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4 **Electrochemical characterization of electrochemically reduced graphene coatings**
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6 **on platinum. Electrochemical study of dye adsorption.**
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22 **Abstract**
23

24 Reduced graphene oxide coatings were synthesized by cyclic voltammetry on Pt
25 electrodes. Electrochemically reduced graphene oxide was analyzed by scanning
26 electrochemical microscopy for the first time. The redox mediator influences the
27 electrochemical response; thus $\text{Ru}(\text{NH}_3)_6^{3+}$ and $\text{Fe}(\text{CN})_6^{3-}$ gave a similar response and
28 Fe^{3+} gave the poorest response. Pt electrodes coated with reduced graphene oxide were
29 also used in the electrochemical adsorption (performed by cyclic voltammetry) of
30 different dyes (Methylene Blue, Procion MX-2R and Amaranth). Electrochemical
31 methods proved to be useful to monitor the adsorption of dyes on the surface of
32 graphene materials. After adsorption, with Methylene Blue and Procion MX-2R, the
33 appearance of a stable redox pair (with 1 electron transfer) was observed. This redox
34 pair was adsorption controlled since the intensity of the redox pair was proportional to
35 the scan rate used. Electrochemical adsorption multiplied by 3 the electrical charge of
36 the Methylene Blue adsorbed on the surface of reduced graphene oxide when compared
37 with simple adsorption at open circuit potential. In the case of Procion MX-2R, the
38 increase obtained was even higher, with a 6-fold increase.
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4 **Keywords:** graphene, reduced graphene oxide, scanning electrochemical microscopy,
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6 dye, adsorption.
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28 **1. Introduction**

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30 Since the discovery of graphene by Novoselov et al. [1], graphene has emerged as a
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32 revolutionary material in the field of physics and materials science due to its electronic
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34 [2], optical [3], thermal [4] and mechanical properties [5,6]. Different methods of
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36 production have been used for the production of graphene and derivatives [7,8]. High
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38 quality graphene crystals are obtained from mechanical exfoliation (the first method
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40 reported by Novoselov et al.) [1], however its production is limited to low quantities
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42 only useful for basic studies. This is why other methods with higher production capacity
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44 have been used, for instance: chemical vapour deposition [7,8] or chemical methods [7-
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46 9]. Among chemical methods, the production of graphene oxide (GO) is of particular
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48 interest due to the low production costs and its versatility. The reduction of GO allows
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50 the deposition of reduced graphene oxide (RGO) on different substrates. The reduction
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52 can be performed thermally, photocatalytically, chemically, electrochemically, etc. [10].
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54 Electrochemical reduction is of particular interest because its ease of operation and
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56 control, and no additional reagents such as dangerous reductants (for instance
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4 hydrazine) are needed [10]. The applications of graphene and derivatives in chemistry
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6 and electrochemistry are varied and numerous and include energy storage [7], sensors
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8 [7], oxygen reduction reaction [11] or photocatalysis [12] among others.
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10 Scanning electrochemical microscopy (SECM) is a powerful technique that has been
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12 used to test the electroactivity of samples ranging from biological applications [13] to
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14 materials characterization such as corrosion processes [14]. Some studies have focused
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16 on the electrochemical characterization of graphene, graphene oxide and reduced
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18 graphene oxide by SECM [15-21]. However, the characterization by SECM of RGO
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20 obtained by electrochemical methods has not been reported in bibliography. This is the
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22 reason why electrochemical characterization by SECM of RGO deposited on Pt
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24 electrochemically was performed in this paper.
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28 The interaction of graphene with organic molecules has been shown to be of interest; for
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30 instance the doping (n or p) of graphene with aromatic molecules has been
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32 demonstrated [22]. Graphene and derivatives have also been shown to be good
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34 adsorbents for dyes due to the π - π stacking interaction between graphene and aromatic
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36 compounds [23,24]. These materials could have applications in dye-sensitized
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38 biosensors [25] or charge transfer complexes [26-28]. In this paper, the electrochemical
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40 adsorption of different dyes by cyclic voltammetry (CV) is proposed as a method to
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42 monitor the adsorption of the dye and a more efficient way of adsorbing dyes than open
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44 circuit adsorption. The RGO/dye complexes were also later characterized by CV in
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46 order to evaluate the adsorption products as well as its electrochemical properties.
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56 **2. Experimental**

57 **2.1. Reagents and materials**

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4 All reagents used were of analytical grade.

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6 For the synthesis: Monolayer graphene oxide (GO) powders were acquired from
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8 Nanoinnova Technologies S.L. (Spain). Lithium perchlorate (LiClO_4) was purchased
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10 from Merck. Pt wires (0.5 mm diameter, 99.99% purity) were acquired from Engelhard-
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12 Clal. The effective length of the electrodes used (where reaction occurred) was 2 cm
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14 (total area of 0.31 cm^2). The area of the electrodes was controlled with Teflon®.

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16 For the characterization: Sulphuric acid (H_2SO_4) and potassium chloride (KCl) were
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18 purchased from Merck. Hexaammineruthenium (III) chloride ($\text{Ru}(\text{NH}_3)_6\text{Cl}_3$), potassium
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20 ferrocyanide (III) $\text{K}_3\text{Fe}(\text{CN})_6$ and iron (III) sulfate pentahydrate ($\text{Fe}_2(\text{SO}_4)_3 \cdot 5\text{H}_2\text{O}$) were
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22 used as received from Acrōs Organics. Methylene Blue (MB), Procion MX-2R
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24 (PMX2R) and Amaranth (AM) were purchased from Panreac, Zeneca and Fluka,
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26 respectively.
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30 When needed, solutions were deoxygenated by bubbling nitrogen (N_2 premier X50S).
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32 Ultrapure water was obtained from an Elix 3 Millipore-Milli-Q Advantage A10 system
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34 with a resistivity near to $18.2 \text{ M}\Omega \text{ cm}$.
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40 2.2. Synthesis of reduced graphene oxide on Pt

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42 An Autolab PGSTAT302 potentiostat/galvanostat was used to perform cyclic
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44 voltammetry (CV) as well as electrochemical impedance spectroscopy (EIS)
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46 measurements. GO was reduced on the surface of Pt by CV. The solution used for the
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48 synthesis contained ultrapure water, 3 g L^{-1} GO and 0.1 M LiClO_4 (supporting
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50 electrolyte). Pt electrodes were pretreated with a flame treatment to clean their surface
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52 [29]. A three-electrode configuration was used for the synthesis: a Pt wire was used as
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54 counter electrode and Ag/AgCl (3.5 M KCl) was used as reference electrode. To
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4 perform the electrochemical synthesis, the potential was cycled between +0.6 V and -
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6 1.4 V at 50 mV s⁻¹ for 40 scans.
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10 2.3. Field emission scanning electron microscopy (FESEM)

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12 A Zeiss Ultra 55 FESEM was used to observe the morphology of the samples, using an
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14 acceleration voltage of 3 kV. Energy dispersive X-ray (EDX) measurements were
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16 performed between 0 and 10 kV.
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22 2.4. Electrochemical characterization by cyclic voltammetry (CV)

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24 After synthesis, the electrodes were characterized by CV in 0.5 M H₂SO₄ to test their
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26 characteristic capacitive behavior. Electrodes were also tested with different redox
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28 systems (0.01 M Ru(NH₃)₆³⁺ / 0.1 M KCl; 0.01 M Fe(CN)₆³⁻ / 0.1 M KCl and 0.02 M Fe³⁺
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30 / 0.5 M H₂SO₄) to test their reversibility and therefore the electrochemical behavior of
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32 the electrode surface.
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38 2.5. Electrochemical impedance spectroscopy (EIS)

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40 The same configuration used for the synthesis of RGO on Pt was used for the EIS
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42 characterization of the electrodes in 0.5 M H₂SO₄ solution.
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45 The experimental results were also fitted using a non-linear least squares fitting
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47 minimization method by ZView software (version 2.7).
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52 2.6. Scanning electrochemical microscopy (SECM)

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54 SECM measurements were carried out with a scanning electrochemical microscope of
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56 Sensolytics. A three-electrode configuration cell consisting of a 25- μ m-diameter Pt
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58 microelectrode, a Pt wire auxiliary electrode and Ag/AgCl (3.5 M KCl) reference
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4 electrode. Measurements were performed with the same redox systems used in the CV
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6 characterization: 0.01 M $\text{Ru}(\text{NH}_3)_6^{3+}$ / 0.1 M KCl; 0.01 M $\text{Fe}(\text{CN})_6^{3-}$ / 0.1 M KCl and 0.02
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8 M Fe^{3+} / 0.5 M H_2SO_4 . All the experiments were carried out in an inert nitrogen
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10 atmosphere.

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12 The samples were glued to microscope slides with epoxy resin. The microelectrode
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14 operated at a potential of -0.4 V, 0 V, -0.1 V for the 0.01 M $\text{Ru}(\text{NH}_3)_6^{3+}$ / 0.1 M KCl, 0.01
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16 M $\text{Fe}(\text{CN})_6^{3-}$ / 0.1 M KCl and 0.02 M Fe^{3+} / 0.5 M H_2SO_4 systems, respectively. At
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18 these potentials, the oxidized form of the redox mediator (Ox) is reduced (Red) at a
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20 diffusion controlled rate. Approach curves were obtained by recording the tip reduction
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22 current as the microelectrode tip was moved in z direction (approaching the sample).
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24 Approach curves give us an indication of the surface's electroactivity. These curves
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26 were compared to the theoretical ones (positive and negative feedback models). The
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28 substrate's surface in all the measurements was at their ocp.
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36 2.7. Electrochemical behavior of dyes on the surface of Pt/RGO electrodes

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38 The electrochemical behavior of different dyes was tested by means of CV. Solutions
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40 containing $5 \cdot 10^{-3}$ M of MB, PMX2R and AM and 0.5 M H_2SO_4 were used for this
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42 purpose. A three-electrode configuration was used. Potential was cycled between -0.2 V
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44 and +0.7 V for 100 scans to produce the adsorption of the dyes. An experiment was also
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46 performed at ocp in the same conditions to evaluate the spontaneous adsorption of dyes
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48 during 1 hour. The potential evolution during ocp adsorption was monitored by means
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50 of chronopotentiometry (zero current). The electrodes were characterized previously
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52 and after dyes' adsorption in 0.5 M H_2SO_4 solutions to determine possible adsorption
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54 products on the surface of RGO. To evaluate dye adsorption, the electrodes were rinsed
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56 with water several times in order to eliminate the dye not adsorbed. The electrodes were
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4 also characterized at different scan rates to determine if the processes were diffusion or
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6 adsorption controlled and determine the number of electrons involved.
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10 11 12 13 14 **3. Results and discussion**

15 16 17 3.1. Field emission scanning electron microscopy (FESEM)

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20 Fig. 1 shows the FESEM micrographs and EDX analysis of the Pt/RGO electrode
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22 obtained by means of cyclic voltammetry, sweeping the potential from +0.6 V to -1.4 V
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24 for 40 scans. The whole surface of the Pt electrode was coated by RGO sheets; in Fig.
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26 1-a RGO sheets deposited on Pt have been magnified for better observation. EDX was
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28 used to analyze chemically the composition of the sample (Fig. 1-b). C, O and Pt
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30 appeared in the spectrum; C and O arise from GO. The presence of Pt is due to the
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32 penetration of the X-ray that is in the order of μm , much higher than the thickness of the
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34 coating. The O/C atomic ratio obtained was 0.08, which indicates a high reduction of
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36 the GO sheets when compared with other methods [10].
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48 Fig. 2-a shows the voltammetric characterization of Pt and Pt/RGO electrodes in 0.5 M
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50 H_2SO_4 solution. As can be seen, the deposition of RGO on Pt inhibits the appearance of
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52 the characteristic oxidation and reduction processes on the platinum surface. The
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54 voltammetric profile shows the characteristic capacitive behavior of RGO. The
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56 oxidation/reduction peaks that appear between +0.2 V and +0.5 V have been attributed
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58 to a redox pair of oxygen containing groups [30,31] that are too stable to be reduced by
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4 cyclic voltammetry [30]. The electrochemical reduction is not capable of eliminating
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6 completely the oxidized functional groups and C-OH, C=O and C-O-C groups are still
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8 present after electrochemical reduction [32]. However the O/C ratio obtained by
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10 electrochemical method is lower than the one achieved by chemical reduction methods
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12 [21], which implies that a more efficient reduction of GO is achieved by
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14 electrochemical methods.
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18 Fig. 2-b shows the voltammetric characterization of Pt/RGO electrodes with different
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20 redox mediators ($\text{Fe}(\text{CN})_6^{3-}$, $\text{Ru}(\text{NH}_3)_6^{3+}$ and Fe^{3+}). The peak to peak potential
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22 separation for the different redox mediators was 101, 121 and 538 mV for $\text{Ru}(\text{NH}_3)_6^{3+}$,
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24 $\text{Fe}(\text{CN})_6^{3-}$, and Fe^{3+} , respectively. The Fe^{3+} redox mediator has been shown to be
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26 sensitive to surface oxides. The presence of surface oxides accelerates the electron
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28 transfer [33,34]. In this case the difference of 538 mV indicates a reduced content of
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30 oxides on the RGO's surface. Hence the $\text{Ru}(\text{NH}_3)_6^{3+}$ was the best redox mediator
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32 followed very closely by $\text{Fe}(\text{CN})_6^{3-}$, both mediators have been shown to have higher
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34 apparent heterogeneous electron transfer rate constants than Fe^{3+} redox mediator on
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36 RGO surface [35]. However the Fe^{3+} redox mediator can be used as an indicator of the
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38 presence of surface oxides.
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45 Fig. 3. shows the electrochemical characterization of Pt and Pt/RGO electrodes by EIS
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47 in 0.5 M H_2SO_4 solutions. The Nyquist plots for Pt and Pt/RGO are shown in Fig. 3-a
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49 and Fig. 3-b, respectively. The equivalent circuit used to adjust the data is shown in the
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51 inset of each figure. The adjustment of the data to the equivalent circuits is shown as a
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53 continuous line and the experimental data are shown as dots. The equivalent circuits are
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55 composed of:
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59 **Re:** electrolyte resistance between the reference and the working electrode.
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4 **CPE:** constant phase element simulating the non-ideal behavior of the capacitor.

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6 It is composed of CPE-T which gives the value of pseudo-capacitance at the
7 electrolyte/RGO interface and CPE-P which gives an idea about the behavior of
8 the CPE. When CPE-P is equal to 1, the CPE is equal to a capacitor (C). If CPE-
9 P equals 0.5, the CPE represents the case of semi-infinite linear diffusion (and a
10 straight line with 45 degree slope would be recorded on the Nyquist diagram).
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18 **Rct:** corresponding to the charge transfer resistance at the Pt/electrolyte
19 interface, in parallel with the CPE element. The combination in parallel of CPE
20 and Rct is responsible for the depression of the semicircle. This element only
21 appears on the Pt electrode since Pt/RGO presents a capacitive behavior as
22 observed previously by CV.
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30 If the Nyquist plots for both samples are compared, the differences can be easily
31 observed. The charge transfer process (Rct) is responsible for the appearance of the
32 semicircle on Pt electrode characterization (Fig. 3-a). In the Pt/RGO sample, the
33 capacitive behavior predominates as can be seen from the almost vertical line obtained
34 in the Nyquist plot (Fig. 3-b). The inclination of the line indicates the deviation from the
35 ideal capacitive behavior, represented by the CPE in the equivalent circuit. If it were a
36 pure capacitor, a vertical line should be obtained. Table 1 shows the values of the
37 parameters obtained after fitting data with the corresponding equivalent circuits. The
38 most noteworthy fact is the increase in the pseudo-capacitance when Pt was coated with
39 RGO (an increase of around 56 times was obtained). This increase of capacitance is
40 attributed to the large surface area of RGO coating and the presence of the remaining
41 surface oxides [36]. The value of CPE-P was in both cases close to 1, this fact indicates
42 that the CPE behaves as a capacitor. The value of charge transfer resistance obtained for
43 Pt was $1.77 \cdot 10^{-5} \Omega$.
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3.3. Scanning electrochemical microscopy characterization

SECM was used to test the electroactivity of the Pt/RGO coatings with different redox mediators ($\text{Fe}(\text{CN})_6^{3-}$, $\text{Ru}(\text{NH}_3)_6^{3+}$ and Fe^{3+}). SECM technique was operated under feedback mode, where the reduction tip current of the redox mediator is registered as the microelectrode approaches the surface of the sample to study. In this study, the different redox mediators were reduced on the surface of the microelectrode, then the reduction current was measured. The potential of the microelectrode was fixed at -0.1 V, 0 V and -0.4 V for Fe^{3+} , $\text{Fe}(\text{CN})_6^{3-}$ and $\text{Ru}(\text{NH}_3)_6^{3+}$, respectively. At these potentials, the oxidized form of the redox mediator (Ox) is reduced (Red) on the microelectrode's surface at diffusion controlled rate (i_∞). The measured reduction diffusion current is defined as $i_\infty = 4 \cdot n \cdot F \cdot D \cdot C \cdot a$, where n is the number of electrons, F is the Faraday constant, D is diffusion coefficient, C is the bulk concentration of the redox mediator and a is the radius of the microelectrode tip.

In approach curves, the normalized reduction current registered at the microelectrode (I) is represented vs. the normalized distance (L). The normalized current is defined as follows: $I = i/i_\infty$ where i is the current measured at the microelectrode tip at a defined normalized distance and i_∞ is the diffusion current defined above. The normalized currents depend on RG ($RG=Rg/a$), where Rg is the radius of the insulating glass surrounding the Pt tip of radius a and the normalized distance L ; where $L=d/a$ (d is the microelectrode-substrate separation). The RG of the microelectrode used in this work was $RG \geq 20$.

Depending on the conductivity of the sample, as well as the distance between the microelectrode and sample, different situations can arise:

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- If the microelectrode is far enough from the surface of the sample, no interaction between the microelectrode and the sample is observed. In this case, the diffusion reduction current of the redox mediator is achieved (i_{∞}). By definition, the normalized current (I) is equal to 1.
 - When the microelectrode approaches the surface of the sample and there is an interaction between the sample and electrode, two situations can take place depending on the conductivity of the sample:
 - If the sample is insulating, when the microelectrode approaches the surface of the sample, there is a hindrance to the diffusion of reduced redox species (Red) due to the low distance between microelectrode and sample. The surface of the sample is not able to regenerate (oxidize) (Ox) the reduced form of the redox mediator (Red). As the distance between microelectrode and sample becomes smaller, the diminution of the current is greater. In this case the normalized current (I) is lower than 1, since values of reduction current are lower than that of the diffusion current (i_{∞}). This case is known as negative feedback.
 - Conversely, if the sample is conductive, when the microelectrode approaches a conductive substrate, there is an increase in the reduction current of the redox mediator registered. The surface of the sample is able to regenerate (oxidize) (Ox) the reduced form of the redox mediator (Red). As the microelectrode approaches the surface of the sample the effect is increased, since a greater flux of Ox species is present. In this case, the normalized current (I) is higher than 1, since values of reduction current are higher than that of the diffusion current (i_{∞}). This case is known as positive feedback.

Experimental approach curves were compared with a theoretical approach one for the positive feedback model, according to equation 1. According to Rajendran et al. [37], Pade's approximation gives a close and simple equation with less relative error for all distances and is valid for $RG > 10$. The approximate formula of the steady-state normalized current assuming positive feedback for finite conductive substrate together with finite insulating glass thickness is:

$$I_{r^c} = \left[\frac{1 + 1.5647/L + 1.316855/L^2 + 0.4919707/L^3}{1 + 1.1234/L + 0.626395/L^2} \right] \quad (1)$$

Fig. 4 shows the SECM characterization of the Pt/RGO electrodes with the different redox mediators. First of all, the microelectrode was positioned above the Pt/RGO wire. In order to achieve a proper location of the microelectrode, the reduction current of the redox mediator was measured with the microelectrode at a constant height (z) above the sample as the microelectrode moved laterally in the x direction. The maximum current was obtained in the center of the wire since the gap between microelectrode and sample was minimal. At this position, when the microelectrode approaches the Pt/RGO surface, a positive feedback situation was observed and an increase in the reduction current was observed. The exception to this behavior was the Fe^{3+} redox mediator, where slight positive feedback or even negative feedback was obtained (Figure not shown). These results are consistent with the fast and reversible behavior of $Ru(NH_3)_6^{3+}$ and $Fe(CN)_6^{3-}$ compared to Fe^{3+} (Fig. 2).

Fig. 4-a, b, c, shows the different approach curves obtained with the different redox mediators. In the case of $Ru(NH_3)_6^{3+}$ and $Fe(CN)_6^{3-}$ redox mediators, values of positive feedback around 1.7-1.8 were obtained. For the case of Fe^{3+} , slight values of positive feedback or even negative feedback were obtained. The values of positive feedback

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4 reported in bibliography have been around 1.7 ($L=0.5$) for graphene obtained by
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6 chemical vapor deposition and employing FeMeOH as mediator [15].
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10 11 12 3.4. Dyes characterization on Pt/RGO electrodes 13

14 15 3.4.1. Methylene Blue characterization 16

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18 Fig. 5-a shows the voltammetric characterization of a Pt/RGO electrode in $5 \cdot 10^{-3}$ M
19 Methylene Blue / 0.5 M H_2SO_4 solution. The apparition of a redox pair with the
20 cathodic peak at +0.23 V and the anodic one at +0.26 V can be observed. This redox
21 pair has been attributed to the reduction of methylene blue (MB) to leucomethylene blue
22 (LMB) [38]. Different scan rates were used to characterize the electrochemical behavior
23 of the dye on the Pt/RGO electrode and it was observed that this process was diffusion
24 controlled (figure not shown). The intensity of the anodic and cathodic peaks after
25 subtracting the background current arising from RGO deposit was not proportional to
26 the scan rate. The intensity of both peaks was proportional to the square root of the scan
27 rate, indicating a diffusion controlled process that takes place on the RGO/electrolyte
28 interface. The representation of $\log(I)$ vs. the scan rate also gave a slope near to 0.5 for
29 both peaks, confirming a diffusion controlled process. Hence, this redox peak is
30 attributed to the redox processes of dye in solution.
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49 There was little variation of the redox pair due to the dye in solution with the number of
50 scans. However, as the scan number increased the appearance of a new redox pair at
51 around +0.15 V could be seen, and the intensity of this pair increased with the scan
52 number as can be observed in Fig. 5-a. The appearance of this redox pair at lower
53 potentials was attributed to the adsorption of the dye species [38]. After 100 scans, the
54 Pt/RGO-MB electrode was taken out from solution and washed with ultrapure water
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4 several times in order to remove the dye not adsorbed. Afterwards, the electrode was
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6 characterized in 0.5 M H₂SO₄ solution to evaluate the adsorbed species. Fig. 5-b shows
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8 the characterization of Pt/RGO electrode prior and after MB adsorption
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10 (electrochemical adsorption). The apparition of a redox pair with the anodic peak at
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12 +0.16 V and the cathodic one at +0.14 V could be observed. The peak to peak potential
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14 difference that was close to 0 mV, the current (I) of oxidation and reduction peaks and
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16 their electrical charge, which were almost equal, indicated that the process was
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18 adsorption controlled.
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23 Fig. 5-c shows the voltammetric characterization of Pt/RGO-MB electrode obtained
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25 after electrochemical adsorption in 0.5 M H₂SO₄ solution using different scan rates. No
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27 significant variation of the peak potentials was observed with the scan rate, indicating a
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29 surface-confined process with fast electron transfer [23]. In Fig. 5-d, the intensity of the
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31 anodic and cathodic peaks is represented vs. the scan rate used. The RGO contribution
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33 to the intensity of both peaks was subtracted. The representation of I vs. scan rate was
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35 linear, indicating that in this case, the process was adsorption controlled. On the other
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37 hand, the representation of I vs. $v^{1/2}$ was not linear, excluding a diffusion controlled
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39 process (figure not shown). The representation of log(I) vs. log(v) gave also a linear
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41 dependence with slope close to 1, confirming an adsorption controlled process.
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47 The number of electrons involved in the process was calculated by means of the
48
49 following equation [39]:
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$$51$$
$$52 \quad i_p = \frac{n \cdot F \cdot Q \cdot v}{4 \cdot R \cdot T} \rightarrow \frac{i_p}{v} = \frac{n \cdot F \cdot Q}{4 \cdot R \cdot T} \rightarrow n = \frac{\text{slope} \cdot 4 \cdot R \cdot T}{F \cdot Q} \quad (1)$$
$$53$$
$$54$$
$$55$$

56 Where:

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59 i_p , is the intensity of the anodic or cathodic oxidation peaks (A).
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4 n, is the number of electrons involved in the reaction.
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6
7 Slope, is the slope obtained in the representation of i_p vs. v .
8

9
10 v , is the scan rate ($V s^{-1}$).
11

12
13 F, is the Faraday constant ($96485 C mol^{-1}$).
14

15
16 T, is the temperature (298 K).
17

18
19 Q, is the charge associated with the anodic or cathodic peak (C).
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22 R, is the gas constant ($8.31 V C K^{-1} mol^{-1}$).
23

24
25 The number of electrons involved in the reaction was calculated by means of Eq. 1,
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27 giving a value of 1.17 and 0.92 electrons for anodic and cathodic processes,
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29 respectively. Hence the number of electrons transferred is 1 and the deviations could be
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31 due to experimental errors.
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35 To characterize the stability of the Pt/RGO-MB electrode, it was cycled for 100 scans in
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37 0.5 M H_2SO_4 solution. A gradual reduction of the peaks' intensity with the scan number
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39 until it stabilized. The loss of intensity could be attributed to the loss of part of the dye
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41 adsorbed on RGO's surface. Fig. 6 shows the representation of I/I_0 ratio for anodic and
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43 cathodic peaks, as can be seen there is an initial decrease and it stabilizes around a value
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45 higher than 0.6 for 100 scans.
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49 Another experiment was performed to characterize the spontaneous adsorption of MB
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51 on the Pt/RGO electrode. For this reason, the Pt/RGO electrode was placed in contact
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53 with the dye solution, with the same electrochemical configuration previously used.
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55 However, in this case no potential was imposed. Starting from 0 V, the potential was
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57 allowed to reach its ocp and was monitored vs. time. The time used to perform the
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4 adsorption was the same time used to perform the 100 CV scans at 50 mV s^{-1} (1 h). The
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6 potential tended toward $+0.38 \text{ V}$ after an hour of measurement (figure not shown). After
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8 this adsorption's phase, the Pt/RGO-MB electrode was washed several times with water
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10 and characterized in $0.5 \text{ M H}_2\text{SO}_4$ solution by CV (Fig. 5-b, blue line). The same
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12 oxidation and reduction peaks observed previously with electrochemical adsorption due
13
14 to MB adsorption appeared in the voltammogram. Both peaks were also adsorption
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16 controlled since the intensity of the peak was proportional to the scan rate used. Fig. 5-b
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18 shows the comparison of the voltammograms of a Pt/RGO-RB electrode obtained
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20 electrochemically and another obtained at ocp. As can be seen, the values of current
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22 obtained with the electrochemically obtained Pt/RGO-MB electrode doubled the values
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24 obtained with the Pt/RGO-RB electrode synthesized at ocp. This indicates that the
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26 electrochemical adsorption is more efficient than the natural adsorption. The
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28 electrochemical adsorption allows the assembly of more MB molecules on the RGO
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30 structure. The charge (C) of the anodic and cathodic peaks was also approximately 3
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32 times higher in the case of electrochemical adsorption. For example, the electrical
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34 charge for the reduction peak was $455 \mu\text{C cm}^{-2}$ for the Pt/RGO-MB electrode obtained
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36 electrochemically vs. $149 \mu\text{C cm}^{-2}$ for the Pt/RGO-MB electrode obtained at ocp.
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47 3.4.2. Procion Orange MX-2R characterization

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50 Fig. 7-a shows the characterization of the PMX2R adsorption on Pt/RGO electrodes by
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52 CV. The adsorption was performed in a $5 \cdot 10^{-3} \text{ M PMX2R} / 0.5 \text{ M H}_2\text{SO}_4$ solution for
53
54 100 scans. The 1st, 10th, 30th, 50th and 100th voltammograms have been represented in
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56 the same figure to observe the evolution. From the 1st voltammogram, an oxidation peak
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58 appeared at $+0.44 \text{ V}$ and a reduction one appeared at $+0.36 \text{ V}$ after the 2nd scan. This
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4 peak is attributed to the oxidation and reduction of dye in solution, respectively. As the
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6 scan number performed increased, a new oxidation peak appeared around +0.37 V (in
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8 addition to the one observed at +0.44 V), both peaks were superimposed and can be
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10 observed in the 100th scan. The appearance of the new peak can be ascribed to the
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12 adsorbed dye, in the same way that happened for MB. The reduction peak at +0.36 V
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14 also increased its intensity with the number of scans, indicating the adsorption of the
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16 dye. After the 100th scan, the electrode was taken out from solution and rinsed several
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18 times with ultrapure water. Thereafter, the electrode was characterized in 0.5 M H₂SO₄
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20 to observe the adsorbed products (Fig. 7-b). The Pt/RGO voltammetric response has
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22 also been represented for comparison. As can be seen, a redox pair appeared at around
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24 +0.37 V. As in the Pt/RGO-MB electrode, the peak to peak potential difference was
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26 nearly 0 mV, the current (I) of oxidation and reduction peaks and their electrical charge
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28 was almost equal, pointing out an adsorption controlled process.
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34 Different scan rates were used to characterize the adsorption product on the surface of
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36 the Pt/RGO electrode (5, 10, 25, 50, 100, 150, 200, 250, 300, 350, 400, 450 and 500 mV
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38 s⁻¹) (Fig. 7-c). No variations were observed in the peak potentials when varying the scan
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40 rate, indicating a surface-confined process with fast electron transfer as took place with
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42 MB. The peak intensity (I) of oxidation and reduction processes was represented vs. the
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44 scan rate used (Fig. 7-d). To calculate the intensity of oxidation and reduction peaks, the
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46 background current arising from RGO coating contribution was subtracted. As the peak
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48 intensities were proportional to the scan rate used (v), this indicated that the process was
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50 adsorption controlled. The representation of I vs. v^{1/2} was not linear meaning there was
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52 no diffusion controlled process (Figure not shown). The log (I) was represented vs. the
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54 log (v) for both processes and both slopes tended to 1, confirming an adsorption
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4 controlled process (Figure not shown). The number of electrons involved in the redox
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6 process was also 1.
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9 The stability of the Pt/RGO-PMX2R electrode was tested by cyclic voltammetry for
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11 100 scans in 0.5 M H₂SO₄ solution (Fig. 8). As can be seen, the intensity of oxidation
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13 and reduction peaks was progressively reduced. However, the diminution of both
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15 adsorption peaks on the Pt/RGO-PMX2R electrode was lower than in the case of the
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17 Pt/RGO-MB one. The current ratios (I/I_0) for oxidation and reduction peaks after 100
18
19 scans was 0.75 and 0.88, respectively (Fig. 8). The adsorption of PMX2R is more stable
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21 than the MB one. The adsorption of dyes on graphene substrate is dominated by π - π
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23 stacking and hydrophobic interactions [23]. The increased stability of adsorbed PMX2R
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25 could be due to the presence of chlorotriazine groups in the dye structure that could
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27 serve as fixation points with the remaining functional groups of RGO.
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33 Another experiment was performed to observe the spontaneous adsorption of the
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35 PMX2R dye. For this reason, the Pt/RGO was placed in contact with the dye solution as
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37 it was performed for the MB ocp adsorption. The potential tended to +0.37 V (Figure
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39 not shown). After this adsorption phase, the Pt/RGO-PMX2R electrode was washed
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41 several times with water and characterized in 0.5 M H₂SO₄ solution (Fig. 7-b). The
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43 same oxidation and reduction peaks were obtained; however, in this case, the intensity
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45 of the dye's peaks in relation to the RGO voltammetric background was lower. The
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47 process was also adsorption controlled since the peak intensity was proportional to the
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49 scan rate and not to the square root of the scan rate (Figure not shown). Fig. 7-b
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51 compares the voltammograms after OCP and electrochemical adsorption. As can be
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53 seen, the voltammetric adsorption produce an increase in the anodic and cathodic
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55 current peaks when compared with OCP adsorption. The electrochemical adsorption is
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57 more efficient in the adsorption of PMX2R. The charge (C) of the anodic and cathodic
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4 peaks was also approximately 6 times higher in the case of electrochemical adsorption.
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6 For example, the electrical charge for the reduction peak was $162 \mu\text{C cm}^{-2}$ for the
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8 Pt/RGO-PMX2R electrode obtained electrochemically vs. $26 \mu\text{C cm}^{-2}$ for the Pt/RGO-
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10 PMX2R electrode obtained at ocp.
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17 3.4.3. Amaranth characterization

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20 Fig. 9-a shows the voltammetric characterization of a Pt/RGO electrode in $5 \cdot 10^{-3} \text{ M}$
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22 Amaranth / $0.5 \text{ M H}_2\text{SO}_4$ solution. In the first scan, two peaks appeared, one anodic
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24 peak at $+0.44 \text{ V}$ and one cathodic peak at -0.05 V . The anodic peak suffered a reduction
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26 in intensity with the increasing number of scans, however the potential at which this
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28 took place was not displaced. On the other hand, the cathodic peak suffered a reduction
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30 in intensity and the potential at which the process took place was also displaced towards
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32 lower potentials. After the 100 adsorption scans, the electrode was washed several times
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34 with ultrapure water and characterized in $0.5 \text{ M H}_2\text{SO}_4$. Fig. 9-b shows the comparison
35
36 of the voltammograms before and after amaranth adsorption. After dye adsorption some
37
38 redox processes appear between 0 and $+0.4 \text{ V}$. However they are not as defined as they
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40 were in the case of MB or PMX2R.
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46 The usefulness of CV to monitor the adsorption of dyes on Pt/RGO electrodes was
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48 demonstrated. The quantity of dye adsorbed is substantially increased when compared
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50 with ocp adsorption. Reduced graphene oxide (RGO) structure presents zones where the
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52 sp^2 structure of pristine graphene has been restored but also presents other zones where
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54 functional groups are still present [21]. The main mechanisms of adsorption of the dyes
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56 on RGO are π - π stacking and hydrophobic interactions on the zones where the sp^2
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58 structure has been restored and charge transfer on the zones where the functional groups
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4 are still present. Hence, the mechanism of adsorption will depend on the structure of the
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6 dye [24]. Graphene oxide (GO) has been shown to be a good adsorbent for cationic dyes
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8 due to its negatively charged surface which increase electrostatic interaction between
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10 the cationic dye and GO [24]. For the same reason GO is not good for the adsorption of
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12 anionic dyes since both of them present negative charges and electrostatic repulsion
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14 takes place. Reduced graphene oxide (RGO) presents affinity for both of them, being
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16 higher in the case of anionic dyes (95% for anionic dyes and 50% for cationic dyes)
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18 [24]. The electrochemically-induced adsorption enhances the adsorption of the dye due
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20 to the polarization of the RGO surface and the creation of electrostatic interaction
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22 between the dye and the RGO surface. Small influence should be expected for dyes with
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24 low polarity. The CV induced adsorption could also be used to increase the adsorption
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26 of other products, which adsorption on graphene derivatives has been reported. For
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28 instance, the enzyme adsorption for the production of biosensors [25,40-44] or
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30 enzymatic biofuel cells [44]. This procedure would increase the sensibility of the
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32 biosensors.
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45 **4. Conclusions**

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48 Reduced graphene oxide (RGO) coated Pt electrodes were obtained by electrochemical
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50 reduction. The Pt/RGO electrodes were characterized by cyclic voltammetry (CV) and
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52 electrochemical impedance spectroscopy (EIS), showing the appearance of the
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54 capacitive behaviour of RGO. The electrochemically obtained RGO coated electrodes
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56 were characterized by scanning electrochemical microscopy (SECM) for the first time.
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59 The coatings obtained were homogeneous and with good electroactivity. The influence
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4 of the redox mediator used in the response obtained was clearly shown. The peak to
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6 peak potential separation obtained from the voltammograms of the different redox
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8 mediators on Pt/RGO electrodes was 101, 121 and 538 mV for $\text{Ru}(\text{NH}_3)_6^{3+}$, $\text{Fe}(\text{CN})_6^{3-}$,
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10 and Fe^{3+} , respectively. With the first two redox mediators, the electronic transfer was
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12 reversible and with the Fe^{3+} one it was quite irreversible. The Fe^{3+} redox mediator is
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14 oxide sensitive and the high peak to peak potential separation indicates a low quantity
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16 of oxidized groups on the surface of RGO (indicates an effective reduction of GO) as
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18 EDX has also shown. The approach curves obtained by SECM confirmed this tendency,
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20 showing similar values of positive feedback for $\text{Ru}(\text{NH}_3)_6^{3+}$ and $\text{Fe}(\text{CN})_6^{3-}$, and low
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22 values of positive feedback or even negative feedback for the Fe^{3+} redox mediator.
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28 The electrochemical adsorption of different dyes (Methylene Blue (MB), Procion
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30 Orange MX-2R (PMX2R) and Amaranth (AM)) was accomplished by CV on Pt/RGO
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32 electrodes. It has been shown that this technique could be used as a technique to
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34 monitor the adsorption of the dyes. After MB and PMX2R adsorption, the voltammetric
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36 characterization in 0.5 M H_2SO_4 solution showed the appearance of a redox pair at
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38 +0.15 V and +0.36 V, respectively. The processes were adsorption-controlled. The
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40 electrochemical adsorption is more efficient than ocp adsorption which opens the
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42 possibility of employing this technique to enhance the adsorption of other substances
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44 such as enzymes for the production of biosensors.
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23
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Figure captions

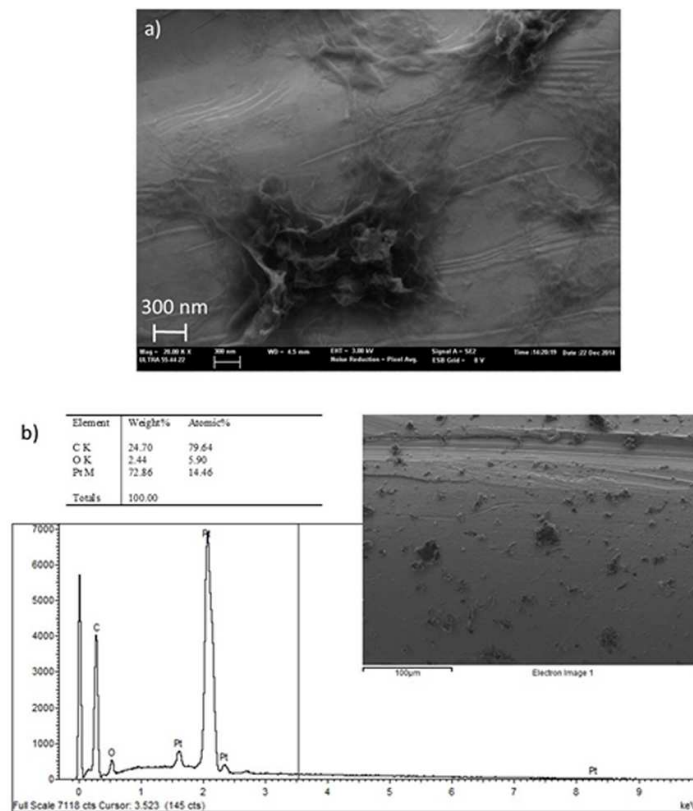


Fig. 1. a) FESEM micrograph of Pt/RGO electrode (x20000). b) EDX and FESEM micrograph of Pt/RGO electrode.

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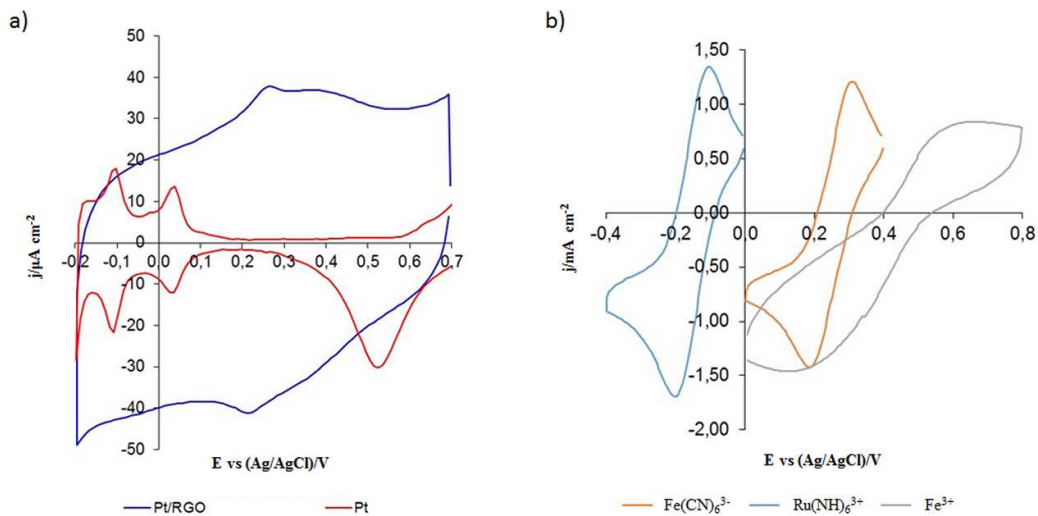


Fig. 2. a) Cyclic voltammograms of Pt and Pt/RGO electrode in $0.5 \text{ M H}_2\text{SO}_4$, scan rate 50 mV s^{-1} . b) Cyclic voltammograms of Pt/RGO electrode in $0.01 \text{ M Ru(NH}_3)_6^{3+} / 0.1 \text{ M KCl}$, $0.01 \text{ M Fe(CN)}_6^{3-} / 0.1 \text{ M KCl}$ and $0.02 \text{ M Fe}^{3+} / 0.5 \text{ M H}_2\text{SO}_4$, scan rate 50 mV s^{-1} .

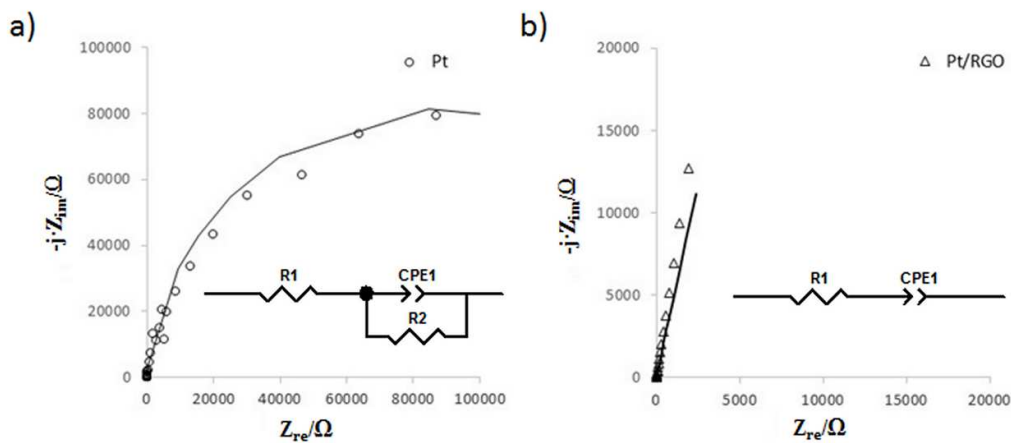


Fig. 3. Nyquist plots for EIS characterization of Pt (a) and Pt/RGO (b) electrodes in $0.5 \text{ M H}_2\text{SO}_4$, frequency range from 10^5 to 10^{-2} Hz .

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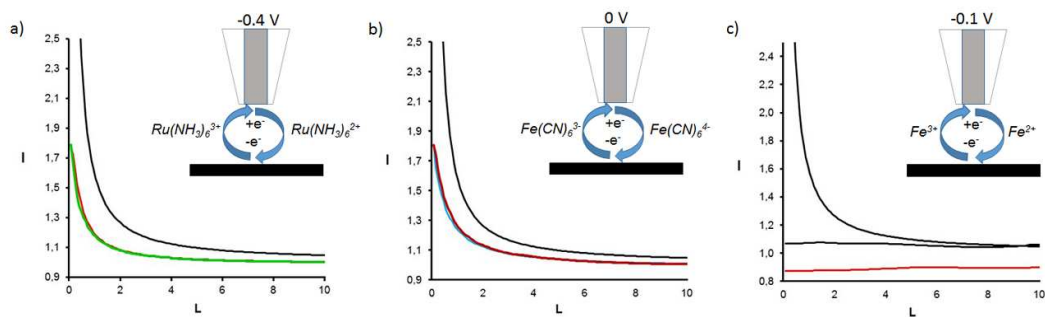


Fig. 4. 2D SECM representations for Pt/RGO wires obtained by vertical displacement of the microelectrode for the different redox systems 0.01 M Ru(NH₃)₆³⁺ / 0.1 M KCl (a), 0.01 M Fe(CN)₆³⁻ / 0.1 M KCl (b) and 0.02 M Fe³⁺ / 0.5 M H₂SO₄ (c). Theoretical positive feedback model has been included as a black continuous line. Data obtained with a 25 μm diameter Pt tip, approach rate 10 μm s⁻¹.

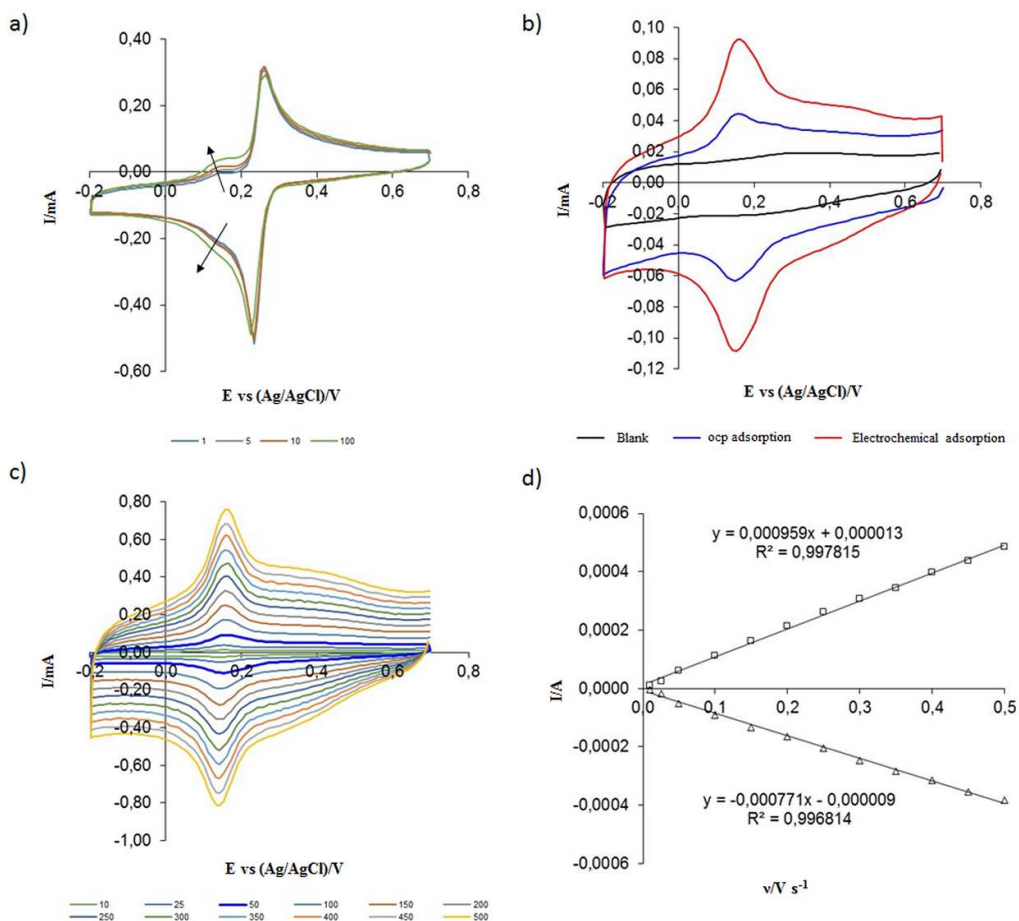


Fig. 5. a) Methylene Blue (MB) adsorption by CV on Pt/RGO electrode performed in $5 \cdot 10^{-3}$ M MB / 0.5 M H_2SO_4 solution during 100 scans (1st, 5th, 10th and 100th scans are represented). b) CV characterization of Pt/RGO electrode in 0.5 M H_2SO_4 prior and after dye adsorption performed electrochemically and at ocp. Characterization and adsorption were performed with a scan rate of 50 $mV s^{-1}$. c) CV characterization of Pt/RGO-MB electrode (electrochemical adsorption) in 0.5 M H_2SO_4 solution with different scan rates: 10, 25, 50, 100, 150, 200, 250, 300, 350, 400, 450 and 500 $mV s^{-1}$). d) Intensity (I) vs. scan rate (v) plot.

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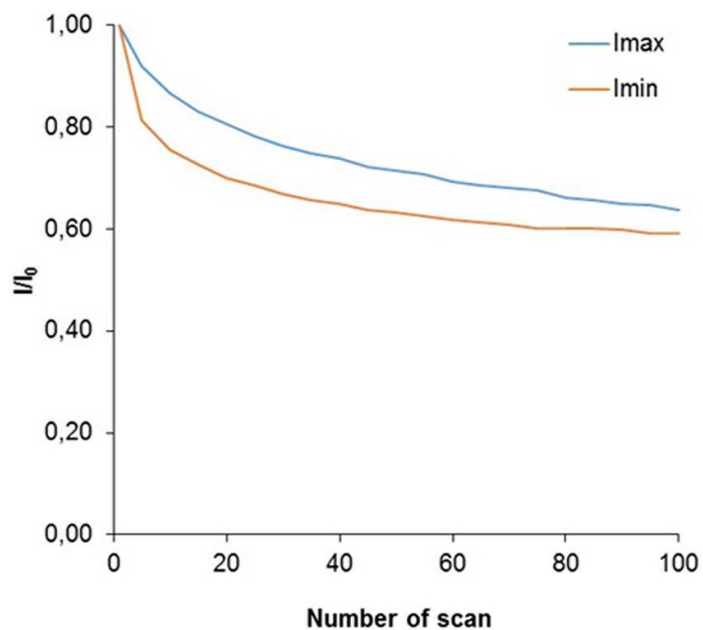


Fig. 6. I/I_0 for anodic and cathodic peaks vs. the number of scan for Pt/RGO-MB electrode in 0.5 M H_2SO_4 solution during 100 scans.

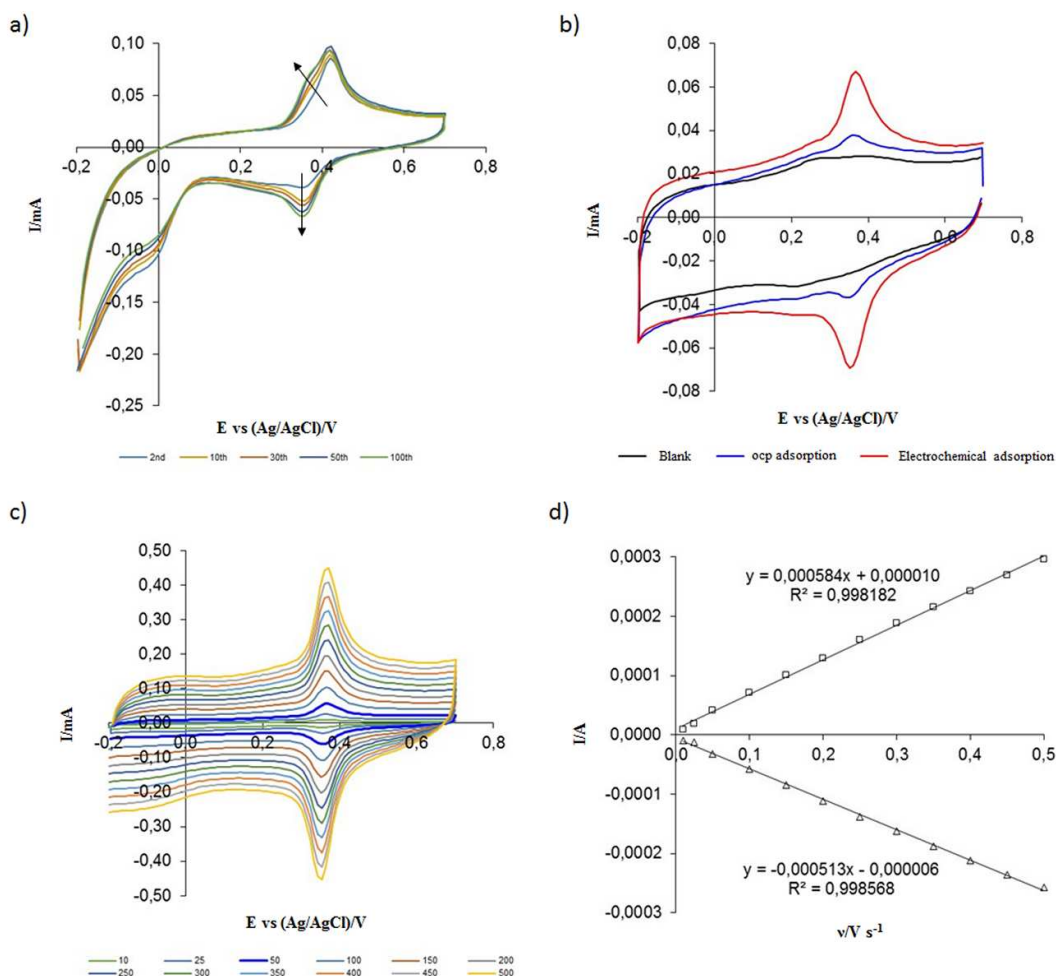


Fig. 7. a) Procion MX-2R (PMX2R) adsorption by CV on Pt/RGO electrode performed in $5 \cdot 10^{-3}$ M PMX2R / 0.5 M H_2SO_4 solution during 100 scans (2nd, 10th, 30th, 50th and 100th scans are represented). b) CV characterization of Pt/RGO electrode in 0.5 M H_2SO_4 prior and after dye adsorption performed electrochemically and at ocp. Characterization and adsorption were performed with a scan rate of $50 mV s^{-1}$. c) CV characterization of Pt/RGO-PMX2R electrode (electrochemical adsorption) in 0.5 M H_2SO_4 solution with different scan rates: 10, 25, 50, 100, 150, 200, 250, 300, 350, 400, 450 and $500 mV s^{-1}$. d) Intensity (I) vs. scan rate (v) plot.

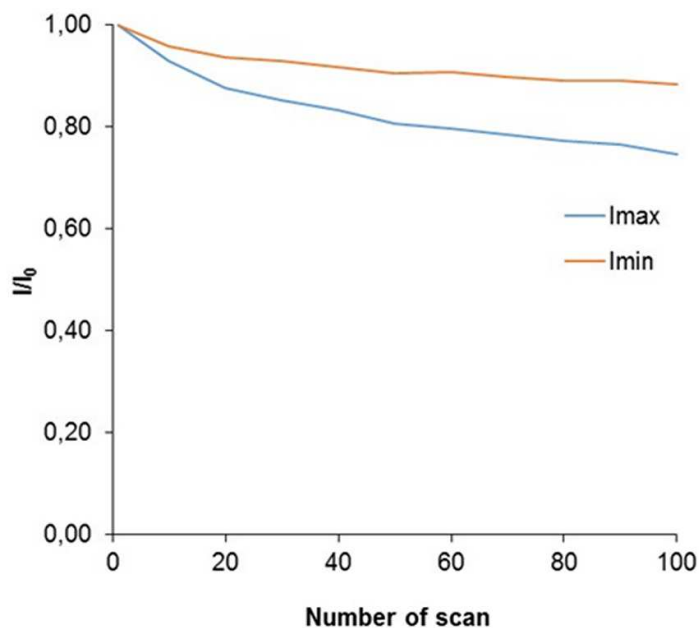


Fig. 8. I/I_0 for anodic and cathodic peaks vs. the number of scan for Pt/RGO-PMX2R electrode in 0.5 M H_2SO_4 solution during 100 scans.

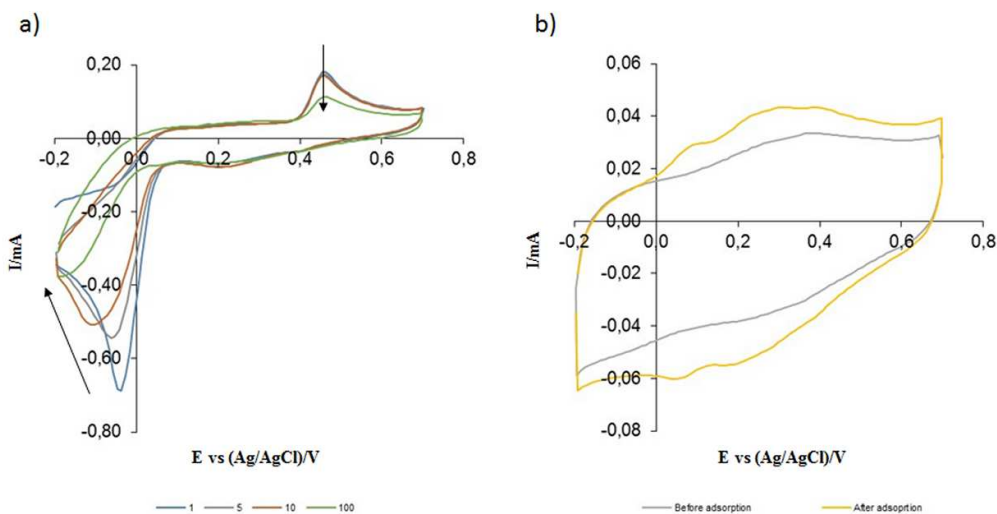


Fig. 9. a) Cyclic voltammograms of characterization of Amaranth adsorption on Pt/RGO electrode in $5 \cdot 10^{-3}$ M Amaranth / 0.5 M H_2SO_4 solution during 100 scans (1st,

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4 5th, 10th and 100th scans are represented). b) Cyclic voltammograms of Pt/RGO
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6 electrode prior and after dye adsorption. Scan rate used, 50 mV s⁻¹.
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21 Table 1. Results of the fitting of impedance data of Pt and Pt/RGO electrodes in 0.5 M
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23 H₂SO₄. Data adjusted with the equivalent circuits shown in Fig. 3.
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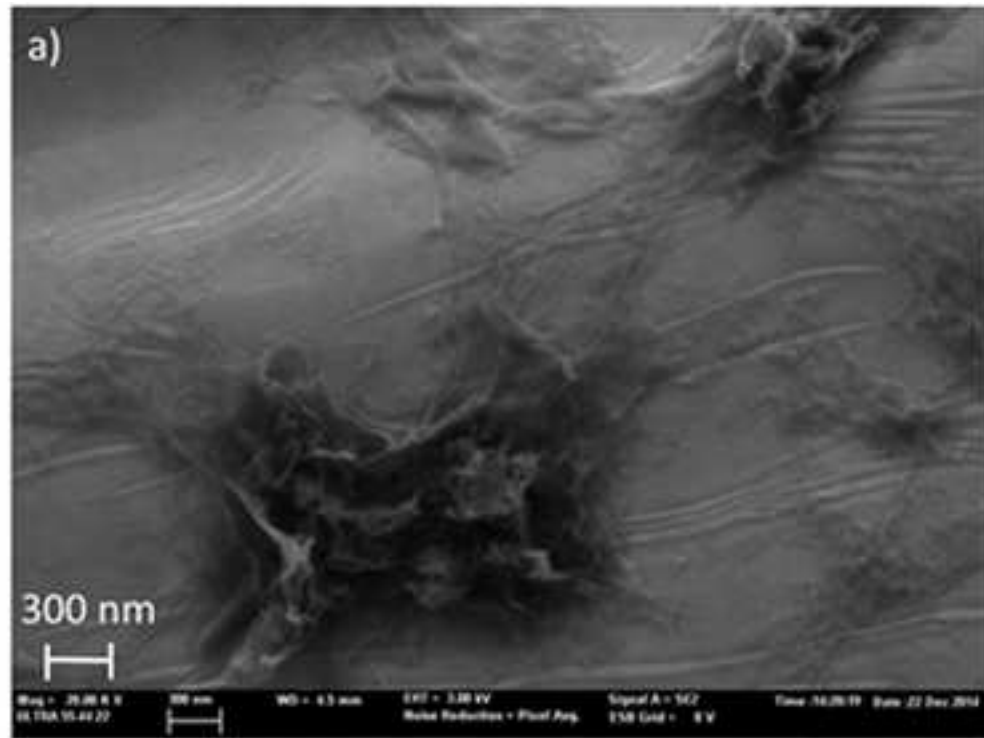
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Electrode	Chi-Sqr	Rs (Ω)	$CPE-T \left(F^{CPE-P} \cdot \Omega^{(1-CPE-P)} \right)$	CPE-P	Rct (Ω)
Pt	0,09	1,59	$1,72 \cdot 10^{-5}$	0,95	$1,77 \cdot 10^5$
Pt/RGO	0,02	2,03	$9,67 \cdot 10^{-4}$	0,87	-

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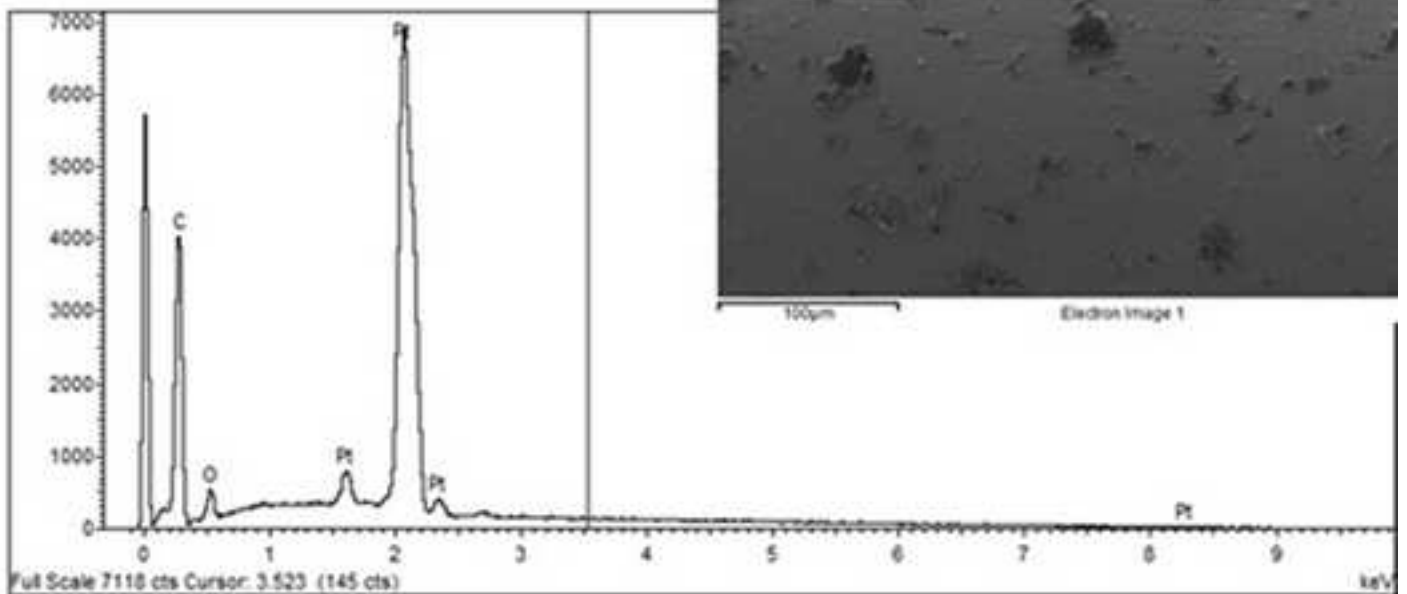
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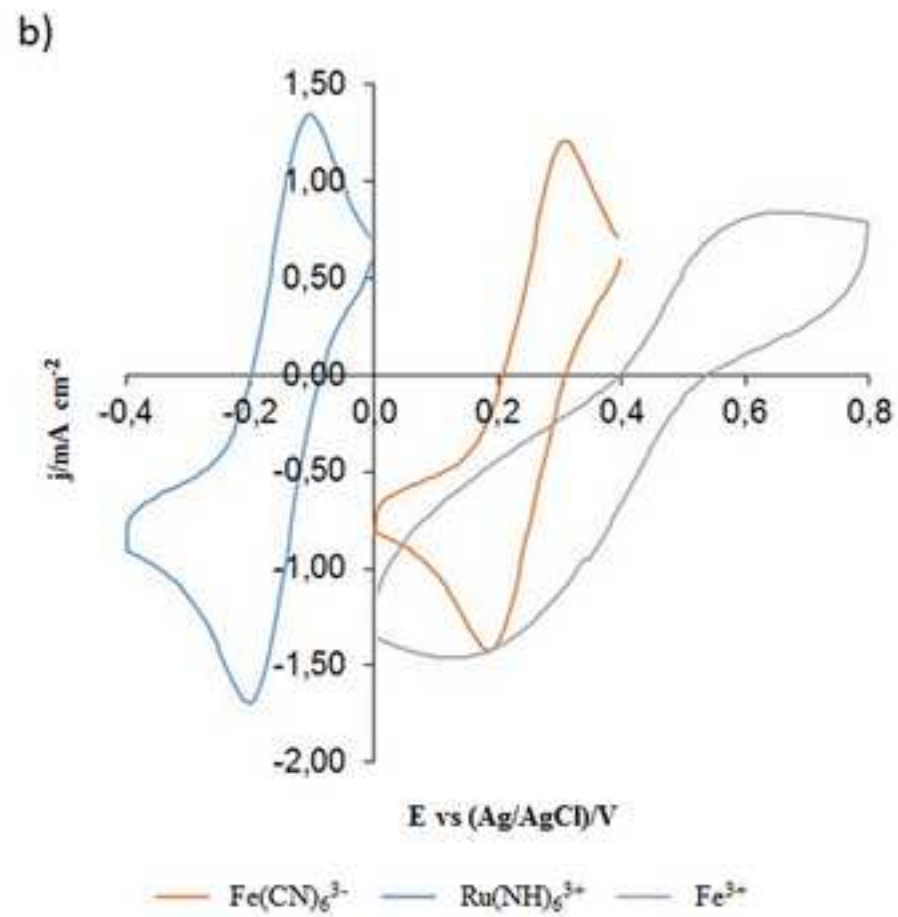
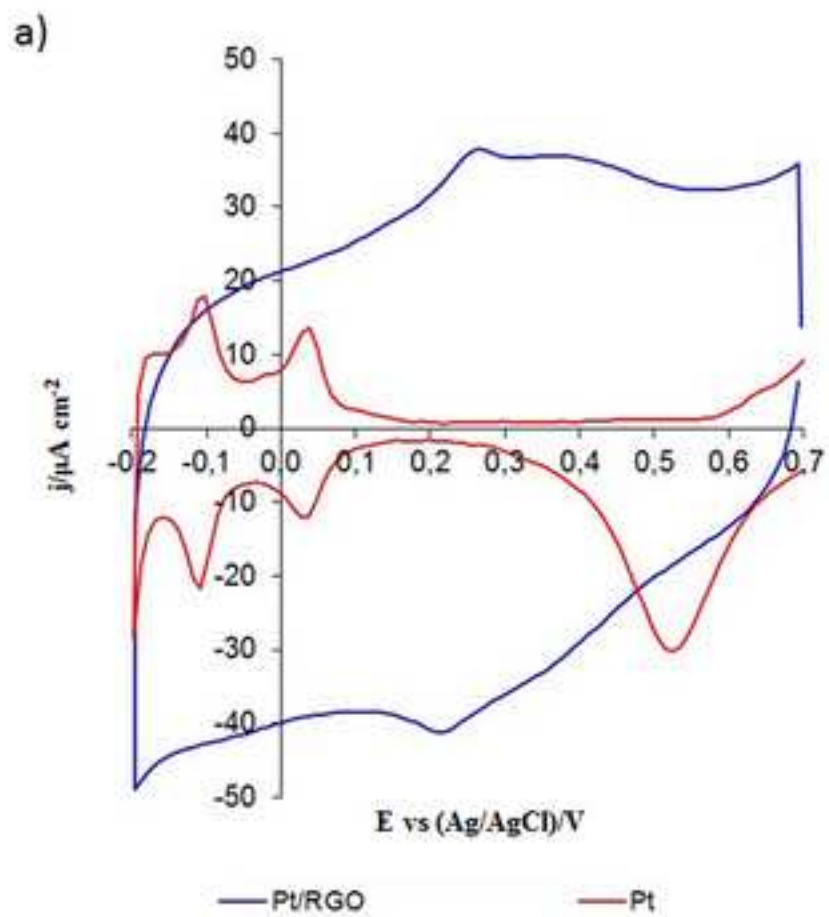


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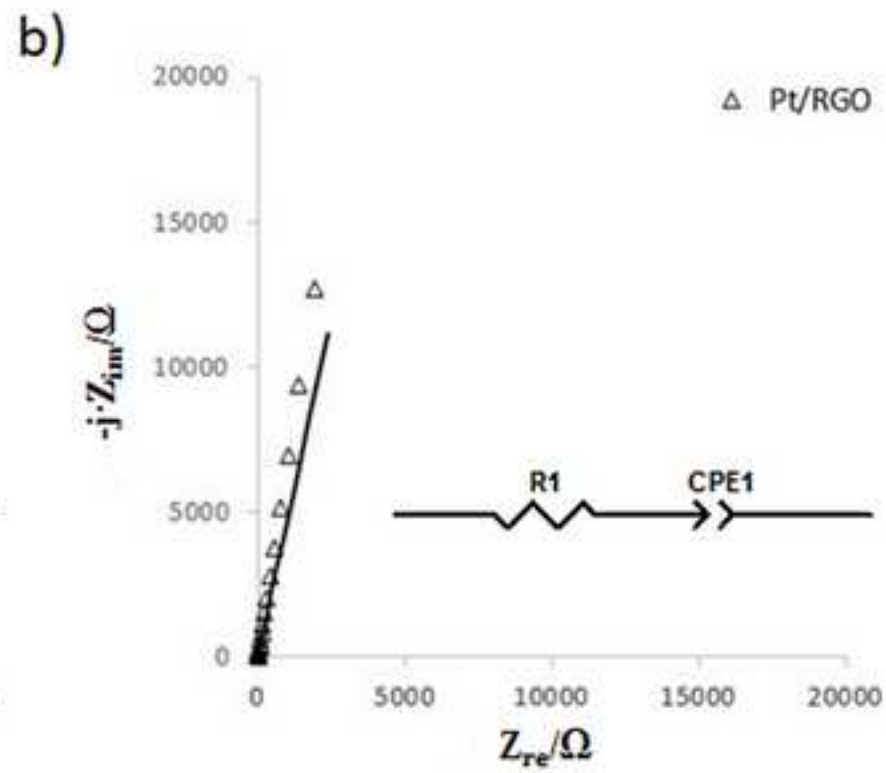
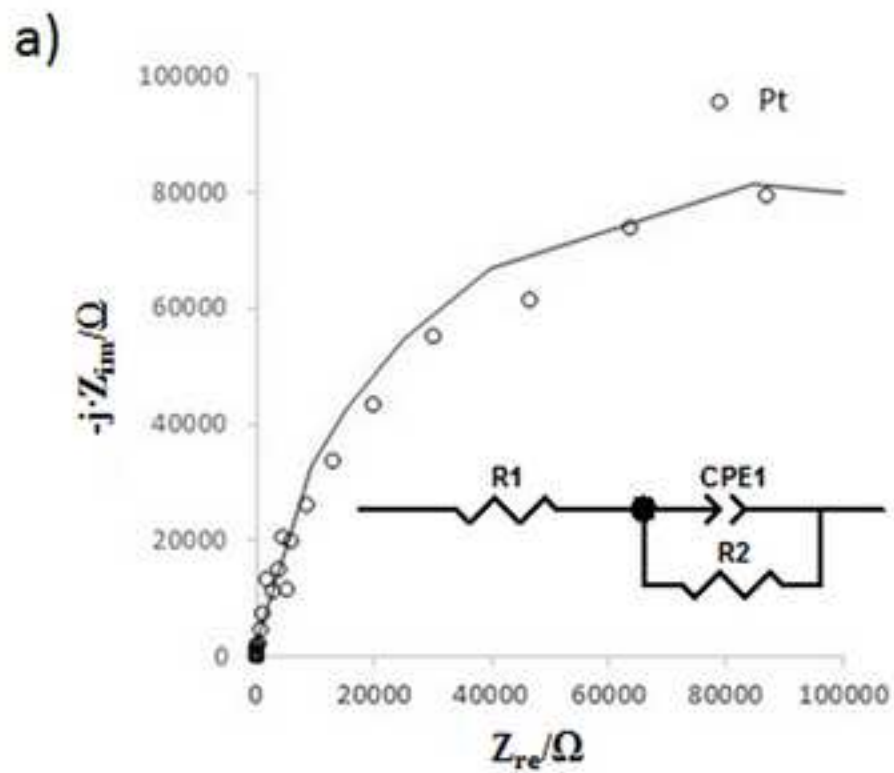
Element	Weight%	Atomic%
C K	24.70	79.64
O K	2.44	5.90
Pt M	72.86	14.46
Totals	100.00	



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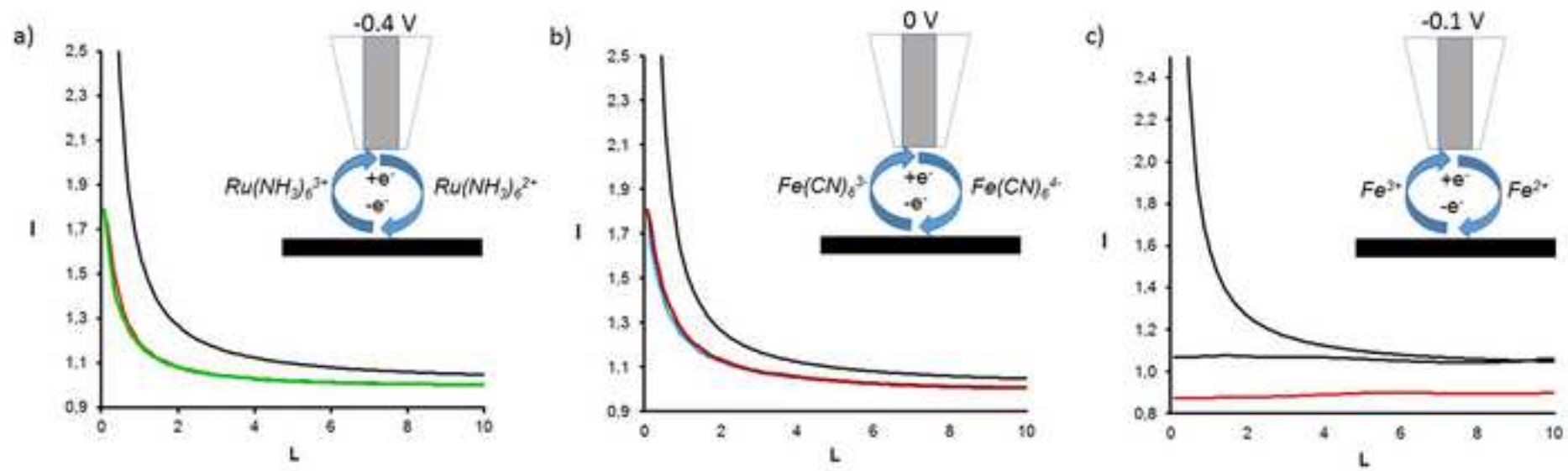


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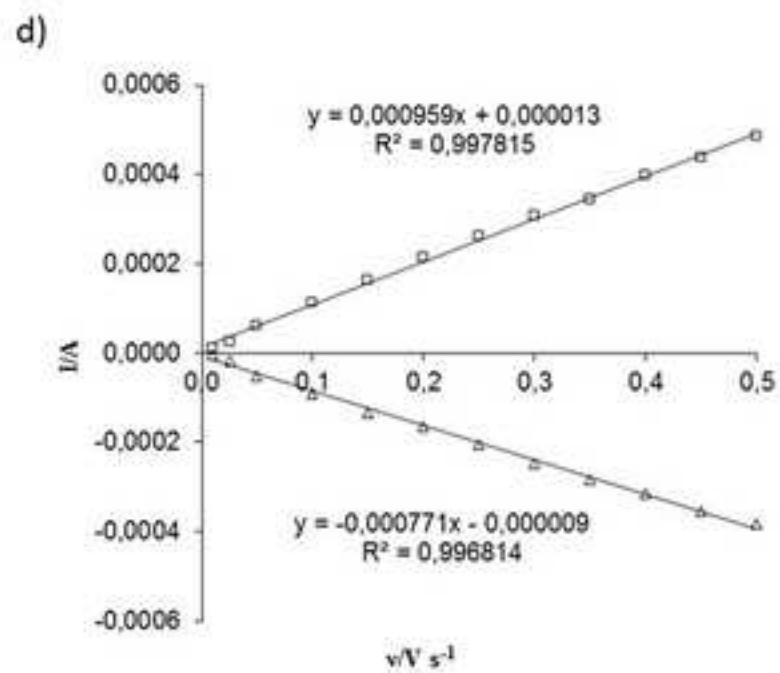
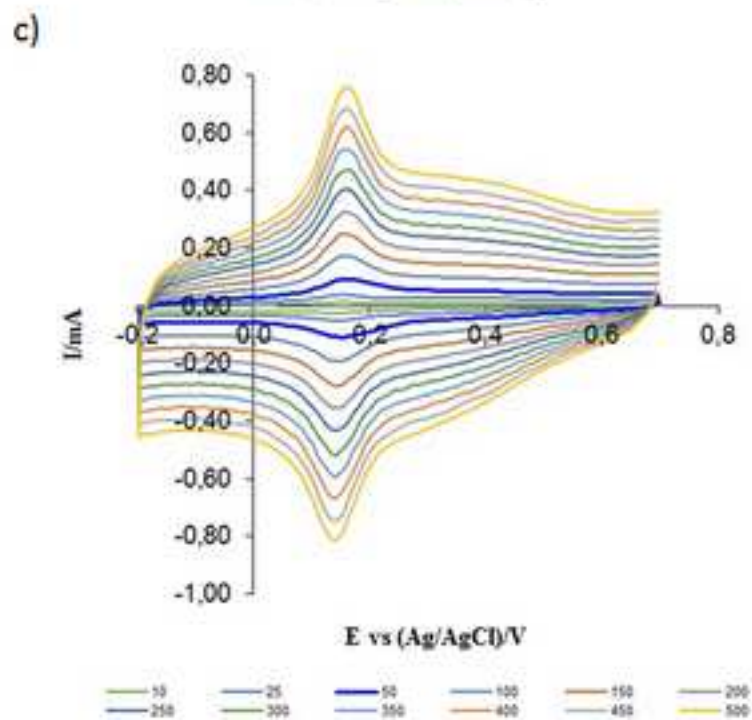
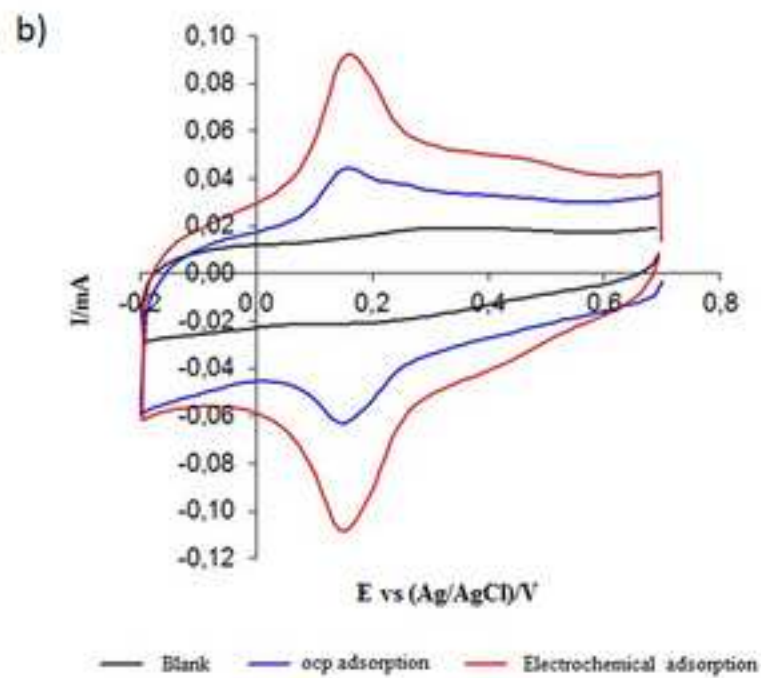
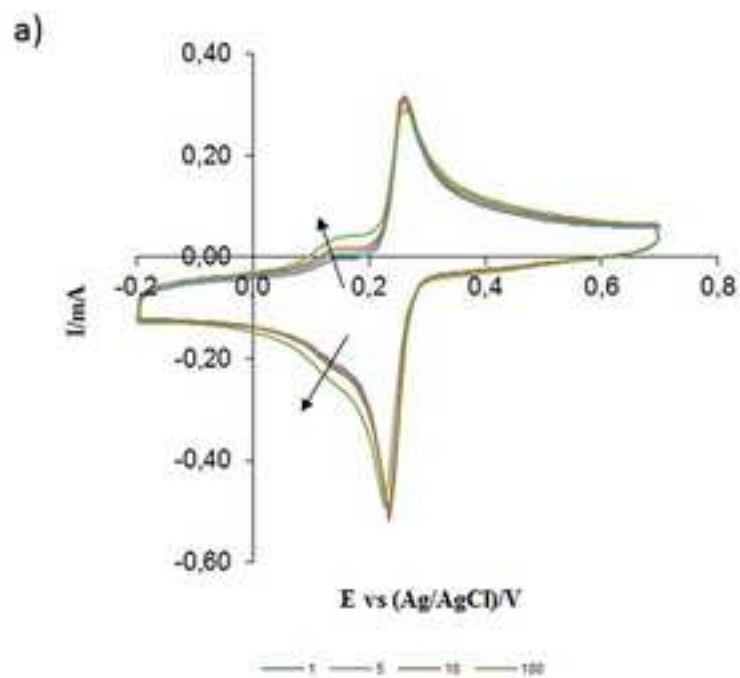
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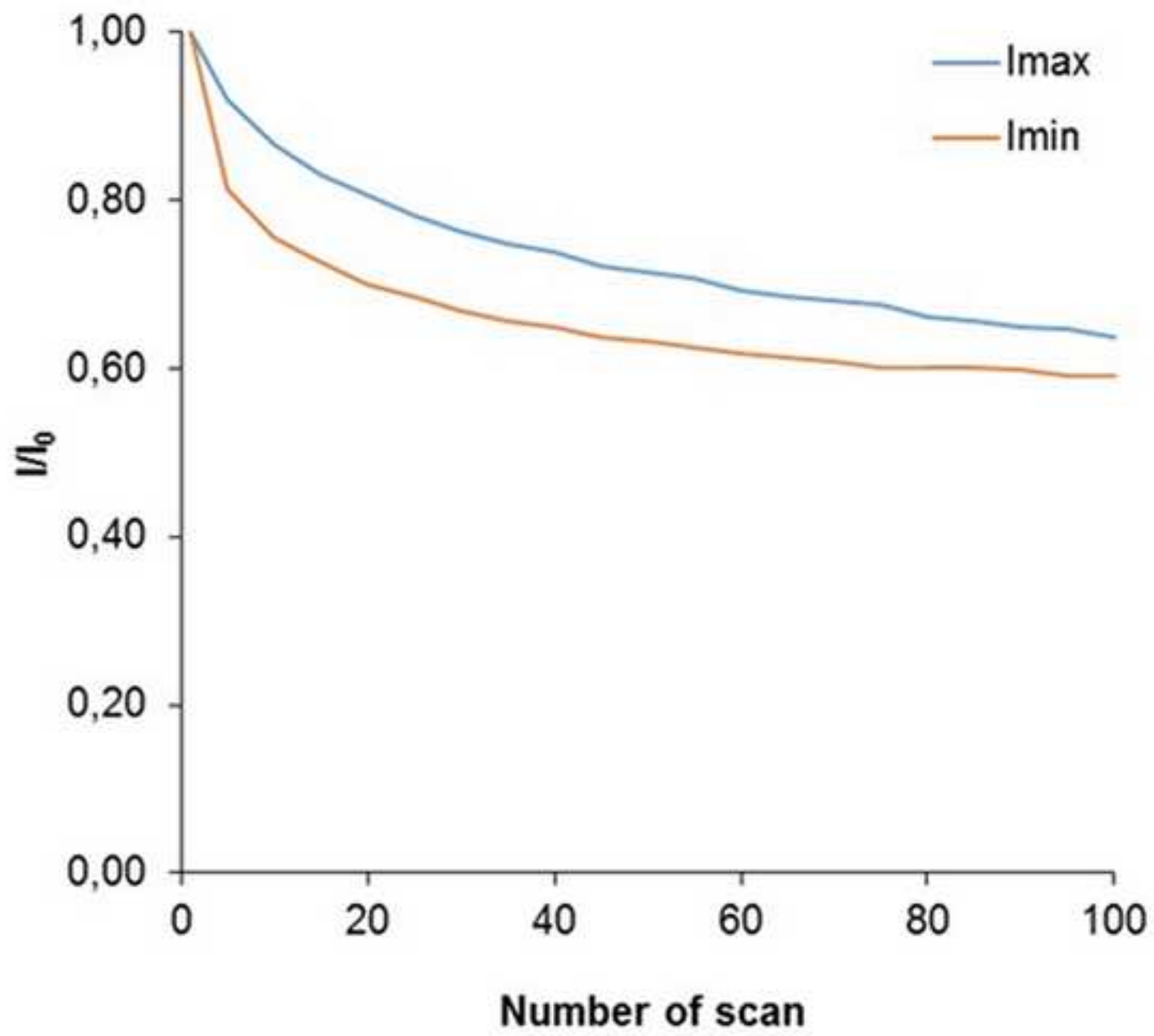


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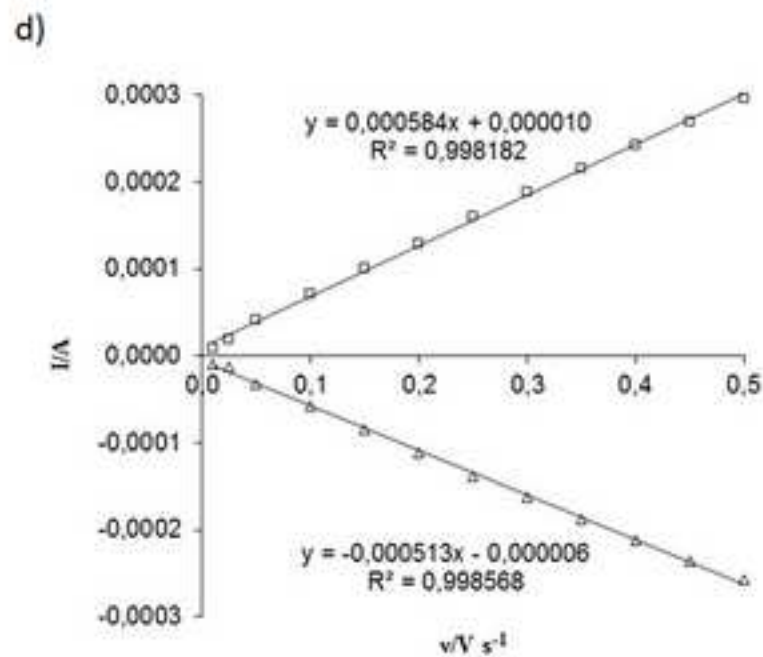
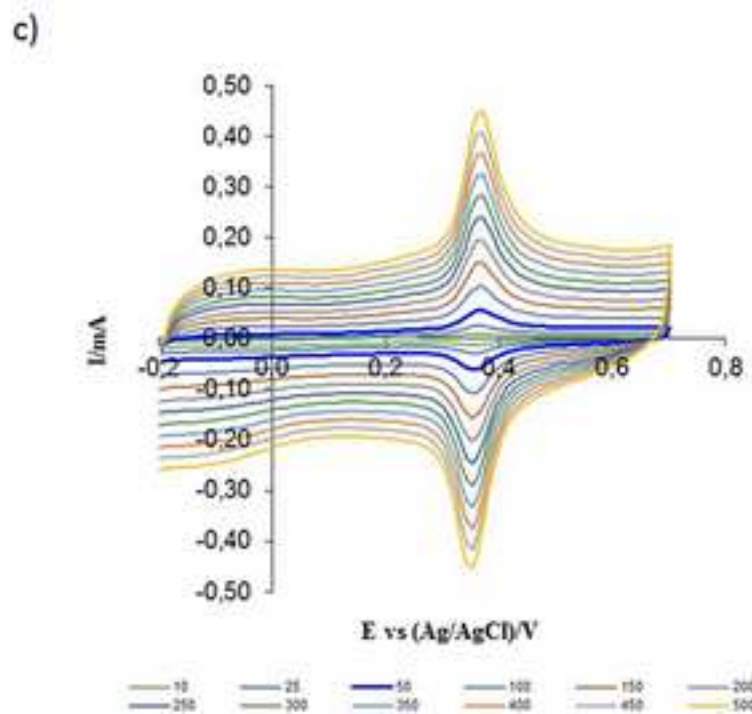
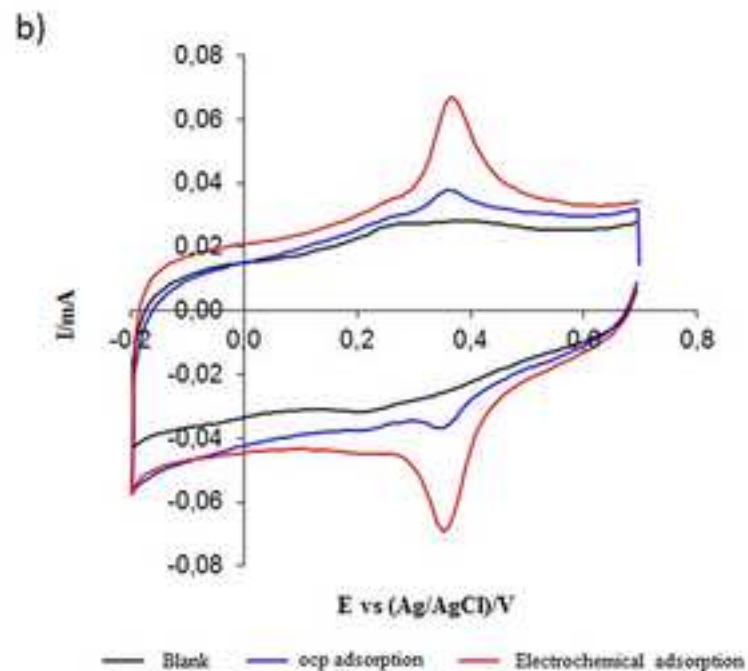
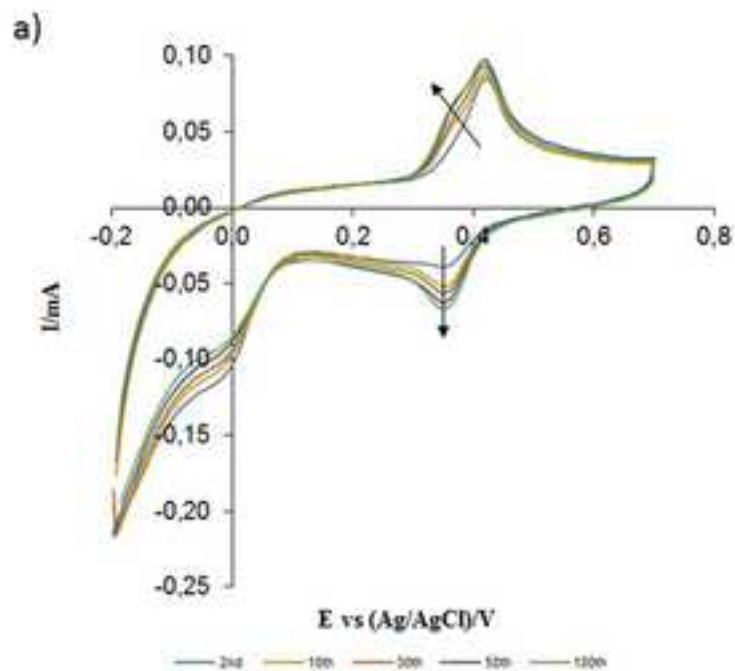


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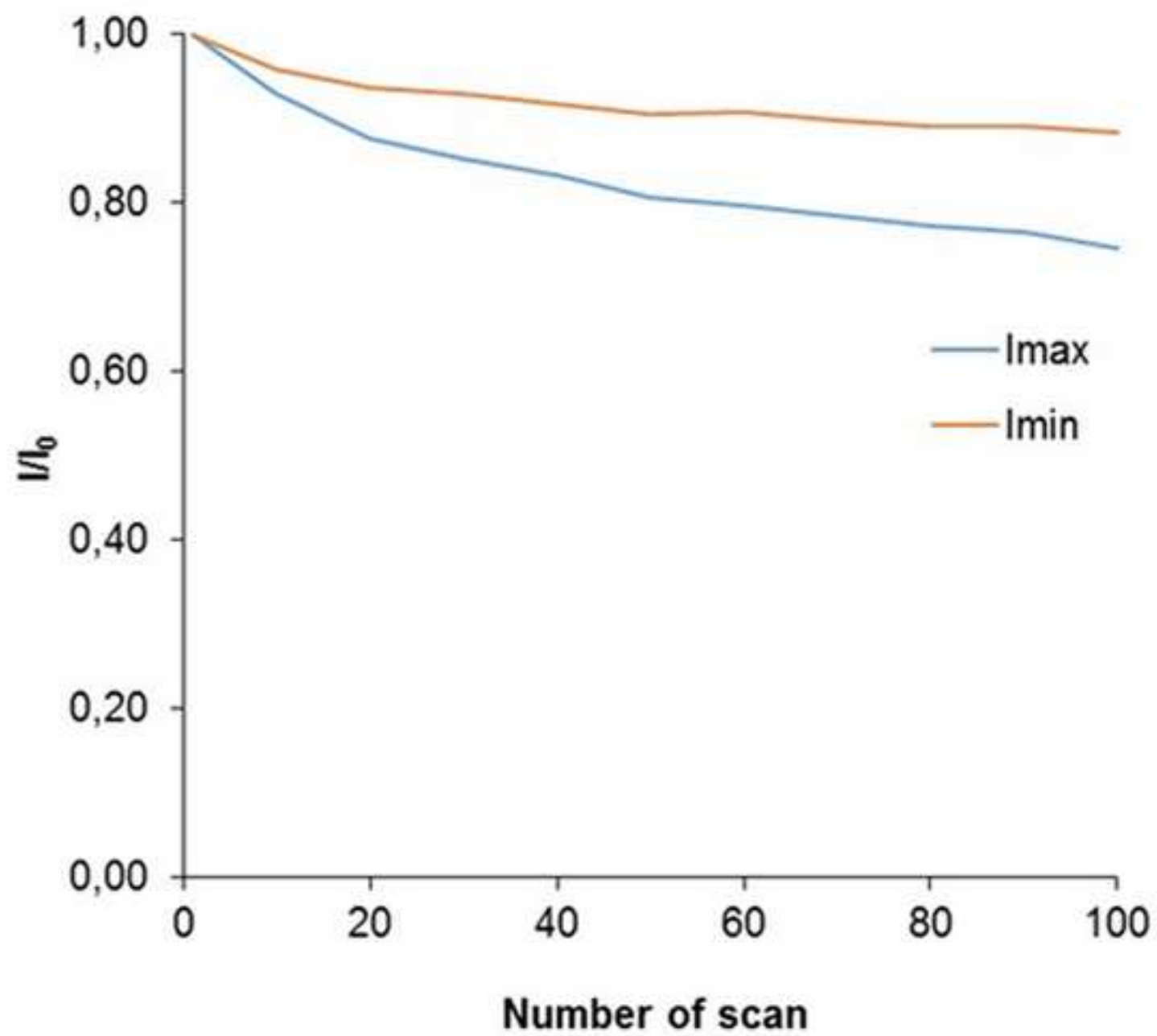
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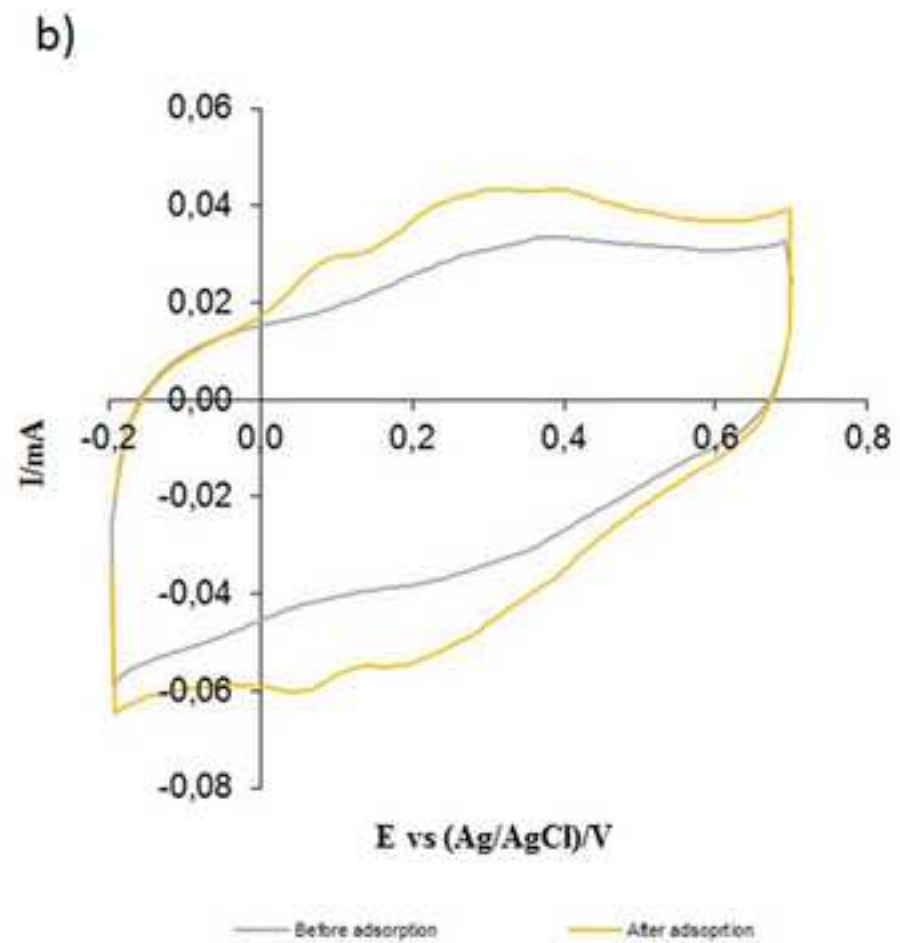
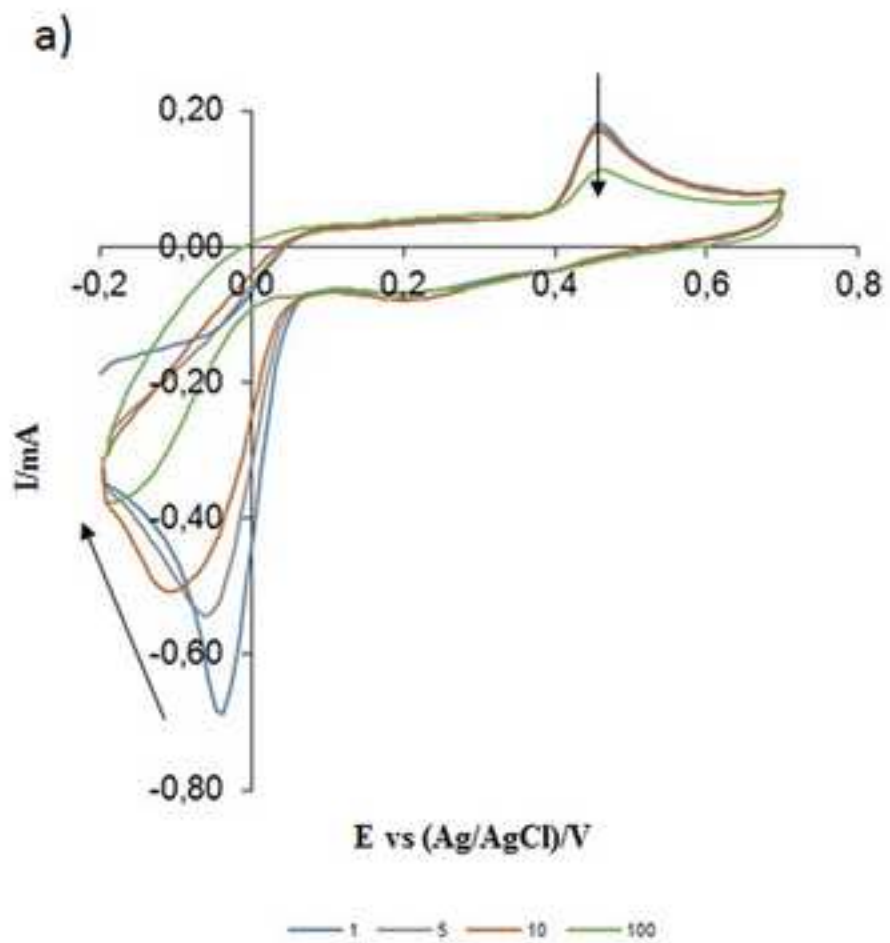


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Supplementary Materials

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