

Heterogeneous Pd-Catalyzed Efficient Synthesis of Imidazolones via Dehydrogenative Condensation between Ureas and 1,2-Diols

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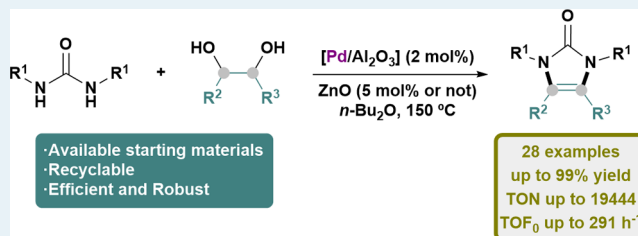
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ABSTRACT: A heterogeneously catalyzed protocol for the acceptorless dehydrogenative condensation between *N,N'*-disubstituted ureas and 1,2-diols to afford imidazolones was developed. Palladium nanoaggregates stabilized onto an alumina matrix with suitable acidic properties, namely, [Pd/Al₂O₃], was designed and successfully applied as efficient and reusable heterogeneous nanocatalyst for this relevant transformation. The methodology developed showed its wide applicability through the synthesis of more than 25 imidazolones with moderate to good yields, reaching a turnover number (TON) of up to 19444 and a initial turnover frequency (TOF₀) > 290 h⁻¹. The active nanostructured catalyst was fully characterized [X-ray diffraction (XRD), high-resolution transmission electron microscopy (HR-TEM), high-resolution scanning transmission electron microscopy (HR-STEM), energy-dispersive X-ray (EDX), Raman spectroscopy, temperature-programmed reduction (TPR), temperature-programmed desorption (TPD)-NH₃, TPD-CO₂, X-ray photoelectron spectroscopy (XPS), Brunauer–Emmett–Teller (BET) area], and mechanistic studies were performed. Moreover, other related Pd-based nanomaterials composed of different acidic or basic inorganic supports were synthesized and extensively compared in this reaction. These studies revealed that the presence of Pd nanoparticles with a wide range of sizes (average particle size 2.8 nm) over a metal oxide support with a high density of acid sites is a key point for the good activity of the material, γ -Al₂O₃ being the optimum support. Furthermore, a Pd–Zn cooperation effect was described for the dehydrogenative condensation of unactivated 1,2-diols, including ethylene glycol, with ureas. Two Pd–Zn bimetallic materials ([Pd/ZnO] and [Pd(5%)–Zn(5%)/Al₂O₃]) were also designed and characterized properly. These materials, as well as the [Pd/Al₂O₃] system in combination with catalytic amounts of ZnO, showed good activity and selectivity in the acceptorless dehydrogenative condensation between ureas and unactivated 1,2-diols. The heterogeneous nature of all of the described catalytic systems was demonstrated, and the reusability of the catalysts was proven.



KEYWORDS: heterogeneous catalysis, dehydrogenation, *N*-heterocycles, organic synthesis, palladium

INTRODUCTION

The development of new methodologies to synthesize heterocycles that fulfill the requirements of green chemistry is a major goal in current organic chemistry and catalysis.¹ In this direction, acceptorless dehydrogenative reactions (AD) are especially interesting processes as they are atom-economical, do not need stoichiometric reagents or O₂, and generate only H₂ and H₂O as secondary products.^{1a,c,m,2} Typically, in these transformations, an alcohol dehydrogenates affording H₂ and a carbonyl compound, which reacts with a coupling partner, generally an amine or another alcohol, to afford the desired condensation product. When applied intramolecularly or with ad hoc substrates, this method can easily afford heterocycles.^{1a,c,m} A large variety of heterocycles have been obtained employing AD strategies with homogeneous catalysts. Pioneer examples in this area involved mainly Ru³ and Ir^{3c,4} complexes as catalysts. In the past years, important efforts have been made to substitute these precious metals for non-noble metals such as Co⁵ or Mn.⁶ However, these processes present obvious

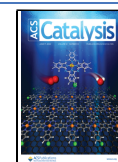
drawbacks from the sustainability viewpoint as they use metal complexes as catalysts, difficult to reuse, and frequently need basic additives. Hence, the development of solid nanostructured materials able to act as dehydrogenating catalysts in AD reactions affording heterocycles is of high interest.^{1m,2d,7} Furthermore, the accurate design of these materials bearing multifunctional features in their structure and avoiding the use of external additives can entail a significant improvement of these processes.

Five-membered cyclic ureas, including imidazolones and imidazolidinones, are relevant heterocycles present in the structure of currently commercialized drugs such as

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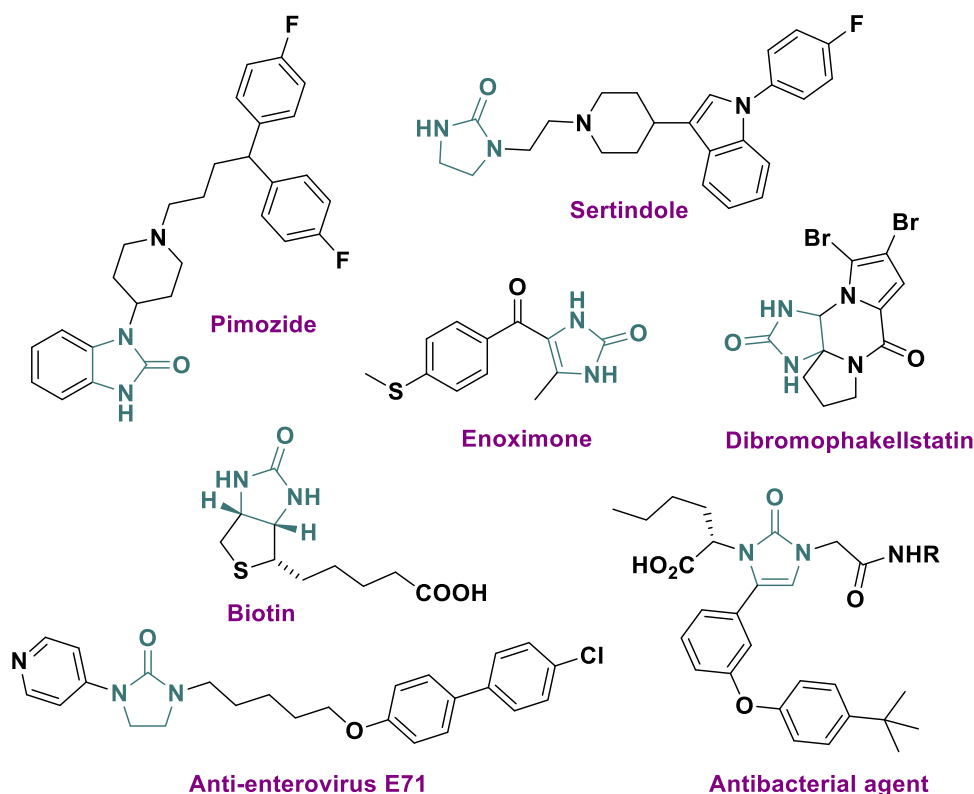


Figure 1. Imidazol(idin)one derivatives used as drugs or described as biologically active compounds.

enoximone,⁸ a cardiovascular agent, or pimozide⁹ and sertindole,¹⁰ two antipsychotics (Figure 1). The imidazol(idin)one scaffold is also present in compounds with antiviral¹¹ or antibacterial¹² activities (Figure 1).

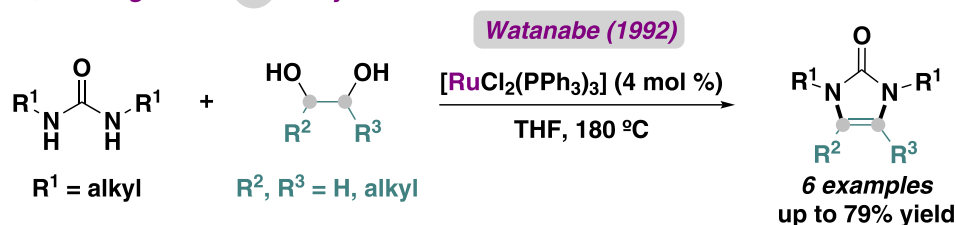
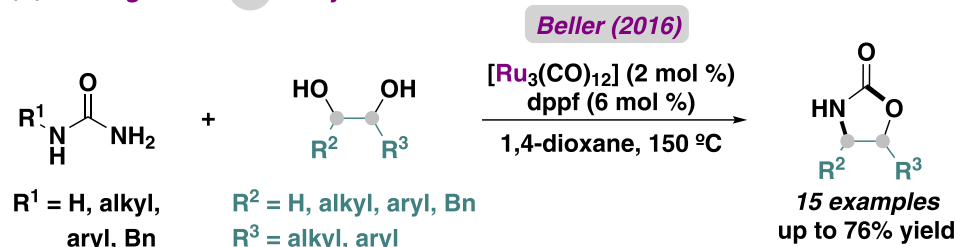
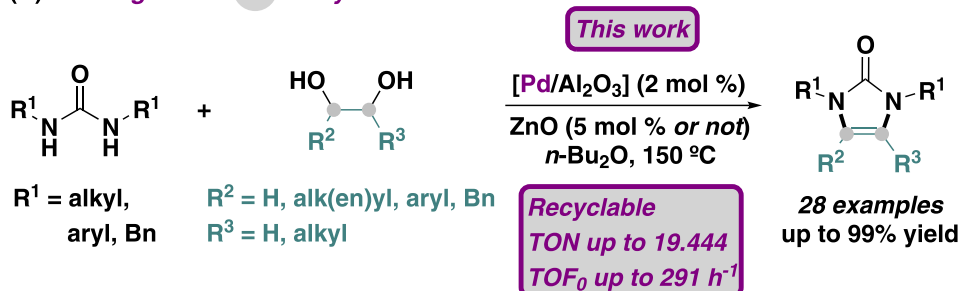
In addition, the cyclic urea structure can also be found in natural products such as dibromophakellstatin,¹³ a molecule with antitumor activity, and biotin¹⁴ or vitamin B7, key for the human metabolism (Figure 1). Hence, in the last two decades, several catalytic protocols have been investigated for the synthesis of imidazolones. Among these methodologies, hydroamidation of propargylic ureas,¹⁵ diamination of olefins or aryl ketones with diaziridines,¹⁶ and diamine carbonylation¹⁷ have been extensively developed. Despite their good applicability on a laboratory scale, these methods employ sophisticated molecules as starting materials or homogeneous species as catalysts. Other less developed methodologies involve heterocycles such as cyclic carbonates,¹⁸ triazoles,¹⁹ or hydantoins as starting materials.²⁰

In this context, developing catalytic methodologies able to afford imidazolones from simple and readily accessible ureas and 1,2-diols via AD condensation is of high interest. Efforts in this area have been made by the group of Watanabe, who described in the 1990s the formation of imidazolones from ureas and 1,2-diols employing a homogeneous Ru complex as the catalyst (Scheme 1A).^{3d} Very related to this, in 2016, Beller and co-workers published the formation of oxazolidinones from ureas and diols through a hydrogen-borrowing process.²¹ In this work, the authors used a Ru complex as the catalyst, and an asymmetric version of the reaction was developed (Scheme 1B). In the heterogeneous catalysis area, only a few examples have been reported for the dehydrogenative activation of diols to afford heterocycles such as (aza)indoles,^{7c,g,22} quinoxalines,²³ or (tetrahydro)quinolines.^{7g} In addition, the dehydro-

genative reaction of ureas with alcohols has been described with a $[\text{Ru}(\text{OH})_x/\text{TiO}_2]$ material, although affording only tertiary amines.²⁴ Therefore, the development of a protocol employing a stable and reusable heterogeneous material to obtain imidazolones from ureas and 1,2-diols is still a point of interest in synthetic and catalytic fields. To succeed in this goal, a material able to catalyze both dehydrogenation and condensation steps should be designed. In this direction, combining transition metal nanoparticles, known to be active in dehydrogenative processes, with inorganic metal oxide supports, having suitable acid–base properties, is a feasible approach to this problem. Here, we describe the first heterogeneously catalyzed protocol to perform the efficient and straightforward synthesis of imidazolones from ureas and 1,2-diols (including ethylene glycol) using a $[\text{Pd}/\text{Al}_2\text{O}_3]$ nanomaterial as a reusable catalyst (Scheme 1C).

RESULTS AND DISCUSSION

As a starting point of our investigation, a variety of solid nanomaterials composed of metal nanoparticles supported over $\gamma\text{-Al}_2\text{O}_3$ were prepared and tested in the reaction between N,N' -dicyclohexylurea **1** and 3-butene-1,2-diol **2** (Table 1, entries 2–9). Alumina was selected due to its demonstrated suitability to act as a metal nanoparticle support in dehydrogenation reactions.^{7c,g,25} Among the tested materials, those presenting Pd, Pt, and Ru nanoparticles afforded imidazolone **3** in good to excellent yields (Table 1, entries 7–9), the Pd-nanostructured material being the one that yielded the best results. Moreover, $[\text{Pd}/\text{Al}_2\text{O}_3]$ also showed excellent activities when it was tested without being subjected to a hydrogenating pretreatment before reaction (Table 1, entry 10), unlike the Pt material whose activity decreased significantly when it was not reduced (Table S1, entry 8).

Scheme 1. Examples of Dehydrogenative Condensations between Ureas and 1,2-Diols^a(A) *Homogeneous Ru-catalysed*(B) *Homogeneous Ru-catalysed*(C) *Heterogeneous Pd-catalysed*

^a(A) Ru homogeneously catalyzed acceptorless dehydrogenation to afford imidazolones, as reported by Watanabe and co-workers; (B) Ru homogeneously catalyzed hydrogen-borrowing to yield oxazolidones, as reported by Beller and co-workers; (C) Pd heterogeneously catalyzed acceptorless dehydrogenation to yield imidazolones, as reported in this work. Bn = benzyl, dppe = 1,1'-ferrocenediyl-bis(diphenylphosphine).

Hence, we selected the [Pd/Al₂O₃] material to continue our study. Different reaction parameters were studied, and it was determined that an initial concentration of urea **1** between 0.5 and 0.75 M (Table S2, entries 4 and 5) and 150 °C (Table S3, entry 5) afforded excellent yields of imidazolone **3**. In addition, the influence of the solvent on the reaction was explored, and the best results were observed when employing dibutyl ether or *o*-xylene as solvents (Table S4, entries 6 and 7). Regarding the catalyst amount, good yields of **3** were obtained with a mol % of Pd larger than 0.5 (80%, Table 1, entry 11, and Table S5), 2 mol % being the optimum catalyst amount affording imidazolone **3** in 90% yield (Table 1, entry 9). Gratifyingly, the [Pd/Al₂O₃] system reached a TON value of 19444 when the reaction was performed at 0.05 mol % Pd for 90 h (Table 1, entry 14) and an initial turnover frequency (TOF₀) value of 291 h⁻¹ at 0.5 mol % Pd (Table 1, entry 11). Moreover, [Pd/Al₂O₃] was compared with the [RuCl₂(PPh₃)₂] complex, described by the group of Watanabe for the synthesis of imidazolones from ureas and 1,2-diols.^{3d} Although the Ru complex afforded imidazolone **3** in good yields, [Pd/Al₂O₃] showed better initial rates and TON and TOF₀ values (Table 1, entry 15, and Figure S1E). In addition, commercially available palladium-based materials such as [Pd/Al₂O₃] and

[Pd/C] were tested under optimized reaction conditions (Table 1, entries 16 and 17, and Figure S1C,D) and were demonstrated to be less active than our [Pd/Al₂O₃] nanomaterial.

With the aim of better understanding the [Pd/Al₂O₃]-catalyzed dehydrogenative condensation of urea **1** and 1,2-diol **2**, kinetic and mechanistic studies were performed. Thus, it was determined that the reaction follows the first order for urea **1**, diol **2**, and the Pd catalyst (Figure S2). The reduction of the alkene moiety in imidazolone **3** pointed out a dehydrogenative mechanism, with the concomitant formation of H₂. This assumption was confirmed by the H₂ detection in the reaction between *N,N'*-dicyclohexylurea **1** and 1-phenylethane-1,2-diol **2** (Figure S3). Moreover, the initial formation rate and yield of **3** did not show significant changes when the reaction was conducted in an inert atmosphere versus in air, whereas the yield of **3** was lower under O₂ conditions (Table S6). The good tolerance of the reaction to be conducted under air conditions is a remarkable advantage. With this information in hand, it can be deduced that the reaction proceeds through two steps: the first dehydrogenation of 3-butene-1,2-diol **2** to 1-hydroxybutan-2-one **4** catalyzed by Pd, followed by a condensation of 1-hydroxybutan-2-one **4** with *N,N'*-dicyclo-

Table 1. Metal-Catalyzed Synthesis of Imidazolone 3 by a Dehydrogenative Condensation between Urea 1 and Diol 2

entry ^a	[cat.] (mol %)	3 (%) ^b	<i>r</i> ₀ 3 (%/h) ^b	TON ^c	TOF ₀ (h ⁻¹) ^d
1	-	0	nd	nd	nd
2	[Fe/Al ₂ O ₃] (2)	0	nd	nd	nd
3	[Co/Al ₂ O ₃] (2)	1	nd	nd	nd
4	[Ni/Al ₂ O ₃] (2)	0	nd	nd	nd
5	[Zn/Al ₂ O ₃] (2)	0	nd	nd	nd
6	[Ag/Al ₂ O ₃] (2)	7	nd	nd	nd
7	[Ru/Al ₂ O ₃] (2)	44	nd	nd	nd
8	[Pt/Al ₂ O ₃] (2)	78	nd	nd	nd
9	[Pd/Al ₂ O ₃] (2)	90	27.5	633	194
10 ^e	[Pd/Al ₂ O ₃] (2)	86	21.0	nd	nd
11	[Pd/Al ₂ O ₃] (0.5)	80	10.5	2222	291
12	[Pd/Al ₂ O ₃] (0.25)	61	3.3	3389	183
13	[Pd/Al ₂ O ₃] (0.05)	33	nd	9167	nd
14 ^f	[Pd/Al ₂ O ₃] (0.05)	70	nd	19 444	nd
15	[RuCl ₂ (PPh ₃) ₂] (2)	71	14.2	36	7
16 ^g	[Pd/Al ₂ O ₃]-ca. (2)	62	6.3	nd	nd
17 ^h	[Pd/C]-ca. (2)	16	26.7	nd	nd

^aStandard reaction conditions: *N,N'*-dicyclohexylurea 1 (112.17 mg, 0.5 mmol), 3,4-dihydroxy-1-butene 2 (84 μL, 1 mmol, 2 equiv), [metal/support] or complex (0.01 mmol, 2 mol %), and *n*-Bu₂O (1 mL) at 150 °C for 16 h. ^bYield of 3 and initial reaction rates (*r*₀) were calculated by gas chromatography (GC) using *n*-dodecane as an internal standard. ^cYield per mol % Pd on the surface (calculated by CO chemisorption). ^dInitial reaction rate per mol % Pd on the surface (calculated by CO chemisorption). ^eReaction run with an unreduced material. ^fRun for 90 h. ^g[Pd/Al₂O₃]-ca. stands for a commercially available Pd/Al₂O₃ material with 5 wt % reduced under H₂ at 200 °C for 2 h. ^h[Pd/C]-ca. stands for a commercially available Pd/C material with 5 wt % reduced under H₂ at 200 °C for 2 h. nd = not determined.

Table 2. Textural and Physicochemical Properties of Pd-Supported Materials^a

entry ^b	catalyst	BET (m ² /g) ^c	Pd part. size (nm) ^d	acid site density (μmol/g) ^e	3 (%) ^f	<i>r</i> ₀ 3 (%/h) ^f	4 (%) ^f	<i>r</i> ₀ 4 (%/h) ^f
1	[Pd/CaO]	42	3.2	6	51	6.8	5	6.0
2	[Pd/MgO]	5	2.6	7	49	10.6	4	4.3
3	[Pd/SiO ₂]	280	4.6	30	52	8.3	33	32.0
4	[Pd/ZrO ₂]	69	2.8	107	54	7.6	8	72.0
5	[Pd/TiO ₂]	42	2.5	127	65	8.3	15	48.6
6	[Pd/Al ₂ O ₃]	180/210 ^g	2.8	200/232 ^h	90	27.5	32	76.7
7	[Pd/Al ₂ O ₃ -1%]	209	2.5	162	71	21.0	16	36.3
8	[Pd/Al ₂ O ₃ -10%]	125	4.2	193	77	14.0	25	43.8
9	[Pd/Al ₂ O ₃ -10 °C/min]	178	5.1	107	78	12.5	27	45.6
10	[Pd/Al ₂ O ₃ -30 °C/min]	170	4.7	197	75	10.8	27	27.7
11	[Pd/Al ₂ O ₃ -300 °C]	160	2.3	223	75	14.5	21	65.9
12	[Pd/Al ₂ O ₃ -600 °C]	183	14.4	67	59	9.3	7	8.4

^aYield and initial rates of their catalytic activity in the dehydrogenative condensation between 1 and 2 and dehydrogenation of 2. ^bStandard reaction conditions for 1,3-dicyclohexyl-4-ethyl-1,3-dihydro-2*H*-imidazol-2-one 3: *N,N'*-dicyclohexylurea 1 (112.17 mg, 0.5 mmol), 3,4-dihydroxy-1-butene 2 (84 μL, 1 mmol, 2 equiv), Pd catalyst (21.3 mg, 0.01 mmol, 2 mol %), and *n*-Bu₂O (1 mL) at 150 °C for 16 h. Standard reaction conditions for 1-hydroxybutan-2-one 4: 3,4-dihydroxy-1-butene 2 (84 μL, 1 mmol), Pd catalyst (21.3 mg, 0.01 mmol, 1 mol %), and *n*-Bu₂O (1 mL) at 150 °C for 1 h. ^cValues calculated from N₂ adsorption isotherms (Brunauer–Emmett–Teller, BET method). ^dAverage diameter of Pd nanoparticles calculated from scanning transmission electron microscopy (STEM) measurements. ^eTotal amount of NH₃ adsorbed by the catalyst determined through temperature-programmed desorption (TPD)-NH₃. ^fYields of 3 and 4 and initial reaction rates were calculated by GC using *n*-dodecane as an internal standard. ^gBET of γ-Al₂O₃. ^hTotal amount of NH₃ adsorbed by γ-Al₂O₃ determined through TPD-NH₃.

hexylurea 1 to afford imidazolone 3. To determine the rate-limiting step of the whole process, we studied kinetically the dehydrogenation of 3-butene-1,2-diol 2 to 1-hydroxybutan-2-one 4 catalyzed by [Pd/Al₂O₃] as well as the condensation

between *N,N'*-dicyclohexylurea 1 and 1-hydroxybutan-2-one 4 in the presence of [Pd/Al₂O₃]. Interestingly, we could measure an initial rate of 76.6%/h for the dehydrogenation process (Table 2, entry 6), whereas the condensation showed a rate of

23.7%/h (Scheme S1C), much more similar to the rate of the global reaction (27.5%/h). Hence, it can be concluded that the condensation is the rate-limiting step of the process. Control experiments of the condensation reaction in the absence of the catalyst or with only calcined γ -Al₂O₃ demonstrated that this step is accelerated in the presence of the γ -Al₂O₃ support (Scheme S1).

The significant relevance of Al₂O₃ in both dehydrogenation²⁶ and condensation steps encouraged us to study the influence of other metal oxides as supports able to stabilize palladium nanoaggregates. Thus, the corresponding [Pd/CaO], [Pd/MgO], [Pd/SiO₂], [Pd/ZrO₂], and [Pd/TiO₂] nanostructured materials were prepared and tested in the dehydrogenative condensation between urea **1** and 1,2-diol **2** (Table 2, entries 1–6). All of the materials afforded imidazolone **3** in moderate yields (49–61%) and with lower initial rates than [Pd/Al₂O₃] (Table 2, entries 1–6). Dehydrogenation and condensation steps were studied independently for all of the Pd materials, revealing that [Pd/Al₂O₃] is the most active catalyst in terms of the initial rate for both steps (Table 2, entries 1–6, and Table S7). Condensation reactions are usually catalyzed in acidic or basic media. In addition, it has been reported that dehydrogenation reactions catalyzed by metal nanoparticles over metal oxide supports are strongly influenced by the acid–base properties of the support.^{25a,c,f,27} Thus, acidic properties of the materials were evaluated by temperature-programmed desorption of ammonia (TPD-NH₃), which enabled us to quantify the acid site density and determine their strength (Table 2 and Figure S24). [Pd/CaO] and [Pd/MgO], considered as basic materials, barely presented acid sites. In contrast, for the other materials, acid sites were detected and quantified in the following order: [Pd/Al₂O₃] > [Pd/TiO₂] > [Pd/ZrO₂] > [Pd/SiO₂]. In all of the cases, the TPD-NH₃ profiles showed a maximum at a temperature between 193 and 196 °C, associated with weak acid sites.²⁸ Interestingly, calcined γ -Al₂O₃ showed a slightly higher number of acid sites than [Pd/Al₂O₃] (Table 2, entry 6), with maximums at 234, 405, and 632 °C associated with the weak, medium, and strong sites, respectively (Figure S24H). In addition, TPD-CO₂ experiments of [Pd/Al₂O₃] and γ -Al₂O₃ were performed, and basic sites were determined to be significantly inferior to acid sites for these materials (70 and 12 μ mol/g for γ -Al₂O₃ and [Pd/Al₂O₃], respectively). An analysis of these TPD-CO₂ profiles reveals for [Pd/Al₂O₃] maximums at 101, 209, and 689 °C associated with the weak, medium, and strong sites, respectively, whereas γ -Al₂O₃ only displays maximums correlated to weak and strong sites (101 and 689 °C) (Fig. S26). The relationships between the number of acid sites and the initial rates of dehydrogenative condensation between urea **1** and 1,2-diol **2**, dehydrogenation of 1,2-diol **2**, and condensation between urea **1** and ketoalcohol **4** were considered (Figure 2). Although, in all of the cases, a maximum is observed for the most acidic material [Pd/Al₂O₃], dehydrogenation appears to be the transformation whose initial rate has a more linear relationship with the number of acid sites in the material.

At this point, several modifications in the [Pd/Al₂O₃] synthesis were explored. The corresponding materials with variations in the palladium loading (1 and 10 wt %, instead of 5 wt %), the calcination ramp (10 and 30 °C/min, instead of 1 °C/min), and the calcination temperature (300 and 600 °C, instead of 450 °C) were prepared and evaluated in the dehydrogenative condensation between urea **1** and 1,2-diol **2**

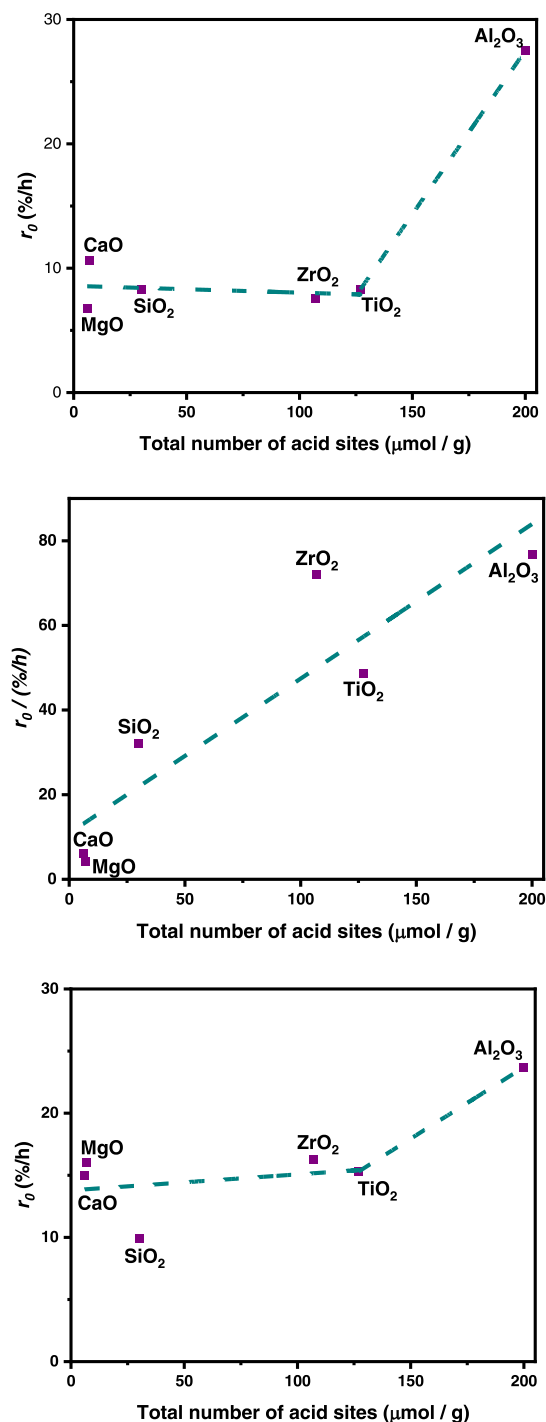


Figure 2. Initial rates (r_0) vs the total number of acid sites for Pd-supported catalysts in the dehydrogenative cyclization between urea **1** and diol **2** to yield imidazol-2-one **3** (top), the dehydrogenation of diol **2** to ketoalcohol **4** (middle), and condensation between urea **1** and ketoalcohol **4** (bottom). Standard reaction conditions: *N,N'*-dicyclohexylurea **1** (0–0.5 mmol), 3,4-dihydroxy-1-butene **2** (0–1 mmol) or 1-hydroxybutan-2-one **4** (0–1 mmol), [Pd/support] material (2 mol %), *n*-dodecane (0.26 mmol) as an internal standard, and *n*-Bu₂O (1 mL) at 150 °C.

as well as in the dehydrogenation of 1,2-diol **2** (Table 2, entries 7–12). All of the studied nanomaterials were shown to be less active than the originally prepared [Pd/Al₂O₃] for both dehydrogenative condensation and dehydrogenation. TPD-NH₃ experiments of these materials showed maximums

between 180 and 208 °C, which are characteristic of weak acid sites (Figure S25). In addition, acid site densities were significantly lower for [Pd/Al₂O₃-10 °C/min] and [Pd/Al₂O₃-600 °C] (Table 2, entries 9 and 12).

To understand the structural features of [Pd/Al₂O₃] that confer this material with such a high activity in the synthesis of imidazolone 3, a detailed characterization was performed. Moreover, to identify the structural aspects that are more relevant to the good catalytic activity of [Pd/Al₂O₃], other palladium materials were also characterized by some of the techniques. Surface areas of all of the materials were determined (Table 2), with [Pd/Al₂O₃] and [Pd/SiO₂] materials being the ones with larger areas.

The X-ray diffraction (XRD) pattern of [Pd/Al₂O₃] (Figure 3, top) shows peaks at 2θ values of 39.9, 46.3, 67.8, 81.9, and

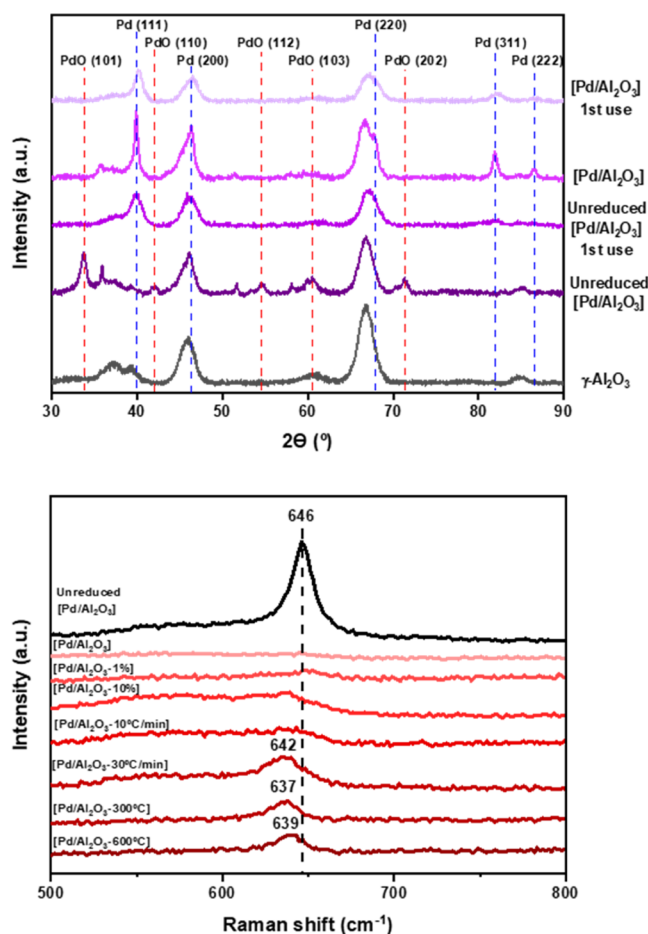


Figure 3. Top: X-ray diffraction patterns of γ -Al₂O₃ and [Pd/Al₂O₃] materials; the diffraction planes of Pd and PdO have been assigned. Bottom: Raman spectra of [Pd/Al₂O₃] materials.

86.4° corresponding to (111), (200), (220), (311), and (222) planes, respectively, of metallic Pd in a cubic close-packed structure (JCPDS card no 00-046-1043). In contrast, unreduced [Pd/Al₂O₃] shows peaks at values of 33.8, 42.2, 54.6, 60.5, and 71.4° corresponding to the planes (101), (110), (112), (103), and (202), respectively, of tetragonal PdO (JCPDS card no 00-041-1107) (Figure 3, top). It is interesting to note that when [Pd/Al₂O₃] was employed as the catalyst without previous reduction, the resulting material after reaction showed an XRD pattern similar to that of reduced [Pd/Al₂O₃]. Hence, this enables us to deduce that PdO crystallites detected

by XRD, typically those larger than 4–5 nm, are reduced under the reaction conditions. In both unreduced and reduced [Pd/Al₂O₃] materials, peak shapes are either broad or show broader tails and narrower tips, suggesting the presence of small crystallites or a mixture of different crystallite sizes.²⁹ Characteristic Pd and PdO peaks were detected in all of the Pd materials, reduced or without reduction treatment (Figures S10 and S12), with the exception of [Pd/Al₂O₃-1%], which showed only the peaks of γ -Al₂O₃ (Figure S12A). In contrast, [Pd/Al₂O₃-10%], [Pd/Al₂O₃-10 °C/min], [Pd/Al₂O₃-30 °C/min], and [Pd/Al₂O₃-600 °C] (Figure S12B–D,F) showed narrower peaks, suggesting the presence of larger Pd crystallites.

To further explore materials' structure and determine Pd nanoparticle sizes, the materials were examined by high-angle annular dark-field–high-resolution scanning transmission electron microscopy (HAADF–HRSTEM) (Figures 4, S17, and S18). Average particle sizes of 3.0 and 2.8 nm were measured for unreduced and reduced [Pd/Al₂O₃] materials, respectively. The Pd materials with supports other than γ -Al₂O₃ showed average particle sizes of around 3 nm, with the exception of [Pd/SiO₂] in which a medium size of 4.6 nm was measured (Table 2 and Figure S17). In the case of materials based on Pd nanoparticles over γ -Al₂O₃, a larger average Pd nanoparticle size was confirmed in materials prepared with higher Pd loadings (10 wt %), at higher calcination temperatures (600 °C), or in faster calcination ramps (10 and 30 °C/min). A uniform distribution of Pd in [Pd/Al₂O₃] could be confirmed by energy-dispersive X-ray (EDX) elemental analysis (Figures 4 and S20). In addition, high-resolution transmission electron microscopy (HR-TEM) images of [Pd/Al₂O₃] were also obtained (Figure S19).

At this point, it was interesting to investigate whether PdO particles with a size inferior to 4–5 nm were present in the reduced materials. To this end, Raman spectra of all of the reduced materials were registered and compared with the spectrum of unreduced [Pd/Al₂O₃]. Remarkably, the PdO peak at 646 cm⁻¹ in the unreduced [Pd/Al₂O₃] completely disappeared after reduction (Figure 3, bottom).³⁰ [Pd/SiO₂] showed a peak at 637 cm⁻¹, suggesting the incomplete reduction of PdO in this material (Figure S14C). In the case of [Pd/TiO₂], signals at 511 and 636 can be assigned to TiO₂ (Figure S14F).³¹ Regarding the other [Pd/Al₂O₃] materials, it is remarkable that [Pd/Al₂O₃-30 °C/min], [Pd/Al₂O₃-300 °C], and [Pd/Al₂O₃-600 °C] displayed signals at 642, 637, and 639 cm⁻¹, which suggests the presence of PdO particles in these reduced materials (Figure 3, bottom).

Complementarily, X-ray photoelectron spectroscopic (XPS) studies of unreduced and reduced [Pd/Al₂O₃] were performed (Figure 5). The Pd 3d spectrum of unreduced [Pd/Al₂O₃] could be deconvoluted into four peaks corresponding to two doublets: one at 337.2 eV (3d_{5/2}) and 342.5 eV (3d_{3/2}) belonging to Pd(0) and the other at 338.9 eV (3d_{5/2}) and 344.5 eV (3d_{3/2}) belonging to Pd(II). In contrast, reduced [Pd/Al₂O₃] only showed a doublet at 336.9 eV (3d_{5/2}) and 342.0 eV (3d_{3/2}) assigned to Pd(0).

Finally, H₂-temperature-programmed reduction (TPR) studies of the Pd materials with different metal oxides as supports revealed the presence of two or more peaks at temperatures lower than 200 °C in all of the cases (Figure S23). In TPR studies, H₂ consumption at higher temperatures is associated with smaller-sized particles, due to stronger metal–support interactions.^{28a,32} Thus, the presence of several

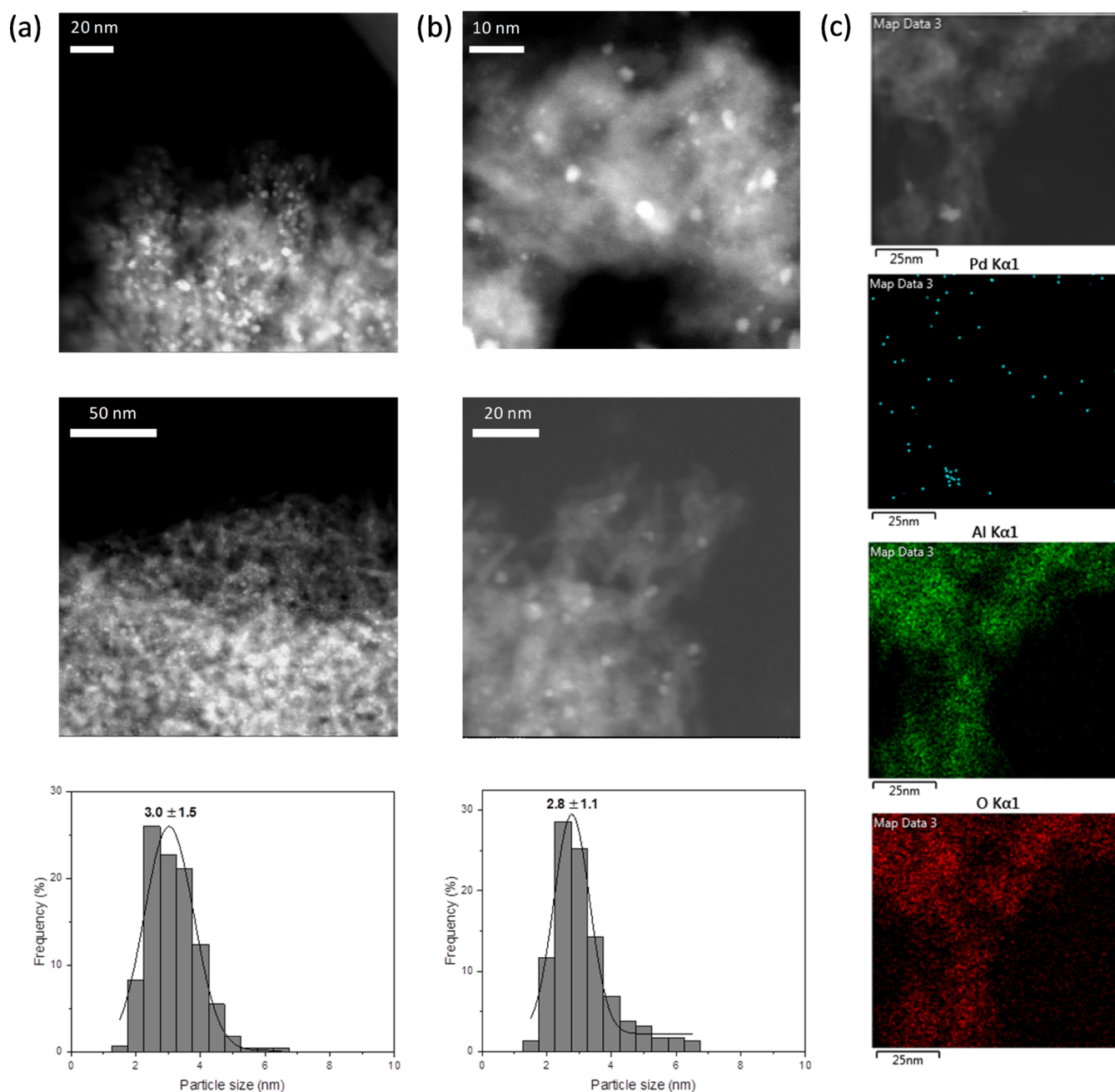


Figure 4. HAADF–HRSTEM images and Pd particle size distribution of unreduced [Pd/Al₂O₃] (a) and [Pd/Al₂O₃] (b) materials; EDX elemental mapping of Pd, Al, and O for [Pd/Al₂O₃] (c).

peaks confirms that the materials contain Pd nanoparticles of different sizes, as the XRD and STEM studies suggested. In addition, a maximum of low intensity between 311 and 409 °C was observed for most of the materials. H₂ consumption at temperatures of around 300 °C was attributed to the reduction of smaller PdO particles or the support.^{28a} It is interesting to note that an important H₂ consumption between 336 and 409 °C was observed for [Pd/Al₂O₃-300 °C] containing a higher amount of smaller particles (Figure S23I). In the case of [Pd/MgO], an intense peak at 638 °C was detected corresponding to the formation of Mg₂H or Mg₂OH species (Figure S23B).³³ Remarkably, TPR profiles of [Pd/Al₂O₃] and [Pd/TiO₂] showed a negative peak at 72 °C (Figure S23F,G), indicating the release of H₂ after the reduction of bulk PdO at room temperature and the formation of β-PdH.^{28a}

With all of this information in hand, it can be deduced that the material composed of Pd(0) nanoparticles of several sizes (2.8 nm average) over the acidic γ-Al₂O₃ is the optimum catalyst for dehydrogenative condensation between urea **1** and 1,2-diol **2**.

Then, the heterogeneous nature of the catalysis was proved by performing a hot filtration test (Figure S5). In addition, inductively coupled plasma (ICP) measurements of the reaction mixture and [Pd/Al₂O₃] after reaction also demonstrated that Pd leaching did not occur under the reaction conditions (Pd content measured by ICP: fresh catalyst, 5.3 wt %; used catalyst, 5.1 wt %; and Pd in solution, 0.004 mg; see Supporting Information, SI, Section S6.2). Thus, the reusability of the material was studied with unreduced [Pd/Al₂O₃] for practical reasons. To our delight, the material could

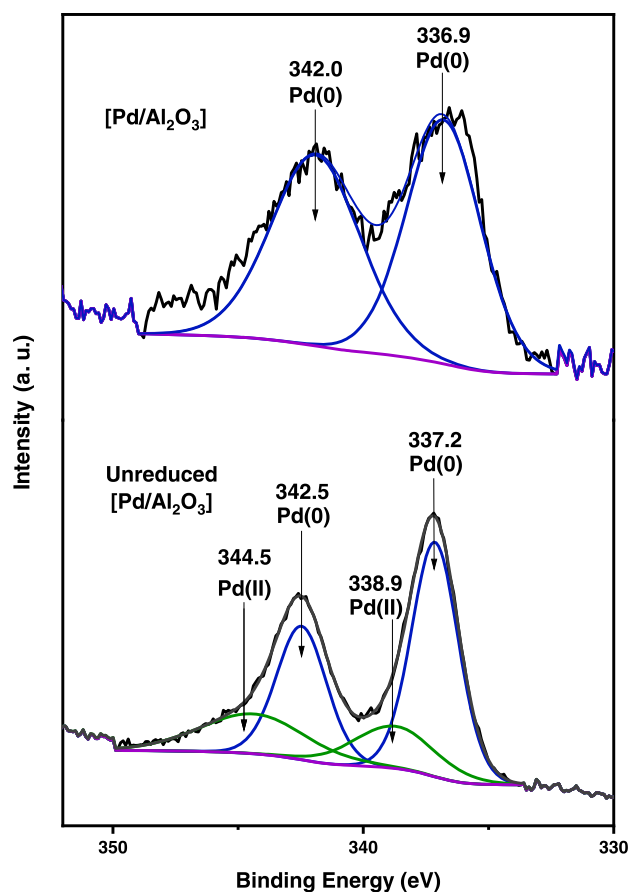


Figure 5. Pd 3d XPS spectra of $[\text{Pd}/\text{Al}_2\text{O}_3]$ materials.

be reused for six cycles, with a calcination treatment after each use to eliminate the deposition of organic compounds on the catalyst's surface, and without significant loss of its activity and selectivity (Figure 6; see SI for the experimental procedure). In fact, initial rates were determined for each use of the catalyst, confirming the good activity of the reused material. As commented before, the XRD pattern of unreduced $[\text{Pd}/\text{Al}_2\text{O}_3]$ after the first use showed typical peaks of Pd(0) (Figure 3, top). No significant changes were observed in the XRD of either the unreduced material after the sixth use or the reduced material after the first use (Figure 3, top and Figure S11). In contrast, XPS studies of reduced $[\text{Pd}/\text{Al}_2\text{O}_3]$ after the first use showed a Pd 3d spectrum that could be deconvoluted into two doublets, indicating the presence of mainly Pd(0) and some amount of PdO in this material (Figure S16C). Moreover, BE values of Pd(0) and PdO in the used material appeared at lower eV values, suggesting the presence of larger Pd nanoparticles.^{28a,34} In fact, HAADF–HRSTEM studies of unreduced $[\text{Pd}/\text{Al}_2\text{O}_3]$ after the first and sixth uses showed a significant increase in the average particle size (Figure S21). Despite the presence of larger particles, these materials also displayed Pd particles with a size <5 nm; thus, it is not possible to determine whether the catalytic activity corresponds to a specific Pd particle size or to the presence of a wide variety of particles.

Once the reusability of the material was demonstrated, we decided to investigate its range of application for the synthesis of a variety of imidazolones. First, we studied the reactions of a variety of ureas with 1,2-diols bearing an alkenyl or phenyl group in the β position to one of the hydroxyl groups (Scheme 2). A wide range of imidazolones were obtained from 3-butene-1,2-diol **2** and N,N' -substituted ureas. N,N' -dialkyl-substituted ureas afforded the corresponding imidazolones **3**, **5**, and **6** in moderate to good yields (50–79%). To our delight,

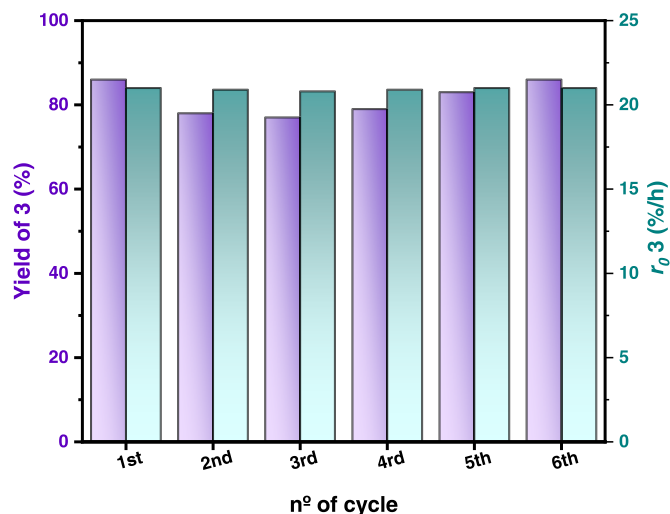
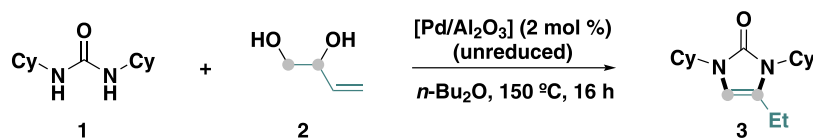
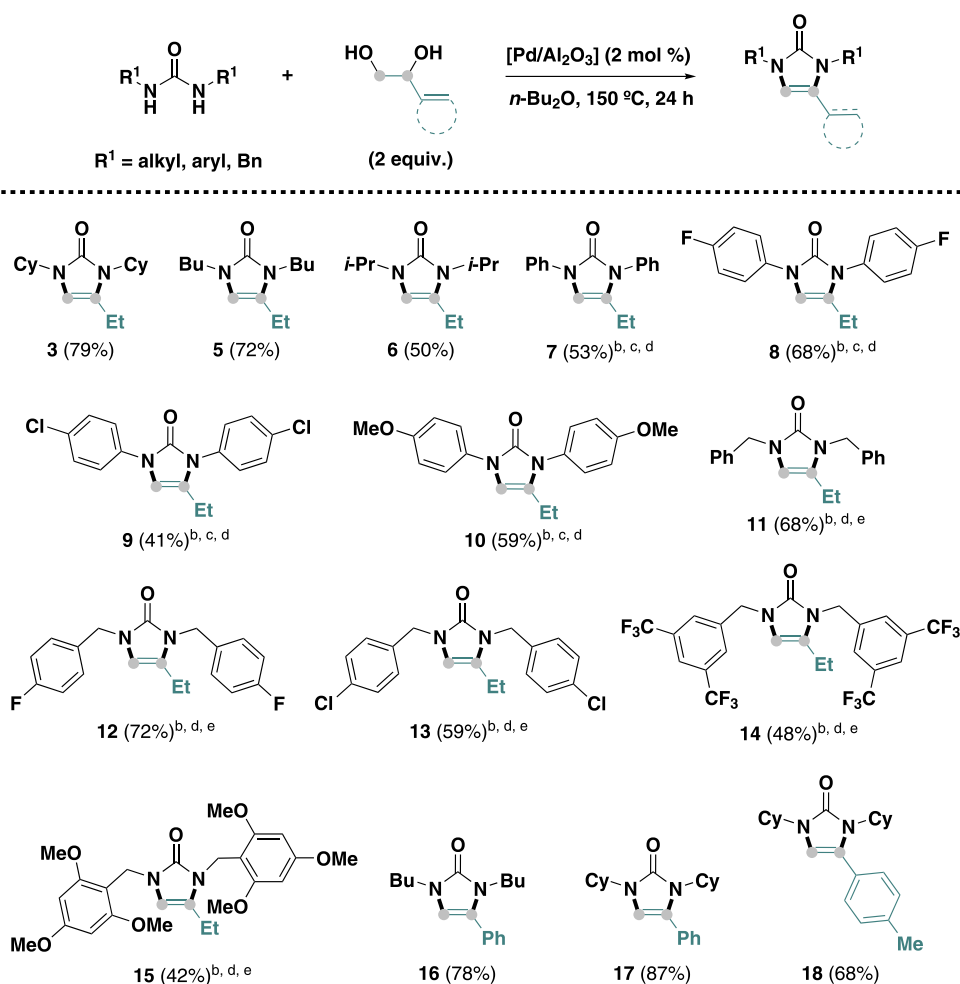


Figure 6. $[\text{Pd}/\text{Al}_2\text{O}_3]$ catalyst reuse for dehydrogenative cyclization of urea **1** and diol **2** to synthesize imidazol-2-one **3**. Standard reaction conditions: N,N' -dicyclohexylurea **1** (590.9 mg, 2.5 mmol), 3,4-dihydroxy-1-butene **2** (0.42 mL, 5 mmol, 2 equiv), $[\text{Pd}/\text{Al}_2\text{O}_3]$ (unreduced) (106.4 mg, 0.05 mmol, 2 mol %), n -dodecane (225 mg, 1.3 mmol) as an internal standard, and n -Bu₂O (5 mL) at 150 °C for 16 h.

Scheme 2. [Pd/Al₂O₃]-Catalyzed Synthesis of Imidazol-2-ones from *N,N'*-Disubstituted Ureas and 3,4-Dihydroxy-1-butene (2) or 1-Aryl-1,2-ethanediols^a

^aStandard reaction conditions: *N,N'*-disubstituted urea (0.5 mmol), 1,2-diol (1 mmol, 2 equiv), [Pd/Al₂O₃] (2 mol % Pd, 21.3 mg), and *n*-Bu₂O (1 mL) at 150 °C for 24 h. Isolated yields after column chromatography on neutral alumina are given within parentheses. ^bUsing *o*-xylene as the solvent. ^cRun for 16 h. ^dTraces of the corresponding mixture of oxazolones were detected. ^eIsolated yields after column chromatography on silica are given within parentheses. Bn = benzyl.

aryl-substituted ureas could also be employed in our protocol. Electron-donating as well as electron-withdrawing functionalities in arenes were well tolerated, and the corresponding imidazolones 7–10 could be isolated (41–68%). Moreover, *N,N'*-dibenzyl ureas were also explored as substrates for this reaction and successfully afforded the corresponding imidazolones 11–15 in moderate to good isolated yields (42–72%). In these cases, good tolerance to aromatic ring substituents was also observed, including F and CF₃ groups. For both aryl- and benzyl-substituted ureas, traces of the corresponding oxazolones were detected. In these cases, the reactions were performed using *o*-xylene instead of dibutyl ether as the solvent due to the better solubility of ureas and improved selectivities in this solvent. In addition, phenyl- and *o*-tolyl-substituted 1,2-diols were reacted with *N,N'*-dialkyl-substituted ureas, yielding the *N*-alkyl-substituted imidazolones 16–18 in good to excellent yields (68–87%).

However, when the dehydrogenative condensation between *N,N'*-dicyclohexylurea 1 and 1,2-pentanediol 19 was attempted under the typical reaction conditions, the corresponding imidazolone 20 was obtained in almost negligible yields (Figure 7 and Table S9). This result showed that our protocol

was limited to the use of activated 1,2-diols. With the aim of achieving a more applicable method, we decided to explore the possibility of using ZnO as an additive, able to activate 1,2-diols.^{7c,g,22,35} To our delight, the combination of [Pd/Al₂O₃] nanomaterial with small amounts of ZnO (5 mol %) resulted in an active catalytic system that afforded the corresponding imidazolone in high yield (Figure 7 and Table S9).

With this information in hand, the design of a material able to catalyze the acceptorless dehydrogenation of unactivated 1,2-diols and ureas was attempted. In this direction, we prepared a material based on Pd nanoparticles stabilized over a ZnO support. Furthermore, several bimetallic Pd–Zn-containing nanostructured materials using γ -Al₂O₃ as a solid matrix were also prepared. Gratifyingly, both [Pd/ZnO] and [Pd(5%)–Zn(5–10%)/Al₂O₃] materials were found to be active catalysts for the acceptorless dehydrogenative condensation between *N,N'*-dicyclohexylurea 1 and 1,2-pentanediol 19 (Figure 7 and Table S9). Pd–Zn nanomaterials have been intensively investigated in the past years due to their interesting applications in relevant processes such as CO₂ hydrogenation,³⁶ reforming/dehydrogenation of methanol,³⁷ semihydrogenation of alkynes,³⁸ etc. In these cases, the

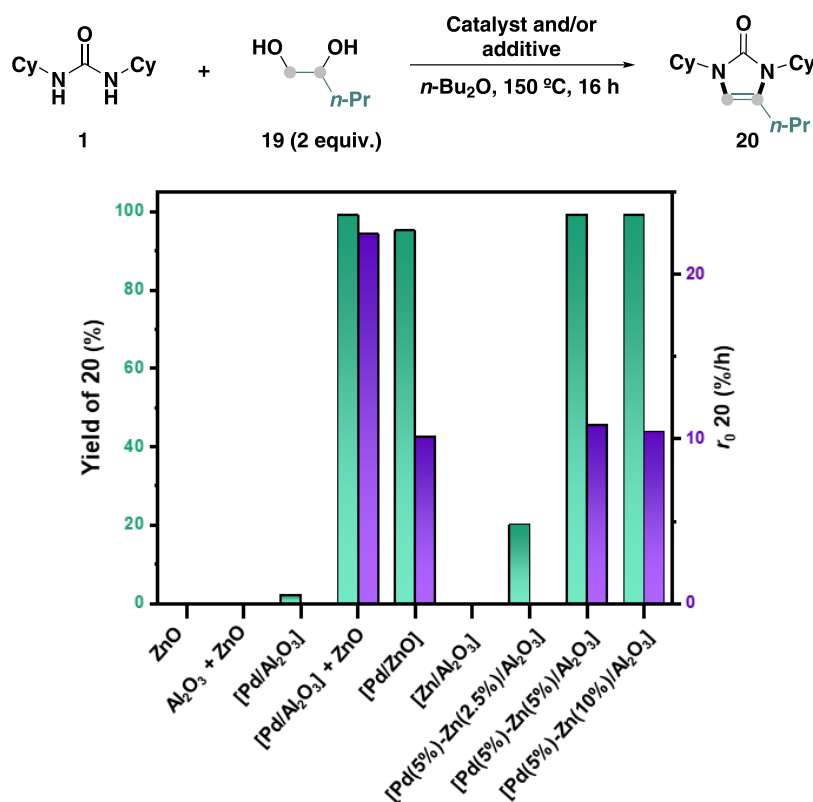


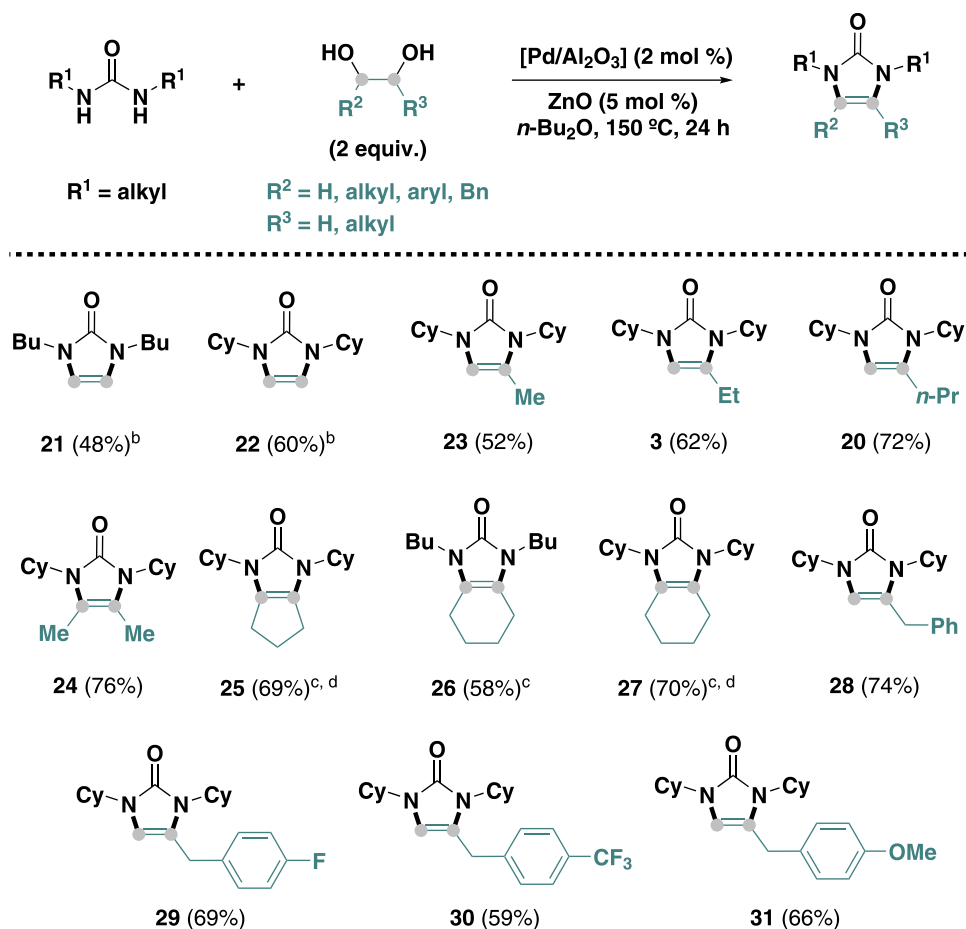
Figure 7. Study of the catalytic system for the acceptorless dehydrogenative condensation between *N,N'*-dicyclohexylurea **1** and 1,2-pentandiol **19**. Standard reaction conditions: *N,N'*-dicyclohexylurea **1** (112.17 mg, 0.5 mmol), 1,2-pentandiol **19** (107 μ L, 1 mmol, 2 equiv), *n*-Bu₂O (1 mL), calcined γ -Al₂O₃ (21.3 mg) or the corresponding catalyst (0.01 mmol, 2 mol % Pd), and ZnO (2 mg, 0.025 mmol, 5 mol %) when indicated at 150 $^{\circ}$ C for 16 h. The yield of **20** and initial reaction rates were calculated by GC using *n*-dodecane as an internal standard.

formation of Pd–Zn alloys has been reported in materials where Pd nanoaggregates are supported over a ZnO matrix, as well as in the case of materials based on Pd–Zn bimetallic species over different metal oxide supports.

To gain further insights into the structure of our materials, [Pd/ZnO] and [Pd(5%)–Zn(5%)/Al₂O₃] were characterized. The BET surface areas were determined to be 18 m²/g for [Pd/ZnO] and 164 m²/g for [Pd(5%)–Zn(5%)/Al₂O₃]. In addition, TPD-NH₃ studies of [Pd(5%)–Zn(5%)/Al₂O₃] showed an acid site density of 141 μ mol/g, whereas the density determined for [Pd/ZnO] was 49 μ mol/g, significantly lower than that of [Pd/Al₂O₃] (200 μ mol/g) (Figures S24D and S25G). These materials showed the main NH₃ desorption peak at temperatures between 159 and 180 $^{\circ}$ C, values generally associated with weak acid sites. Interestingly, the presence of two other peaks at 424–449 $^{\circ}$ C and 621–626 $^{\circ}$ C was also detected, indicating the coexistence of other types of acid sites in these materials.

XRD patterns of the two materials showed the characteristic peaks of tetragonal PdO crystallites in the case of materials before reduction and the peaks of the metallic Pd in a cubic close-packed structure for materials after reduction (Figures S10D and S12G). In addition, [Pd/ZnO] showed two peaks at 42.3 and 44.1 $^{\circ}$ that were assigned to the reflection of the (111) and (200) β -Pd–Zn alloy crystal planes, respectively (Figure S13).^{36,37a,38b} For [Pd(5%)–Zn(5%)/Al₂O₃] material, the peak corresponding to the (111) plane of the alloy was observed, whereas the peak corresponding to the (200) plane is overlapped with γ -Al₂O₃ reflections (Figure S13). In all of the cases, broad peak shapes were observed, suggesting the

presence of small nanoparticles. With the aim of confirming this observation, the materials were examined by HAADF–HRSTEM (Figures S17D and S22A). An average particle size of 2.9 nm was measured for [Pd/ZnO] (Figure S17D), whereas a larger particle size of 5.8 nm was detected for [Pd(5%)–Zn(5%)/Al₂O₃] (Figure S22A). Raman spectra of the materials were also registered, and the absence of PdO particles with a size <4–5 nm was confirmed (Figures S14D and S15). Energy-dispersive X-ray (EDX) experiments of [Pd(5%)–Zn(5%)/Al₂O₃] were performed, confirming the good dispersion and intimate contact of both metal centers (Figure S22B–D). Temperature-programmed reduction experiments showed for both materials a main peak at temperatures between 75 and 79 $^{\circ}$ C assigned to the main Pd nanoparticles as well as a peak at higher temperatures between 278 and 358 $^{\circ}$ C that could belong to the reduction of smaller nanoparticles, the corresponding support, or the alloy formation^{37a} (Figure S23D,H). To further investigate the possible formation of a Pd–Zn alloy, XPS analysis of [Pd(5%)–Zn(5%)/Al₂O₃] was performed (Figure S16D,E). The Pd 3d signal can be deconvoluted into two main peaks at 334.8 eV (3d_{5/2}) and 340.2 eV (3d_{3/2}) assigned to Pd(0), similar to those recorded for [Pd/Al₂O₃], but at slightly lower eV values, which agree with a larger particle size.^{28a,34} In addition, Pd 3d spectra of [Pd(5%)–Zn(5%)/Al₂O₃] show another doublet at higher BE values (336.1 and 342.3 eV) that was assigned to the formation of a Pd–Zn alloy.^{36,37,38a} Moreover, the alloy formation is further supported by the observation of a shoulder (1013.7 eV) ascribed to the peak of

Scheme 3. [Pd/Al₂O₃]-Catalyzed Synthesis of Imidazol-2-ones from *N,N'*-Dialkyl Ureas and Alkyl or Benzyl-1,2-diols^a

^aStandard reaction conditions: *N,N'*-dialkylurea (0.5 mmol), 1,2-diol (1 mmol, 2 equiv), [Pd/Al₂O₃] (2 mol % Pd, 21.3 mg), ZnO (5 mol %, 2 mg), and *n*-Bu₂O (1 mL) at 150 °C for 24 h. Isolated yields after column chromatography on neutral alumina are given within parentheses. ^bRun at 90 h. ^cUsing [Pd/Al₂O₃] (5 mol % Pd). ^dZnO (10 mol %) was added.

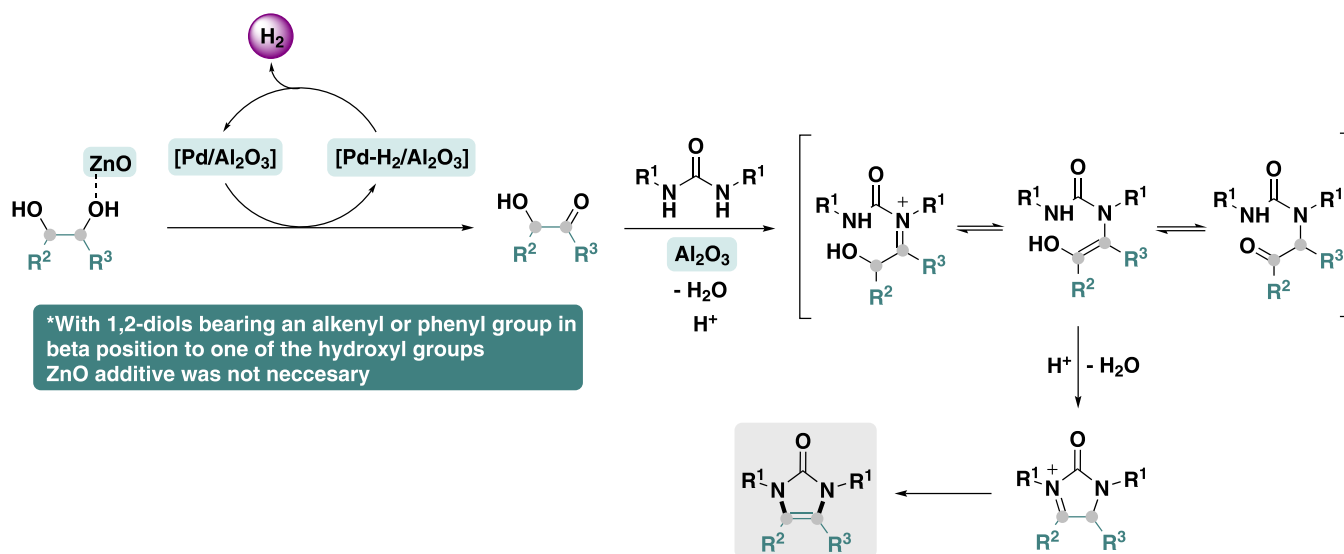


Figure 8. Proposed mechanism for the [Pd/Al₂O₃]-ZnO-catalyzed acceptorless dehydrogenation between ureas and 1,2-diols to afford imidazolones.

ZnO (1023.0 eV) in the Zn LMM Auger spectra, which was assigned to metallic zinc.^{36b,37a}

Initial rates of the acceptorless dehydrogenative condensation between urea **1** and 1,2-pentandiol **19** were evaluated for the three types of catalytic systems, and it was determined that

the [Pd/Al₂O₃]-ZnO combination was the more active system. This fact can be related to the major accessibility of γ -Al₂O₃ in this material and the higher number of acid sites. The heterogeneous nature of the [Pd/Al₂O₃]-ZnO combination and [Pd(5%)-Zn(5%)/Al₂O₃] catalytic system was investigated. First, a hot filtration test was performed for both systems, and neither of them showed leaching of active metal species (Figures S8 and S9). Moreover, additional ICP measurements of [Pd/Al₂O₃]-ZnO and [Pd(5%)-Zn(5%)/Al₂O₃] materials after reaction and reaction waters further demonstrated the heterogeneity of the system (see SI, Section S7.3). Hence, reusing experiments were attempted for both catalytic systems. To our delight, both systems were demonstrated to be reusable in two catalytic cycles (Figures S6 and S7).

Once the feasibility of the dehydrogenation of unactivated diols using the Pd-Zn cooperative catalysis was demonstrated, we decided to evaluate the general applicability of the reaction with these kinds of substrates (Scheme 3). For practical reasons, and due to its good activity and stability, we performed this study with the [Pd/Al₂O₃]-ZnO catalytic system. Remarkably, employing this protocol, imidazolones **21** and **22** were obtained from the corresponding *N,N'*-dialkyl ureas and ethylene glycol in moderate yields (48–60%) over long reaction times. Other unactivated diols such as 1,2-propanediol, 1,2-butanediol, 1,2-pentanediol, and 2,3-butanediol also afforded the corresponding imidazolones **23**, **3**, **20**, and **24** in good yields (52–72%). Bicyclic imidazolones **25**, **26**, and **27** were successfully obtained (58–70%) from dialkyl ureas and cyclic 1,2-diols employing 5 mol % [Pd/Al₂O₃] and ZnO as the catalytic system. Finally, the acceptorless dehydrogenative condensation between *N,N'*-dicyclohexylurea **1** and several 3-phenylpropane-1,2-diols was explored. Gratifyingly, the corresponding imidazolones **28**–**31** were obtained in good to moderate yields (59–74%) and remarkable tolerance was exhibited to both electron-donating or electron-withdrawing substituents in the phenyl ring.

A reaction mechanism was proposed based on all of the performed experiments (Figure 8). First, a Pd-catalyzed dehydrogenation of the corresponding diol to the ketoalcohol takes place, with the concomitant formation of a Pd hydride species followed by H₂ generation (*vide supra*). This dehydrogenation is assisted by [Pd/Al₂O₃] acid sites.²⁶ In the case of unactivated diols, the presence of a Zn species is required for alcohol activation.^{7c,g,22,35} For activated diols, such as 1-phenylethane-1,2-diol **S11**, able to react using [Pd/Al₂O₃] as the catalyst, control experiments showed that the dehydrogenation occurs in the α position with respect to the activating group (Scheme S2). Then, the first Al₂O₃-catalyzed condensation between the ketoalcohol and the urea is proposed to form an iminium cation. The equilibrium of this species with an enamine-enol compound and a carbonyl compound explains the second condensation that affords a five-membered cyclic compound. Finally, the cyclic iminium reorganizes to enamine to afford the final imidazolone. In the case of 1,2-diols with an alkene function in their structure, a double-bond hydrogenation is observed to take place. This is easily explained as a consequence of the large reducibility of alkenes in the presence of a Pd catalyst and the formed H₂. As demonstrated before, kinetic studies have shown that the rate-determining step of the reaction is the Al₂O₃-catalyzed condensation, in which Pd does not play a role. To gain further insights into this mechanism, kinetic experiments with

several substituted phenylethane-1,2-diols were performed, and their normalized rates ($\log K_R/K_H$) were plotted against the corresponding Hammett constants (Table S8 and Figure S4).³⁹ If the rate-determining step of the reaction was the condensation, a linear relationship with a positive slope would be the expected result.²⁶ However, a more complex behavior was observed. More specifically, for electron-withdrawing substituents, a lack of sensitivity as well as very low rates were measured, whereas for electron-donating substituents, a positive slope was detected. This kind of complex behavior has been associated with changes in the rate-determining step in the function of the specific substrates.⁴⁰ In our case, a plausible explanation would be that the dehydrogenation of the corresponding 1,2-diol can be totally hampered in the presence of phenylethane diols with electron-withdrawing substituents, less prone to C-H activation.

CONCLUSIONS

To sum up, an efficient, robust, and reusable nanostructured solid catalytic system was developed for the synthesis of imidazolones from easily available ureas and 1,2-diols. A catalyst based on Pd nanoparticles stabilized over a γ -Al₂O₃ matrix, [Pd/Al₂O₃], was described for the first time as an active and selective material able to mediate the 1,2-diol dehydrogenation to a ketoalcohol followed by the first condensation, tautomeric equilibrium, and the second condensation to yield the corresponding imidazolone. This protocol has shown its applicability through the synthesis of a wide range of imidazolones (28 new molecules). With the aim to better understand this process and the key features of the active centers in the catalyst, several materials based on Pd nanoparticles over γ -Al₂O₃ and various metal oxide supports with different properties were obtained and compared catalytically and structurally (XRD, HR-TEM, STEM, EDX, Raman spectroscopy, TPR, TPD-NH₃, TPD-CO₂, XPS, and BET). These investigations allowed us to deduce that Pd nanoparticles with a wide range of sizes (2.8 nm medium size) stabilized onto a γ -Al₂O₃ support containing a large number of acid sites forms the ideal catalytic system. Kinetic studies have shown that the material's acidity has a larger impact on the dehydrogenation step than on the condensation step. In addition, γ -Al₂O₃ was demonstrated to be able to promote the condensation step. Furthermore, we were able to design and characterize several bimetallic Pd-Zn-based materials, [Pd/ZnO] and [Pd(5%)-Zn(5%)/Al₂O₃], for the acceptorless dehydrogenation of unactivated 1,2-diols. Finally, Pd-Zn was applied cooperatively, through the use of a catalytic system based on a [Pd/Al₂O₃]-ZnO composite, to the acceptorless dehydrogenative condensation between ureas and unactivated 1,2-diols, including ethylene glycol. Remarkably, [Pd/Al₂O₃], [Pd(5%)-Zn(5%)/Al₂O₃], and [Pd/Al₂O₃]-ZnO catalytic systems demonstrated robustness and reusability.

This work identifies the first heterogeneous solid catalyst capable of performing the straightforward synthesis of imidazolones from ureas and 1,2-diols. In our opinion, the remarkable stability of the nanostructured catalyst presented here and the wide availability of the starting materials make this method an interesting alternative for accessing new imidazolone scaffolds in an atom-economical, practical, and more sustainable manner.

EXPERIMENTAL SECTION

General Information. All unreduced and reduced catalysts were analyzed by X-ray powder diffraction (XRD) using a Cubix-Pro PANalytical diffractometer equipped with a detector PANalytical X'Celerator (Cu K α radiation). The amount of Pd contained in the fresh and used catalysts was determined by inductively coupled plasma-optical emission spectroscopy (ICP) using Varian 715-ES after the dissolution of the solid samples in an HF/HNO₃/HCl aqueous solution (1:1:3 vol). Liquid nitrogen adsorption was analyzed using N₂ adsorption isotherms at -196 °C in a Micrometrics FlowSorb equipment. The specific surface areas of the reduced catalysts were calculated by applying the Brunauer–Emmett–Teller (BET) model over the range $P/P^0 = 0.05–0.25$ of the isotherms. Fresh and used catalysts were observed by STEM and TEM using a JOEL JEM 2100F electron microscope working at 200 kV. Temperature-programmed reduction with H₂ (H₂-TPR) experiments were carried out in Micrometrics Autochem 2910 equipped with a TCD detector, using 50 mg of freshly calcined catalyst and increasing the temperature from room temperature to 800 °C with a heating ramp of 10 °C/min under 10% H₂/Ar (vol %) and a constant flow rate of 50 mL/min. Ammonia thermoprogrammed desorption (NH₃-TPD) profiles were obtained after a previous pretreatment step of the previously calcined and reduced catalyst (100 mg, with a pellet size of 0.4–0.8 nm) under a He flow from room temperature to 450 °C; after cooling to 100 °C, adsorption of NH₃ was allowed at 100 °C, followed by a cleaning step using He flow to eliminate the physisorbed NH₃, and the thermoprogrammed desorption was carried out by heating the samples from 100 to 700 °C at a heating rate of 10 °C/min. The evolved NH₃ was analyzed using Micrometrics Autochem II equipped with a TCD detector connected online with an Omnistar mass spectrometer. CO₂ thermoprogrammed desorption (CO₂-TPD) profiles were obtained after a previous pretreatment step of the previously calcined and reduced catalyst (100 mg, with a pellet size of 0.4–0.8 nm) under a He flow from room temperature to 450 °C; after cooling to 50 °C, adsorption of CO₂ was allowed at 50 °C, followed by a cleaning step using He flow to eliminate the physisorbed CO₂, and the thermoprogrammed desorption was carried out by heating the samples from 50 to 800 °C at a heating rate of 10 °C/min. The evolved CO₂ was analyzed using Micrometrics Autochem II equipped with a TCD detector connected online with an Omnistar mass spectrometer. Pd metal dispersion of the samples was estimated from the CO adsorption using the double-isotherm method on a Quantachrome Autosorb-1C equipment. Prior to adsorption, the samples (300 mg, with a pellet size of 0.4–0.8 nm) were reduced in situ in flowing pure hydrogen at the same reduction temperature as that applied before catalysis (200 °C for 2 h and 3 °C/min). After reduction, the samples were degassed at 1333×10^{-3} Pa for 2 h at the reduction temperature, and then the temperature was lowered to 25 °C for 1 h. Then, pure CO was admitted and the first adsorption isotherm (i.e., the total CO uptake) was measured. After evacuation at 35 °C, the second isotherm (i.e., the reversible CO uptake) was measured. The amount of chemisorbed CO was calculated by subtracting the two isotherms. The pressure range studied was 0.511×10^4 Pa. The dispersion of Pd was calculated from the amount of irreversibly adsorbed CO assuming a stoichiometry of Pd/CO = 1. The Raman spectra of the power catalysts were analyzed

using an excitation of 514 nm in a Renishaw inVia Raman spectrometer. The XPS spectra were recorded with a SPECS spectrometer equipped with a Phibos 150 MCD-9 multi-channel analyzer, using a non-monochromatic Al K α (1486.6 eV) X-ray source. The spectra were recorded with an X-ray power of 100 W, a pass energy of 30 eV, and under an operating pressure of 10^{-9} mbar. The XPS spectra were referenced to the C 1s peak (284.5 eV), and spectral processing was performed using the CASA XPS software.

General Procedure for Catalyst Preparation. [Pd/Al₂O₃] was prepared with 5 wt % Pd metal by impregnation of γ -Al₂O₃ (0.847 g) with a solution of K₂PdCl₄ (0.153 g, 0.47 mmol) in a mixture of water:acetone (1:8, 48 mL). The mixture was stirred for 16 h and then evaporated to dryness under vacuum at 40 °C. The resulting powder was calcined in a furnace in air with a heating ramp of 1 °C/min up to 450 °C and held at that temperature for 4 h to obtain the oxidized catalyst. The sample was activated before reaction by heating the solid powder in a stream of N₂ (100 mL/min) with a heating ramp of 2 °C/min to 200 °C; the material was held at 200 °C under H₂ for 2 h and then cooled down to room temperature under a N₂ atmosphere to obtain the final catalyst [Pd/Al₂O₃].

[Pd/Al₂O₃-x%] materials, where x% is the Pd loading (wt %), were obtained using the required amounts of K₂PdCl₄ and γ -Al₂O₃ in each case and following the general method described previously. [Pd/Al₂O₃-x°C/min], calcined at different heating ramps (10 and 30 °C/min), and [Pd/Al₂O₃-x°C], calcined at different final calcination temperatures (300 and 600 °C), were also obtained following the general procedure with the corresponding variations. For the corresponding materials with different supports, the general procedure was followed, changing the γ -Al₂O₃ to CaO, MgO, ZrO₂, TiO₂, SiO₂, or ZnO. Commercial CaO and MgO supports were calcined before their use at 500 °C under air flow, for 2 h at a heating ramp of 5 °C/min, and commercial ZrO₂ was calcined before its use at 250 °C under air flow, for 3 h at a heating ramp of 3 °C/min. For the corresponding [metal/Al₂O₃] materials other than palladium, K₂PdCl₄ was replaced by the corresponding amounts of FeCl₃, CoCl₂, Ni(NO₃)₂·6H₂O, Zn(acac)₂, AgNO₃, RuCl₃, and K₂PtCl₄ and the general method was followed, except for the Ru catalyst, which was directly heated in a stream of N₂ (100 mL/min) with a heating ramp of 1 °C/min to 450 °C, held at that temperature under H₂ for 2 h, and then cooled down to room temperature under a N₂ atmosphere. The other Metal/Al₂O₃ catalysts were activated before reaction by heating the solid powder in a stream of N₂ (100 mL/min) with a heating ramp of 2 °C/min to 200 °C for [Ag/Al₂O₃], 450 °C for [Pt/Al₂O₃], and 600 °C for [Fe/Al₂O₃], [Co/Al₂O₃], [Ni/Al₂O₃], and [Zn/Al₂O₃], held at that temperature under H₂ for 2 h, and then cooled down to room temperature under a N₂ atmosphere to obtain the final catalysts. The bimetallic [Pd(5%)–Zn(5%)/Al₂O₃] catalyst was prepared by impregnation of γ -Al₂O₃ (0.797 g) with a solution of K₂PdCl₄ (0.153 g, 0.47 mmol) and Zn(acac)₂·xH₂O (23.7 wt % Zn) (0.211 g, 0.76 mmol) in a mixture of water:acetone (1:10, 110 mL) and the general procedure was followed. The bimetallic [Pd(5%)–Zn(2.5%)/Al₂O₃] and [Pd(5%)–Zn(10%)/Al₂O₃] catalysts were prepared analogously, adapting γ -Al₂O₃ and Zn(acac)₂·xH₂O amounts to the required weight percentage.

General Procedure for the Synthesis of Imidazolones via Dehydrogenative Cyclization between N,N'-Disub-

stituted Ureas and 1,2-Diols. A 7 mL glass vial containing a stirring bar was sequentially charged with the corresponding N,N' -disubstituted urea (0.5 mmol), 1,2-diol (1 mmol, 2 equiv), $[\text{Pd}/\text{Al}_2\text{O}_3]$ (2 or 5 mol % Pd), ZnO (5 or 10 mol %), if indicated, and $n\text{-Bu}_2\text{O}$ (1.0 mL) as the solvent under an air atmosphere. Afterward, the reaction vial was capped with a septum and placed into an aluminum block, which was preheated at 150 °C. After the indicated time (16, 24, or 90 h), the reaction vial was cooled down to room temperature, diluted with ethanol, and centrifuged, and the supernatant was analyzed by GC. Then, the solvent was evaporated under a reduced pressure, and the crude of the reaction was purified by neutral-alumina or silica gel column chromatography (n -hexane/AcOEt) to yield the desired cyclic product.

■ ASSOCIATED CONTENT

SI Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acscatal.2c01423>.

Experimental procedures, optimization of reaction conditions, kinetic and mechanistic studies, additional experiments, compound and material characterization data, and NMR spectra of isolated compounds (PDF)

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Author Contributions

This paper was written through the contributions of all authors. All authors have given approval to the final version of the manuscript.

Notes

The authors declare no competing financial interest.

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