all of the fuels, the average difference between the predicted and measured TSI values was 2.0 and the
333 maximum observed difference between a predicted and measured TSI value was 2.7. These results were
334 considered to be within the reproducibility of the TSI value when obtained from the ASTM smoke point
335 measurement and calculated with the method defined by Calcote and Manos [60].



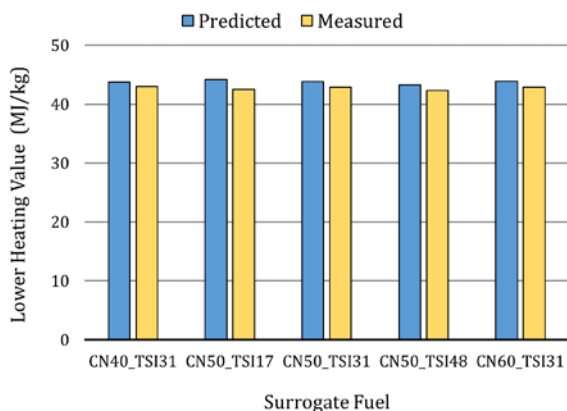
336

337 **Figure 3.** A comparison of predicted and measured TSI values for five surrogate fuels.

338 *4.3.2. Lower Heating Value*

339 The results for lower heating value are given in **Figure 4.** Relatively small changes in the LHV were
340 observed as the blend ratios were adjusted to control cetane number and TSI. The measured LHV was
341 consistently less than the predicted values. For the predicted values, the average LHV was 43.8 MJ/kg with

342 a range of 0.9 MJ/kg. For the measured values, the average was 42.7 MJ/kg with a range of 0.7 MJ/kg. The
343 average difference between the predicted and measured LHV was 1.06 MJ/kg (2.5%) and the maximum
344 observed difference was 1.65 MJ/kg (3.8%).

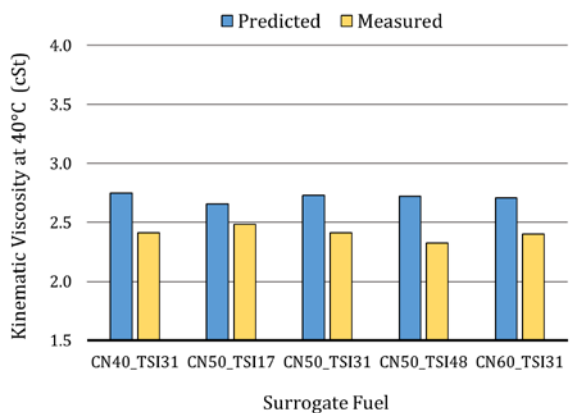


345

346 **Figure 4.** A comparison of predicted and measured LHV for five surrogate fuels.

347 4.3.3. Kinematic Viscosity

348 **Figure 5** shows that adjusting the blend ratios to control cetane number and TSI value had little impact on
349 the kinematic viscosity. The predicted values were slightly greater than the measured values. For these
350 five surrogates, the predicted values averaged 2.71 cSt while the measured values averaged 2.41; a
351 difference of only 0.3 cSt. The maximum observed difference was 0.39 cSt.

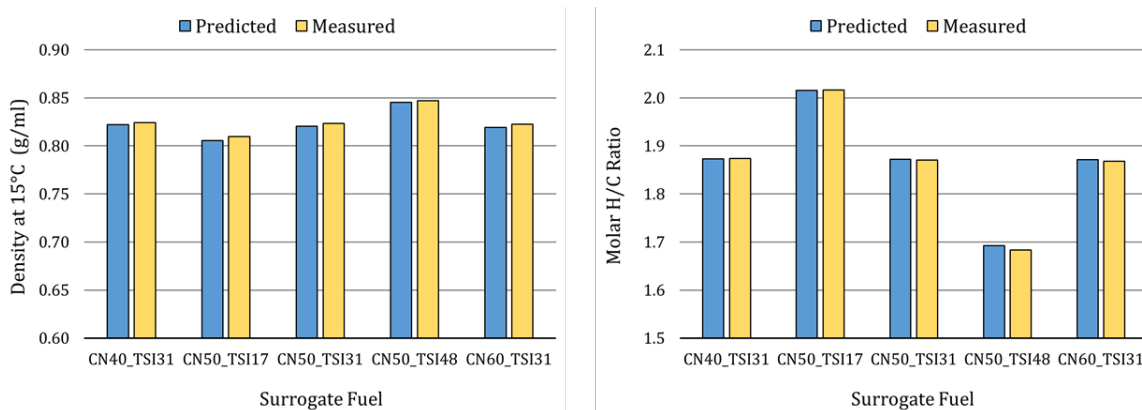


352

353 **Figure 5.** A comparison of predicted and measured kinematic viscosities for five surrogate fuels.

354 *4.3.4. Density and Molar H/C*

355 As shown in **Figure 6**, very close agreement was obtained between the predicted and measured values for
 356 density and molar H/C. For density, the predicted values for the five surrogate fuels ranged from 0.806 to
 357 0.845 g/ml. The average difference between the predicted and measured density was only 0.003 g/ml with
 358 a maximum difference of only 0.004 g/ml. The molar H/C ranged from 1.693 to 2.016. The average
 359 difference between the predicted and measured values was only 0.003 and the maximum difference was
 360 0.009.

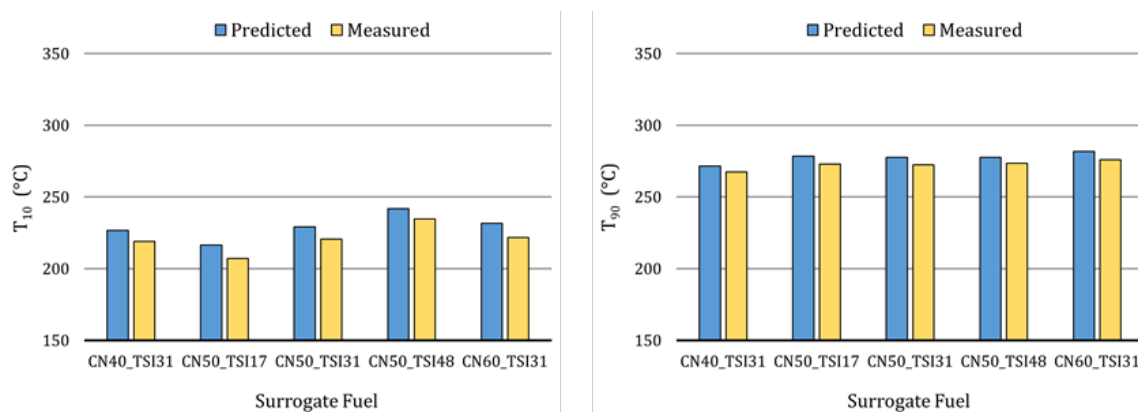


361

362 **Figure 6.** A comparison of predicted and measured density and molar H/C values for five surrogate fuels.

363 4.3.5. T_{10} and T_{90} Distillation Temperatures

364 The predicted surrogate fuel distillation curves were evaluated with the T_{10} and T_{90} distillation
 365 temperatures, see **Figure 7**. On average, the predicted temperatures for T_{10} were 8.6°C greater than the
 366 measured values. The maximum observed difference was 10°C. A modestly increasing T_{10} trend was
 367 observed in surrogates CN50_TSI17, CN50_TSI31 and CN50_TSI48. This was due to a decrease in the
 368 decahydronaphthalene volume fraction and an increase in the 1-methylnaphthalene as the TSI value was
 369 raised from 17 to 48. For these fuels, the predicted values for T_{90} were slightly greater than the measured
 370 values. On average, the predicted temperatures for T_{90} were 4.9°C higher than the measured values. The
 371 maximum observed difference between the predicted and measured T_{90} was 5.7°C.



372

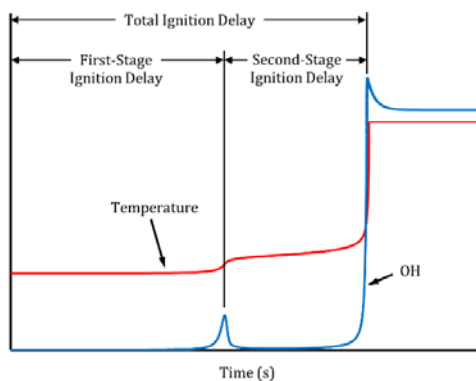
373 **Figure 7.** A comparison of predicted and measured T_{10} and T_{90} distillation temperatures for five surrogate
 374 fuels.

375 *4.4. Ignition Delay Evaluation*

376 The fuel cetane number provides a global indication of ignition quality. It is also necessary to understand
 377 the potential for the surrogate fuels to exhibit two-stage ignition, Negative Temperature Coefficient (NTC)
 378 and Zero Temperature Coefficient (ZTC) phenomenon [68]. In addition, the ignition behavior should
 379 respond as expected to blend formulations that control CN and TSI. To answer these questions, closed-
 380 homogeneous reactor simulations were conducted using the surrogate palette components and a set of five
 381 surrogate fuels. The fuels included CN50_TSI31 (baseline surrogate) coupled with CN40_TSI31 and
 382 CN60_TSI31 to explore the cetane number effect and the baseline surrogate coupled with fuels CN50_TSI17
 383 and CN50_TSI48 to evaluate the impact of TSI with a constant CN.

384 Many of the reactor simulations demonstrated two-stage ignition, NTC and ZTC phenomenon. Regarding
 385 two-stage ignition, for this work the first-stage ignition was determined by the occurrence of the first
 386 hydroxyl radical (OH) peak and the total ignition delay was established by the second OH peak (see **Figure**
 387 **8**). Several pure fuel components and surrogate fuels exhibited the NTC or ZTC phenomenon. For NTC,

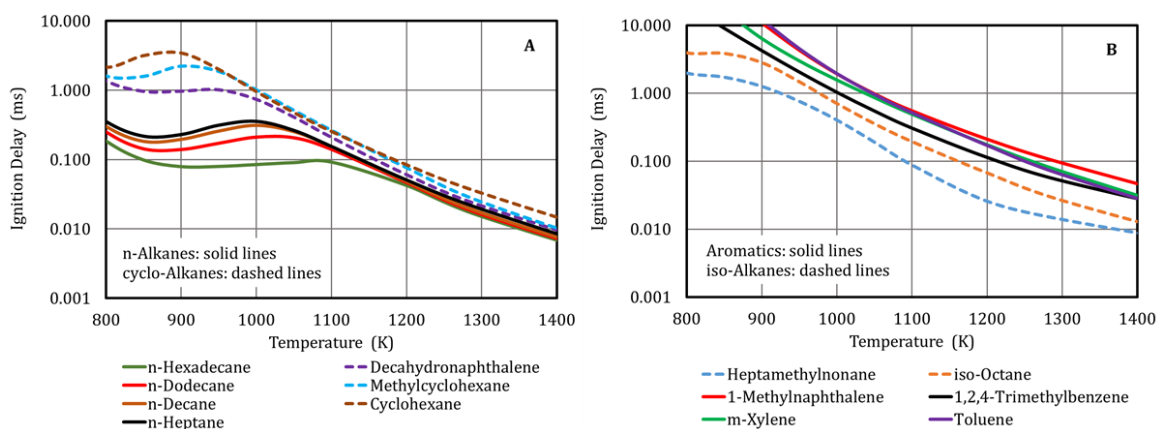
388 increases in reactor initial temperature increased the ignition delay period as opposed to shortening the
389 ignition delay. For ZTC, increased temperature had little impact on ignition delay.



390

391 **Figure 8.** An example of a closed-homogeneous reactor simulation showing two-stage ignition delays
392 identified by peak OH concentrations.

393 To comprehend the ignition characteristics of the surrogate fuel palette, **Figure 9** shows the impact of
394 temperature and hydrocarbon specie on the total ignition delay for reactor initial conditions of $\Phi=1.0$ and
395 pressure=50 bar. **Figure 9A** contains n-alkanes and cyclo-alkanes while **Figure 9B** includes aromatics and
396 iso-alkanes. The four hydrocarbon classes exhibited unique behaviors. The n-alkanes had the shortest
397 ignition delays and the largest NTC regions. The cyclo-alkanes and iso-alkanes had longer ignition delays
398 and smaller NTC regions or even ZTC regions. For these hydrocarbons, the NTC/ZTC regions occurred at
399 ignition delays greater than 1.0 ms. The aromatics had the longest ignition delays and did not exhibit NTC
400 or ZTC behavior under these conditions. Compared to the other n-alkanes, n-hexadecane demonstrated a
401 lesser NTC behavior that occurred over a broader temperature range. In fact, under these reactor
402 conditions the n-hexadecane approached the ZTC phenomenon. Decahydronaphthalene exhibited
403 NTC/ZTC in the 850-950K region while heptamethylnonane approached ZTC near 800-850K.



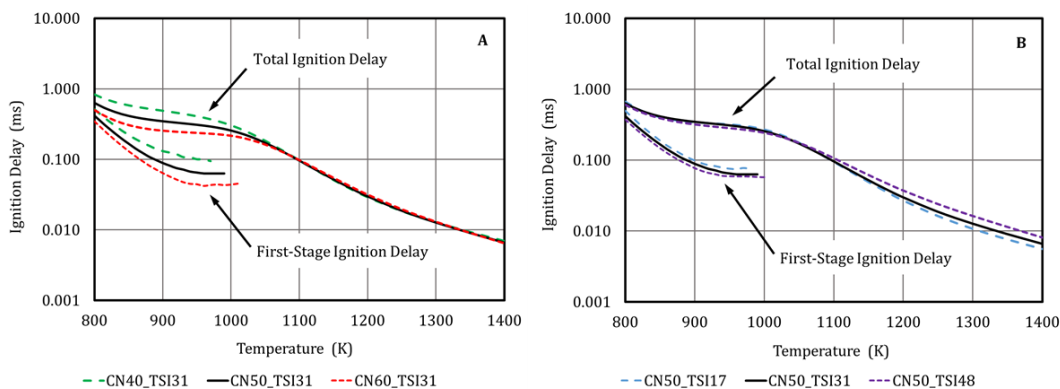
404

405 **Figure 9.** Results showing the total ignition delays for the surrogate palette components. **Figure 9A**
 406 contains n-alkanes and cyclo-alkanes and **Figure 9B** includes aromatics and iso-alkanes. Note the
 407 differences in ignition delay and NTC behavior between the hydrocarbon classes and within the classes.
 408 Closed-homogeneous reactor initial conditions: Temperature: 800-1400K, Equivalence Ratio = 1.0,
 409 Pressure = 50 bar.

410

411 To examine the effects of fuel cetane number, **Figure 10A** shows the ignition delay results for three
 412 surrogate fuels having cetane numbers of 40, 50 and 60 with the same TSI value of 31. All of the fuels
 413 exhibited two-stage ignition and the ZTC behavior for reactor temperatures less than ~1000K. The
 414 simulation results show that first-stage and total ignition delays were shortened as the fuel cetane number
 415 was increased from 40 to 60. Increasing the cetane number also slightly increased the temperature range
 416 of the ZTC behavior. For these simulations, the ignition delay became independent of cetane number at
 417 reactor temperatures above ~1050K. To investigate the effect of changing the fuel TSI at a constant cetane
 418 number, **Figure 10B** shows three surrogate fuels with a cetane number of 50 and TSI values of 17, 31 and
 419 48. All three surrogate fuels had essentially the same first-stage and total ignition delays demonstrating
 420 that the changes in blend formulation to control TSI had little impact on the ignition delays. Recall that
 421 CN50_TSI17 does not contain 1-methylnaphthalene while CN50_TSI48 contains 0.27v/v 1-

422 methylnaphthalene. The reactor simulations suggest that, depending on the reactor conditions, the
 423 surrogate fuels can exhibit two-stage ignition and NTC/ZTC behavior. The results also suggest the surrogate
 424 fuels provide independent control of fuel cetane number and threshold soot index.



425

426 **Figure 10.** Results showing the first-stage and total ignition delays for five surrogate fuels. **Figure 10A**
 427 includes three surrogate fuels with cetane numbers of 40, 50 and 60 and with TSI=31. **Figure 10B** contains
 428 three surrogate fuels with cetane number=50 and TSI values of 17, 31 and 48. Closed-homogeneous reactor
 429 initial conditions: Temperature: 800-1400K, Equivalence Ratio = 1.0, Pressure = 50 bar.

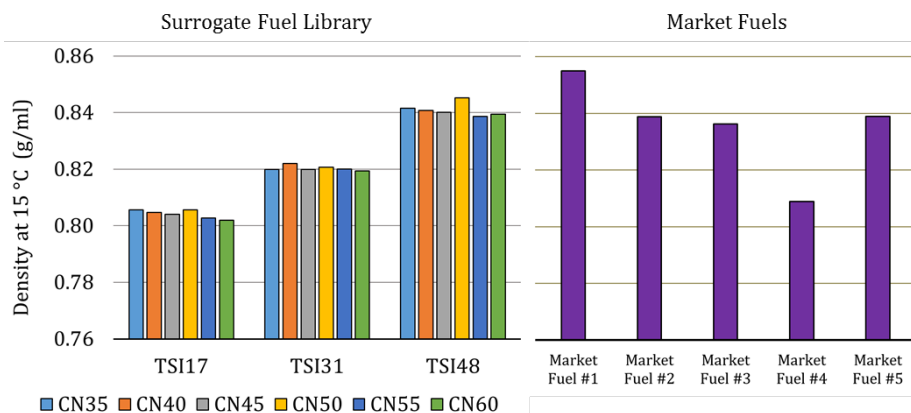
430 4.5. Market Fuel Comparison

431 To ensure the Surrogate Fuel Library was representative of real-world fuels, the predicted properties were
 432 compared to the five market fuels shown in **Table 2**. In the figures below, the chart on the left shows the
 433 predicted values for the surrogates. The surrogates are grouped by their TSI values and sorted in the order
 434 of increasing cetane number. The chart on the right shows the measured values for the market fuels.

435 4.5.1. Density

436 Results for density are shown in **Figure 11**. For a given TSI value the surrogate densities were reasonably
 437 steady. Since n-hexadecane and heptamethylnonane have the same density, manipulating their volume
 438 fractions to control cetane number did not impact the density of the surrogate fuels. The surrogate fuel

439 densities increased by about 5% as the TSI value was increased from 17 to 48 due to increased amounts of
 440 1-methylnaphthalene. The surrogate fuel densities ranged from 0.802 to 0.845 g/ml and were mostly
 441 within the range spanned by the market Diesel fuels.

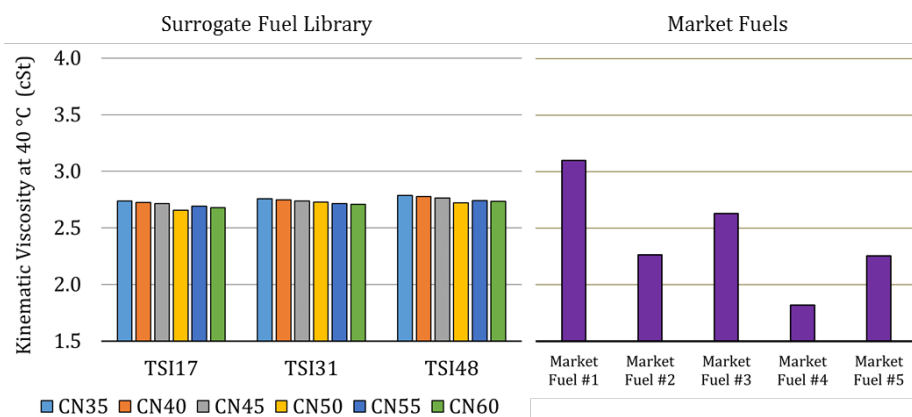


442

443 **Figure 11.** Surrogate fuel predicted densities compared to the measured densities from the market fuels.

444 *4.5.2. Kinematic Viscosity*

445 **Figure 12** provides the results for kinematic viscosity. For the Surrogate Fuel Library, adjusting the blend
 446 ratios to control cetane number and TSI had very little impact on the kinematic viscosity. As cetane number
 447 varied from 35 to 60 the viscosity decreased by about 0.05 cSt. Increasing the TSI from 17 to 48 increased
 448 viscosity by about 0.05 cSt. For the surrogate fuels, the average kinematic viscosity was 2.73 cSt while the
 449 market fuels averaged 2.41 cSt. The viscosities of the surrogate fuels were within the range of the market
 450 fuels and the requirements established in ASTM D975 [41].

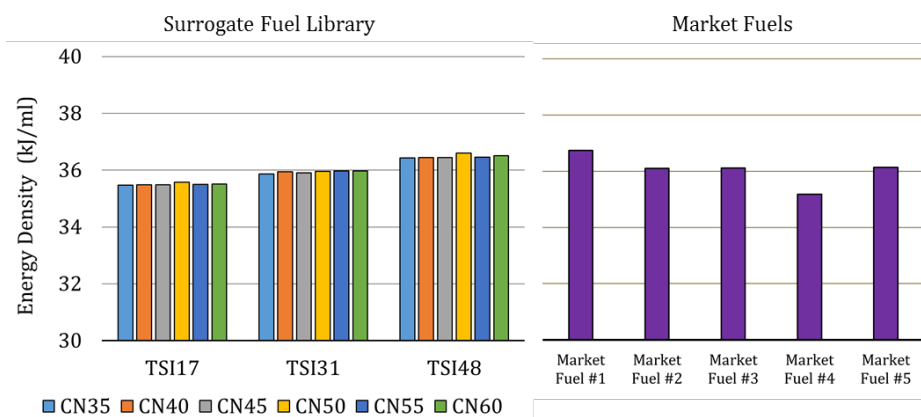


451

452 **Figure 12.** Surrogate fuel predicted viscosities compared to the measured viscosities from the market fuels.

453 *4.5.3. Energy Density*

454 The energy density (kJ/ml) was calculated by multiplying the fuel density and heating values. The results
 455 are given in **Figure 13**. For the surrogate fuels, the energy density was not influenced by changes in cetane
 456 number and increased modestly as TSI increased from 17 to 48. The values for the surrogate fuels spanned
 457 about the same range as the market fuels. The average for the surrogate fuels was 35.97 kJ/ml compared
 458 to an average of 36.06 kJ/ml for the market fuels.

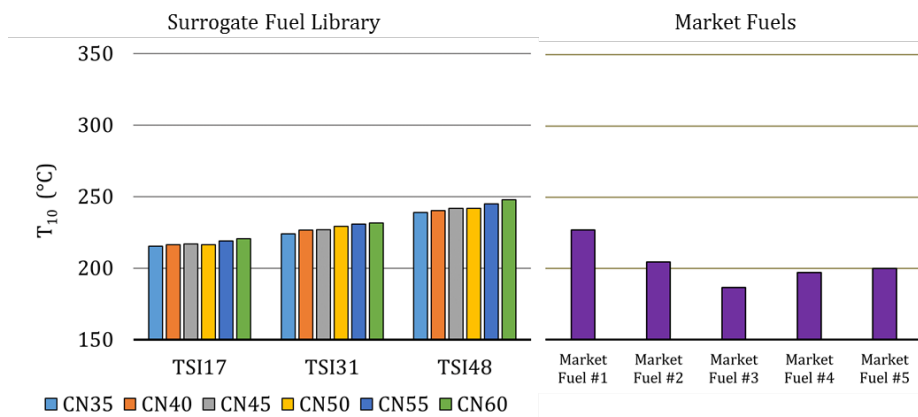


459

460 **Figure 13.** Surrogate fuel predicted energy densities compared to the measured energy densities from the
 461 market fuels.

462 *4.5.4. Distillation Temperatures*

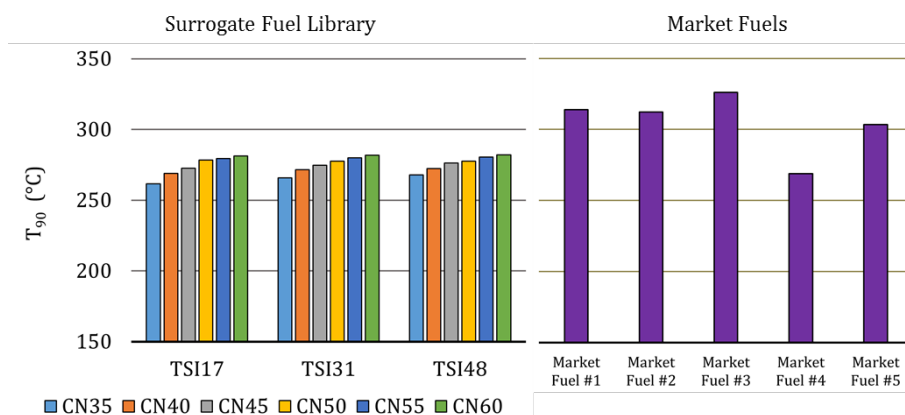
463 The T_{10} distillation temperature results are shown in **Figure 14**. For a given TSI value increasing the cetane
 464 number from 35 to 60 increased the T_{10} distillation temperature by about 10°C. For a given cetane number,
 465 increasing the TSI from 17 to 48 raised the T_{10} distillation temperature by around 25°C. For all of the
 466 surrogates, T_{10} averaged 230°C compared to an average of 203°C for the market fuels. The T_{10} range for the
 467 surrogates was 33°C compared to 40°C for the market fuels.



468

469 **Figure 14.** Surrogate fuel predicted T₁₀ distillation temperatures compared to the measured T₁₀ distillation
 470 temperatures from the market fuels.

471 **Figure 15** shows the T₉₀ distillation temperature results. For a given TSI value, increasing the cetane
 472 number from 35 to 60 raised the T₉₀ by about 17°C. In general, at a given cetane number the T₉₀ was not
 473 affected by surrogate blend changes to control TSI. The T₉₀ averaged 275°C for the surrogate fuels
 474 compared to an average of 305°C for the market fuels. The market fuels had a T₉₀ range of 57°C compared
 475 to only 20°C for the surrogate fuels.



476

477 **Figure 15.** Surrogate fuel predicted T₉₀ distillation temperatures compared to the measured T₉₀ distillation
 478 temperatures from the market fuels.

479 **5. Summary and Conclusions**

480 The objective of this work was to provide fully representative multi-component surrogate Diesel fuels that,
 481 along with their chemical kinetic mechanisms, can be brought to routine use in applied research, industrial
 482 applications, and most importantly, the engine designer's toolkit. The results are summarized as follows:

- 483 • A process was developed that coupled the Reaction Workbench – Surrogate Blend Optimizer (SBO)
 484 with blending rules established by this work to create a Diesel Surrogate Fuel Library.
- 485 • A surrogate fuel palette consisting of 13 hydrocarbon species was selected from the 55 available
 486 species within the ANSYS Model Fuel Library. From this palette, the surrogate fuel objectives and
 487 requirements were achieved with four components: n-hexadecane, 2,2,4,4,6,8,8-
 488 heptamethylnonane, decahydronaphthalene and 1-methylnaphthalene.
- 489 • The combustion, physical and chemical properties of the baseline Diesel fuel (a market fuel) were
 490 accurately matched by the baseline surrogate fuel.

- 491 • The SBO fuel property predictions were validated. A set of five surrogate fuels that spanned a
492 cetane range from 40 to 60 and a TSI range from 17 to 48 were blended and tested. Good agreement
493 was obtained between the SBO predicted and the ASTM measured fuel properties.
- 494 • The Surrogate Fuel Library was validated. A comparison of the 18 surrogate fuels with five market
495 Diesel fuels showed good agreement for density, kinematic viscosity, energy density (kJ/ml), and
496 the T₁₀ and T₉₀ distillation temperatures.
- 497 • To support future Diesel spray, combustion and emission investigations, the densities, viscosities,
498 surface tensions and lower heating values of the surrogate fuels were in close agreement with full-
499 range petroleum Diesel fuels.
- 500 • The library provides a broad range of fuel cetane numbers to quantify the impact of this key
501 property on new combustion technologies and a wide range of fuel sooting tendency useful for the
502 improvement and validation of models to predict soot and exhaust particles.

503

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508

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699

700 **Appendix**

701 Table A1. Blend volume fractions, mass fractions, and predicted fuel properties for six surrogate fuels with
 702 cetane numbers ranging from 35 to 60 (in increments of 5) and a TSI value of 17.

| Predicted Fuel Property | CN35_ TSI17 | CN40_ TSI17 | CN45_ TSI17 | CN50_ TSI17 | CN55_ TSI17 | CN60_ TSI17 |
|----------------------------------|----------------|----------------|----------------|----------------|----------------|----------------|
| n-Hexadecane (v/v) | 0.13 | 0.20 | 0.25 | 0.34 | 0.37 | 0.43 |
| Heptamethylnonane (v/v) | 0.57 | 0.50 | 0.45 | 0.33 | 0.33 | 0.27 |
| Decahydronaphthalene (v/v) | 0.30 | 0.30 | 0.30 | 0.33 | 0.30 | 0.30 |
| 1-Methylnaphthalene (v/v) | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 |
| n-Hexadecane (m/m) | 0.123 | 0.188 | 0.236 | 0.320 | 0.350 | 0.407 |
| Heptamethylnonane (m/m) | 0.550 | 0.484 | 0.436 | 0.319 | 0.321 | 0.263 |
| Decahydronaphthalene (m/m) | 0.327 | 0.328 | 0.328 | 0.361 | 0.329 | 0.330 |
| 1-Methylnaphthalene (m/m) | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 | 0.000 |
| Cetane Number | 34.8 | 40.7 | 45.0 | 53.5 | 55.2 | 60.3 |
| TSI | 19.0 | 18.2 | 17.6 | 16.6 | 16.2 | 15.5 |
| LHV (MJ/kg) | 44.040 | 44.090 | 44.130 | 44.160 | 44.230 | 44.280 |
| Density (g/ml) | 0.806 | 0.805 | 0.804 | 0.806 | 0.803 | 0.802 |
| Kinematic Viscosity at 40°C(cSt) | 2.737 | 2.724 | 2.714 | 2.654 | 2.692 | 2.680 |
| Molar H/C | 2.017 | 2.017 | 2.017 | 2.016 | 2.016 | 2.016 |
| T ₁₀ (°C) | 215.3 | 216.5 | 217.0 | 216.5 | 219.2 | 220.7 |
| T ₂₀ (°C) | 218.9 | 220.3 | 221.5 | 221.2 | 224.3 | 226.4 |
| T ₃₀ (°C) | 222.9 | 224.9 | 226.6 | 226.8 | 231.3 | 233.6 |
| T ₄₀ (°C) | 228.0 | 231.1 | 233.2 | 234.5 | 239.3 | 242.3 |
| T ₅₀ (°C) | 234.1 | 237.8 | 241.0 | 244.3 | 248.9 | 252.8 |
| T ₆₀ (°C) | 240.8 | 245.7 | 249.4 | 254.6 | 258.7 | 263.1 |
| T ₇₀ (°C) | 247.4 | 253.6 | 257.4 | 264.6 | 267.1 | 271.6 |
| T ₈₀ (°C) | 254.4 | 260.9 | 264.9 | 272.2 | 274.0 | 277.2 |
| T ₉₀ (°C) | 261.7 | 268.9 | 272.6 | 278.5 | 279.6 | 281.4 |

703

704 Table A2. Blend volume fractions, mass fractions, and predicted fuel properties for six surrogate fuels with
 705 cetane numbers ranging from 35 to 60 (in increments of 5) and a TSI value of 31.

| Predicted Fuel Property | CN35_ TSI31 | CN40_ TSI31 | CN45_ TSI31 | CN50_ TSI31 | CN55_ TSI31 | CN60_ TSI31 |
|----------------------------------|----------------|----------------|----------------|----------------|----------------|----------------|
| n-Hexadecane (v/v) | 0.19 | 0.26 | 0.31 | 0.37 | 0.43 | 0.48 |
| Heptamethylnonane (v/v) | 0.51 | 0.44 | 0.39 | 0.33 | 0.27 | 0.22 |
| Decahydronaphthalene (v/v) | 0.20 | 0.18 | 0.19 | 0.18 | 0.18 | 0.18 |
| 1-Methylnaphthalene (v/v) | 0.10 | 0.12 | 0.11 | 0.12 | 0.12 | 0.12 |
| n-Hexadecane (m/m) | 0.177 | 0.242 | 0.289 | 0.345 | 0.401 | 0.449 |
| Heptamethylnonane (m/m) | 0.487 | 0.420 | 0.373 | 0.316 | 0.259 | 0.211 |
| Decahydronaphthalene (m/m) | 0.216 | 0.194 | 0.205 | 0.195 | 0.195 | 0.195 |
| 1-Methylnaphthalene (m/m) | 0.121 | 0.145 | 0.133 | 0.145 | 0.145 | 0.145 |
| Cetane Number | 35.5 | 40.5 | 45.2 | 49.9 | 55.0 | 59.2 |
| TSI | 31.1 | 32.8 | 30.9 | 31.5 | 30.8 | 30.3 |
| LHV (MJ/kg) | 43.74 | 43.73 | 43.80 | 43.81 | 43.86 | 43.90 |
| Density (g/ml) | 0.820 | 0.822 | 0.820 | 0.821 | 0.820 | 0.819 |
| Kinematic Viscosity at 40°C(cSt) | 2.756 | 2.749 | 2.736 | 2.728 | 2.716 | 2.707 |
| Molar H/C | 1.897 | 1.873 | 1.884 | 1.872 | 1.872 | 1.871 |
| T ₁₀ (°C) | 224.1 | 226.8 | 227.0 | 229.2 | 230.9 | 231.8 |
| T ₂₀ (°C) | 227.1 | 230.8 | 231.5 | 234.0 | 235.5 | 236.9 |
| T ₃₀ (°C) | 231.4 | 234.5 | 236.0 | 238.9 | 241.2 | 243.1 |
| T ₄₀ (°C) | 235.4 | 239.3 | 241.2 | 244.3 | 247.0 | 249.5 |
| T ₅₀ (°C) | 239.9 | 244.3 | 246.9 | 250.1 | 254.0 | 256.9 |
| T ₆₀ (°C) | 245.0 | 249.4 | 252.7 | 256.9 | 260.4 | 263.9 |
| T ₇₀ (°C) | 250.7 | 255.4 | 259.5 | 263.4 | 267.2 | 270.2 |
| T ₈₀ (°C) | 257.0 | 262.2 | 266.8 | 270.2 | 274.2 | 276.7 |
| T ₉₀ (°C) | 265.7 | 271.7 | 274.8 | 277.7 | 279.9 | 281.8 |

706

707 Table A3. Blend volume fractions, mass fractions, and predicted fuel properties for six surrogate fuels with
 708 cetane numbers ranging from 35 to 60 (in increments of 5) and a TSI value of 48.

| Predicted Fuel Property | CN35_ TSI48 | CN40_ TSI48 | CN45_ TSI48 | CN50_ TSI48 | CN55_ TSI48 | CN60_ TSI48 |
|----------------------------------|----------------|----------------|----------------|----------------|----------------|----------------|
| n-Hexadecane (v/v) | 0.26 | 0.32 | 0.38 | 0.42 | 0.50 | 0.56 |
| Heptamethylnonane (v/v) | 0.44 | 0.38 | 0.32 | 0.25 | 0.20 | 0.14 |
| Decahydronaphthalene (v/v) | 0.05 | 0.05 | 0.05 | 0.06 | 0.05 | 0.04 |
| 1-Methylnaphthalene (v/v) | 0.25 | 0.25 | 0.25 | 0.27 | 0.25 | 0.26 |
| n-Hexadecane (m/m) | 0.238 | 0.293 | 0.349 | 0.384 | 0.460 | 0.515 |
| Heptamethylnonane (m/m) | 0.413 | 0.357 | 0.301 | 0.234 | 0.189 | 0.132 |
| Decahydronaphthalene (m/m) | 0.053 | 0.053 | 0.053 | 0.063 | 0.053 | 0.043 |
| 1-Methylnaphthalene (m/m) | 0.296 | 0.297 | 0.297 | 0.319 | 0.298 | 0.310 |
| Cetane Number | 34.8 | 39.9 | 45.0 | 48.4 | 55.2 | 59.9 |
| TSI | 48.8 | 48.1 | 47.5 | 48.9 | 46.2 | 46.8 |
| LHV (MJ/kg) | 43.290 | 43.340 | 43.380 | 43.310 | 43.470 | 43.490 |
| Density (g/ml) | 0.842 | 0.841 | 0.840 | 0.845 | 0.839 | 0.839 |
| Kinematic Viscosity at 40°C(cSt) | 2.788 | 2.776 | 2.765 | 2.720 | 2.742 | 2.734 |
| Molar H/C | 1.725 | 1.724 | 1.724 | 1.693 | 1.723 | 1.711 |
| T ₁₀ (°C) | 239.1 | 240.4 | 241.8 | 241.8 | 245.0 | 248.0 |
| T ₂₀ (°C) | 240.6 | 242.1 | 244.3 | 244.2 | 247.7 | 250.6 |
| T ₃₀ (°C) | 242.1 | 244.3 | 246.6 | 246.8 | 250.7 | 253.5 |
| T ₄₀ (°C) | 244.3 | 246.7 | 249.1 | 249.4 | 254.0 | 256.7 |
| T ₅₀ (°C) | 246.7 | 249.3 | 251.9 | 252.5 | 257.1 | 259.8 |
| T ₆₀ (°C) | 249.3 | 252.0 | 255.1 | 256.8 | 261.8 | 264.5 |
| T ₇₀ (°C) | 252.4 | 256.6 | 259.8 | 261.9 | 267.1 | 269.6 |
| T ₈₀ (°C) | 258.0 | 262.3 | 266.9 | 268.9 | 273.6 | 275.8 |
| T ₉₀ (°C) | 267.8 | 272.4 | 276.2 | 277.6 | 280.4 | 282.1 |

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710