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Additional Information

1 **An overview of operations and processes for circular management of dredged**
2 **sediments**

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12 **Keywords**

13 Circular economy; dredged sediment; heavy metals; organic pollutants; sediment
14 treatment.

15

16 **Abstract**

17 Dredging is an essential technique to maintain proper water depths in ports and bays.
18 Many dredged sediments are considered as toxic waste due to their significant amounts
19 of metals and other pollutants. In consequence, they need to be treated to reduce this
20 toxicity and avoid pollutant resuspensions. Physical operations and chemical, thermal
21 and biological processes have been conventionally used to this aim, but the traditional
22 linear sediment approach is often unsustainable and economically and environmentally
23 demanding. Considering the increasing people's awareness in environmental issues,
24 more efficient dredged sediment management schemes are required. Some authors are

25 making significant efforts to improve circularity in sediment management processes by
26 taking advantage of the mineral composition of sediments to obtain products for the
27 building and road construction sectors, therefore decreasing the need of raw materials
28 while reducing the amounts of sediments wasted to landfills. However, information
29 related to the characteristics of these products, their mechanical behaviour and their
30 functionality is still scarce, being sediment-based by-products developed mainly at low
31 Technological Readiness Level (TRL), showing low global impact in the market. To
32 implement circular economy in the dredged sediment sector, some technical and socio-
33 political barriers must be still overcome. To this aim, further research and technological
34 applications must be developed, with the support of decision makers and stakeholders.
35 This review aims at giving an overview of the circular trends applied to toxic dredged
36 sediment management, pointing at current opportunities, barriers and constraints that
37 hinder its wide development.

38

39 1. Introduction

40 Sediments are solid particles of sand, silt, clay and other substances that result from the
41 erosion of rocks, soils and other solids. They are one of the main elements of aquatic
42 ecosystems and serve as habitat and food resources to water life (Bortone and Palumbo,
43 2007). Sediments are transported by natural and human activities and settle at the
44 bottom of water bodies, which may hinder boat navigation and the physicochemical
45 balance of water masses (Ferrans et al., 2019; Mehdizadeh et al., 2021; Pal and Hogland,
46 2022). Moreover, sediment accumulation in dams can significantly decrease their water
47 storage capacity (de Vincenzo et al., 2018). To maintain adequate depths in water ways
48 and dams, regular dredging is needed (Chen et al., 2019; Norén et al., 2020). Apart from

49 maintenance, there are other dredging activities such as the construction of new
50 waterways or remediation dredging (Bortone and Palumbo, 2007). All these practices
51 imply the production of large amounts of dredged sediments, accounting for around 300
52 million of m³ per year only in Europe (Snellings et al., 2016). Dredged sediments have
53 been globally considered as a waste to be got rid of (Beddaa et al., 2020), being many of
54 them considered as toxic due to their high pollutant concentrations (Section 3).
55 Sediments categorised as toxic by current regulations (Section 4) are only allowed to be
56 either directly disposed in landfills for toxic wastes or to be treated to reduce their
57 toxicity to admissible levels.

58 Considering the high amounts of dredged sediments produced worldwide and the
59 increasing legal requirements in terms of sediment management, the “no action”
60 scenario as well as conventional practices such as direct disposal in confined facilities
61 are no longer feasible economically, environmentally and socially (Barjoveanu et al.,
62 2018; Mehdizadeh et al., 2021; Pal and Hogland, 2022; Pellenz et al., 2020). Sediment
63 dredging therefore represent a challenge for port authorities (Loudini et al., 2020b),
64 which are usually open to a new approach of sediment management that help them to
65 cope with this environmental problem. In this respect, increasing number of studies are
66 trying to apply Circular Economy (CE) principles to the dredged sediment management
67 sector, i.e., to transform management processes to consider sediments a source of
68 sustainable resources instead of a toxic waste (Section 6).

69 This review aims at giving a new insight to conventional dredged sediment management,
70 highlighting the novel trends that aim to manage dredged sediments according to
71 circular economy principles and pointing at current opportunities, barriers and
72 constraints that hinder its wide development. Previously, an overview of sediment

73 characteristics, current legislation and the conventional treatment processes to reduce
74 the toxicity of sediments will be given.

75

76 2. Methodology

77 The study is divided in the following sections: 1) an Introduction section where current
78 generic issues related to sediment management are addressed; 2) the description of the
79 methodology followed in this manuscript; 3) the analysis of the main characteristics of
80 dredged sediments, focusing on those that make them be considered as toxic wastes; 4)
81 as this consideration is also dependent on specific regulations, these are also reviewed;
82 5) the evaluation of operations and processes to treat toxic dredged sediments, which
83 has been conventionally carried out in a linear approach; 6) the novel approach of
84 sediment management based on circularity, which not only focuses on reducing
85 pollutants but also on decreasing impacts of treatment processes while recovering by-
86 products. Some pilot cases developed in research projects are described. Socio-political
87 barriers for the development of this approach are also evaluated in this section.

88 To develop this study, a deep search on the Elsevier Scopus and Google Scholar
89 database was carried out using the following keywords as search queries: “dredged
90 sediment”, “sediment treatment”, “dredged sediment circular economy” and “dredged
91 sediment treatment process”. Generally, results were limited to the last five years
92 (2017-2022) to give an updated approach, especially for the literature related to circular
93 economy in sediment management (Section 6). However, since the conventional
94 dredged sediment treatment has been widely investigated during last two decades, for
95 the analysis of the linear treatment approach (Section 5), the searching time period was
96 lengthened to the last twenty years. Other criteria for the selection of the literature

97 were related to: the quality of the results, assessed by the impact factor of the journals
98 and the number of citations; articles related to sediment treatment and management
99 on site (without dredging) were excluded; the studies analysed tried to cover as many
100 regions as possible to make an overall overview of current situation; articles based on
101 process engineering were prioritised while others which focus on aspects such as
102 pollutant transport between sediments and water or toxic effects of sediment pollutants
103 in wildlife were discarded.

104

105 3. Characteristics of dredged sediments

106 Marine dredged sediments contain quite variable characteristics, even in zones that are
107 close to each other (Table 1). These differences depend on many factors such as the
108 intrinsic characteristics of the raw materials that form the sediments, the degree of
109 erosion, the economic activities in the surroundings, and even the dredging time at
110 which sediments are produced (Safhi et al., 2020). Hence, adequate sediment
111 characterisation is essential to assess the most appropriate sediment management
112 process for each case.

113 Generally, dredged sediments contain high amounts of salts (Doni et al., 2018; Wang et
114 al., 2018a) and water, which is present in high variable range, i.e., 24-90% (Zhao et al.,
115 2022). A significant part of this water is difficult to be removed as it remains bound to
116 sediments by electrical charges (Chi et al., 2018). These characteristics tend to hinder
117 sediment treatment operation and processes (Section 5). In addition, sediments are
118 commonly dominated by silt and clay fractions, which normally account for 60-90% of
119 the solid content of sediments (Ferrans et al., 2021; Wang et al., 2018b, 2018a). These
120 fractions, due to their higher specific surface, tend to accumulate more pollutants than

121 coarser particles like sand and gravel (Anand et al., 2021; Mymrin et al., 2017; Todaro et
122 al., 2018; Yoobanpot et al., 2020). Furthermore, sediment pH tends to be slightly basic,
123 i.e. around 8.0-8.8 (Doni et al., 2018; Wang et al., 2018a; Zhou et al., 2022).
124 Consequently, many sediments present significant concentrations of precipitated
125 metals (Debnath et al., 2021; Pal and Hogland, 2022; Todaro et al., 2016; Wang et al.,
126 2018b). Metals such as copper, zinc, cadmium, chromium, nickel, plumb, and arsenic are
127 often found in dredged sediments in the order of tens and/or hundreds of mg per Kg
128 (Table 1). In the case of iron, the concentration in sediments can reach the order of $\text{g}\cdot\text{Kg}^{-1}$
129 ¹ (Fonti et al., 2013; Lopez et al., 2022). Many authors have also found hydrocarbons and
130 other organic pollutants in sediments also in the range of $\text{g}\cdot\text{Kg}^{-1}$, including TBT, TPH,
131 PAHs, and PCBs (Table 1), as well as significant amounts of nutrients (Doni et al., 2018;
132 Maletic et al., 2019; Ferrans et al., 2021). These pollutants can be resuspended and re-
133 enter to water bodies, often entailing serious environmental, health and ecological
134 issues due to the persistence of these pollutants and their negative effects on living
135 organisms and water quality (Barjoveanu et al., 2018; Debnath et al., 2021; Liu et al.,
136 2022; Maletic et al., 2019; Norén et al., 2020; Zhang et al., 2021). Appropriate
137 management of toxic sediments is therefore essential to maintain adequate
138 environmental quality and economic activities in ports, harbours and bays, underlying
139 the need for clear legislation that regulates their possible uses and applications.

140 [TABLE 1 NEAR HERE]

141

142 4. Regulations regarding dredged sediments

143 At European level there are directives, laws and regulations where sediments are
144 mentioned directly or indirectly, also considering sediment management (Bortone and

145 Palumbo, 2007). They indicate, according to their maximum pollutant levels and their
146 mobility, which sediments are considered as toxic waste and the specific applications to
147 which sediments are allowed (Buceta et al., 2015; Ferrans et al., 2021). These European
148 guidelines and conventions have been adopted in numerous countries (in Europe and
149 beyond) but there is a lack of uniformity and coherence in them in terms of
150 characteristics to be analysed, limits of pollutant concentrations, categories of
151 classification of sediments, etc. (Jersak et al., 2016; Sapota et al., 2012), as can be seen
152 in Table 2. By means of example, in Italy, the legislative framework about sediment
153 management (DM 173, 2016) regulates the sediment ocean disposal, their use for
154 nourishment and backflow activities for limited environments. The choice of
155 management options is dictated by the sediment quality class (sediment type A, B, C, D
156 and E), which is determined through criteria of integration weighted by both
157 ecotoxicological and chemical hazard class. In particular, the ecotoxicological
158 classification is based on a judgment of ecotoxicological risk elaborated by the weighted
159 integration of the results of all the components of the entire battery of bioassay tests.
160 The chemical classification is based on the development of a chemical Hazard Quotient
161 (HQ) index which considers the type and number of non-compliant parameters, as well
162 as the extent of such exceedances (DM 173, 2016). When the sediments are directly or
163 indirectly (i.e., after treatment) disposed or used to obtain by-products, these final
164 products have to be also submitted to release tests to assess the pollutant mobility
165 (Bortone and Palumbo, 2007; Zhao et al., 2022). The leachates that come from a release
166 test in water of the matrices for a period of 24 hours cannot overpass the thresholds
167 reported in DM 5th February 1998.

168 In the case of France, the decision on sediment suitability for sea disposal is primarily
169 based on chemical findings, being the ecotoxicological analyses only advised to be done
170 on guidelines. According to the concentration limits of the required chemical
171 parameters (such as particle size, metals, trace elements and organic micro-pollutants),
172 N1 (high quality) and N2 (medium quality) levels are legally defined. Only in the cases
173 where any of the compounds exceeds the N2 threshold, a biological characterisation of
174 sediments is needed (Mugnai et al., 2018; Tessier et al., 2011).

175 On the other hand, in Spain, sediment characterisation is carried out in two steps: one
176 preliminary step to analyse their potential toxicity and a secondary step based on
177 chemical and biological characterisations. If the dredged material presents silt-clay
178 fraction lower than 10%, total organic carbon (TOC) concentration lower than 2%, and
179 EC50 of the bacterium *Vibrio fischeri* higher than 2000 mg·L⁻¹, they are not required to
180 be submitted to the second step where some target metals, hydrocarbons and phenols
181 are analysed (Buceta et al., 2015). If sediments overpass the defined limits in one of the
182 target pollutants, they will be defined as toxic waste and have to be managed according
183 to Law 22/2011 *on Contaminated Wastes and Soils*. Non-toxic sediments are classified
184 in three different categories according to their quality in terms of chemical
185 concentrations: A (highest quality), B, and C (lowest quality). Only type-C sediments are
186 submitted to biological characterisation (Buceta et al., 2015).

187 [TABLE 2 NEAR HERE]

188 The degree of restriction of the legislation will determine (amongst other factors) the
189 level of treatment to which sediments will be subjected and, consequently, the first step
190 to develop the appropriate management of dredged sediments is to analyse their
191 chemical and physical characteristics (Ferrans et al., 2019; Zhou et al., 2022).

192

193 **5. Dredged sediment treatment operations and processes**

194 Non-toxic sediments can be directly used in land for soil filling, construction purposes,
195 coastal nourishment and as an amendment in agriculture, horticulture, and forestry as
196 long as they comply with the pollutant-specific regulations or are classified in the
197 appropriate category (as explained in Section 4). In these cases, they could be also
198 disposed directly in landfills or oceans, which are common and simple techniques but
199 present considerably high environmental impacts (Akcil et al., 2015; Barjoveanu et al.,
200 2018; Bhairappanavar et al., 2018). In case of landfilling of toxic sediments, apart from
201 the huge land requirements, dredged sediments can be only disposed in facilities that
202 present appropriate soil characteristics and rigorous dumpsite management to assure
203 their safe deposit, avoiding toxic emissions (Mehdizadeh et al., 2021; Pal and Hogland,
204 2022; Pellenz et al., 2020; Wang et al., 2019). There are a reduced number of these
205 landfills for toxic compounds in comparison to facilities for inert materials, which not
206 only increases the difficulty of managing the dredged sediments, but also raises the
207 treatment and transport costs drastically (Bhairappanavar et al., 2018; Carpenter et al.,
208 2018; Kim et al., 2016). In fact, while landfill costs for inert sediments is around 27 \$·t⁻¹,
209 they increase up to 67-80 \$·t⁻¹ when wastes are toxic (Norén et al., 2020). Considering
210 these aspects together with the increasingly restrictive legislation in terms of dredged
211 sediment management and general public's awareness in environmental issues, direct
212 disposal and confinement of sediments is not recommended (Todaro et al., 2016; Zentar
213 et al., 2009).

214 To reduce the toxicity of dredged sediments in order to dispose them afterwards
215 (minimising toxic risks) or to obtain by-products from them (Section 6.1), several

216 physical operations (usually) combined with chemical, thermal or biological processes
217 have been developed along last decades (Maletic et al., 2019).

218 This review will mainly deepen in treatment operations and processes which are
219 commonly used to treat toxic sediments ex-situ. In-situ sediment remediation processes
220 such as capping or electrokinetic remediation (Benamar et al., 2019; Debnath et al.,
221 2021; Maletic et al., 2019) will not be taken into account since no dredging is needed.

222

223 *5.1. Physical operations*

224 Physical operations aim to separate sediment fractions according to their size and to
225 reduce the content of water and pollutants in sediments through mechanical
226 separation, dewatering and washing (Debnath et al., 2021).

227

228 *5.1.1. Mechanical separation*

229 Mechanical separation allows dividing dredged sediments into different fractions
230 according to their size (e.g., sand, silt and clay) or to their mineral composition based on
231 differences in the particles' specific weights or in the conditions of the particles' surfaces
232 (Hakstege, 2007). It can be carried out by centrifugation, screening, flocculation,
233 sedimentation or by using hydrocyclones, spirals or combinations of these techniques
234 and technologies (Kim et al., 2016; Mulligan et al., 2001; Pal and Hogland, 2022). Since
235 the smaller sediment particles (silt and clay) retain higher amounts of metals and
236 organics due to their larger surface-volume ratio as aforementioned, mechanical
237 separation also enables to concentrate pollutants into these fractions (Pal and Hogland,
238 2022). This can help to reduce the amounts of toxic wastes to be managed as long as
239 the coarser fractions accomplish with the authorities' requirements. The treatment

240 costs for sediment separation are in the range of 3 - 11 €·m⁻³ (ref. year 2007), depending
241 on the operation, scale and local conditions (Hakstege, 2007).

242

243 5.1.2. Dewatering

244 Dewatering consists of the removal of water from sediments to reduce their volume
245 and, in turn, to decrease the costs of downstream treatments. Dewatering can be
246 carried out by natural drainage and evaporation (Bortone and Palumbo, 2007) but these
247 techniques require vast space and long retention times, while the degree of dewatering
248 is limited. To increase dewatering performance and reduce land demand, mechanical
249 units such as filter presses, draining screens, vacuum filters, or membranes could be
250 used. By way of example, dry matter content of sediments can increase from 40-45% to
251 65-80% by using filter presses. The costs of this operation vary in the range of 10-35 €·m⁻³
252 ³(ref. year 2007) (Hakstege, 2007). However, when the organic content of sediments is
253 high (especially in terms of extracellular polymeric substances (EPS)), more water is
254 bound to sediments, hindering dewatering. To release the interstitial water and
255 facilitate its removal, chemical conditioners such as iron and aluminium salts, or organic
256 polymers like polyacrylamide (PAM) and poly dimethyldiallylammonium chloride
257 (PDMDAAC), can be used (Chi et al., 2018; Zhao et al., 2022).

258 It must be highlighted that mechanical separation and dewatering are not able to reduce
259 the toxicity of the sediments significantly. They mainly concentrate pollutants in certain
260 fractions to reduce the volume of wastes to be treated. For this reason, these operations
261 often need to be combined with other processes to assure the safe use of the products
262 obtained from sediment or their safe disposal (Hakstege, 2007).

263

264 5.1.3. Washing

265 One possibility to reduce the pollutants contained in sediments is washing. This
266 operation can simply consist of mechanical washing with water or can be improved by
267 adding chemicals such as acids, bases, chelants, surfactants, and others (Debnath et al.,
268 2021; Ferrans et al., 2021; Pal and Hogland, 2022; Polettini et al., 2009). Acid washing is
269 usually effective to remove heavy metals with their subsequent release to the washing
270 solution (usually water) (Mulligan et al., 2001). Washing also extracts salts from marine
271 sediments (Doni et al., 2018; Todaro et al., 2020), which is usually beneficial for
272 downstream processes or for possible applications of the sediments treated. Strong
273 acids such as nitric, hydrochloric and sulfuric acids can be used to reach the acid
274 conditions in the washing solution (Löser et al., 2007). Ferrans et al. (2021) also studied
275 metal extraction with weaker acids (i.e., chelating agents which are less abrasive to
276 sediments) such as ethylenediaminetetraacetic acid (EDTA) and ethylenediamine-
277 disuccinic acid (EDDS), obtaining extraction efficiencies in the range 29.7 – 74.1% for
278 lead, zinc, copper arsenic and nickel. However, chromium was scarcely extracted (2.1-
279 3.1%).

280 The performance of each acid is variable and should be thus a matter of study as it
281 depends on several variables such as chemical dosage, contact time, liquid-solid ratio,
282 pH, temperature and the number of extraction steps (Beiyuan et al., 2018; Ferrans et
283 al., 2021). Washing is usually more effective when applied in coarser particles, being
284 smaller fractions more difficult to clean (Hakstege, 2007; Jeon et al., 2015). For this, the
285 washing process can be more effective if it is preceded by a mechanical separation step.
286 Anyhow, acid washing operations are quite expensive, being in the range of 40–73 \$·m⁻³

287 ³ (ref. year 2009) (Pal and Hogland, 2022; Tsai et al., 2009), which is something to take
288 into account when the sediment treatment scheme is designed.

289

290 *5.2. Chemical processes*

291 Chemical treatment includes all the sediment treatment processes where chemical
292 reactions occur, for instance, dechlorination, oxidation, chemical stabilisation and
293 coagulation (Debnath et al., 2021; Kim et al., 2016). They are applied to sediments with
294 the purpose of improving the stabilisation of the final by-products obtained from
295 sediments and/or to reduce the toxicity and bioavailability of pollutants (Hakstege,
296 2007; Todaro et al., 2018; Wang et al., 2018a).

297

298 5.2.1. Chemical oxidation

299 Chemical oxidants such as ozone, potassium permanganate, hydrogen peroxide,
300 Fenton's reagent, and activated sodium persulphate can be effective to transform the
301 organic pollutants contained in sediments into non-hazardous compounds. In fact,
302 Ferrarese et al. (2008) reported PAH degradations over 95% when Fenton's reagent,
303 hydrogen peroxide and potassium permanganate were used at dosages of 100 mmols
304 per 30 g of sediments. However, removal efficiencies are highly variable depending on
305 the reagent used, while the optimum dose should be determined for each specific case
306 (Ferrarese et al., 2008; Maletic et al., 2019). It must be noted that chemical oxidation is
307 not commonly efficient to degrade metals (Bortone and Palumbo, 2007; Mulligan et al.,
308 2001).

309

310 5.2.2. Solidification/Stabilisation (S/S)

311 Chemical reagents such as lime, silicates, cement and others can be added to polluted
312 sediments with the goal of immobilising and stabilising the metals contained in the
313 dredged sediments by increasing the compressive strength of the matrix and decreasing
314 their leachability, thus becoming less mobile (Kou et al., 2021; Maletic et al., 2019;
315 Radenovic et al., 2020). This way, even if metals are not removed, the risk of being
316 released to air, water and soil is significantly reduced. This process is commonly known
317 as solidification/stabilisation (S/S) (Barjoveanu et al., 2018; De Gisi et al., 2020; Hossain
318 et al., 2020; Radenovic et al., 2020; Tang et al., 2020).

319 As an advantage, S/S is less expensive than other processes to reduce metal toxicity such
320 as those based on thermal processes (Amar et al., 2021), but it has to be considered that
321 the additives used in the process, together with the type of pollutant, water content and
322 characteristics of the dredged material will significantly influence the process
323 performance, and in consequence, the costs and impacts (Wang et al., 2015; Zhou et al.,
324 2022). For instance, arsenic, lead, chromium (VI), mercury, cadmium, copper and zinc
325 are normally stabilised successfully by S/S. However, the stabilisation of other metals
326 could be less effective (Mulligan et al., 2001). In addition, sediments with high saline
327 contents, high amounts of low-size fractions or high organic pollutant concentrations
328 normally present low performance in this type of process (Barjoveanu et al., 2018; De
329 Gisi et al., 2020; Norén et al., 2020; Todaro et al., 2020). Anyhow, continuous monitoring
330 is required as solidification can be reversible (Pal and Hogland, 2022; Tang et al., 2020).
331 Consequently, this process cannot be widely applied to treat toxic dredged sediments
332 and is often combined with other techniques. It must be also considered that S/S
333 processes increase the reagent requirements exponentially when water content in

334 sediments is higher than 20% or when chlorinated hydrocarbons concentrations surpass
335 5% (Mulligan et al., 2001).

336

337 *5.3. Thermal processes*

338 Thermal treatments entail the use of high temperature, i.e., in the range of 800 - 1200°C
339 (Safhi et al., 2020; Zhao et al., 2022), to separate the pollutants contained in sediments
340 by desorption, oxidation or by sintering or melting the sediments to change their
341 composition with the goal to reduce metal mobility, thus decreasing their potential
342 toxicity. However, thermal processes are characterised by being highly energy-
343 consuming (Kou et al., 2021; Pal and Hogland, 2022). Hence, operating conditions (i.e.,
344 temperature and time of calcination) must be optimised to decrease costs, impacts and
345 minimise undesirable phenomena that commonly occurs in these kinds of processes
346 such as the reduction of internal porosity, and granulometry modification.

347 In comparison to chemical processes, thermal treatments usually obtain sediments with
348 better characteristics such as improved studied the pozzolanic reactivity (Amar et al.,
349 2021; Benzerzour et al., 2017; Snellings et al., 2016). However, the gases produced
350 during the process have to be treated to degrade the pollutants that were removed from
351 the sediments, increasing the complexity and costs of the treatment. Furthermore,
352 thermal technologies are prone to breakdowns, which reduces the process reliability
353 (Mulligan et al., 2001; Pal and Hogland, 2022; Todaro et al., 2016). Obviously, water
354 content of sediments will decrease thermal process performances. In fact, water
355 content should not be higher than 30% to be thermally treated (Hakstege, 2007). Pre-
356 treatment to reduce the water content of sediments could be therefore needed for
357 thermal treatment. Not considering pre-treatment, the costs of thermal processes can

358 rise up to 50 – 70 €·t⁻¹ (ref. year 2007) (Hakstege, 2007). For all these reasons, thermal
359 processes should be carried out only in specific occasions, being thus minimised in
360 circular management schemes (Section 6).

361

362 5.3.1. Thermal desorption

363 Thermal desorption has been traditionally used to remove volatile organic compounds
364 (VOCs) and other (light) organic harmful compounds due to the differences between the
365 volatility of the pollutants and of dredged sediments (Hakstege, 2007). By applying
366 moderately high temperatures, compounds such as mineral oil, aromatics, PAH's, PCB's,
367 cyanides, chlorinated solvents and TBT can effectively move from sediments' surface to
368 the gas phase (Hakstege, 2007; Todaro et al., 2016). The maximum temperature
369 achieved during thermal treatment will depend on the compounds that are wanted to
370 be removed. For instance, to remove heavy mineral oil, temperatures higher than 450°C
371 are needed while they need to be raised to 550°C when the main pollutant is PCB
372 (Bortone and Palumbo, 2007). On the other hand, metals such as mercury, arsenic and
373 cadmium could be removed from sediments at temperatures around 800 °C (Mulligan
374 et al., 2001). Thermal desorption can be combined with other thermal processes such
375 thermal oxidation and thermal immobilisation (Bortone and Palumbo, 2007).

376

377 5.3.2. Thermal oxidation and immobilisation

378 When high temperatures are applied to sediments, organic pollutants will not only
379 volatilise but will be also burned (thermal oxidation) (Pal and Hogland, 2022). With
380 respect to the inorganic materials contained in sediments, the application of
381 temperatures in the range 820-1100 °C make compounds like SiO₂, Al₂O₃, CaO, Fe₂O₃,

382 etc., melt. With the subsequent solidification step, metals remain fixed to sediments
383 (thermal immobilisation) (Snellings et al., 2016; Zhao et al., 2022).

384 Thermal immobilisation can be used to obtain several products like bricks, light weight
385 aggregates (LWA) and others that could be used to implement the circularity of the
386 process (Section 6). In this respect, heating and cooling times are important parameters
387 that have to be controlled to maximise the quality of the final by-product and minimise
388 the energy consumption (Zhao et al., 2022).

389

390 5.3.3. Vitrification

391 Vitrification consists of the use of electricity to destroy and/or immobilise pollutants on
392 sediments. High voltage is applied to the sediments to reach very high temperatures (up
393 to 3000 °C) in order to turn the sediments into liquid phase. Then, sediments are
394 solidified after cooling down creating a vitreous material where the pollutants that were
395 not destroyed during heating remain fixed (Mulligan et al., 2001; Todaro et al., 2016).
396 This process can be very effective in removing pollutants. However, it is very
397 energetically and environmentally costly, and generally requires intensive pre-
398 treatment. It must be also considered that toxic gases, that have to be treated, can be
399 also produced during vitrification (Colombo et al., 2012; Pal and Hogland, 2022; Todaro
400 et al., 2016).

401

402 5.4. Biological processes

403 Biological processes for sediment treatment (also known bioremediation) consists of the
404 oxidisation of biodegradable pollutants such as PAHs, mineral oil and hydrocarbons to
405 transform them into non-hazardous compounds by the action of microorganisms or

406 plants (Amar et al., 2021; Doni et al., 2015; Feng et al., 2022). This can occur by the
407 natural capacity of indigenous microbes, often requiring huge land surfaces; by
408 biostimulation, which entails the introduction of nutrients and oxygen into the polluted
409 sediments to boost microbial activity; or even by bioaugmentation, i.e., the addition of
410 external microorganisms to the sediments (Doni et al., 2018; Fodelianakis et al., 2015;
411 Wu et al., 2014).

412 It must be considered that these techniques are generally extensive, so that they
413 present much lower operating costs, but the times required for the degradation are
414 noticeably high (Pal and Hogland, 2022). By way of example, Doni et al. (2018) observed
415 a removal of 46% of total petroleum hydrocarbons (TPH) from raw sediments after three
416 months of biological treatment by adding a bioactivator (a mix of microorganisms,
417 enzymes, and nutrients), while it fell to 15% when natural attenuation was carried out.
418 On the other hand, Liu et al. (2017a) achieved PAH removals of 42-83% after 91 days of
419 incubation by adding acetate as co-substrate and nitrate as electron acceptor. In
420 addition, bioremediation tend to be less predictable than other processes (Maletic et al,
421 2019). Consequently, industrial applications of biological processes to sediment
422 treatment are limited.

423 Table 3 shows a summary of the sediment treatment operations and processes
424 described in Section 5. Although the maturity and technical applicability of the single
425 units described is currently reached, they are not usually effective nor efficient (in terms
426 of economic and environmental impacts) to decontaminate toxic sediments on their
427 own. It can be summarised that, generally, physical treatments are mostly used as pre-
428 treatment to separate sediment fractions and reduce water, salinity and pollutant
429 contents to facilitate downstream processes. Chemical treatments are usually effective

430 in terms of reducing toxicity of sediments but depending on the case, large amounts of
431 reagents could be needed. Regarding thermal processes, they are normally effective but
432 highly energy and environmentally demanding, while biological treatments present low
433 impacts in terms of carbon footprint but are not usually cost-effective. Consequently,
434 these treatment operations and processes must be combined to form relatively complex
435 sediment treatment schemes with the goal to look for feasible options to reduce
436 sediment toxicity.

437 [TABLE 3 NEAR HERE]

438

439 6. Circular sediment management and resource recovery

440 As aforementioned in Section 5, conventional sediment treatment operations and
441 processes usually require high amounts of resources and present significant operating
442 costs and environmental impacts. Hence, a linear sediment treatment strategy which
443 only focus on pollutant removal and toxicity reduction (Figure 1) is often not sustainable
444 (Maletic et al., 2019; Spadaro and Rosenthal, 2020; Zheng et al., 2019).

445 [FIGURE 1 NEAR HERE]

446 With the goal to maximise the performance of the sediment treatment, different
447 operations and processes have been traditionally combined in order to adapt the
448 treatment scheme to the sediments' characteristics and composition: water content,
449 metals and organic concentrations, size distribution, etc. The quantitative and
450 qualitative variability of the sediments' characteristics together with the specificity of
451 the treatment objectives of each processing unit make sediment treatment
452 configurations noticeably different from each other. By way of example, the
453 BioGenesisSM sediment washing technology (Figure 2a) was developed in the 1990s and

454 uses physical operations and chemical processes to wash and decontaminate the
455 sediments. This technology has been already implemented in the ports of Venice, New
456 York and New Jersey. The pollutant removal normally varies in the range 60-80%,
457 depending on the sediment matrix, pollutant types and concentrations and the extent
458 of treatment (Hakstege, 2007). The treatment costs are scale-dependant, being
459 reported as 55-80 €·m⁻³ when treating 300,000 m³·y⁻¹, and 90-130 €·m⁻³ when treating
460 50,000 m³·y⁻¹ (Hakstege, 2007). On the other hand, METHA treatment (Figure 2b) for the
461 sediment separation was developed in the Port of Hamburg (Germany) (Bortone and
462 Palumbo, 2007). It is based on a two-stage separation. In the first one, the 63 µm silt is
463 separated from the sand by hydrocyclones and upstream flow classifiers. When the
464 particle size distribution is predominant in the range of 20 - 100 µm, it is advised to also
465 separate the 20 µm fraction. In this case, hydrocyclones and downstream spiral
466 concentrators are used. The products obtained during the separation steps are
467 dewatered using different systems such as draining screens and vacuum filters. The
468 dewatering of the flocculated silt suspension is done in two stages with the application
469 of a belt filter press and a high-pressure press or alternatively with a membrane filter
470 press.

471 [FIGURE 2 NEAR HERE]

472 As an alternative to these conventional linear sediment treatment schemes, and
473 (mainly) due to more restrictive environmental regulations and increasing public
474 awareness of sustainability, the way dredged sediments are managed is currently
475 changing to move towards the Circular Economy (CE) principles (Laboyrie et al., 2018;
476 Yoobanpot et al., 2020).

477 Within the CE concept, the economic activities become auto-regenerative by converting
478 materials traditionally considered as waste into raw matter. This substitutes the
479 conventional model into a more efficient paradigm (Puyol et al., 2017; Spadaro and
480 Rosenthal, 2020). In the case of dredged sediments since 90% of them are considered
481 useful for certain applications (Bhairappanavar et al., 2018), many authors have focused
482 on obtaining by-products from these treated sediments to increase the feasibility of
483 these processes (Section 6.1). This way, an added value can be obtained from a “waste”
484 while the volume of sediments disposed in landfills is reduced (Amar et al., 2021;
485 Mehdizadeh et al., 2021; Yang et al., 2020). But the CE concept not only focuses on
486 taking advantage of the materials contained in wastes. It is also related to the
487 improvement of all production chains to make them more sustainable and
488 environmentally friendly, increasing their energy and cost efficiency and reducing
489 carbon, water and land footprints (Figure 3). In this respect, substituting reagents and
490 binding materials from non-renewable sources (such as cement, sand, lime, clays and
491 others) by those traditionally considered as wastes presents multiple benefits in terms
492 of environmental sustainability since both resource consumption and the impacts of
493 wasting materials are reduced. However, a sustainable and economically efficient
494 scheme to manage polluted dredged sediments have not been yet established (Todaro
495 et al., 2016; Yang et al., 2020). Moreover, most of the processes and configurations
496 aimed at applying CE principles still present low Technological Readiness Level (TRL),
497 most of them having been only tested in lab conditions without evaluating the
498 product(s) obtained on site. Data at industrial or semi-industrial scale and tests in-situ
499 of the obtained by-products are needed to widely implement sustainable dredged
500 sediment management. In this respect, innovative projects such as *SEDI.PORT.SIL* and

501 *ECOSSEDRA* have being recently developed to enhance circularity in sediment
502 management.

503 [FIGURE 3 NEAR HERE]

504 The SEDI.PORT.SIL project was developed to treat sediments from the Port of Ravenna
505 (Italy). The entrance to the pilot plant consists of a mixed of sediment and water which
506 is submitted to washing and dewatering operations. The coarser material (i.e., sand)
507 returned clean and ready to be reused while the fine clay fraction can undergo two
508 different treatments. In the first, a certain amount of clay goes to a plasma fusion plant
509 to extract silicon iron alloys and slag (inert material). The latter is obtained by
510 vitrification through rapid cooling. Heat is also produced (in the form of water at 90°C).
511 This can be sold to surrounding industrial plants that can benefit from this energy
512 contribution in an industrial symbiosis (IS) approach (Domenech et al., 2019). The
513 second process is fed with the material exceeding the inlet capacity of the furnace,
514 which is finally reclaimed for landfarming. The material is submitted to biological
515 degradation, which make the material be free of organic pollutants (Figure 4a).

516 On the other hand, *ECOSSEDRA* Project emerges by the need for a shift in the dredged
517 sediment management system in the Port of Ancona (Italy). Traditionally, these
518 sediments have been directly disposed in the port's dumpsite, which is a non-
519 sustainable practice which is no longer permitted. *ECOSSEDRA* aims at circular
520 management of these dredged sediments to obtain materials for road construction in a
521 sustainable and efficient way (Figure 4b). The management scheme used in *ECOSSEDRA*
522 is formed by widely consolidated processes and operations (for instance, acid washing,
523 dewatering, etc.). The innovation, sustainability and circularity of the Project mainly lies
524 on the following:

- 525 i) *ECOSSEDRA* develops a sediment management scheme prototype (mid-scale)
526 where the product obtained (road construction material) will be tested on-
527 site to analyse its characteristics as commercial by-product. This will allow
528 obtaining transferable results to large scale.
- 529 ii) The management scheme of *ECOSSEDRA* will be developed according to the
530 latest Industry 4.0 paradigms, i.e., it will be automatised by a control system
531 in order to look for the most efficient operation and for the minimum carbon
532 footprint during the process.
- 533 iii) The application of the CE principles to toxic sediments is usually complicated
534 since many sediment treatment processes require the use of considerable
535 amounts reagents, water and energy (as explained in Section 5). *ECOSSEDRA*
536 evaluates the most efficient environmental use of resources, for instance, by
537 reusing the process wastewater and other by-products such as gravel
538 fraction, following a zero-pollution approach (Čavoški, 2020).
- 539 iv) The toxic sediments from Ancona port will be used for producing road
540 materials since the human exposure to these materials is much lower than if
541 they were used in the construction sector (Section 6.1.2). In consequence,
542 possible long-term risks (that have not been yet tested) would be minimised.
543 Other uses such as sediment-based embankments will be also evaluated.
- 544 v) To approach circularity during the management process, it is important to
545 mix the treated dredged sediments with low-carbon recycled materials such
546 as those exposed in Table 4, or others like road milling material or demolition
547 rubble.

548 vi) The results will be analysed considering all the relevant parameters of the
549 sediment management process, i.e., economic, environmental, technical,
550 social and risk-based factors.

551 [FIGURE 4 NEAR HERE]

552

553 *6.1. Products obtained from sediments*

554 6.1.1. Sediment fractions: sand, silt and clay

555 When dredged sediments present good quality, i.e., they contain low amounts of
556 pollutants (according to corresponding legislation), they do not need to be treated or
557 just need to be submitted to slight treatment. In these cases, sediments can easily be
558 fractioned in sand, silt and clay. Sand appears as a valuable material in construction and
559 can be also used as filling or filtering material. It is the most profitable fraction of
560 sediments and normally present the best quality in terms of contamination (Doni et al.,
561 2018). Silt has a market as sealing material or secondary raw material in the ceramic
562 industry; while clay, apart from being used in the ceramic industry, can also act as filling
563 material (Hakstege, 2007; Wang et al., 2018a). However, as commented before, vast
564 amounts of dredged sediments worldwide contain pollutants that usually hinder the
565 direct use of sediment fractions, especially in the case of the smallest ones (silt and clay)
566 as they tend to accumulate most of the pollutants (Doni et al., 2018; Zentar et al., 2009).

567

568 6.1.2. Construction materials

569 Due to their mineral compositions, sediments can be used as a binder in the production
570 of construction materials such as bricks, LWA, and cement with the goal to save
571 construction costs (Loudini et al., 2020b; Maletic et al., 2019; Mehdizadeh et al., 2021;

572 Zhao et al., 2022). To do this, sediments generally need to be submitted to a
573 combination of processes and operations since the presence of pollutants or the
574 inappropriate granulometry could significantly decrease the quality of the final product
575 by reducing its strength and durability (Ferrans et al., 2019). In this respect, S/S (Section
576 5.2.2) is a common process to obtain building materials (Kou et al., 2021).

577 LWA are commonly classified as particles with density lower than $2.0 \text{ g}\cdot\text{cm}^{-3}$ (Ayati et al.,
578 2018). Conventional LWA are built by low-dense natural minerals which are becoming
579 limiting. Silt and clay contained in dredged sediments are suitable material to substitute
580 these minerals due to their high content in quartz, feldspar and aluminosilicate minerals,
581 which are essential to produce LWA (Liu et al., 2017b; Wan et al., 2022; Wei et al., 2014;
582 Zhao et al., 2022). This way, dredged sediments can be recycled while the natural
583 mineral consumption is decreased. Sand fraction can be also used, but at lower
584 proportion than silt and clay (Hakstege, 2007). Many authors have developed technical
585 ways to obtain LWA from dredged sediments during last decades. It basically consists of
586 a thermal immobilisation process where the dredged sediments and the material/s used
587 as binder/s are aggregated and, due to heat, expanded to reduce its total density. The
588 heat also helps to immobilise the pollutants in the aggregates (as previously explained
589 in Section 5.3), although it must be assured that the final product present low
590 leachability and complies with the regulations (Bortone and Palumbo, 2007). The
591 production costs for LWA from sediments in a new installed plant vary in the range 23 -
592 $41 \text{ €}\cdot\text{m}^{-3}$ (Hakstege, 2007), although this cost is very dependent on the water content of
593 sediments. Considering that the import price of LWA is usually in the range of 80 -150
594 $\text{€}\cdot\text{t}^{-1}$ (Lim et al., 2020), it can be assumed that LWA production from sediments can be a
595 profitable process. However, the main limitation of sediment based LWA lies on the

596 need to satisfy the quality standards of commercial products since sediment-based LWA
597 often present poorer properties such as water absorption, particle density, compressive
598 strength, shrinkage, and microstructure in comparison to conventional ones. This is
599 highly influenced by the distribution of size fractions, the type of metal that the
600 sediments contain as well as their concentrations (Amar et al., 2021; Beddaa et al., 2020;
601 De Gisi et al., 2020; Liu et al., 2017b).

602 To improve these characteristics, binders are usually added to the aggregate, although
603 this activity can significantly increase the impacts of the process (Kou et al., 2021; Wang
604 et al., 2019; Zhou et al., 2022). For instance, the use of ordinary Portland cement (OPC),
605 which is one of the most common binders to produce LWA (Wang et al., 2018b), implies
606 a generation of $842 \text{ kgCO}_2\cdot\text{t}^{-1}$ of clinker (Amar et al., 2021). Many authors are doing
607 noteworthy efforts to reduce the economic and environmental impacts of this process.
608 To this aim, renewable binders obtained from wastes such as sludge, fly ash, slags, glass,
609 and even blue-green algae have been tested (Table 4) with the goal of reducing resource
610 consumption and the amount of materials to be landfilled, thus improving circularity.
611 However, a feasible scheme to manage polluted sediments has not been yet established
612 (Todaro et al., 2016; Yang et al., 2020).

613 Dredged sediments can be also successfully recovered by including them in cementitious
614 material thanks to their chemical characteristics (Amar et al., 2018; Dang et al., 2013);
615 or alternatively, in concretes (Achour et al., 2019; Rozière et al., 2015; Yang et al., 2020)
616 or mortars (Benslafa et al., 2015; Mehdizadeh et al., 2021; Zhao et al., 2018). In this
617 respect, De Gisi et al. (2020) reported a high sediment recovery efficient by producing
618 974 kg filling materials per ton of dredged sediments. The production process is mainly
619 affected by the temperature and time of calcination, and the substitution rate of

620 sediment. In this respect, Benzerzour et al. (2017) obtained best mortar properties at
621 850 °C for 1 h, and a substitution rate of 8%. The substitution rate will vary according to
622 the mineral characteristics of the sediments, which have significant influence on the
623 final product's properties (Benzerzour et al., 2017). For instance, Mehdizadeh et al.
624 (2021) obtained improved packing density and fluidity when 5% of cement mortar was
625 replaced by fine sediments; while the 60-min static yield stress decreased when
626 sediment substitution was in the range 5%–15%. On the other hand, Zhao et al. (2018)
627 reported sediment content in cementitious material up to 20% without negatively
628 influencing the mortar's compressive strength.

629 When sediments present considerable amounts of metals, organics and salts, the
630 cementitious matrix is often negatively affected. In fact, organic compounds and metals
631 such as zinc, cadmium or chromium can decrease the mortar structural strength by
632 modifying the hydration reactions. Consequently, high-polluted sediments need to be
633 either subjected to intensive pre-treatment to remove their pollutants or added large
634 amounts of binders to immobilise them (Benzerzour et al., 2017; Wang et al., 2018a;
635 Yang et al., 2020), which would decrease the feasibility, sustainability and commerciality
636 of these sediment-based by-products (Mymrin et al., 2017). In this respect, calcination
637 and grinding costs are generally around 45€ - 105 €·t⁻¹ (Benzerzour et al., 2017).

638 Dredged sediments have been also used to manufacture bricks and blocks, which
639 present higher added value than cementitious materials (Lafhaj et al., 2008; Said et al.,
640 2015). The process is similar to other construction products, i.e., combinations of
641 physical operations to pre-treat the building materials followed by a thermal process to
642 synthesise the bricks (Samara et al., 2009). In this respect, Samara et al. (2009) operated
643 a full-scale industrial plant which produced 15,000 bricks with a sediment substitution

644 ratio of 15%. According to their study, these sediment-amended bricks presented 63%
645 and 40% higher compressive strength and firing shrinkage, respectively; and 10% and
646 13% lower porosity and water absorption, respectively, than those obtained using
647 quartz sand. Consequently, these bricks were sturdier and lesser prone to
648 decomposition. In addition, Slimanou et al. (2021) reported sediment-based bricks to
649 have low thermal conductivities in the range of $0.21 - 0.46 \text{ W}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$, thus these bricks
650 could act as insulator materials. However, the production costs as well as the carbon
651 footprint of sediment-based bricks are usually high, which limits the process feasibility
652 (Yang et al., 2020). Furthermore, as bricks are aimed at structural purposes in
653 construction, their standard quality required is much higher than for other less valuable
654 products such as LWA. In relation to this, the market is still reluctant to accept bricks
655 (and other construction materials) made from polluted sediments due to the possible
656 risks associated (Lim et al., 2020; Spadaro and Rosenthal, 2020). Higher efforts should
657 be thus made to assure the long-term safety use of sediments in these products to
658 improve the public acceptance.

659 [TABLE 4 NEAR HERE]

660

661 6.1.3. Road material

662 Another option to take advantage of dredged sediments is using them in the road sector
663 (Kasmi et al., 2017; Loudini et al., 2020b; Siham et al., 2008). By means of example,
664 Loudini et al. (2020b) used dredged sediments with 7% OPC to obtain road foundation
665 layers at lab-scale. Since the final product is not used for structural purposes, the
666 characteristic requirements of these sediment-based products are usually less strict,
667 and, as the contact with human beings is much shorter than for building materials, the

668 long-term risks are noticeably lower. This not only enables to use dredged sediments in
669 higher percentages than in construction materials but could also ease their social
670 acceptance. However, to the best of our knowledge, the characteristics of sediment-
671 based road materials have not been widely tested at large scale.

672 It must be considered that sediments dominated by fine particles hinder their
673 application as road materials since they need higher chemical and granulometric
674 stabilisations, which implies the use of higher amounts of binders such as cement, lime,
675 etc. (Miraoui et al., 2012). This, together with other sediment characteristics such as
676 high metal content, hampers the elaboration of the product and reduces its application
677 possibilities. Further research to study the mechanical behaviour and functionality of
678 sediment-based road materials is needed to overcome these barriers, which is one of
679 the goals of ECOSEDRA project.

680

681 6.1.4. Other products

682 There are other processes that are being currently evaluated with the aim to use
683 dredging sediments to obtain by-products. For instance, since polluted sediments
684 contain significant amounts of metals (Table 1), metal extraction from them appears as
685 a sustainable alternative to traditional metal production from mines (Ferrans et al.,
686 2021; Hasegawa et al., 2019). However, there is still a long way to make this process
687 feasible at large scale since metal extraction is complex and dependant on multiple
688 factors such as the level of pollution in the sediments, the metal speciation and the
689 properties of the sediment matrix. Moreover, metal extraction processes usually
690 present high risks of environmental pollution (Akcil et al., 2015; Norén et al., 2020).

691 To sum up, despite some authors have reported theoretical cost-benefits in the
692 production of sediment-based materials (Yang et al., 2020; Zhao et al., 2022), their
693 characteristics and properties such as the flexural and compressive strength, dry
694 density, thermal conductivity, and water absorption tend to show lower quality in
695 comparison to those obtained from non-renewable sources, especially when recycled
696 materials are used as binders (Spadaro and Rosenthal, 2020; Wang et al., 2018a; Yang
697 et al., 2020). Consequently, the products obtained from circular management
698 configurations usually present limited applications. In addition, depending on the
699 recycled material employed as binder, the percentage of sediments in the products is
700 sometimes as low as 14-20% (Kou et al., 2021; Wang et al., 2019, 2018b), which can limit
701 the quantities of sediments to be applied in the construction industry. Furthermore, the
702 development of large-scale configurations to obtained sediment-based products that
703 are technically, economically and environmentally feasible and able to compete in the
704 current market with the conventional ones is still lacking (Norén et al., 2020; Spadaro
705 and Rosenthal, 2020).

706

707 *6.2. Socio-political barriers for Circular Economy application in sediments*

708 Apart from the technical and operational issues described in Section 6.1, one of the main
709 barriers for the wide commercialisation of sustainable and circular sediment-based
710 products lies on their poor social acceptance since project managers, regulators, and
711 contractors could perceive long-term risks associated to their use (Spadaro and
712 Rosenthal, 2020; Zheng et al., 2019). Legislation is a powerful tool to improve people's
713 awareness by assuring the safety and quality of sediment-based products, but it has to
714 be specific, clear and standard. Too generic and not numerically quantified limits could

715 create controversies between regulating administrations and sediment-based
716 producers, who could slow down the transition to circularity. In addition, differences in
717 national regulations (Section 4) could hinder international markets of by-products due
718 to legal discrepancies between countries. In the case of sediment-based products, it is
719 also important to adapt the legislation to the final use. As explained in Section 6.1, the
720 level of risk is not the same for building than for road construction purposes. On the
721 other hand, regulations that are too conservative, even if they are case specific, can also
722 hinder the production of circular sediment-based materials as they could limit the
723 economic, technical and environmental feasibility of the management process. For
724 instance, in France, dredged sediments are treated as waste by law, even though 90%
725 of them were inert in 2017 (Beddaa et al., 2020).

726 Extra efforts to overcome technical and socio-political barriers are being developed by
727 researchers and environmental stakeholders. In this respect, the European Commission
728 has recently approved *PROMISCES* project, which aims to identify and overcome
729 bottlenecks to deliver the ambitions of the European Green Deal (COM, 2019) and the
730 Circular Economy Action Plan (COM, 2020). Other efforts are being doing on the
731 alignment between the objectives of researchers, technological developers and other
732 stakeholders such as regulators and market distributors. In order to boost circular
733 products on the market, producers have to be aware of the market needs and
734 consumers and contractors should be more flexible to consider not only the final
735 characteristics of the by-products but also the overall steps in production chains.
736 Similarly, regulators could play a key role in the transition to CE practices. First, the
737 biggest efforts should be made in reducing the pollution in origin with the goal to
738 maintain the quality of marine sediments. Moreover, by penalising more significantly

739 non-circular products and practices such as landfilling, regulators can motivate the
740 transition to the sustainable production of sediment-based products (Norén et al.,
741 2020). Initiatives like the EU taxonomy (Lucarelli et al., 2020) are expected to increase
742 CE applications (in the sediment sector and beyond) by encouraging companies to
743 acquire more environmentally sustainable practices and motivating consumers to
744 demand for greener products. However, more data regarding large-scale circular
745 sediment management should be generated to improve social acceptance and give
746 security to producers, policy makers and the general public.

747

748 Conclusions

749 Dredged sediments management is an issue of increasing concern. As they are
750 characterised by containing high proportions of silt and clay fractions, they tend to
751 adsorb and accumulate toxic pollutants such as heavy metals and organic contaminants,
752 which makes them be considered as toxic wastes. Physical operations and/or chemical,
753 thermal and biological processes are needed to reduce their pollutant content and the
754 risk of pollutant resuspensions to the environment. The type and degree of treatment is
755 mainly determined by the sediments' characteristics, including not only their pollutant
756 concentrations but also their water (free and interstitial) content and their size
757 distribution. The treatment scheme is also influenced by legal requirements, although
758 there is a lack of uniformity and coherence in national regulations in terms of the
759 sediment characteristics to be analysed, the pollutant concentration limits and the
760 categories for the classification of sediments.

761 Conventional dredged sediment treatment techniques, which goal is mainly the
762 reduction of the toxicity of sediments, are usually economically and environmentally

763 demanding. However, with the increasing people's awareness in environmental issues
764 and the more restrictive regulation that hinder certain classical applications of
765 sediments, more sustainable and circular approaches for the management of dredged
766 sediments are being sought.

767 Some authors have evaluated the possibility to take advantage of the mineral
768 composition of sediments to obtain by-products that can be used for building and road
769 construction purposes with the goal to decrease the need of raw materials in these
770 sectors and reduce the amounts of sediments wasted. In fact, the production of
771 sediment-based light-weight aggregates, concrete, mortar, bricks, and road foundation
772 layers are being increasingly assessed (mainly at lab scale). However, the production of
773 these sediment-based materials is not always feasible and, in most cases, they present
774 lower quality in terms of structural properties in comparison to conventional non-
775 circular products. The transition to circular economy in sediment management not only
776 implies to obtain by-products from sediments, but also to decrease the overall impacts
777 of the sediment management scheme, for instance by using recycled materials as
778 binders instead of raw resources, minimising transport costs, and reducing overall waste
779 production to approach zero-pollution ambition. However, the commercialisation of
780 sustainable and circular sediment-based products has to deal with socio-political
781 barriers such as low social acceptance, insufficient support from administrations and
782 stakeholders, lack of standard regulations and the limited alignment between the
783 objectives of circular sediment-based producers, consumers and regulators. Significant
784 efforts are being made to overcome these barriers through initiatives such as the EU
785 taxonomy, and the development of innovative projects like *PROMISCES* and *ECOSSEDRA*.

786 However, useful results that could be extrapolated to industrial applications of circular
787 economy in the sediment sector are still scarce and deserved to be further investigated.

788

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803

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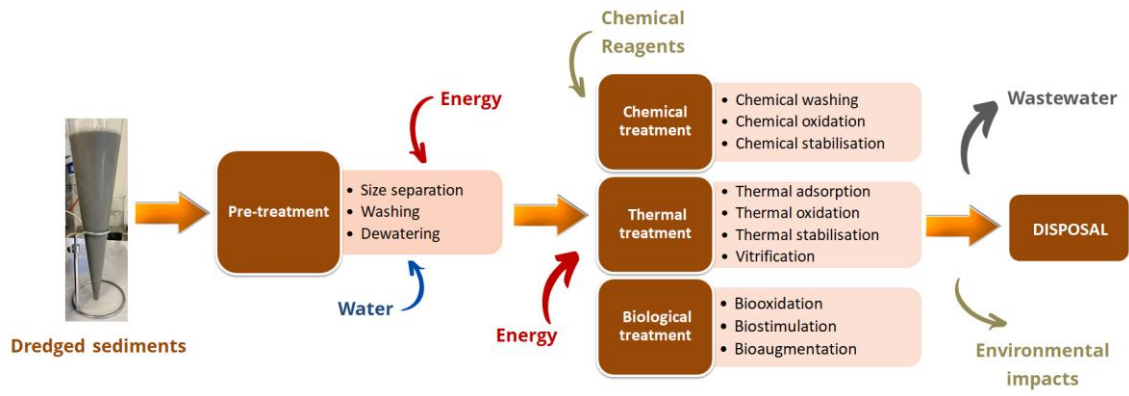
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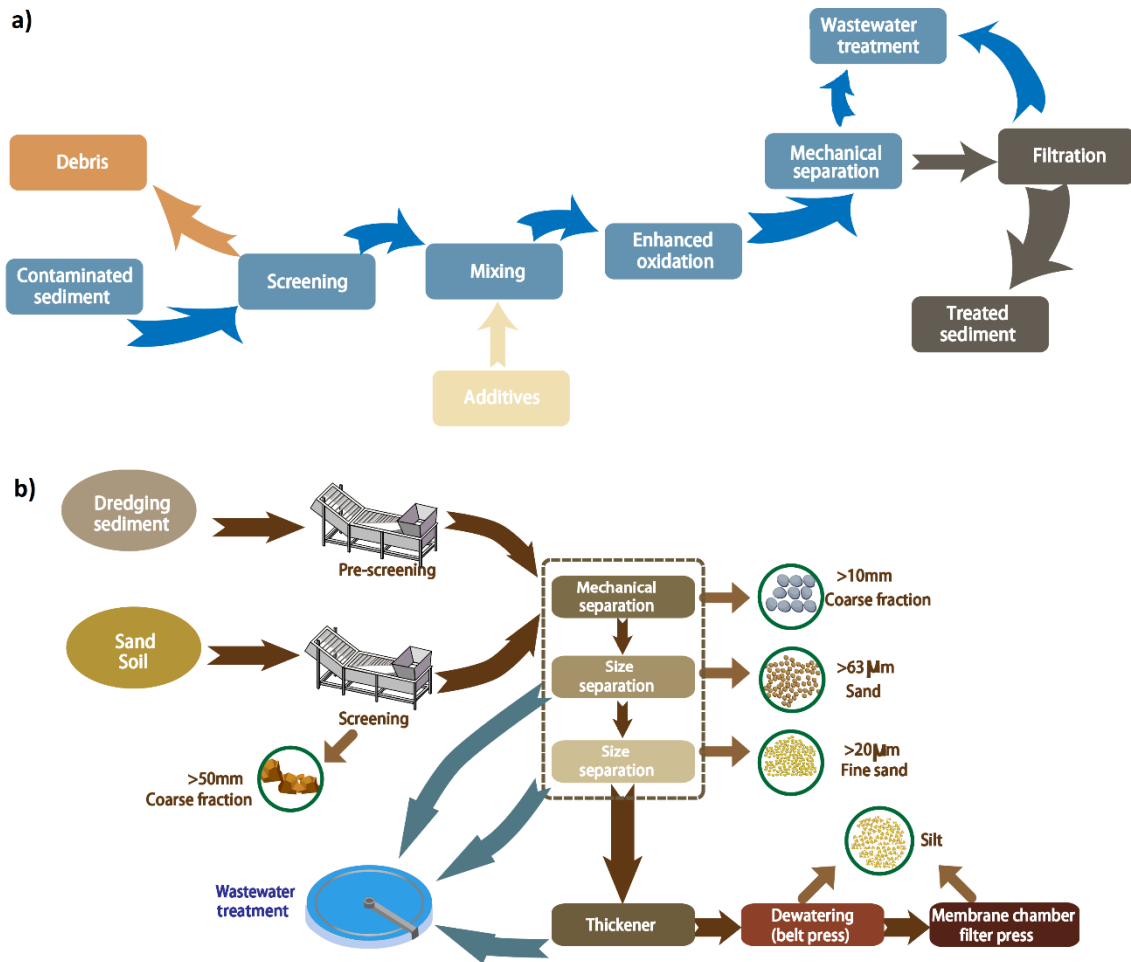


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Figure 1. General configuration of linear sediment treatment.

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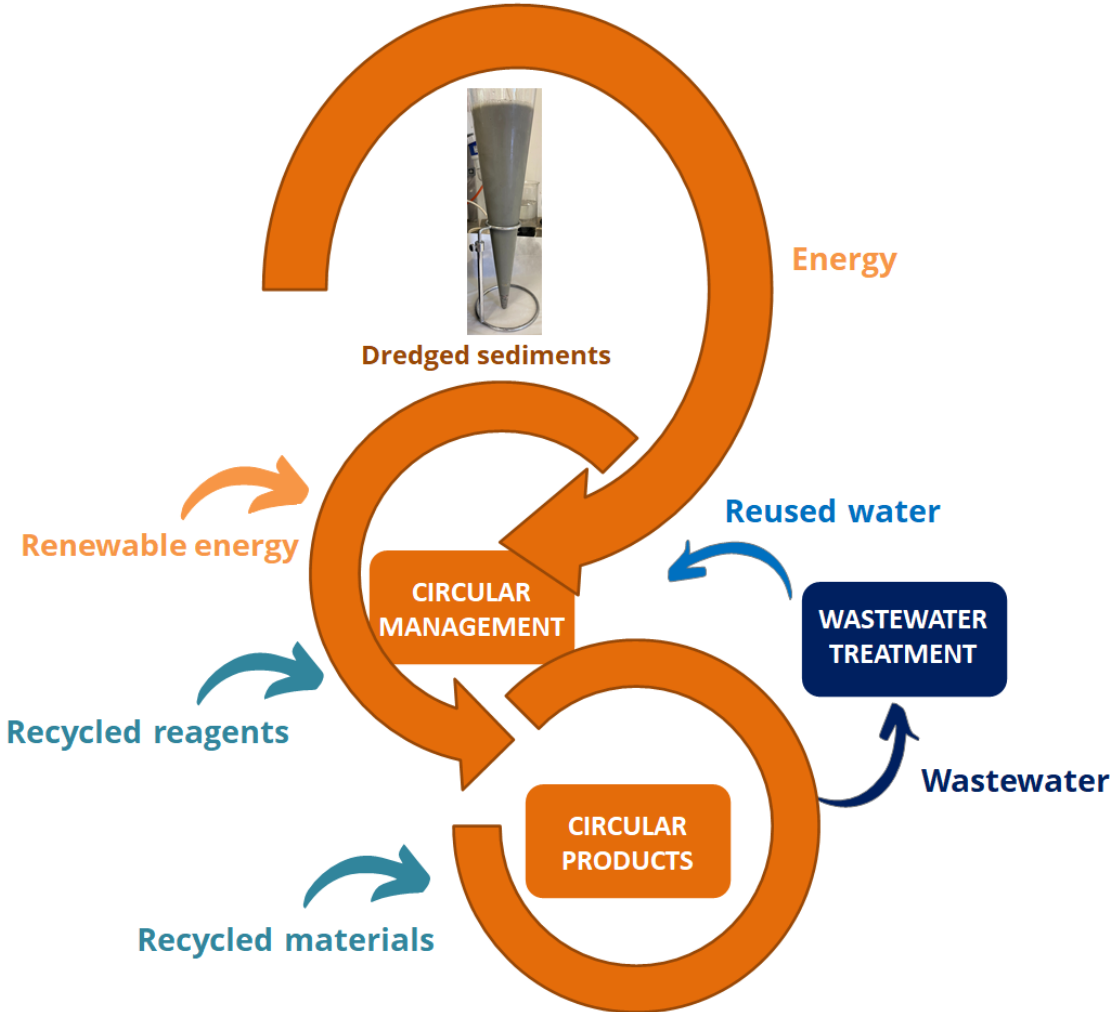
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1153 *Figure 2. Simplified scheme of: a) the BioGenesisSM sediment treatment scheme; b) the*

1154 *METHA sediment treatment scheme.*

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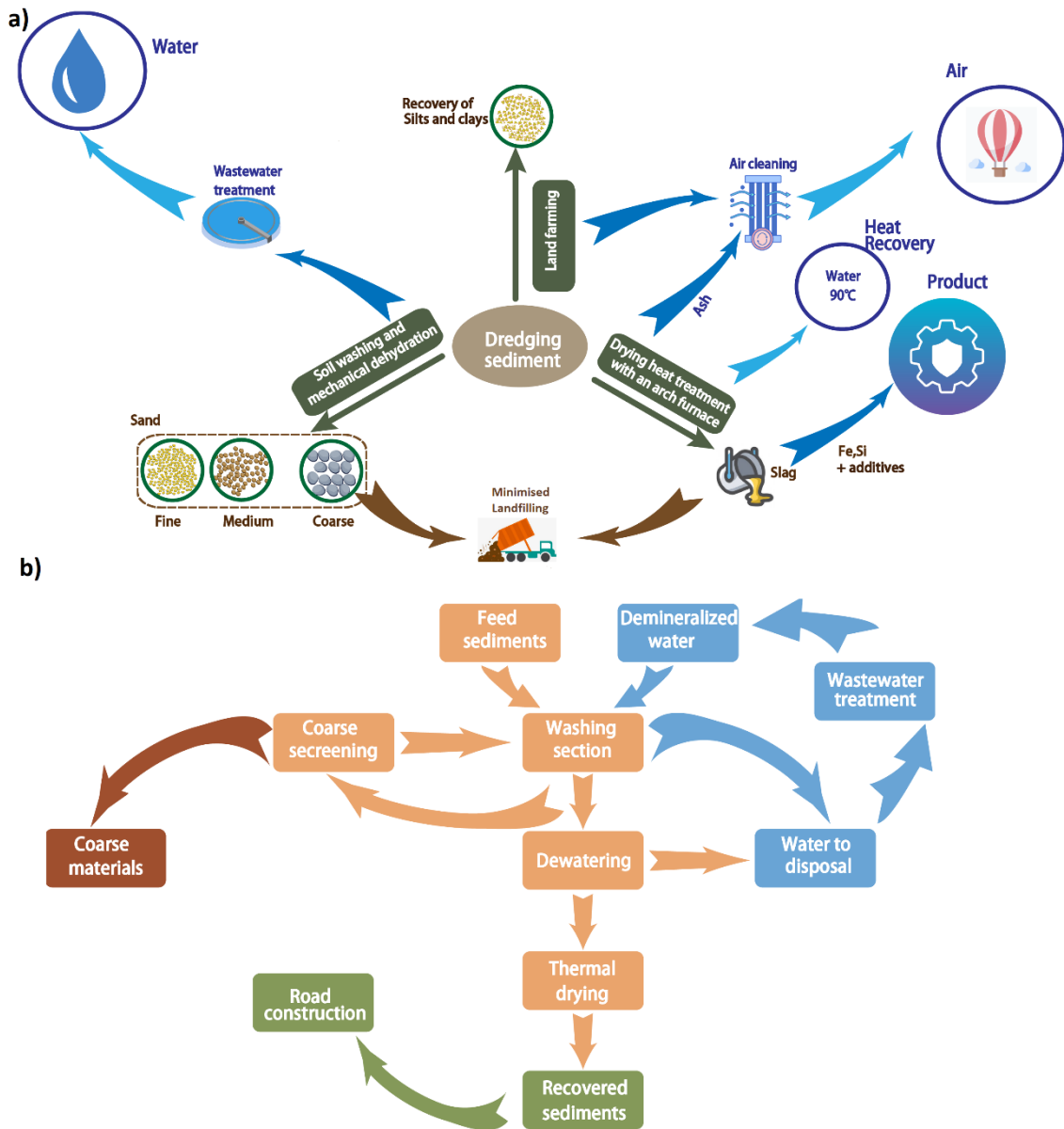
New circular sediment treatment



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1157 *Figure 3. General configuration of circular sediment management strategy.*

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1160 *Figure 4. Simplified sediment management scheme of: a) the SEDI.PORT.SIL project, b)*

1161

ECOSEDRA project.

1162

Table 1: Main characteristics of dredged sediments from different locations.

Reference	Ben											Wang				
	Fonti et al. (2013)	Hadj Ali et al. (2014)	Ben Hadj Ali et al. (2014)	Doni et al. (2018)	Ferrans et al. (2021)	Lopez et al. (2022)	Loudini et al. (2020a)	Loudini et al. (2020b)	Norén et al. (2020)	Norén et al. (2020)	Todaro et al. (2018)	Wang et al. (2018a)	Wang et al. (2018b)	Zhao et al. (2022)	Zhou et al. (2022)	
Location	Port of Ancona (Italy)	Rades harbour (Tunisia)	Gabes harbour (Tunisia)	Livorno harbour (Italy)	Malmfjärden bay (Sweden)	Galveston bay (USA)	Safi harbour S1 (Morocco)	Safi harbour S2 (Morocco)	Gothenburg port (Sweden)	Oskarshamn port (Sweden)	Gulf of Taranto (Italy)	Hong Kong coast	Kwun Tong Typhoon Shelter (Hong Kong)	Tai Lake (China)	Lamma Island (Hong Kong)	
Granulometry (%)	Gravel	-	<1	<1	N.D.	-	-	1	0	-	-	-	10	-	-	48.7
	Sand	-	≈18	≈44	63	10-20	-	41	99.5	-	-	19.4	30	6.1	-	51.1
	Silt- Clay	80	≈81	≈55	37	80-90	-	58	0.5	-	-	80.6	60	93.9	-	0.2
Physico-chemical characteristics	Humidity (%)	40	65-80	-	-	70-78	-	-	-	-	-	44.8	42	58.9	89.9	23.9
	pH	-	-	-	8.3	6.7	-	-	-	-	-	8.8	8.0	7.2	-	8.1
	Conductivity (μS·cm ⁻¹)	-	-	-	16,800	-	-	-	-	-	-	4,100	-	-	-	-
Nutrients (mg·Kg ⁻¹)	TN	-	-	-	3,840	8563-9488	-	-	-	-	-	-	-	-	-	-
	NH ₄	-	-	-	14.1	-	-	-	-	-	-	-	-	-	-	-
	NO ₃	-	-	-	20.0	-	-	-	-	-	-	-	-	-	-	-
	TP	-	-	-	650	740-1159	-	-	-	-	-	-	-	-	-	-
Organic compounds (mg·Kg ⁻¹)	Total organics	28,000	67,600-68,300	70,300-109,700	19,300	129,000	-	50,000	0	-	-	123,000	-	64,000	5741	25,500
	TBT	-	-	-	-	-	-	-	-	150	N.D.	-	-	-	-	-
	TPH	-	-	-	5447	-	-	-	-	-	-	-	-	-	-	-
	PAHs (μg·Kg)	-	-	-	-	-	-	-	-	-	-	5,389	-	-	-	-
	PCBs (μg·Kg)	-	-	-	-	-	-	-	-	-	-	1,669	-	-	-	-
	Cu	33	-	-	123	40	0.8-351.8	-	-	50	1100	10.5	-	1700	70.85	378.5

Metals (mg·Kg⁻¹)	Zn	83	-	-	240	120	4.3-336.6	-	-	200	400	16.6	-	410	104.3	138.5	
	Cd	0.5	-	-	N.D.	N.D.	0.02-0.5	-	-	0.4	4	-	-	2.6	-	1.8	
	Cr	70	-	-	64.0	24	1.5-70.8	-	-	40	50	54.0	-	240	84.49	29.7	
	Ni	40	-	-	49.1	23	1.1-30.3	-	-	20	60	38.2	-	68	-	23.6	
	Pb	12	-	-	59.7	44.9	1.8-29.2	-	-	40	560	87.4	-	120	65.06	101.1	
	As	10	-	-	-	8.3	1.3-20.0	-	-	-	-	12.3	-	-	-	7.8	
	Co	-	-	-	-	-	-	-	-	-	-	7.1	-	-	-	-	
	Al	-	-	-	-	-	1,6- 54,003	-	-	-	-	-	-	-	-	-	-
	Fe	22,00 0	-	-	-	-	636- 23,655	-	-	-	-	-	-	-	-	-	-
	Sb	-	-	-	-	-	0.1-1.5	-	-	-	-	-	-	-	-	-	-
	Mn	-	-	-	-	-	6.1-694.5	-	-	-	-	-	-	-	-	-	-
	Hg	-	-	-	-	-	0.01-0.4	-	-	-	-	-	-	-	-	-	-
	V	-	-	-	-	-	-	-	-	-	-	53.3	-	-	-	-	-

1164 N.D.: non detected; NH₄: ammonium; NO₃: nitrate; PAHs: polycyclic aromatic hydrocarbons; PCBs: poly chlorinated biphenyls; TBT: tributyltin; TN: total nitrogen; TP: total -
1165 phosphorus; TPH: total petroleum hydrocarbon.
1166 S1 of Safi harbour corresponds to the basin zone of the port and S2 corresponds to the channel zone of the port.

1167 Table 2: Characteristics of the regulations relative to dredged sediment management in
 1168 Italy, France and Spain.

	ITALY	FRANCE	SPAIN
Reference regulation related to handling and management of marine dredged sediments.	Ministerial Decree n° 173 of 15th July 2016. DM 5th February 1998.	Environmental Code and the circular of 4/07/2008.	Guidelines for the characterisation of dredged material and their relocation within waters of the maritime-terrestrial public domain (2014). Law 22/2011 on Contaminated Wastes and Soils.
Parameters to be evaluated	<ul style="list-style-type: none"> • Macroscopic description; • Physical parameters; • Chemical parameters; • Ecotoxicological analysis: battery of 3 tests on all samples. 	<ul style="list-style-type: none"> • Physical parameters; • Chemical parameters; • Biological characterisation: only in the cases where any of the compounds exceeds the N2 threshold. 	<ul style="list-style-type: none"> • Physical parameters; • Chemical parameters (only for those potentially toxic according to previous testing); • Biological parameters (only for non-toxic sediments, quality C).
Other requirements	<ul style="list-style-type: none"> • Microbiological investigations for sea diving and coastal nourishment in proximity to bathing and aquaculture areas. • Mineralogical investigations in case of coastal nourishment. • Study of benthic communities for immersion in the sea over 3 nmi and nourishment. 	<ul style="list-style-type: none"> • Determination of nitrogen and phosphorus for sediment discharged in sensitive areas; • Faecal contamination to avoid impacts on shellfish, mariculture, or bathing areas. • Biological characterisation of the affected site in case of sediment immersion, if at least one element 	<ul style="list-style-type: none"> • Previous toxicity test (PTT), consisting of the inhibition of the luminescence of the bacterium <i>Vibrio fischeri</i> by direct contact of sediment suspensions and measured as EC50 concentration. • Bio-essays.

	<ul style="list-style-type: none"> Release tests in water of the matrices for a period of 24 hours. The leachates from these tests cannot overpass the pollutants thresholds reported in DM 5th February 1998. 	<p>exceeds the N2 threshold.</p> <ul style="list-style-type: none"> The particle size has to be considered in case of reuse for nourishment. 	
Management options	Based on the sediment quality class determined by a weighted integration criteria regarding the ecotoxicological hazard class and chemical hazard class.	Based on concentration limits of some physical and chemical parameters such as particle size, metals, organic micro-pollutants.	Based on two-step characterisation: one preliminary step to analyse their potential toxicity and a second step based on chemical and biological characterisation.
Classification	5 sediment quality classes: A > B > C > D > E.	Categories: N1 (low pollutant concentrations); N2 (mid pollutant concentrations).	Classified as non-toxic or toxic (when overpasses some legal limits). 3 quality classes for non-toxic sediments: A > B > C.
References	Bortone and Palumbo (2007).	Mugnai et al. (2018); Tessier et al. (2011)	Buceta et al. (2015)

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nmi: nautic miles.

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1171 Table 3: Main characteristics of conventional dredged sediments treatment processes.

	Treatment	Goal of the process	Target wastes	Performance	Main impacts	Costs	References
Physical operations	Mechanical separation	To divide sediments in sand, silt and clay fractions	Sediments	Generally high performance	Energy consumption (M). Water consumption (L).	3 - 11 € (2007)·m ⁻³	Bortone and Palumbo (2007) Kim et al. (2016) Mulligan et al. (2001) Pal and Hogland (2022)
	Dewatering	To remove interstitial water	Water	Up to 80% of water removal (improved with chemical conditioners)	Energy consumption (M) Use of chemicals (L)	10-35 € (2007)·m ⁻³	Bortone and Palumbo (2007) Chi et al. (2018) Zhao et al. (2022)
	Washing	To reduce pollutant and salt concentration in sediments	Metals, salts.	Depending on the reagent, dosage, contact time, temperature and number of extractions (each case must be evaluated). Worse performance for smaller fractions.	Use of chemicals (M) Water pollution (M). Water consumption (H) Energy consumption (L).	40-73 € (2009)·m ⁻³	Beiyuan et al. (2018) Doni et al. (2018) Ferrans et al. (2021) Jeon et al. (2015) Pal and Hogland (2022) Papadopoulos et al. (1997) Polettoni et al. (2009) Tsai et al. (2009)

Chemical treatment	Chemical oxidation	To degrade pollutants into non-hazardous compounds.	Organic pollutants	Depending on the chemical reagent, type of pollutant and water content. Poor metal removal.	Use of chemicals (H). Air treatment (L). Water consumption (L). Ecotoxicity (M) Environmental impacts (M-H)	Depending on the process conditions	Bortone and Palumbo (2007) Debnath et al. (2021) Ferrarese et al. (2008) Maletic et al. (2019) Todaro et al. (2016)
	Solidification/Stabilisation (S/S)	To immobilise pollutants to reduce their mobility and bioavailability.	Metals.	Good performance with As, Pb, Cr(VI), Hg, Cd, Cu, Zn. Poor performance with high water, organics, salts contents and with certain metals. Lower impacts than thermal treatment	Use of chemicals (H). Energy Consumption (M) Risk of pollutant release (M) Ecotoxicity (M) Environmental impacts (M-H)	10 – 41 € (2007)·m ⁻³	Amar et al. (2021) Barjoveanu et al. (2018) Hossain et al. (2020) Kou et al. (2021) Maletic et al. (2019) Mulligan et al. (2001) Norén et al. (2020) Radenovic et al. (2020) Tang et al. (2020) Todaro et al. (2020) Wang et al. (2015)
Thermal treatment	Thermal desorption	To separate VOCs from sediments.	Organic pollutants	High for VOCs (T = 450-500°C); for some metals (T = 800 °C).	Energy consumption (M-H). Air pollution (M). Ecotoxicity (M)	50 – 70 € (2007)·t ⁻¹	Bortone and Palumbo (2007) Mulligan et al. (2001) Pal and Hogland (2022) Todaro et al. (2016)

					Environmental impacts (M-H)		
Thermal oxidation	To degrade organic pollutants.	Organic pollutants.	High performance temperature adequate.	if is	Energy consumption (H). Air pollution (M). Environmental impacts (M-H)	50 – 70 € (2007)·t ⁻¹	Amar et al. (2021) Bortone and Palumbo (2007) Pal and Hogland (2022) Snellings et al. (2016)
Thermal immobilisation	To immobilise metals to reduce their mobility and bioavailability.	Metals.	Depending on the sediment characteristics. Generally higher performance than chemical S/S. Bricks, aggregates and other materials can be produced.		Energy consumption (H). Air pollution (M). Ecotoxicity (M) Environmental impacts (H)	50 – 70 € (2007)·t ⁻¹	Snellings et al. (2016) Zhao et al. (2022)
Vitrification	To destroy and/or immobilise pollutants.	Metals.	Very effective.		Energy consumption (HH). Air pollution (M). Ecotoxicity (M) Environmental impacts (H)	Depending on the process conditions	Colombo et al. (2012) Mulligan et al. (2001) Norén et al. (2020) Todaro et al. (2016)

Biological processes	To degrade pollutants by microbial activity.	Biodegradable pollutants.	Low degradation rates.	Land requirements (H).	Depending on the process conditions	Amar et al. (2021) Liu et al. (2017a) Maletic et al. (2019) Doni et al. (2018) Feng et al. (2022) Fodelianakis et al. (2015) Wu et al. (2014)
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1172 *L: Low impact; M: Medium Impact; H: High Impact.*

1173 *€/\$(xx): value of money in €/\$(xx) referred to year xx; CDF: confined disposal facilities; VOCs: volatile organic compounds.*

Table 4: Circular production of construction materials obtained from dredged sediments.

Product	Sediment content (%)	Binders	Scale	Treatment operation and processes	Product characteristics	Positive impacts	Costs	References
Sediment-based zeolite	-	Sodium metaaluminate, cadmium chloride, sodium silicate, sodium chloride, hydrochloric acid, sodium hydroxide.	Lab	Mechanical separation, Hydrothermal treatment	High specific surface: 516.36 m ² /g.	Capacity of Cd removal from wastewater.	-	Chen et al. (2021)
Filling material	85-90	Quicklime (10% wt), activated carbon, organocaly	Pilot	S/S	Unconfined compressive strength: 18.2-28.1 KPa. Suitable for environmental enhancement.	No pre-treatment of sediment needed (lower costs and impacts). High sediment recovery: 97.4%.	-	De Gisi et al. (2020)
LWA	66	Steel slag (27%) and waste glass (7%).	Lab	Thermal stabilisation	Reduced water absorption: 2.2%. Increased compressive strength: 23.1 MPa.	Alternative for the disposal of dredged sediments. Waste reduction.	-	Lim et al. (2020)
LWA	50	Sewage sludge	Lab	Thermal stabilisation	Density: 836 kg m ⁻³ Compressive strength: 13.7 MPa. Water absorption < 12%.	Reduction of toxicity of sediments. Waste reduction.	-	Liu et al. (2018)

Mortar	20	OPC (60%); CCS (10 %), GGBS (10%).	Lab	Stabilisation	Lower flexural and compressive strength when only sediments were used as binder. Low pozzolanic activity.	Reduction in the use of cement and consumption of mining materials.	-	Kou et al. (2021)
Bricks	15-20	Clay	Lab	Thermal stabilisation	Increase of mechanical properties: 20.6-32.5% Low thermal conductivity: 0.21-0.46 W·m ⁻¹ ·K ⁻¹ (insulating material)	Resource recovery. Possible economic and environmental benefits.	-	Slimanou et al. (2020)
Blocks	15	CCR (5%), OPC (20%), ISSA (5%), fly ash (5%), GGBS (20%).	Lab	S/S	Addition of CCR, GGBS and fly ash provided relative high strength.	Carbon sequestration: 4.3 %wt Reduction of sediment toxicity. Waste reduction.	-	Wang et al. (2018b)
Fill material/ Blocks	14-47.5	OPC, biochar (1-2%), ISSA	Lab	Stabilisation	Improvement of immobilisation of pollutants due to biochar.	Alternative for disposal in landfills for toxic wastes.	-	Wang et al. (2019)
LWA	80-90	Slag waste containing dioxins (10-20%)	Lab	Thermal stabilisation	No presence of dioxins nor metal leaching	Dioxins removal. Waste reduction.	-	Wei et al. (2014)
Foamed concrete	30	OPC, foam (0-80% v/v) and silica fume (10%).	Lab	Stabilisation	Compressive strength: 2.1-18.8 MPa. Dry density: 620.6-1442 kg·m ⁻³ .	Without heating nor pressurising. Reduction of wastes.	40.98-50.88 \$·m ⁻³	Yang et al. (2020)

					Thermal conductivity: 0.173-0.516 W·m ⁻¹ ·K ⁻¹ . Water resistance coefficient: 0.43-0.73.			
Fill material	82.5-88.5	OPC (1.5-7.5%) and fly ash (10%).	Lab	Stabilisation	Large quantities of calcium silicate hydrate.	Improved properties in comparison with stabilising only with cement or fly ash	-	Yoobanpot et al. (2020)
Road construction material	94-98	CSA cement	Lab	S/S	Compressive strength: 0.5-1.91 MPa. Splitting tensile strength: 0.057-0.119 MPa. Elastic modulus: 0.41-1.07 GPa.	CSA is a greener binder than OPC.	-	Zentar et al. (2021)
Ceramsite (LWA)	60	Blue-green algae (20%); 20% of additives (fly ash:calcium oxide:kaolin)	Lab	Dewatering; thermal stabilisation	Product accomplished the National Standard as building material.	Simultaneous reduction of lake pollutants: toxic dredged sediments and algae. Economical profit: 2.3\$.m ⁻³ .	18.8 \$.m ⁻³	Zhao et al. (2022)
Fill material	70	ISSA (20%); OPC (10%)	Lab	S/S	Low leachate concentrations even under simulative acidic rainfall conditions.	Decrease of cement consumption.	-	Zhou et al. (2022)

1175 CCR: calcium carbide residue; CCS: calcium carbide slag; GGBS: ground granulated blast-furnace slag; ISSA: incinerated sewage sludge ash; LWA: lightweight aggregates; OPC:
1176 ordinary Portland cement; S/S: Stabilisation-solidification.
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