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An AZA-Fused π -Conjugated Microporous Framework Catalyzes the Production of Hydrogen Peroxide

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ABSTRACT: In order to produce hydrogen peroxide in small-scale electrochemical plants, selective catalysts for the oxygen reduction reaction (ORR) towards the desired species are required. Here, we report about the synthesis, characterization, ORR electrochemical behavior and reaction mechanism of an aza-fused π -conjugated microporous polymer, which presents high selectivity towards hydrogen peroxide. It was synthesized by polycondensation of 1,2,4,5-benzenetetramine tetrahydrochloride and triquinoyl octahydrate. A cobalt-modified version of the material was also prepared by a simple post-synthesis treatment with a Co(II) salt. The characterization of the material is consistent with the formation of a conductive robust porous covalent laminar poly-aza structure. The ORR properties of these catalysts were investigated using rotating disk and rotating disk-ring arrangements. The results indicate that hydrogen peroxide is almost exclusively produced at very low overpotentials on these materials. Density functional theory calculations provide key elements to understand the reaction mechanism. It is found that, at the relevant potential for the reaction, half of the nitrogen atoms of the material would be hydrogenated. This hydrogenation process would destabilize some carbon atoms in the lattice and would provide segregated charge. On the destabilized carbon atoms, molecular oxygen would be chemisorbed with the aid of charge transferred from the hydrogenated nitrogen atoms and solvation effects. Due to the low destabilization of the carbon sites, the resulting molecular oxygen chemisorbed state, which would have the characteristics of a superoxide species, would be only slightly stable, promoting the formation of hydrogen peroxide.

KEYWORDS. Electrocatalyst, Oxygen reduction, Hydrogen peroxide production, Microporous framework, Conjugated covalent porous polymer.

INTRODUCTION

Hydrogen peroxide is a commodity chemical used mainly as a bleaching agent, though it has other important applications, such as water disinfection. It is currently primarily produced using the anthraquinone route. This is a complex process, which gives rise to side reactions, originating a net consumption of anthraquinone, and which requires of several separations. As a result, it can be only deployed effectively in large-scale plants. Moreover, the centralized production approach introduces additional drawbacks, such as large inversions, massive storage requirements and costs of transport to the consumption sites. Therefore, an alternative production method, which can be implemented in small-scale plants to allow a distributed production on demand, would be a more convenient technology.

Interestingly, hydrogen peroxide is usually yielded as an undesired by-product of the oxygen reduction reaction (ORR) in

fuel cells. In the complete ORR to water four electrons are exchanged. However, when only two electrons can be exchanged, hydrogen peroxide is produced. On the most part of catalysts, the ORR evolves simultaneously through both routes at different rates. For fuel cell applications, the catalyst must be optimized towards the complete reduction to water. However, ORR catalysts can be alternatively optimized towards the exchange of two electrons process, giving rise to the concept of electrochemical cell of production of hydrogen peroxide. The electrochemical synthesis of hydrogen peroxide could be implemented at the consumption site in small plant, adapting the production to the demand and avoiding the drawbacks inherent to a centralized production. Additionally, if the overpotential for the ORR was low, energy could be obtained from a cell where the anode reaction would be the hydrogen oxidation reaction, since the cell potential would be positive. Thus, finding appropriate catalysts with a low overpotential for the ORR producing exclusively hydrogen peroxide is very attractive for practical purposes. The cell could have the typical

1 configuration of a polymer membrane fuel cell, in which hy-
2 drogen peroxide is synthesized instead of water. Some years
3 ago, only cationic (*aka.* acidic) membranes were available in
4 the market, which restricted the use of this technology to elec-
5 trocatalysts working in acidic media. However, the advent of
6 reliable anionic membranes opens new possibilities for the use
7 of electrocatalysts working in alkaline media. Nevertheless
8 they still have lower stability, than cationic membranes, espe-
9 cially in the presence of hydrogen peroxide.¹

10 Gold and doped platinum electrodes have shown good ORR
11 activity for hydrogen peroxide production at low overpoten-
12 tials.²⁻⁵ However, the high cost of these metals prevents their
13 use. On the other hand, under alkaline conditions, carbon
14 materials are active for hydrogen peroxide production at rela-
15 tively high overpotentials. When these materials are doped
16 with nitrogen, their ORR activity improves, but increasing
17 their selectivity towards the formation of water.⁶⁻¹⁸ Computa-
18 tional results suggest that the ORR activity of these materials
19 depends on the specific location of the nitrogen-dopants,^{19,20}
20 In a pair of previous works,^{21,22} the role played by different
21 forms of nitrogen-dopants in the activation of the molecular
22 oxygen on graphitic materials was elucidated. The need of
23 destabilized carbons and available charge, and the role played
24 by the hydrogenation of pyridinic nitrogen-dopants and the
25 solvation effect were established. In view of those results, it
26 can be argued that, for optimal hydrogen peroxide production
27 purposes, a chemisorbed state of molecular oxygen, with su-
28 peroxide characteristics and a small stability would be the
29 ideal situation. A slightly adsorbed superoxide implicates a
30 slightly adsorbed hydrogen peroxide anion, which favor their
31 desorption, yielding hydrogen peroxide in the solution. Our
32 previous results suggest that such a kind of active sites could
33 be enabled by pyridinic nitrogen-dopants at the zigzag edges
34 of graphitic materials.²²

35 The assembling of porous materials from molecular build-
36 ing blocks allows the control not only of the composition but
37 also of the microstructure, which is essential for a heterogene-
38 ous catalyst. Aza-fused π -conjugated microporous polymers
39 (Aza-CMPs), assembled from molecular building blocks,
40 present a high number of pyridinic nitrogen-dopants at zig-zag
41 edges. Additionally, having a very well defined structure, with
42 only one type of nitrogen functionality, the identification of
43 active sites and catalytic mechanisms is simpler for these
44 materials. They were studied by Kou *et al.*, showing excellent
45 electrochemical properties, like large capacitance and high
46 energy and power densities.²³ For these reasons, Aza-CMPs
47 were selected as promising selective ORR catalysts towards
48 hydrogen peroxide in this research. Here, we report about the
49 synthesis, characterization, ORR electrochemical behavior and
50 reaction mechanism of the aza-fused π -conjugated mi-
51 croporous polymer (Aza-CMP) shown in Figure 1, obtained
52 by the polycondensation reaction with water formation be-
53 tween 1,2,4,5-benzenetetramine tetrahydrochloride and
54 triquinoyl octahydrate. We have also studied the electrochemi-
55 cal behavior of the Aza-CMP modified with Co(II) because
56 the incorporation of metals can lead to a modified activity.^{15,17}
57 As will be shown, these materials exhibit high activity for
58 hydrogen peroxide production at low overpotentials. Density
59 functional theory (DFT) calculations provide insights in order
60 to understand the reaction mechanism.

EXPERIMENTAL AND COMPUTATIONAL METHODS

Preparation of the Aza-CMP. 532.5 mg (1.875 mmol) of 1,2,4,5-benzenetetramine tetrahydrochloride in 15 mL of anhydrous DMF and 390 mg (1.25 mmol) of triquinoyl octahydrate in 5 mL of anhydrous DMF were mixed and refluxed for 48 h under argon. The dark brown solid was purified upon hot extraction with methanol for 24 h using a Soxhlet. The resulting solid was dried under vacuum at 150 °C for 24 h. Yield 304.6 mg (91 %). Elementary analysis for **Aza-CMP**, C (52.47 %), H (3.84 %), N (23.92 %). TGA indicates a mass loss of *ca.* 7 % between 20-250 °C that is assigned to the solvent trapped at the pores. At 250 °C the material starts its chemical decomposition.

Preparation of the Aza-CMP@Co. The **Aza-CMP** materi-
al was modified with Co(II) using two different reagents:
cobalt(II) sulfate heptahydrate and cobalt(II) acetylacetonate (Co(acac)₂). In the first case, 25 mg of **Aza-CMP** were immersed in 3.7 mL of a 25 mg/mL CoSO₄·7H₂O in methanol solution. The suspension was stirred during 24 h at room temperature. The solid was filtered and then it was washed with methanol until the filtrate became colorless. Finally, the product was dried at 100 °C at vacuum conditions. With these quantities the Co:N molar ratio is 2:1, while after all the process this ratio in the obtained material is 1:293 (0.13 % wt. of Co). In the second case, 25 mg of **Aza-CMP** were immersed in 10 mL of a 2.8 mg/mL Co(acac)₂ in methanol solution. The subsequent procedure is the same as used for the CoSO₄·7H₂O. With these quantities the Co:N molar ratio is 2:3, and after all the process this ratio in the final material, is 1:192 (0.20 % wt. of Co). Both modification procedures lead to very similar electrochemical behavior slightly better for the material prepared with CoSO₄·7H₂O. For that reason, only the electrochemical results corresponding to the Aza-CMP modified with cobalt sulfate are shown.

Preparation of the catalyst inks and the catalyst film on the electrode. For the preparation of the catalyst film on the electrode, the catalyst was first dispersed in a water/alcohol/Nafion ionomer solution to form an ink. The Nafion ionomer is added to enhance the adhesion of the catalyst film to the electrode surface.²⁴ The inks for all cases were prepared immersing 5 mg of the catalyst in a solution containing 4 mL of water, 1 mL of isopropanol (Merck, for analysis EMSURE®) and 50 μ L of 5 wt% Nafion ionomer solution (Sigma-Aldrich). The catalyst ink was then transferred to an ultrasonicator and sonicated for 60 min. Before each measurement, the catalyst ink was sonicated again to assure that the catalyst particles were well dispersed. Then, 10 μ L of the ink were deposited onto the electrode fully covering the glassy carbon but avoiding the deposition on the Teflon shield. For drying the ink droplet, the electrode was rotated at 700 rpm and was kept in Ar atmosphere until the film was completely dry. By using this method, a reproducible and uniform film covering the entire glassy carbon surface was obtained.^{24,25}

Electrochemical measurements. Two different experi-
mental set-ups were used for the electrochemical measure-
ments. First, the characterization of the electrodes and the
ORR studies were performed using a glassy carbon rotating
disk electrode (RDE (surface area: 0.164 cm²), which the **Aza-**
CMP and **Aza-CMP@Co** catalysts were deposited on. After

1 these experiments, the quantification of hydrogen peroxide
2 produced during the ORR was performed using a rotating
3 ring-disk electrode (RRDE), composed of a glassy carbon disk
4 on which the catalyst film was deposited (surface area: 0.164
5 cm²) and a platinum ring where the hydrogen peroxide is
6 detected. For both set-ups, the experiments were carried out, at
7 room temperature, in a three-electrode electrochemical cell de-
8 oxygenated using Ar (Air Liquide, N50), for the electrode
9 characterization. A gold wire was used as counter electrode
10 and the reference electrode was a reversible hydrogen elec-
11 trode (RHE) connected to the cell through a Luggin capillary.
12 The working solutions were prepared using NaOH·H₂O
13 (Merck, Suprapur 99.99%). Ultrapure water (Elga PureLab
14 Ultra, 18.2 MΩ cm) was used for the preparation of the solu-
15 tions and glassware cleaning.

16 For the ORR studies, the electrochemical cell was bubbled
17 with O₂ (Air Liquide Alphagaz) until the solution was saturat-
18 ed. The experiments using the RDE were performed with an
19 EDI101 rotating electrode, whose rotation rate was controlled
20 by a Radiometer CTV 101 apparatus. In this case, a signal
21 generator EG&G PARC 175 and an eDAQ EA161 potentiostat
22 with an eDAQ e-corder ED401 recording system were used
23 for the electrochemical measurements. The RRDE experi-
24 ments were carried out using a Pine AFMSRXE Electrode
25 Rotator, and the electrochemical measurements were taken
26 with an EG&G Bi-Potentiostat Model 366A and an eDAQ e-
27 corder ED401.

28 In all cases, the glassy carbon electrodes were first polished
29 with alumina from higher to lower particle sizes. After this
30 process, they were sonicated and finally rinsed with ultrapure
31 water. Then, the electrodes were transferred to the electro-
32 chemical cell where a cleaning electrochemical procedure was
33 performed: the electrode was cycled between 0.06 V and 1.7 V
34 (*vs* RHE) until a stable cyclic voltammogram was obtained.
35 For the RRDE measurements, the platinum ring was also
36 cycled between 0.06 V and 1.7 V (*vs* RHE). After the elec-
37 trode characterization and the ORR study on the bare elec-
38 trode, the catalyst film was deposited for the electrochemical
39 characterization and the study of its electrocatalytic activity. In
40 the case of the RRDE, special care was taken to ensure that the
41 ink droplet does not cover the platinum ring. For hydrogen
42 peroxide detection at the platinum ring of the RRDE, the po-
43 tential of the ring is maintained at 1.1 V (*vs* RHE) while the
44 potential at the disk is swept between 0.06 V and 1.0 V (*vs*
45 RHE). Under the considered set-up and cell conditions, the
46 only species present in the cell solution that can be oxidized at
47 1.1 V is hydrogen peroxide (actually, for this pH value, HOO-
48). Thus, the measured ring current is directly proportional to
49 the amount of hydrogen peroxide formed on the disk. All the
50 experiments have been repeated at least three times, obtaining
51 always consistent results.

52 **Computational methods.** The monodentate chemisorption
53 of molecular oxygen on different sites of the investigated
54 material was explored running different periodic DFT calcula-
55 tions under the GGA approximation and using the PBE func-
56 tional²⁶ and numerical basis sets of double-numerical plus
57 polarization quality²⁷ as implemented in the Dmol3 code.²⁸
58 Neutral and charged charge conditions compensated by a
59 charge helium were considered. All the electrons were explic-
60 itly included in the calculations under a spin unrestricted ap-
proach. The effects of non-zero dipole moments in the cells

were cancelled by means of external fields.²⁹ Full and partial
optimizations were carried out depending on the goal.

Moreover, since previous results²¹ indicate that solvation
effects are important in the mechanisms, continuum solvation
effects were taken into account by means of the COSMO
model,³⁰ meanwhile hydrogen bonds were captured by includ-
ing additional explicit water molecules as solvation effect
treatment.²¹ To verify the quality of the selected solvation
effect treatment, solvation energies were computed for oxygen
and superoxide, obtaining values that were found to be con-
sistent with those expected.

The investigated material was modeled using a periodic cell
comprising 42 graphitic atoms (30 carbon and 12 nitrogen
atoms) and a vacuum slab of 20 Å. The shortest distance be-
tween periodic images was *ca.* 16.57 Å. Moreover, since pre-
vious results indicate that the hydrogenation of pyridinic
nitrogen in graphitic materials could play a role in the molecu-
lar oxygen activation,²² different hydrogenation states were
explored searching for the relevant one.

An orbital cutoff radius of 3.7 Å was used in the numerical
basis set for all the atoms. The optimization convergence
thresholds were set to 1.0×10⁻⁵ Ha for the energy, 0.002 Ha/Å
for the force, and 5.0×10⁻³ Å for the displacement. The SCF
convergence criterion was set to 1.0×10⁻⁶ Ha for the energy.
Brillouin zones were sampled, under the Monkhorst-Pack
method,³¹ using grids corresponding to distances in the recip-
rocal space of the order of 0.02 1/Å, which was enough to
avoid using thermal smearing as convergence aid. A value of
78.54 was used as the dielectric constant in the continuous
solvation model.

In order to capture hydrogen bonds, an explicit water mole-
cule was included in the models targeted to visualization, in
addition to the continuum solvation model, as solvation effect
treatment. However, considering our previous results,²¹ for
models targeted to energetics evaluations, five explicit water
molecules were included in the model, in addition to the con-
tinuum solvation model, as solvation effect treatment. A typi-
cal configuration of the formed explicit water solvation shell
can be observed in the supporting information.

Chemisorbed states were searched for running full optimiza-
tions. The relevance of each one of them was established
determining its stability. For such a purpose, the energetics for
the shortest distances of the reactions paths were estimated
performing several constrained optimizations. For each reac-
tion path, the basic configuration and treatment was main-
tained, but the distance between the carbon acting as active
site and the nearest atom of the oxygen molecule was varied
and constrained during the optimization process. To facilitate
comparisons, the displayed total energies were referred to their
respective references, calculated as the adsorbent energy plus
that corresponding to the adsorbate complex in the bulk. Note
that only relatively short C-O distances were considered. Thus,
the final convergence to the alignment level of the respective
references, at very long distances, is not displayed. The rea-
sons for doing so were three. First, it has been pointed out that,
because of the required change in the spin multiplicity, non-
adiabatic effects could be implicated in the chemisorption of a
solvated oxygen molecule. Second, for some of the considered
cases, long distances between adsorbent and adsorbate give
rise to very challenging models for which states of different
spin multiplicity are very close in energy. Third, when solva-

tion effects are sufficiently captured, the available charge from the surface is assigned to the solvated oxygen molecule, during the optimization process, giving rise to a solvated superoxide anion, even when the oxygen molecule has not even yet come close to the surface. All these difficulties are circumvented by considering only relatively short C-O distances. For the shortest distances, the required spin multiplicity change has already taken place, the most favorable spin multiplicity of the solutions are much more clearly defined, and an eventual charge transfer to oxygen can be better explained. All the calculations were run under automatic spin multiplicity conditions. For the relevant configurations, it was verified that, along the considered distances, the most favorable spin multiplicity was invariant. Despite of only the shortest distances were considered, still useful insights were derived about the investigated mechanism.

RESULTS AND DISCUSSION

Synthesis and characterization of the Aza-CMP material.

Preparation of **Aza-CMP** was carried out following a different route to that previously used by Kou *et al.*²³ Indeed our approach does not use catalyst and solvothermal conditions but just a reflux of DMF (Figure 1). Thus, this preparation avoids contamination of the resulting material with the metallic catalyst, which can affect the electrocatalytic results.

The formation of **Aza-CMP** was confirmed by solid-state ¹³C cross polarization/magic angle spinning nuclear magnetic resonance (CP-MAS NMR) (Figure S1) and FTIR spectroscopies (Figure S2), and elemental analysis. In the FT-IR spectra the band corresponding to the symmetric stretching vibration C=C st appears at 1644 cm⁻¹ while the signal corresponding to the C-C vibrations of the aza-aromatic rings is located at 1475 cm⁻¹. At 1253 cm⁻¹ can be observed the band corresponding to the symmetric tension vibration C=N st. The ¹³C CP-MAS NMR spectrum is also in agreement with the formation of the Aza-CMP material as it shows three signals corresponding to the three different carbon atoms in the polymer. The signal at 141 ppm corresponds to the carbon atoms of the phenyl edges connected to aza units, the signal at 129 ppm can be assigned to the carbon atoms of the triphenylene cores on vertices, and the signal at 105 ppm is due to the carbon atoms of the phenyl edges.

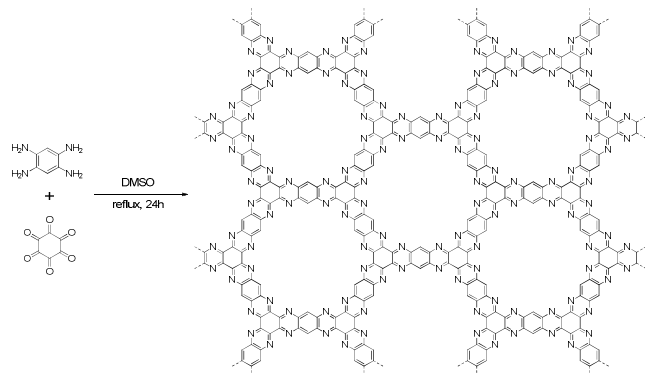


Figure 1. Formation reaction and structure of **Aza-CMP**.

Thermogravimetric analysis of **Aza-CMP** shows <10% weight loss at 150 °C assigned to the loss of volatiles (H₂O, DMF) trapped in the pores (figure S3). At 250 °C the material starts its chemical decomposition showing <20% weight loss

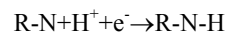
at 450 °C indicating the good thermal stability of **Aza-CMP**. The presence of the trapped solvent at the pores can explain the discrepancies observed for the observed elementary analysis (C, 52.47 %; H, 3.84 %; N, 23.92 % vs theoretical values calculated for C₁₅H₃N₆: C, 67.42 %; H, 1.13 %; N, 31.45 %). In agreement to similar Aza-CMPs,²³ **Aza-CMP** is amorphous and do not show clear peaks in X-ray powder diffraction measurements (Figure S4). To investigate the porous structure of **Aza-CMP**, nitrogen sorption isotherms were measured at 77 K (Figure S5). **Aza-CMP** exhibits typical type I isotherms, which are characteristic of microporous materials. The Brunauer-Emmet-Teller (BET) surface area and pore volume of **Aza-CMP** were calculated to be 566 m²/g and 0.29 cm³g⁻¹, respectively.

Interestingly, pressed pellets of **Aza-CMP** shows an AC conductivity value of 3×10⁻⁵ Sm⁻¹ that can contribute to its electrocatalytic performances. (Figure S6).

Figure S7 provides large area atomic force microscopy (AFM) images of diluted suspensions of **Aza-CMP** deposited by drop-casting on SiO₂ (SI for experimental details). The topographic images show large density of nanolayers with minimum heights of *ca.* 2 nm and over micron length lateral dimensions. This picture suggests a morphological description of the **Aza-CMP** material deposited on the electrodes.

The effective incorporation of the Co(II) into the **Aza-CMP@Co** was examined by XPS. The Co 2p spectra (figure S8) shows four peaks at 780.7, 782.5, 785.7 and 788.8 eV, which are in agreement with those observed in Co(II) complexes with nitrogen ligands.³² Thus, the spectra indicates that the Co(II) is incorporated into the Aza-CMP forming complexes with the nitrogen atoms in the lattice.

Electrochemical behavior of Aza-CMP. Effect of the modification with Co. Prior to the ORR experiments, the behavior of **Aza-CMP** with and without cobalt modification was electrochemically characterized in 0.1 M NaOH. Figure 2 shows the voltammetric profiles of the glassy carbon supporting electrode alone, and with the deposit of the **Aza-CMP** unmodified and modified with Co(II). As can be seen, after the deposition of the **Aza-CMP**, the apparent double layer of the electrode slightly increases and a new pair of very small peaks appear at 0.16 V. The apparent double layer in carbon materials is mainly related to the redox chemistry of the functionalities present in the carbon. The virtual invariance of the double layer indicates that the **Aza-CMP** material does not have any functional groups in the material capable of having a redox process, aside from those related to the peaks at 0.16 V, which assures the quality of the material. This latter peaks can be associated to the hydrogenation of the nitrogen atoms, as has been proposed for nitrogen-doped graphene³³ according to the following reaction:



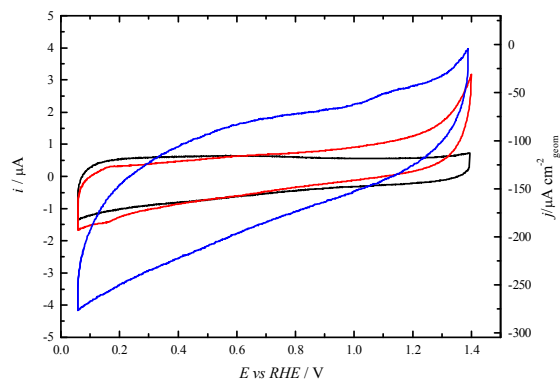


Figure 2. Voltammetric profiles of the **Aza-CMP** (red line), **Aza-CMP@Co** (blue line) and glassy carbon (black line) electrodes in Ar saturated 0.1 M NaOH. Scan rate: 50 mV s⁻¹.

When the **Aza-CMP** material is modified with Co(II), the double layer increases, which clearly indicates that the cobalt has been clearly incorporated into the **Aza-CMP** materials (Figure 2). However, the peaks at 0.16 V disappear. It is expected that Co(II) is incorporated into the **Aza-CMP** by complexing to the nitrogen atoms. Thus, the complexation would prevent the hydrogenation reaction of the N atoms, leading to the disappearance of the peak. An additional proof of the effective incorporation of the Co(II) into the material can be obtained when the hydrogen evolution reaction is studied on those materials. Carbon is a very bad catalyst for this reaction, as can be seen in Figure 3. At an overpotential of ca. -0.9 V, the measured currents for the reaction are almost negligible. On the other hand, it is known that metallic Co has some activity for the reaction, and thus the incorporation of cobalt atoms into the **Aza-CMP** network leads to a significant diminution of the overpotential for this reaction, with a practical onset for the reaction of ca. -0.5 V. This fact corroborates the incorporation of the Co(II) into the **Aza-CMP** material.

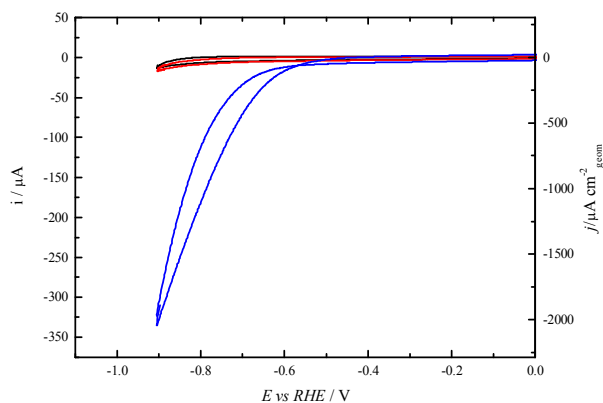


Figure 3. Voltammetric profiles of the **Aza-CMP** (red line), **Aza-CMP@Co** (blue line) and glassy carbon (black line) electrodes showing the hydrogen evolution reaction in Ar saturated 0.1 M NaOH. Scan rate: 50 mV s⁻¹.

Oxygen reduction reaction. Figure 4 shows the results for the ORR on the three electrodes. For the glassy carbon support, the activity is low. The onset for the glassy carbon electrode is ca. 0.55 V, and currents (in absolute values) show a slow increase as the potential is made more negative. This

means that the reaction is mainly controlled by the kinetics of the process. Moreover, the process is not following the typical Butler-Volmer (B-V) kinetics. For B-V kinetics, a fast increase in the currents should be expected after the onset, as observed for metallic electrodes.³⁴ In this case, the increase is very gentle, and even a small plateau is observed around 0.4 V, suggesting that an inhibition process is taking place on the electrode as the potential is made more negative. This inhibition process is partially compensating the expected increase for the B-V kinetics, giving rise to the observed moderate increase in currents. For an ideal electrocatalyst, the expected shape of the voltammetric profile would have a sigmoidal shape, reaching a maximum value, which is called limiting diffusion current. This current value is obtained when the electrode kinetics is very fast and the reaction rate is controlled by the diffusion of the reactants to the surface of the electrode. This diffusion limited current can be easily calculated using the Levich equation:

$$i_{\text{lim}} = -0.62nAFD^{2/3}v^{-1/6}c_b\omega^{1/2}$$

where n is the number of electrons exchanged in the process, A is the geometrical area of the electrode, D is the diffusion coefficient, ν , the kinematic viscosity, c_b , the bulk concentration of oxygen and ω , the rotation rate. Using the reported values D and c_b for oxygen and ν ,³⁵ and the geometrical area of the electrode (0.164 cm²), a current value of 0.450 mA is obtained when hydrogen peroxide is formed ($n=2$) or 0,900 mA for water ($n=4$) for 2500 rpm. These values are equivalent to a current density values per geometrical area of 2.74 mA cm⁻² and 5.49 mA cm⁻², respectively.

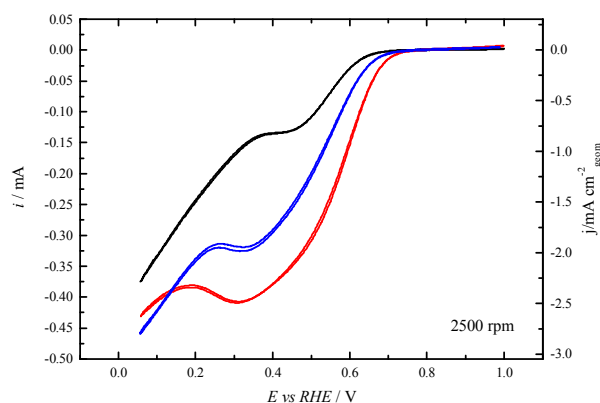


Figure 4. ORR reduction currents in a RDE for the **Aza-CMP** (red line), **Aza-CMP@Co** (blue line) and glassy carbon (black line) electrodes in O₂ saturated 0.1 M NaOH solution at 2500 rpm. Scan rate: 50 mV s⁻¹.

When the **Aza-CMP** was deposited on the glassy carbon, a significant increase in the electrocatalysis of the reaction is observed. The onset for the reaction is ca. 0.65 V and the increase in the current as the potential is made more negative is steeper than that observed in the GC. This fact clearly indicates that the **Aza-CMP** has higher activity for the ORR than the GC electrode. Moreover, around 0.4 V, the current reaches a quasi-steady state value, which is very close to the limiting current value for hydrogen peroxide formation. This would suggest that hydrogen peroxide is the main product of the reaction. As aforementioned, for this pH value, hydrogen

peroxide is in the form of HOO^- ($\text{p}K_a=11.65$). On the other hand, the modification of the **Aza-CMP** with Co does not produce the expected behavior. Metallic modification of the carbon materials are normally linked to higher activity.³⁶ However, in this case, the onset is displaced to slightly lower potential values and the currents are smaller than those recorded for the unmodified **Aza-CMP**.

In order to determine the final product in the reduction of oxygen, that is, whether hydrogen peroxide or water is obtained as final product, RRDE experiments were carried out. As aforementioned, the Pt ring is set at 1.1 V, so that the hydrogen peroxide can be detected. Figure 5 shows the currents measured in the ring (top panels) and disk (bottom panels) for the ORR. As can be seen, the shape of the current vs. potential for the ring and disk is symmetrical, which indicates that the ratio hydrogen peroxide/water production is almost independent of the electrode potential.

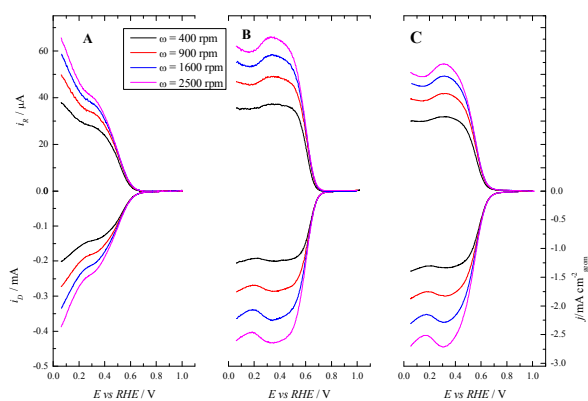


Figure 5. RRDE experiments for the ORR on the glassy carbon(A), **Aza-CMP** (B) and **Aza-CMP@Co** (C) electrodes in O_2 saturated 0.1 M NaOH solution at different rotation rates. Scan rate: 50 mV s^{-1} .

The quantitative analysis of the hydrogen peroxide production can be performed by analyzing the currents measured in the ring and disk electrodes. The total number of electrons exchanged in the reduction process, n , can be calculated as follows:

$$n = 4 \frac{i_D}{i_D + \frac{i_R}{N}}$$

where N is the collection efficiency of the ring (0.218 for the present geometrical arrangement), and i_D and i_R the measured currents for the disk and ring electrodes, respectively. Figure 6 shows the values for n calculated for the three electrodes. As expected, the number of electrons is nearly independent of the potential. Moreover, the number is always close to two, revealing that the major product is always hydrogen peroxide. This number increases slightly when the **Aza-CMP** is modified with Co(II), indicating that the presence of Co catalyzes slightly the reduction of hydrogen peroxide to water. Therefore, **Aza-CMP** is an excellent electrocatalyst for the oxygen reduction to hydrogen peroxide. It must be highlighted that the equilibrium potential for this reaction is 0.68 V, and the onset potential obtained in the present conditions for the reaction is ca. 0.65 V, that is, the overpotential for effective currents in

the reduction process of oxygen to water peroxide is below 100 mV. Additionally, the current efficiency for hydrogen peroxide formation and selectivity of the reaction can be calculated using the ring and disk currents. As can be seen in Figure 7, the current efficiencies for the **Aza-CMP** is around 70% whereas the selectivity is above 80%, indicating the excellent performance of the catalyst.

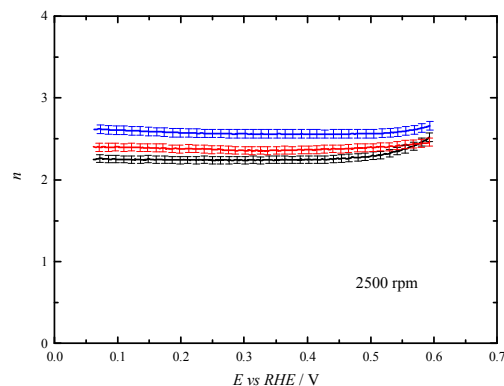


Figure 6. Dependence of the number of electrons transferred in the ORR reaction on the **Aza-CMP** (red line), **Aza-CMP@Co** (blue line) and glassy carbon (black line) electrodes in O_2 saturated 0.1 M NaOH solution.

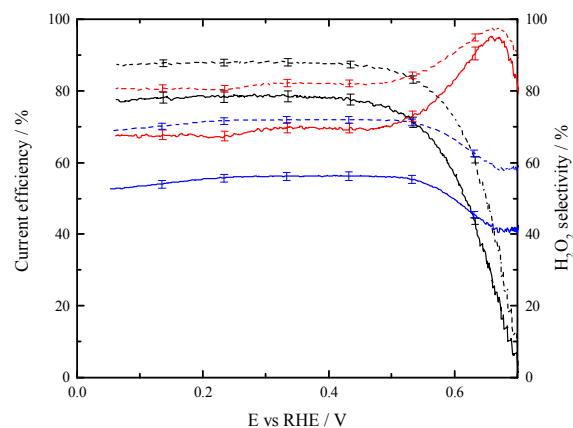
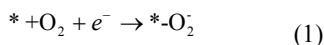


Figure 7. Current efficiency (full lines) and hydrogen peroxide selectivity (dashed lines) for the ORR reaction on the **Aza-CMP** (red line), **Aza-CMP@Co** (blue line) and glassy carbon (black line) electrodes in O_2 saturated 0.1 M NaOH solution.

In order to determine the Tafel slope of the process, which provides some insight into the reduction mechanism, kinetic currents in absence of diffusion effects were calculated using the Koutecky-Levich analysis plots using the following equation:

$$\frac{1}{I} = \frac{1}{I_{kin}} + \frac{1}{B\omega^{1/2}}$$

where I_{kin} is the kinetic current, and B is the proportionality factor between the diffusion limiting current and $\omega^{1/2}$. Figure 8 shows the Tafel plots for **Aza-CMP** and **Aza-CMP@Co**. In both cases, Tafel slopes values are ca. 110 mV, which is normally associated with a mechanism in which the rate-determining step is the first electron transfer, that is, the formation of an adsorbed superoxide species according to the following reaction:



where * denotes the active site on the material where the adsorption of O_2 takes place.

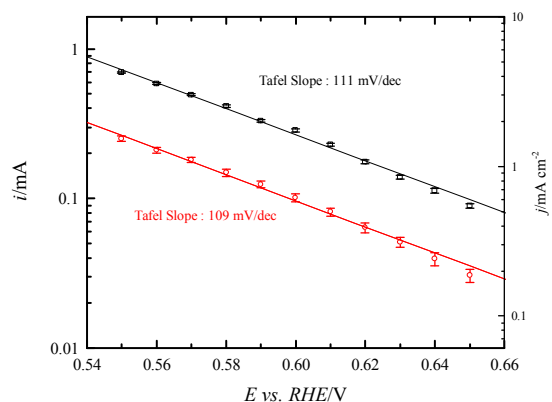


Figure 8. Tafel plots for the ORR obtained from the kinetics currents for the **Aza-CMP** (black line) and **Aza-CMP@Co** (red line).

In catalysis, benchmarking of the prepared catalysts is a very important issue.^{37,38} In electrochemistry, the comparison should be made using the current density using the active area at a constant potential. For metals, by means of well-defined surface reactions (such as oxide formation, hydrogen adsorption or monolayer deposition) active areas can be determined. However, for materials like the here investigated, with ill-defined surface processes, such a kind of determination is not possible. Instead, for this case, the current density referred to the geometrical area is used for comparison. At 0.60 V, which is equivalent to an overpotential of -0.08 V, the measured current density at 1600 rpm is -1.17 mA cm^{-2} , which is half the expected limiting current for a $2 e^-$ process at this rotation rate. The best performing alloy at this potential value, a PtHg alloy, only yielded ca -0.3 mA cm^{-2} , with similar selectivity for hydrogen peroxide formation at this potential value (ca. 75%).^{4,5} On the other hand, no significant currents are measured for nitrogen doped carbons (with an ill-defined structure) at this potential value.^{39,40} These comparisons highlights the excellent performance of the **Aza-CMP** material for the synthesis of hydrogen peroxide.

DFT calculations on the reaction mechanism. As aforementioned the **Aza-CMP** material has excellent properties for the reduction of oxygen to hydrogen peroxide. Moreover, the kinetic analysis suggests that the rate determining step would be the adsorption process to yield a superoxide. For a better understanding of the electrocatalysis of the reaction and to determine the active site on the **Aza-CMP** material, DFT calculations have been carried out. In a previous work,²¹ it was emphasized that, to activate oxygen on graphitic materials by means of monodentate chemisorption on carbon, two specific conditions would have to be fulfilled: a sufficiently destabilized carbon atom would have to be accessible and additional available charge would have to be provided. Changing from sp^2 hybridization state to sp^3 , the destabilized carbon atom would bond to oxygen; meanwhile the available charge would be localized on the adsorbed oxygen, stabilized by the solvation effect. Therefore, the chemisorbed oxygen species would have superoxide characteristics, which has been identified as the first intermediate in the reaction. Additionally, in a recent

previous work,²² it has been pointed out that hydrogenated pyridinic nitrogen in graphitic materials would destabilize their adjacent carbon atoms, and that the charge involved in such a hydrogenation would remain segregated, becoming available for reduction processes. As can be observed in Figure 9, which shows the periodic model of the **Aza-CMP** material used in our DFT calculations, the material presents several carbon atoms neighboring to pyridinic nitrogen that, if were hydrogenated, could promote the molecular oxygen activation. Therefore, prior to explore adsorption properties, the relevant hydrogenation state of the nitrogen atoms to consider should be determined.

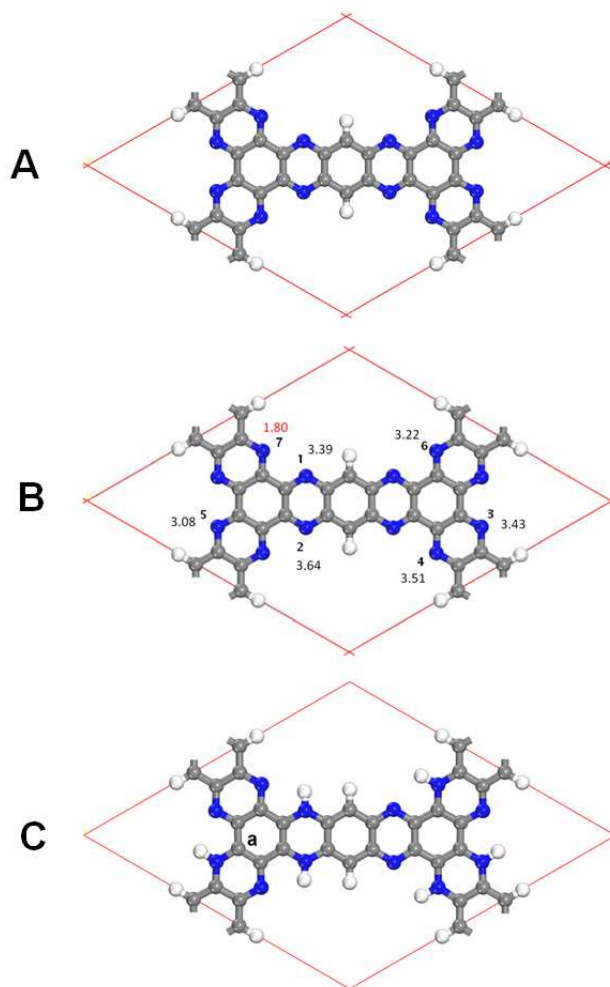
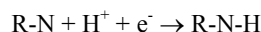


Figure 9. Periodic models of **Aza-CMP**. (A) Lattice (a broader supercell is also displayed in Figure S9). (B) Hydrogenation order of the pyridinic nitrogen atoms calculated by DFT and energies in eV of the process. (C) Relevant hydrogenation state (hexahydrogenated) and carbon atom tested as active site (labelled as a).

Nitrogen atoms can be hydrogenated through the reaction



The standard redox potential of this process can be calculated using the approach introduced by Anderson and col.^{20,36} which uses the strength of the N-H bond and the standard redox potential for the reaction $\text{H}^+(\text{aq}) + e^- = \text{H}(\text{aq})$. In the initial lattice (Figure 9A), the position of all the nitrogen atoms is equivalent, but as the hydrogenation process on a first nitrogen

atom takes place, the symmetry and equivalence of the nitrogen atoms is lost and differences in the energy of hydrogenation for the rest of nitrogen atoms appear. Figure 9B shows the order of hydrogenation of the different nitrogen atoms and the energy of the N-H bond. The N-H bond energy of the nitrogen atom labeled as **1** is 3.39 eV, which corresponds to standard potential of 1.29 V, that is, a potential which is positive to the onset of the ORR. Moreover, the hydrogenation of this first nitrogen atom favors the hydrogenation of the opposite nitrogen one in the same ring, since now the bond energy is 3.6 eV.

Therefore, it can be considered that both atoms hydrogenate simultaneously at a potential of *ca.* 1.3 V. The next atoms to be hydrogenated are those in the farthest ring in the lattice, those labelled as **3** and **4**, almost at the same potential. From that point, the hydrogenation process gets complicated due to the presence of steric problems. For instance, the hydrogenation of the nitrogen atom labelled as **7** has steric repulsion due to the presence of a hydrogen atom in the nitrogen atom **1**. Thus, the only nitrogen atoms in the cell for which there are no steric problems in the lattice are those labelled as **5** and **6**, which are hydrogenated at *ca.* 1.0-1.1 V. Finally, the N-H bond energy for carbon **7** is *ca.* 1.8 eV, which corresponds to a redox potential of *ca.* -0.3 V. All of these results clearly indicate that all the nitrogen atoms labelled from **1** to **6** would be hydrogenated at the onset of the ORR in a potential range between 1.1 and 1.4 V and no changes in the hydrogenation state of the material would occur during the ORR. In this sense, it should be noted that an oxidation current is measured above 1.1 V in the voltammogram of Figure 2, which can correspond to the dehydrogenation process.

Once the relevant hydrogenation state of the **Aza-CMP** material has been determined (Figure 9C), the activity towards the ORR of the material and the active site can be investigated. To this end, the adsorption of O₂ to form a superoxide species, which is considered both the first step and also the limiting step of the whole of the process, is studied as in previous reports.^{21,22} When the carbon atom labelled **a** in Figure 9C is tested for activation, under neutral charge conditions, the monodentate chemisorbed state of molecular oxygen displayed in Figure 10 is found, which is qualitatively similar to the ones previously found on others nitrogen-doped graphitic materials.^{21,22} From Figure 10B can be appreciated that charge is contributed from the hydrogenated pyridinic nitrogen atoms to the adsorbed oxygen enabling the chemisorbed state. The partial charges of Mulliken displayed in Figure 10C assign *ca.* 0.83 e⁻ to the chemisorbed species, indicating clearly that it has superoxide characteristics. Moreover, in Figure 10A, the presence of an abnormally short hydrogen bond between the adsorbed oxygen and the explicit water molecule can be identified, evidencing the relevance of the stabilizing role played by the solvation effect. However, when the energetics of the process displayed in Figure 11 is considered, it can be observed that, despite de fact that the found chemisorbed state is favorable by 0.52 eV, it is only stable by *ca.* 0.11 eV when compared to the physisorbed state. The reason for so small stability would be that the carbon atom involved in the chemisorbed state would not be sufficiently destabilized. This observation would be completely consistent with previous results,²¹ where it is found that hydrogenated pyridinic-nitrogen dopants in graphitic materials destabilize their adjacent carbon atoms mainly at armchair edges, giving rise to less effective destabilization at zig-zag edges. Moreover, the consequence of this observation would be key for hydrogen peroxide production purposes. Being a clearly favorable step, molecular oxygen could be activated. However, supporting only

slightly stable chemisorbed states, the scission of the O-O would be hindered, originating the selectivity towards the hydrogen peroxide production. Other carbon atoms were also explored for activation, though no additional insights were found.

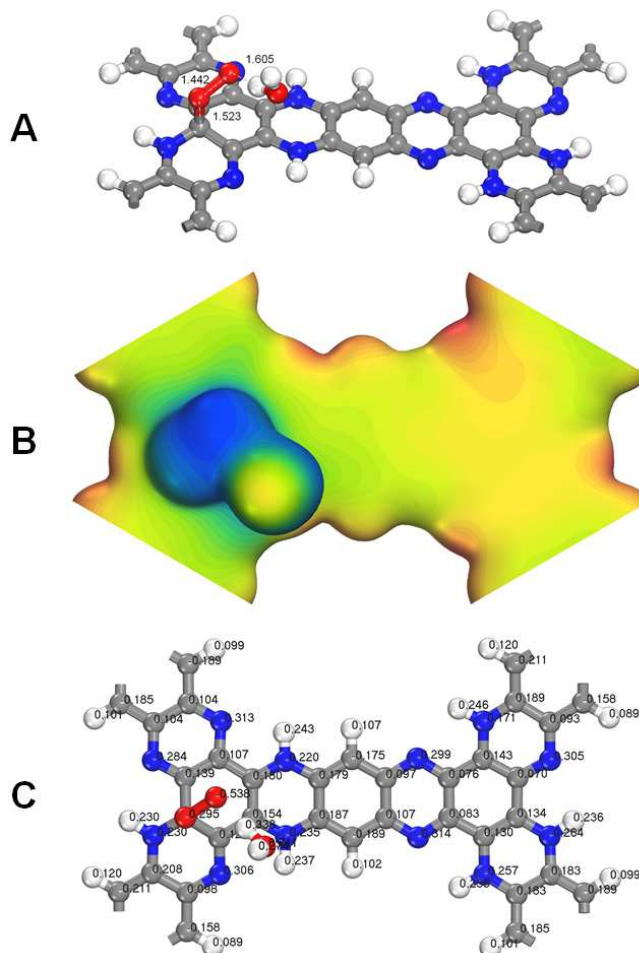


Figure 10. Monodentate chemisorbed state of molecular oxygen on the carbon atom labelled as **a** in Figure 9C. An explicit water molecule in addition to a continuum model was used as solvation effect treatment. (A) Adsorbent-adsorbate-solvent geometry [Å]. (B) Electrostatic potential [Ha/e⁻] mapped on the electron isodensity surface $\rho = 0.01 \text{ e}/\text{Å}^3$. (C) Mulliken partial charges [e⁻].

Given that, as the potential is made more negative, the charge of the electrode becomes more negative, the effect of the electrode potential can be examined by adding negative charge to the model. Moreover, such a kind of result can be used to explain the differences between the reactivity in acid and alkaline solutions. As the pH increases, the potential in the SHE scale at which the ORR shifts towards more negative values, and therefore, the surface charge of the electrode becomes more negative. For this case (Figure 9C), when a negative charge is added to the model, the adsorption energy for the oxygen species rises to 1.63 eV, meanwhile the stability in comparison with the physisorbed state rises to 0.18 eV, indicating that as the potential is made more negative (or the pH increases) the formation of the adsorbed superoxide species is more favorable. This effect explains the increased activity of the material as the pH increases, since the observed activity in acidic solutions is very low.

In brief, as it has been introduced, the formation of a chemisorbed superoxide state on graphitic materials poses two conditions: a carbon that is able to shift from a sp^2 to sp^3 hybridization and charge supplied by the material. For the investigated material, the presence of a hydrogenated nitrogen atom neighboring the considered carbon atom facilitates the hybridization state switching, whereas the charge is supplied from other hydrogenated nitrogen atoms. Therefore, the hydrogenation of the nitrogen atoms is a key element in this mechanism. When only four hydrogenated nitrogen atoms are considered, the adsorbed state becomes unstable, preventing the reaction, as observed in Figure 11. The investigated chemisorbed state becomes more stable when the charge on the electrode becomes negative.

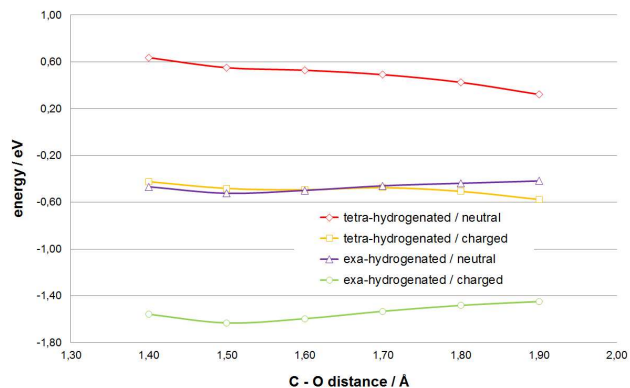


Figure 11. Total energies, referred to their respective references (adsorbent energy plus that corresponding to the adsorbate complex in the bulk), for an oxygen molecule located on top of the carbon atom *a*, for the different configurations estimated at different constrained distances between the carbon atom and the nearest oxygen atom of the molecule. Five explicit water molecules in addition to a continuum model were used as solvation effect treatment. A typical configuration of the formed explicit water solvation shell can be observed in Figure S10.

In comparison with other investigated carbon materials,¹⁴ the activity of the **Aza-CMP** material used as electrode for the ORR is smaller, though its selectivity towards the production of hydrogen peroxide is higher. Both observations can be explained by the lower stability of the adsorbed superoxide state on the investigated material in comparison with those present in other graphitic materials.^{21,22} An activating step less favorable implicates a smaller activity, meanwhile an adsorbed superoxide state presenting lower stability implicates that the adsorbate can be more easily desorbed upon protonation to the solution to yield HOO^- in alkaline media.

CONCLUSION

An electrochemical cell of hydrogen peroxide production requires of a catalyst for the oxygen reduction reaction optimally selective towards the goal. Moreover, the optimization of a catalyst requires of the control not only of the composition but also of the microstructure. The assembling of materials from molecular building blocks provides an excellent framework to achieve such a kind of control. Here, by using a polycondensation reaction between 1,2,4,5-benzenetetramine tetrahydrochloride and triquinoyl octahydrate, an aza-fused π -conjugated microporous polymer has been synthesized. The material shows excellent electrocatalytic properties for hydro-

gen peroxide formation at low overpotentials. The well-defined molecular structure of the polymer has allowed the use of DFT calculations to study the reduction mechanism and identifying the key elements that activate the material for the reaction. It has been shown that the hydrogenation of the nitrogen atoms is a key element in the activation of the neighboring carbon atom to adsorb oxygen.

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Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

ASSOCIATED CONTENT

Supporting Information. Additional experimental characterization data of the materials and computational details are provided as Supporting Information. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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2 SYNOPSIS TOC. In this work we show the excellent electrocatalytic performance for the hydrogen peroxide production of a
3 robust aza-fused π -conjugated microporous framework. Its reaction mechanism has been rationalized using theoretical calcu-
4 lations.
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