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Additional Information

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3

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16

17 **Abstract**

18 A new fermented almond “milk” that combined the properties of both almonds and probiotics was
19 considered to cover the current versatile health-promoting foods’ demand. Almond *milk* fermentation with
20 probiotic *Lactobacillus reuteri* and *Streptococcus thermophilus* was studied by using a Central Composite
21 design with response surface methodology and different factors (glucose, fructose, inulin and starters) were
22 optimised to assure high probiotic survivals in the final product. The optimal formulation was
23 physicochemically characterised throughout cold storage (28 days) and both probiotic survivals to *in vitro*

24 digestion and proteolysis were quantified. Results showed that a high probiotic population ($>10^7$ cfu/mL)
25 was obtained in the previously optimised almond *milk* throughout storage time, which correspond to the
26 addition of 0.75 g of glucose/100mL, 0.75 g of fructose/100mL, 2 g/100mL inulin and 6 mL/100mL
27 inoculum. Glucose was used as main nutrient and the production of mannitol by *L.reuteri* was detected.
28 The fermentation process increased the viscosity values, forming a weak gel structure, whose physical
29 properties hardly changed. Probiotic bacteria notably survived (51%) to the *in-vitro* digestion, surely related
30 to the inulin presence, which would add value to the developed product by enhancing the potential health
31 benefits of its consumption.

32

33 **Keywords**

34 *L. reuteri*, prebiotic, fermentation, response surface methodology, survivals.

35

36 **1. INTRODUCTION**

37 The term of “probiotics” was defined as live microorganisms that when administered in adequate
38 amounts confer a health benefit on the host (FAO/WHO, 2001), being the lactobacilli and bifidobacteria
39 genera the most widely recognised (Rivera-Espinoza and Gallardo-Navarro, 2010).

40 The use of probiotics, as a whole concept (live microorganisms), in fermented food product
41 manufacturing is not new; although the aims have moved from food preservation and organoleptic
42 improvements (Kopp-Hoolihan, 2001) towards benefits for health, such as reduction of
43 hypercholesterolemia and host immune system modulation, among others (Saad *et al.*, 2013). Nevertheless,
44 in order to effectively provide health functionalities, the minimum recommended number of viable
45 probiotic bacteria is 10^7 colony forming per unit (cfu)/g or mL of a product at the time of consumption
46 (Sanz and Dalmau, 2008). *L. reuteri* ATCC 55730 is a well-established probiotic strain (Casas and
47 Mollstam, 1997) which could be used to develop beneficial products for targeted groups such as the

48 paediatric population, since these probiotic bacteria have been reported to improve symptoms of infantile
49 colic (Savino *et al.*, 2007), feeding tolerance and gut functions in pre-term infants (Indrio *et al.*, 2008),
50 reduce constipation (Coccorullo *et al.*, 2010) and modulate cytokine patterns involved in atopic diseases
51 (Miniello *et al.*, 2010).

52 Although the dairy industry is the major sector involved in developing probiotic products, other food
53 areas have recently become involved such as nut, cereal or other vegetable *milk* industries. The so-called
54 vegetable *milks* have special relevance since, besides their nutritional and health benefits, they contain
55 prebiotic compounds or can be easily added (i.e. inulin) which make them interesting and useful to produce
56 synbiotic (combination of probiotic and prebiotic) products. In addition to the health benefits, prebiotics
57 such as inulin are reported to provide fermented products technological benefits, since they can increase
58 the viscosity of the final product and have a synergic effect on probiotic survival during processing and
59 storage (de Souza-Oliveira *et al.*, 2009).

60 There is a wide range of commercial vegetable *milks*, although the ones derived from almond nuts have
61 been the subject of interest due to the known impact of their compounds on some current chronic diseases
62 such as cardiovascular diseases, type 2 Diabetes mellitus, obesity and some cancers (Kamil and Chen,
63 2012). Almond nuts are rich in mono- and polyunsaturated fatty acids (mainly oleic and linoleic acids),
64 vegetable proteins, dietary fibre, phytosterols, polyphenols, vitamins and minerals (Yada *et al.* 2011); most
65 of those compounds have antioxidant properties and have a proven beneficial effect on plasma lipid profile,
66 low-density lipoprotein oxidation and inflammatory processes, among others (Liu, 2012; Egert *et al.*, 2011;
67 Jones *et al.*, 2011). Moreover, almond nuts have a high K/Na ratio and the carbohydrates present have a
68 low glycemic index (suitable for diabetics) (Li *et al.*, 2009). Therefore, almond *milks* could be very useful
69 in the industrial production of new non-dairy fermented products with functional features in which the
70 nutritional and health benefits of almonds and probiotic bacteria are included.

71 Previous fermentation studies carried out with almond *milk* and different lactic bacteria showed us that
72 a non-formulated almond *milk* has a low carbohydrate content (around 0.3 g/100 mL of *milk*), in comparison
73 with cow milk (4-5 g/100 mL) or soy beverages (1.7 g/100 mL) (Champagne *et al.*, 2009). This low
74 carbohydrate content affects directly the acidification level that can be attained (Chang and Stone, 1990),
75 which remained above 5 after 24 hours (Bernat, 2013). Thus, carbohydrate supplementation of almond *milk*
76 was needed to improve the growth and acidification of the mixed culture used.

77 The aim of this study was to evaluate the fermentative process of almond *milk* with the mixed culture
78 *L. reuteri* ATCC 55730 and *S. thermophilus* CECT 986 (ratio 1:1). To this end, the effect of different,
79 previously chosen factors (glucose, fructose and inulin and starters contents) were analysed and optimised
80 to define the most suitable almond *milk* formulation in which sufficient probiotic bacteria survivals is
81 ensured in the final product. The fermented almond *milk* with the optimum factor values was characterised
82 as to its physicochemical and probiotic survival properties throughout storage time at 4 °C with the aim of
83 determining the shelf life of the developed product.

84

85 **2. MATERIALS AND METHODS**

86

87 **2.1 Almond *milk* processing**

88 Almond *milk* was produced by soaking and grinding almonds (*Prunus amygdalus L. cv. dulcis*) supplied
89 by Frutos Secos 3G S.L. (Valencia, Spain). The extraction was carried out in the Sojamatic 1.5 (Sojamatic®;
90 Barcelona, Spain), a piece of equipment specifically designed for the production of vegetable *milks*, with a
91 nut:water ratio of 8:100. The milky liquid obtained was then microfluidised in a high pressure homogeniser
92 (M-110P model; Microfluidics Int. Corp., Westwood, MA, USA) by applying 172 MPa and further on
93 pasteurised (85 °C/30 min). The use of high pressures of homogenisation (HPH) contributed to the *milk*
94 being of better quality in terms of its physical stability, since this innovative technology is able to reduce

95 the size of fat globule particles such a way that flocculation and coagulation phenomena are delayed (Pereda
96 *et al.*, 2007). Moreover, HPH may contribute to a better probiotic fermentation response, reducing
97 coagulation times, acquiring sufficient probiotic survival, improving texture and mouthfeel and/or
98 preventing syneresis (Cruz *et al.*, 2009; Patrignani *et al.*, 2007).

99 The compounds pre-selected as factors, glucose, fructose and inulin were added prior to the heat
100 treatment to prevent further re-contaminations. The monosaccharides were purchased from Sosa
101 Ingredients S.L. (Barcelona, Spain), while the inulin came from Beneo-Orafti (Tienen, Belgium).

102

103 **2.2 Preparation of fermented almond *milk***

104

105 **2.2.1 Inoculum preparation**

106 *Lactobacillus reuteri* ATCC 55730 (Biogaia, Stockholm, Sweden) and *Streptococcus thermophilus*
107 CECT 986 (CECT, Valencia, Spain) were activated from their frozen forms (stored in 40g/100 mL glycerol
108 at -80 °C), by transferring them to their selective broths until optimal bacterial growth is obtained. The
109 selective broths were MRS (Scharlab, Barcelona, Spain) for the probiotic *Lactobacillus* and M17 (Difco™,
110 New Jersey, USA) for *S. thermophilus*. Incubation conditions were 37 °C/24h/anaerobically for *L. reuteri*,
111 in which anaerobiosis was created by using anaerobic jars and a CO₂-generator system (AnareroGen™,
112 Oxoid Ltd, Basingstoke, England) and 42 °C/24h/aerobically for *S. thermophilus*.

113 As regards the starter inoculum, strains were independently incubated in their broths for 24 h and then
114 centrifuged at 8,600 xg-10 min at 4 °C; the supernatant was discarded. Immediately afterwards, bacteria
115 were resuspended in PBS-1x buffer (10 mmol/L phosphate, 137 mmol/L NaCl, 2.7 mmol/L KCl, pH 7.4)
116 until they reached concentrations of 10⁸ colony forming units (cfu) per mL.

117

118 **2.2.2 Experimental design for the almond *milk* fermentation process**

119 Amounts of glucose, fructose, inulin and starter inoculum were selected as factors to obtain fermented
120 almond *milk*. Central Composite Design (CCD) with randomised Response Surface methodology (RSM)
121 was used to study how different combinations of these factors affect almond *milk* fermentation. Other
122 authors also used RSM in the development of probiotic products (Cruz *et al.*, 2010; Yaakob *et al.*, 2012).
123 Statistical analysis of the data was carried out by using an orthogonal CCD 2⁴ + star, which studied the
124 effects of 4 factors in 31 runs. Levels of glucose, fructose, inulin and starter inoculum are shown in Table
125 2. These parameters were established by taking previous fermentation studies with probiotics into account
126 (Angelov *et al.*, 2006; De Souza-Oliveira *et al.*, 2009; Franck, 2002). The variable response was defined as
127 the probiotic survival (cfu/mL) after fermentation process.

128 Fermentation process of the 31 runs obtained in the design was carried out by adding the corresponding
129 starters (prepared by mixing in a 1:1 volume ratio *L. reuteri*:*S. thermophilus* buffer suspensions) to the
130 formulated and pasteurised almond *milk* and incubating them at the optimal temperature of the mixed
131 culture (40 °C). When the pH of the samples reached ≈4.6, fermentation was stopped by cooling them to 4
132 °C, which was the storage temperature until the analyses were performed.

133 A step-wise second grade polynomial fitting was used to model the response variable as a function of the
134 factors. The optimal formulation of the fermented product was established on the basis of the obtained
135 results for the response variable.

136

137 **2.3 Fermented product characterisation**

138 Both the formulated almond *milk* and the optimal fermented product stored for different times were
139 characterised as to their content in different sugars, pH, acidity, particle size distribution and ζ-potential,
140 rheological behaviour and colloidal stability. In almond *milk*, the chemical composition of major
141 components (dry matter, protein, lipids, total sugars and ashes) was obtained. The fermented product was
142 also analysed in terms of starters' viability throughout storage time (1, 7, 14, 21 and 28 days) at 4 °C

143 Moreover the initial starters' proteolytic activity and probiotic survivals to a simulated gastrointestinal
144 digestion were studied. All the analyses were performed in triplicate.

145

146 **2.3.1 Chemical analyses**

147 AOAC official methods of analysis were used to determine moisture (AOAC 16.006), total nitrogen
148 (AOAC 958.48) and fat contents (AOAC 945.16) (Horwitz, 2000). Ashes were obtained following the
149 protocol reported by Matissek *et al.* (1998).

150 Sugar profiles were analysed and the different sugars were quantified using the following equipment:
151 A Metrohm 838 high-performance anion-exchange chromatograph (IC 861) equipped with a pulsed
152 amperometric detector (Bioscan 817) to monitor the separation (Metrohm® Ltd., Herisau, Switzerland).
153 Prior to the analysis, samples were diluted 1:100 with nanopure water. Sample proteins were removed by
154 precipitation with glacial acetic acid and the pH was then reconstituted at initial values. Before injecting
155 samples into the equipment, they were filtered through nylon membranes (0.45 µm). A Metrosep CARB
156 guard (5x4.0 mm) and CARB 1 (250 x 4.6 mm) analysis columns (Metrohm®) were used. 20 µL of sample
157 was injected and eluted (1 mL/min) with 0.1 mol/L NaOH, at 32 °C. An Au working electrode was used
158 and applied potentials were +0.05 V (0-0.40 s) +0.75 V (0.41-0.60 s) and +0.15 V (0.61-1 s). Software
159 ICNet 2.3 (Metrohm®) was used for data collection and processing. The concentration of each sugar was
160 determined from their respective calibration curves, obtained from standard solutions of glucose, fructose
161 and sucrose (Sigma-Aldrich Corp., St. Louis, MO, USA), which were obtained in triplicate.

162 Fibre content was obtained by difference to 100 of the sum of rest of analysed components.

163

164 **2.3.2 Proteolytic activity analyses**

165 The extent of proteolysis in fermented almond *milk* was evaluated by measuring the free amino acids
166 and small peptides using the *o*-phthaldialdehyde method described by Church *et al.* (1983). The absorbance

167 of the solutions was measured at 340 nm in a quartz cuvette by using a UV-visible spectrophotometer
168 (Helios Zeta UV-vis, Thermo Scientific, USA). The starters' proteolytic activity is quantified as the
169 difference in absorbance measured between fermented and non-fermented almond *milks*.

170 Moreover, non-fermented and fermented almond *milk* samples were analysed by size-exclusion
171 chromatography (SEC-HPLC) in order to obtain their unique peptide profiles. *In vitro*-digest inoculated
172 samples were also characterised by SEC-HPLC; these samples were first subjected to a heat treatment (80
173 °C/20 min) in order to suppress any possible residual enzymatic activities. All HPLC analyses were
174 performed in duplicate on Agilent 1200 HPLC system (Agilent Technologies, Palo Alto, CA, USA). SEC-
175 HPLC screening of samples was performed on a BioSep-SEC-S2000 (300 mm x 7.8 mm) column with a
176 gel-filtration chromatography guard column (4 x 3 mm) (Phenomenex, Cheshire, UK). Before injecting
177 samples they were filtered through nylon membranes (0.45 µm). A SEC-HPLC screening method that has
178 great affinity for smaller Mw peptides (up to 20,000 Da) was used. The standards thyroglobulin, aprotinin,
179 cytochrome C, insulin, angiotensin I, angiotensin II, uridine and sodium azide (All Sigma–Aldrich Corp.,
180 St. Louis, MO, USA) were used to prepare a calibration curve for this method. The separations were
181 performed at 30 °C by isocratic elution at a flow rate of 1 mL/min. The injection volume was 10 µL.
182 Detection was at 214 nm. The mobile phase was acetonitrile-H₂O (ratio 45:100) containing 0.1 mL/100
183 mL trifluoroacetic acid.

184

185 **2.3.3 Probiotic survivals to a simulated gastrointestinal digestion (SGID)**

186 Optimised fermented almond *milk* underwent a SGID and the survival of probiotic bacteria was
187 examined. This was also assessed in non-fermented *milk*. SGID was performed as described by Glahn *et*
188 *al.* (1998) but no demineralization was carried out. Porcine pepsin (800-2500 units/mg protein), pancreatin
189 (activity, 4 1 USP specifications) and bile extract were purchased from Sigma-Aldrich® (St. Louis, MO,
190 USA).

191 After the SGID, *L. reuteri* survivals were quantified by using the pour plate technique, which is further
192 on described.

193

194 **2.3.4 Viability of starters**

195 Survival of both *L. reuteri* and *S. thermophilus* in fermented almond *milks* were quantified using the
196 pour plate technique, according to the method described by the International Dairy Federation (International
197 IDF standards, 1997). The selective media used were MRS agar (Scharlab; Barcelona, Spain) for the
198 probiotic strain, which was acidified to pH 5.4 with acetic acid to prevent growths of streptococcus strain,
199 and M17 agar (Difco™; New Jersey, USA) for *S. thermophilus*. Incubation conditions were 37 °C /48
200 h/aerobically for *S. thermophilus* and 37 °C/24 h/anaerobically for *L. reuteri*; Anaerobiosis was created by
201 using anaerobic jars and a CO₂-generator system (AnareroGen™; Oxoid Ltd, Basingstoke, England).
202 Counts were reported as log cfu/mL.

203

204 **2.3.5 pH and titratable acidity (TA)**

205 Measurements of pH in non-fermented and fermented almond samples were carried out at 25 °C using
206 a pH-meter (GLP 21+, Crison Instruments S.A.; Spain). AOAC standard method was chosen to determine
207 TA in samples (AOAC 947.05), which consisted of a titration with 0.1 mol/L NaOH solution, expressing
208 the results as grams of lactic acid per L (Horwitz, 2000).

209

210 **2.3.6 Particle size distribution and ζ -potential**

211 Almond fat globule size distributions in both fermented and non-fermented *milks* were analysed with a
212 laser diffractometer (Mastersizer 2000, Malvern Instruments Ltd, UK). The Mie theory was applied by
213 considering a refractive index of 1.33 and absorption of 0.1. Samples were diluted in de-ionised water at
214 2,000 rpm until an obscuration rate of 10% was attained. Surface weighted mean diameter ($D_{3,2}$) and

215 volume weighted mean diameter ($D_{4,3}$) parameters were quantified and analysed. $D_{4,3}$ is sensitive to the
216 presence of large particles, whereas $D_{3,2}$ is more sensitive to the presence of small particles (Couvreur and
217 Hurtaud, 2007).

218 ζ -potential was determined at 25 °C by using a Zetasizer nano-Z (Malvern Instruments Ltd; UK).
219 Samples were diluted to a fat droplet concentration of 4 g/L using a phosphate buffer solution. The
220 Smoluchowsky mathematical model (Sze *et al.*, 2003) was used to convert the electrophoretic mobility
221 measurements into ζ -potential values.

222

223 **2.3.7 Serum retention capacity (SRC)**

224 SRC of both non-fermented and fermented *milks* was analysed by sample centrifugation (Medifriger-
225 BL, JP-Selecta; Spain). Conditions were 2,500 xg/45 min/20 °C and the amount of serum separation was
226 used to quantify sample stability.

227

228 **2.3.8 Rheological behaviour**

229 The rheological behaviour was characterised in a rotational rheometer (HAAKE Rheostress 1, Thermo
230 Electric Corporation; Germany) with a sensor system of coaxial cylinders, type Z34DIN Ti. The shear stress
231 (σ) was measured as a function of shear rate ($\dot{\gamma}$) from 0 to 512 s⁻¹, using 5 minutes to reach the maximum
232 shear rate and another 5 to fall (up and down curves). The Herschel-Bulkey model (Eq. 1) was fitted to the
233 experimental points of the up curve to determine the flow behaviour index (n), consistency index (K) and
234 yield stress (σ_y) by using a non-linear procedure. Apparent viscosities were calculated at 50 s⁻¹ (Eq. 2),
235 since shear rates generated in mouth when food is being chewed and swallowed are between 10 and 100 s⁻¹
236 (McClements, 2004).

237

$$\sigma = \sigma_y + K \dot{\gamma}^n \quad (1)$$

$$\eta = K \cdot \dot{\gamma}^{n-1} \quad (2)$$

238

239 **2.3.9 Colour parameters**

240 The colour coordinates were measured from the infinite reflection spectrum in a spectrophotometer
 241 (CM-3600 d, MINOLTA Co; Japan). A 20 mm depth cell was used. The CIE L* a* b coordinates were
 242 obtained using illuminant D65/10° observer. The colour of almond *milk* samples was characterised as to
 243 Lightness (L*), chrome (C_{ab}*), hue (h_{ab}*) and Whiteness Index (WI), as defined in equations (3) to (5). The
 244 colour differences (ΔE) between fermented and non-fermented samples were also calculated by using
 245 equation (6).

$$C_{ab}^* = \sqrt{a^{*2} + b^{*2}} \quad (3)$$

$$h_{ab}^* = \arctan(b^*/a^*) \quad (4)$$

$$WI = 100 - \sqrt{(100 - L^*)^2 + a^{*2} + b^{*2}} \quad (5)$$

$$\Delta E = \sqrt{(\Delta L^*)^2 + (\Delta a^*)^2 + (\Delta b^*)^2} \quad (6)$$

246

247 **2.4 Statistical Analysis**

248 Results were submitted to analysis of variance with 95% significance level using
 249 Statgraphics® Centurion XV. Multiple comparisons were performed through 95% LSD intervals.

250

251 **3. RESULTS AND DISCUSSION**

252

253 **3.1 Chemical composition of almond *milk***

254 Values of both peeled almond nut and the derivative *milk* compositions are summarised in Table 1.
255 Results (mean values and standard deviation) are expressed per 100 grams or mL.

256 Results obtained were consistent with those from Yada *et al.* (2011) for sweet almonds (*Prunus*
257 *amygdalus L. cv. dulcis*). With the exception of the sugar content, the almond *milk* composition obtained
258 was what was expected, considering the nut:water ratio (8:100) during extraction. Differences in *milk* sugar
259 content (around 0.3 g/100 mL were expected in the *milk*) are probably due to the heat treatment that the
260 almond *milk* received, which might have caused sugar losses due to caramelisation phenomena (Kroh,
261 1994). As commented on above, this low carbohydrate content affected the acidification level which can
262 be attained and was insufficient for fermentation (data not shown). Thus, carbohydrate supplementation of
263 almond *milk* was needed to improve the growth and acidification of the mixed culture used.

264

265 **3.2 Optimisation of fermentation process**

266 Table 2 shows the experimental response (probiotic survival (log cfu/mL)) obtained for all the
267 formulations of the CCD. As can be seen, all the formulations were suitable for developing a probiotic
268 almond fermented *milk*, since their variable responses were above 7 log cfu/mL, which is the minimum
269 recommended probiotic amount to be present within the food matrix to ensure health effects in consumers
270 (Sanz and Dalmau, 2008).

271 Results from the 31 runs were fitted to a second order polynomial equation and the removal of non-
272 significant terms ($p > 0.05$) was applied when necessary. However, when the exclusion of such terms
273 decreased the explained variance (R^2_{adj}), the term was included in the model. The goodness of the fitted
274 model was evaluated by ANOVA, based on the F-test and on the R^2_{adj} , which provide a measurement of
275 how much of the variability in the observed response values could be explained by the experimental factors
276 and their interactions (Cruz *et al.*, 2010). Table 3 summarises the estimated regression coefficients of the
277 second order model obtained, in which fit parameters from the analysis of variance are included.

278 As can be seen in Table 3, the coefficients for glucose and fructose factors seemed to negatively affect
279 the probiotic survival (values are negative), although the coefficients corresponding to the interactions
280 (second order terms) were positive and explained the overall positive impact of those growth factors on the
281 probiotic counts. This result indicated that neither glucose nor fructose were truly independent, which is
282 statistically known as “multicollinearity” and represents a common problem in regression analyses (Bender
283 *et al.*, 1989). When multicollinearity occurs, the elimination of non-significant explanatory variables in the
284 model is not recommended (Bender *et al.*, 1989). As regards the inulin and inoculum factors, both had a
285 positive effect on the probiotic survival, being the inoculum concentration the factor which most positively
286 influenced ($p < 0.05$).

287 With regards to the model fit, the lack-of-fit parameter was not significant ($p > 0.05$), which indicated
288 that the obtained model is adequate for predicting probiotic *L. reuteri* survival in almond *milk*. In practice,
289 a model is considered appropriate to describe the influence of the dependent variable(s) when the coefficient
290 of determination (R^2) is at least 80% (Yaakob *et al.*, 2012) or values of R^2 adj (variation in the experimental
291 data) over 70% (Cruz *et al.*, 2010). R^2 and R^2 adj of the model did not reach the recommended minimums
292 (Table 3), probably due to the narrow range of experimental response obtained (less than one log cfu/mL).
293 Nevertheless, this model could be a useful tool to make rough predictions.

294 The CCD model was then statistically optimised in order to maximise the viability of the *L. reuteri*
295 (variable response) and the optimum formulation obtained corresponded to the addition of 0.75 g/100 mL
296 of glucose, 0.75 g/100 mL of fructose, 2 g/100 mL of inulin and 6 mL/100 mL of starter inoculum (10^8
297 cfu/mL) to the almond *milk*. With this formulation, it would be expected that probiotic counts in the
298 resulting fermented product would be 7.7 log cfu/mL.

299 The optimal formulation was then submitted to a fermentation process and it reached a pH of $4.83 \pm$
300 0.03 in 8 h at 40 °C with a *L. reuteri* survival of ≈ 8 log cfu/mL, as the model predicted. Despite the pH, the
301 final acidity of this fermented almond *milk* averaged 1.78 ± 0.05 g of lactic acid per L. This value is lower

302 than standard yoghurt, which has a lactic acid content of around 8-10 g/L (Tamime and Robinson, 2000).
303 This acidity could be explained by considering that almond *milk* has a lower buffering capacity than cow
304 milk (Al-Dabbas *et al.*, 2010).

305

306 **3.3 Initial characterisation of fermented samples**

307 At the end of the process, a pH of 4.83 ± 0.03 at 40 °C and a population of *L. reuteri* of 7.93 ± 0.02 log
308 cfu/mL was obtained after 8 h, in agreement with the regression model. *S. thermophilus* reached similar log
309 counts to *L. reuteri* (7.90 ± 0.01 log cfu/mL). The use of these mixed cultures resulted in faster acidifying
310 rates (data not shown), suggesting some type of acidifying symbiosis. This has frequently been observed
311 with traditional cow milk yogurt starter cultures and sometimes pointed out by others author working with
312 others vegetable matrixes such as soy (Champagne *et al.*, 2009), but until now, has not been reported
313 between *L. reuteri* and *S. thermophilus*.

314 The Titrable Acidity (TA) at the end of the fermentation process was 1.78 ± 0.05 g of lactic acid per L.
315 This value is lower than standard yoghurt, which has a lactic acid content of around 8-10 g/L (Tamime and
316 Robinson, 2000), surely due to the much lower protein content of almond milk protein than that of cow
317 milk and to its lower buffering capacity.

318

319 **3.3.1 Proteolytic activity analyses**

320 During industrial processes, starter bacteria are repeatedly exposed to stress conditions, which induce
321 the bacterial proteases synthesis in order to obtain nutrients for their growth (Aguirre *et al.*, 2008); these
322 proteases, besides the almond protein hydrolysis, contributed in flavour and texture of the resulted
323 fermented products (Savijoki, Ingmer and Varmanen, 2006; Tamime and Robinson, 2000).

324 The proteolytic activity was evaluated through the difference in the absorbance values between fermented
325 and non-fermented almond *milk*, this being around 0.080 ± 0.005 , value much below that the activity
326 observed in others probiotic cow-milk's yoghurts ($\Delta A_{340\text{nm}} = 0.1-0.2$) (Vasiljevic *et al.*, 2007).

327 This result allowed us to conclude that the enzymatic system of this starter bacteria contain enzymes
328 which were able to hydrolyse almond proteins in some extent, since the absorbance values in fermented
329 samples were higher than that obtained in non-fermented *milk*. This is also reflected in the peptide
330 chromatogram profile of fermented samples, which is shifted to lower molecular weights, as Figure 1
331 shows. Donkor *et al.* (2005), when working with different probiotic fermented products from vegetable
332 (soy) *milk*, also quantified low proteolytic activities ($\Delta A_{340\text{nm}} < 0.02$). This could be related with the
333 different probiotic strain and different concentration used, which often make difficult the comparison of the
334 data.

335

336 **3.3.2 Simulated gastrointestinal digestion (SGID)**

337 Initially fermented samples were submitted to a SGID to analyse the effect of the digestion process on
338 the almond proteins and on the viability of probiotic bacterial.

339 Figure 1 shows the peptide chromatogram profiles obtained from both non-fermented and fermented
340 *milks* before and after the SGID. As can be observed, the main soluble peptides in the fermented *milks* were
341 constituted by peptides with Mw lower than 400 Da, together with the highest Mw fraction (from 8 to 15
342 kDa). The *in vitro* digestion process of fermented samples led to the disappearance of the major part of the
343 high Mw peptide fraction (from 8 to 15 kDa) and to the generation of greater amount of low Mw peptides
344 (< 2.5 kDa). Hence, fermentation process together with the human digestion might have improved, on the
345 one hand, the bioavailability of almond *milk*'s peptides and, on the other hand, the immune response, as
346 has been observed in soy-based products (Wilson *et al.*, 2005).

347 With regards the viability of the probiotic bacteria, results showed that $51 \pm 7\%$ of *L. reuteri* survived to a
348 SGID, this value being notably higher than the values reported by other authors working with probiotics
349 (20-40%) (Bezkorovainy, 2001). The higher survival might be attributable to the presence of inulin, which
350 is believed to improve probiotic viability (Capela *et al.*, 2006; Kolida *et al.*, 2002; Franck, 2002).

351

352 **3.3.3 Sugar contents**

353 The characterisation of sugar profiles in the products stored for different times is essential in order to
354 know the metabolic activity of the starter bacteria within the almond matrix. Figure 2 shows the
355 chromatograms of both non-fermented and fermented almond *milks* stored for different times (1, 14 and 28
356 days). As can be seen, prior to the fermentation process, our almond *milk* contained in order of importance
357 sucrose, glucose and fructose, besides two other peaks (peaks 4 and 5). These latter were not present in
358 almond nut (data not shown) and so, they must come from the added inulin and, thus, were classified as
359 fructans, which is a term that includes both inulin and their derivatives (Roberfroid, 2005).

360 Moreover, a new peak was identified in fermented products as mannitol (peak 0), due to the fact that its
361 retention time was the same as that of pure mannitol. The appearance of this compound is attributed to the
362 heterofermentative metabolic pathway of the *L. reuteri* strain used, in which fructose is used as an e⁻
363 acceptor to regenerate NAD resulting in mannitol as the end product (Årsköld *et al.*, 2008). Mannitol yield
364 (mol mannitol produced per mol fructose consumed) was 0.81 ± 0.09 which is in agreement with other
365 reported values (Ortiz *et al.*, 2012). The presence of mannitol might be an added value in the product, since
366 it is a non-metabolic sweetener with antioxidant properties (Wisselink *et al.*, 2002).

367 As can be seen in Table 4, immediately after the fermentation process, a significant reduction in the
368 glucose, fructose and sucrose contents occurred, being glucose the major substrate used (13% of the total),
369 followed by the fructose (6%). Champagne *et al.* (2009) also observed the decrease in these sugars in soy
370 beverage when it was fermented using a mixed culture of *L. helveticus* or *B. longum* and *S. thermophilus*.

371

372 **3.4 Fermented samples characterisation throughout storage time**

373

374 **3.4.1 Starter survival and acid production**

375 Table 5 shows the average values of pH and Titratable Acidity (TA) in fermented almond *milk* vs.
376 storage time. This table also includes the bacterial count data of *L. reuteri* and *S. thermophilus* (log cfu/mL)
377 in fermented almond *milk* throughout storage time.

378 As it has been reported, probiotic health benefits are seen to be dependent on the matrix in which they
379 are present and their efficacy is linked with their ability to survive in the gastrointestinal tract (Buddington,
380 2009). Hence, in order to effectively provide such health functionalities, the minimum number of viable
381 probiotic bacteria is suggested as 10^7 cfu/mL by the time of consumption (Sanz and Dalmau, 2008). The
382 viability of both strains decreased throughout storage time ($p < 0.05$), especially for *S. thermophilus*, but the
383 probiotic *L. reuteri* counts were above the minimum recommended level (10^7 cfu/mL) in the whole period
384 analysed.

385 The pH values were almost maintained throughout the time period analysed, the mean value being 4.65.
386 TA increased over storage time, although from the 7th day onwards differences among values were non-
387 significant ($p < 0.05$), being around 2.2 g/L. This low TA value might have a positive effect on the overall
388 sensory acceptance of the final product, since it has a direct impact on sweetness attribute.

389

390 **3.4.2 Sugar contents**

391 Table 4 shows the amount of the different sugars identified in both fermented throughout storage time
392 and non-fermented almond *milks*. Contrary to standard cow milk yoghurts, in which lactose is the only C-
393 source available, in our almond *milk*, the starter bacteria had a variety of options. This strain could use
394 simultaneously glucose or sucrose as energy source and fructose as alternative electron acceptor (Ortiz *et*

395 *al.*, 2012). The assessment of the use of these C-sources is critical to understand the bacterial growth and
396 survivals throughout storage. To enhance mannitol production by *L. reuteri*, fructose should be available at
397 either the lag or log growth phase of cultures grown (Ortiz *et al.*, 2012).

398 As can be observed, both glucose and sucrose gradually decreased ($p < 0.05$) throughout the storage
399 time. These results were predictable, since starter bacteria were viable during the entire storage time (Table
400 5) and, therefore, they consumed these sugars as nutrients. Fructose did not follow the same tendency, since
401 no differences in fructose concentrations were observed in fermented products stored either 1 day or 14
402 days (Table 4). The small amount of fructose available after the fermentation process remained constant
403 throughout storage, which stopped the mannitol production, as can be observed in Table 4. Grobbsen *et al.*
404 (2001) showed that when there is not enough fructose available in the medium, the fructose to mannitol
405 conversion efficiency decreased.

406 In Figure 2, the chromatograms of sugar peaks obtained in HPAC-PAD assays from almond *milk* (AM)
407 and its fermented products at the different storage times are shown. As can be observed, no changes in the
408 long-chain fructan (peak 5) throughout time is detected, which suggests that *L. reuteri* was either not able
409 to degrade this oligosaccharide or did not have to do it due to the fact that there was sufficient nutrient
410 availability within the almond *milk*. Regarding the other fructan (peak 4), a trend towards a reduction seems
411 to be observed but it was not large enough to quantify it. Makras *et al.* (2005) observed that, among the
412 lactobacilli assessed, few of them are able to use inulin-type fructans as a C-source. Hence, most of the
413 added inulin remains preserved in the product, thus, the targeted consumers of the fermented product
414 developed can take advantage of the health benefits that this prebiotic may exert.

415

416 **3.4.3 Colloidal stability parameters: Particle size, ζ -potential and SRC**

417 The measurements of particle size distributions and ζ -potential are directly related to the colloidal
418 stability of almond *milk* emulsions. Table 6 shows the mean particle diameters $D_{4,3}$ and $D_{3,2}$. As was

419 expected, the particle size distributions of fermented samples shifted to bigger sizes (both $D_{4,3}$ and $D_{3,2}$
420 values increased) (Table 6), probably due to the phenomenon of particle flocculation associated to the
421 acidification of the system. Both mean particle diameters reached a maximum value on the 7th storage day
422 after the fermentation process, when the ζ -potential reached the minimum value (Table 6).

423 Table 6 also shows ζ -potential value in both fermented and non-fermented *milks*. Fermentation
424 provoked a lower negative charge of the dispersed particles ($p < 0.05$), which means that the neutralisation
425 of some ionisable groups occurs as a consequence of the change in the pH of the product. The almond
426 protein charge will decrease, thus promoting a reduction in the ζ -potential and repulsive forces among the
427 dispersed particles. This effect will lead to the phenomenon of flocculation in the system, which can give
428 rise to a weak gel structure taking the volume fraction of the dispersed phase into account. Particle
429 flocculation will be responsible for the increase in particle size after fermentation. This result was coherent
430 with the isoelectric point (IP) range of amandin (4.55-6.3) reported by Albillos *et al.* (2009). The wide IP
431 range of amandin shows the high conformational complexity of this almond protein and explains the slight
432 negative values of ζ -potential obtained in fermented samples, since the pH of these samples (Table 5) were
433 above the minimum IP range reported. Usually ζ -potential values lower than ± 25 mV do not ensure the
434 stability of dispersed systems (Roland *et al.*, 2003), although changes in protein conformation did allow us
435 to obtain a stable matrix through the development of a weak gel structure, as commented on below.

436 Table 6 also shows the SRC obtained by sample centrifugation (expressed as percentage of precipitate
437 after centrifugation) in both fermented and non-fermented samples. A greater serum separation occurred in
438 non-fermented samples, while very few differences were observed in the case of fermented samples stored
439 for different lengths of time. These results confirm the formation of a weak gel in the fermented product as
440 a result of the flocculation of dispersed particles due to the action of proteins, which was able to retain part
441 of the serum present in the almond *milk*. Taking into account that neither the fermentation process nor the

442 storage time seems to notably affect inulin, it also contributed to the network formation due to its thickening
443 and gelling capacity (Franck, 2002).

444

445 **3.4.4 Rheological behaviour**

446 Rheological parameters play a key role in the definition of the textural and sensory perception of a new
447 product. Table 7 shows these parameters obtained by using a non-linear regression procedure to fit Eq. 1 to
448 the flow curves of fermented and non-fermented almond *milks*. The apparent viscosity of samples at 50 s⁻¹
449 shear rate and the non-linear correlation coefficient of the fitted model (R²) are also shown.

450 The rheological analyses of all samples showed that both upward and downward shear rate curves
451 demonstrated progressive structural degradation with repeated shearing, thus reflecting their thixotropic
452 nature.

453 The upward shear-rate flow behaviour of the samples could be described by a Herschel-Bulkley model
454 (parameters showed in Table 7), thus showing a shear-thinning behaviour (n<1) in all cases. These
455 parameters were not significantly (p> 0.05) affected either by the fermentation process or the storage time.
456 In Table 7, the values of the hysteresis area at the different storage times can be also observed. Both the
457 apparent viscosity as well as the thixotropic character of the samples increased slightly after the
458 fermentation step (p< 0.05) in line with the formation of a weak gel structure, as was commented on above.
459 On the other hand, *L. reuteri* is also able to synthesise exopolysaccharides and, thus, it might also contribute
460 to the gel formation and to the increase in the viscosity values (Årsköld *et al.*, 2007).
461 Statistical differences in the thixotropic nature of fermented products and in the apparent viscosity due to
462 storage time at 4 °C were non-significant (p> 0.05).

463

464 **3.4.5 Colour measurements**

465 Table 8 shows the colour parameters of both almond *milk* and fermented products cold stored at different
466 times. As can be seen, L^* , h^*_{ab} and WI increased after the fermentation process, while C^*_{ab} decreased ($p <$
467 0.05). These changes in colour coordinates can be attributed to the different level of opacity (Hutchings,
468 1999), which is related to the aggregation level of particles. The higher the luminosity values, the higher
469 the opacity and the lower the chrome, in line with a higher whiteness index. These parameters were barely
470 affected by the storage time at $4\text{ }^\circ\text{C}$ until 21 storage days, at which point C^*_{ab} and h^*_{ab} slightly decreased (p
471 < 0.05). Nonetheless, lightness was not affected by cold storage, while the whiteness (WI) only slightly
472 increased on the last day of assays ($p < 0.05$).

473 The total colour difference (ΔE) values between non-fermented and fermented almond *milks* were not
474 affected by the storage time ($p > 0.05$); the mean value being 2.69 ± 0.03 . According to Francis (1983),
475 values lower than 3 units cannot be easily detected by the human eye.

476

477 **4. CONCLUSIONS**

478 The optimal combination of growth factors which ensured a rapid fermentation of almond *milk* while
479 maintaining significant probiotic yields was 0.75 g/100 mL of glucose, 0.75 g/100 mL of fructose, 2 g/100
480 mL of inulin and 6 mL/100 mL of inoculum. This fermented product showed a $\text{pH} = 4.6$ after fermentation
481 and TA values of 2.3 g/L lactic acid. Fermentation process promoted the major changes in the physical
482 properties of the almond *milk* due to the formation of a weak gel, which induces an increase in the viscosity,
483 luminosity and whiteness index values. On the contrary, the storage time did not induce significant changes
484 in these physical properties. High probiotic survivals were also observed in the fermented almond *milk* after
485 submitting the product to an *in vitro* digestion, thus enhancing the product features to be considered as a
486 functional food. The viability of the probiotic bacteria was maintained within the minimum suggested ($\geq 10^7$
487 cfu/mL) throughout the entire storage time. During this period, consumption of monosaccharides and
488 sucrose, and mannitol production were observed, meanwhile long-chain fructan compounds remained

489 stable. Owing to both the probiotic survivals and the prebiotic compounds present, the fermented developed
490 product can be considered as a synbiotic. Nevertheless, possible functional properties of the developed
491 product have to be assessed both *in vitro* and *in vivo* assays in further studies in order to state the possible
492 health benefits.

493

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498

499

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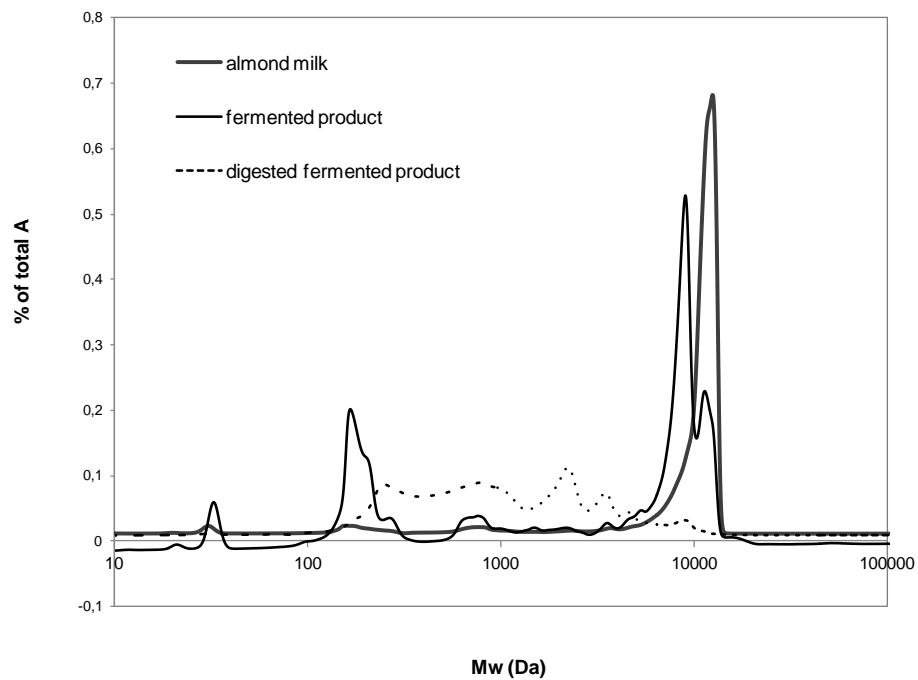


Figure 1 Peptide profile chromatograms of non-fermented (doubled line) and fermented (solid line) almond *milks* and the in vitro digested fermented products (dashed line).

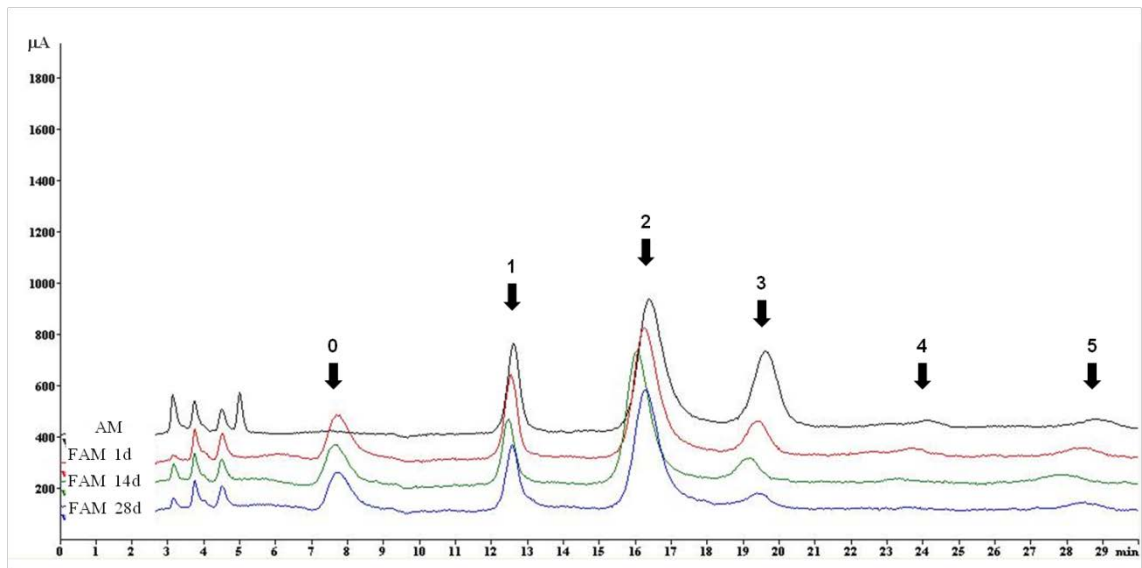


Figure 2 Chromatograms of sugar peaks obtained in HPAC-PAD assays from formulated almond *milk* (AM) and its fermented products after 1 (FAM 1d), 14 (FAM 14d) and 28 (FAM 28d) days of storage at 4 °C. Peaks identified were mannitol (0), glucose (1), fructose (2), sucrose (3) and inulin-type fructans (4 and 5).

Table 1. Chemical composition (mean value and (standard deviation)) of peeled almond nut and the derivative *milk* used.

Composition	Peeled almond nut (g/100 g)	Almond <i>milk</i> (g/100 mL)
Moisture	3.06 (0.05)	93.4 (0.5)
Lipid	55.77 (0.29)	3.96 (0.2)
Protein	22.55 (0.12)	1.37 (0.03)
Ashes	3.86 (0.06)	0.325 (0.012)
Sugars	4.9 (0.4)	0.1285 (0.0003)
Fibre	6.82	0.58

Table 2. Experimental design and probiotic survival after 28 days of storage (log cfu/mL) for fermented almond *milk* formulations of the Central Composite Design.

Run order	FACTORS				RESPONSE
	X ₁	X ₂	X ₃	X ₄	Y (log cfu/mL)
1	0	0	0	0	7.683
2	0	0	0	0	7.392
3	-1	-1	-1	-1	7.601
4	-1	-1	+1	-1	7.596
5	0	0	0	+ α	7.498
6	-1	-1	-1	+1	7.843
7	0	0	0	0	7.790
8	0	0	0	0	7.815
9	-1	-1	+1	+1	7.728
10	+1	-1	-1	-1	7.445
11	- α	0	0	0	7.615
12	-1	+1	-1	+1	7.656
13	+1	+1	+1	+1	7.705
14	+1	+1	-1	+1	7.653
15	0	0	0	0	7.783
16	+1	-1	-1	+1	7.388
17	0	0	0	0	7.292
18	+1	+1	-1	-1	7.278
19	0	0	0	0	7.804
20	-1	+1	+1	+1	7.503
21	+1	-1	+1	-1	7.577
22	0	0	- α	0	7.603
23	-1	+1	-1	-1	7.204
24	0	- α	0	0	7.684
25	0	+ α	0	0	7.479
26	+1	+1	+1	-1	7.392
27	+1	-1	+1	+1	7.513
28	0	0	0	- α	7.225
29	0	0	0	0	7.797

30	-1	+1	+1	-1	7.204
31	+ α	0	0	0	8.006

*Factors X₁, X₂, X₃, X₄ and Y stand for glucose (- α = 0.75, -**1** = 1.5, **0** = 2.25, **1** = 3 and + α = 3.75 g/100 mL), fructose: (- α = 0.75, -**1** = 1.5, **0** = 2.25, **1** = 3 and + α = 3.75 g/100 mL), inulin (- α = 1, -**1** = 2, **0** = 3, **1** = 4 and + α = 5 g/100 mL), inoculum (- α = 4, -**1** = 5, **0** = 6, **1** = 7 and + α = 8 mL/100 mL) and probiotic survivals after fermentation process (log cfu/mL).

Table 3. ANOVA results from the CCD with RSM used in the study adjusted to a second order equation.

Source	Regression coefficient/Value
Constant	4.864
Glucose	-0.304
Fructose	-0.662*
Inulin	0.437
Inoculum	1.042**
Glucose x Fructose	0.145*
Fructose x Fructose	0.076*
Fructose x Inoculum	0.099*
Inulin x Inulin	-0.076**
Inoculum x Inoculum	-0.098**
p-value of lack-of-fit	0.793
R²	0.73
R²-adj	0.61
Standard error of est.	0.153
Mean absolute error	0.079

R² = coefficient of determination **R²-adj** = explained variance

*****: statistically significant at 90% of confidence level

******: statistically significant at 95% of confidence level

Table 4. Concentrations of the different sugars identified in fermented almond *milk* (FAM) and mannitol yield (mean values and (s.d.)) throughout storage time. Concentrations of sugars identified in non-fermented almond *milk* (AM) are included for comparisons.

Sample	Mannitol (g/L)	Glucose (g/L)	Fructose (g/L)	Sucrose (g/L)
AM	-	11.8 (1.6)	7.2 (0.4)	1.64 (0.08)
FAM 1d	1.05 (0.06) ^a	9.1 (0.5) ^a	5.96 (0.13) ^a	0.58 (0.02) ^a
FAM 14d	0.97 (0.06) ^a	8.4 (0.4) ^b	6.01 (0.09) ^a	0.43 (0.03) ^b
FAM 28d	0.89 (0.03) ^b	8.0 (0.7) ^b	5.53 (0.13) ^b	0.243 (0.014) ^c

^{a, b, c} Different letters in same column indicates significant differences between measurement times at 95% of confidence level.

Table 5. Mean values (and standard deviation) of pH, Titratable Acidity (TA) and bacterial counts of non-fermented (AM) and fermented almond *milks* (FAM) throughout storage time (d) at 4 °C.

Sample	pH	TA (g/L of lactic acid)	<i>L. reuteri</i> (log cfu/mL)	<i>S. thermophilus</i> (log cfu/mL)
AM	6.567 (0.006)	0.39 (0.03)	-	-
FAM 1d	4.657 (0.012) ^a	1.90 (0.12) ^a	7.59 (0.04) ^a	7.54 (0.14) ^a
FAM 7d	4.63 (0.02) ^b	2.23 (0.09) ^b	7.30 (0.02) ^b	7.19 (0.14) ^{bc}
FAM 14d	4.657 (0.006) ^a	2.23 (0.0) ^b	7.26 (0.11) ^b	7.33 (0.10) ^{bd}
FAM 21d	4.633 (0.012) ^b	2.19 (0.07) ^b	7.00 (0.16) ^c	6.89 (0.21) ^{ce}
FAM 28d	4.650 (0.019) ^{ab}	2.26 (1.0) ^b	7.06 (0.06) ^c	6.57 (0.24) ^e

^{a-e} Different letters in same column indicates significant differences between different times at 95% of confidence level.

Table 6. Mean particle size $D_{4,3}$ and $D_{3,2}$, ζ -Potential values and serum retention capacity (SRC) after centrifugation of fermented almond *milks* (FAM) throughout time stored at 4 °C. Mean values (and standard deviation). Values of non-fermented *milk* (AM) are included for comparison.

Sample	$D_{4,3}$ (μm)	$D_{3,2}$ (μm)	ζ -Potential (mV)	SRC (volume % of precipitate)
AM	23 (3)	8.7 (0.3)	-16.7 (1.3)	36 (2)
FAM 1d	42.3 (1.7) ^a	16.6 (0.4) ^a	-12.8 (1.0) ^a	43 (2) ^{abc}
FAM 7d	56.9 (1.6) ^b	18.4 (0.9) ^b	-11.9 (1.2) ^b	42 (3) ^{bc}
FAM 14d	41 (3) ^a	16.7 (0.6) ^a	-13.9 (0.8) ^c	39 (0.7) ^c
FAM 21d	39.8 (1.4) ^a	14.8 (0.9) ^c	-13.0 (0.5) ^a	45 (3) ^{ab}
FAM 28d	39 (2) ^a	13.8 (1.3) ^c	-14.1 (1.5) ^c	48 (3) ^a

^{a-d} Different letters in same column indicates significant differences between samples analysed at 95% of confidence levels.

Table 7. Mean values (and standard deviation) of yield stress (σ_y), flow behaviour index (n), consistency index (K), apparent viscosity (η) at a shear rate of 50 s^{-1} and hysteresis area in both non-fermented (AM) and fermented almond *milks* (FAM) throughout storage time (d). R^2 : non-linear correlation coefficient.

Sample	σ_y (Pa)	n	K (Pa·sⁿ)	R^2	$\eta_{50} \cdot 10^3$ (Pa·s)	Hysteresis (ΔA (Pa/s))
AM	0.317 (0.002)	0.77 (0.07)	0.0239 (0.0014)	1	9.3 (1.4)	108 (24)
FAM 1d	0.300 (0.016)	0.78 (0.05)	0.0247 (0.0011)	0.999	10.04 (1.15)	144 (17)
FAM 7d	0.314 (0.010)	0.769 (0.013)	0.0269 (0.0005)	1	10.9 (0.5)	170 (10)
FAM 14d	0.30 (0.03)	0.749 (0.014)	0.0315 (0.0007)	0.999	11.8 (0.7)	155 (27)
FAM 21d	0.35 (0.02)	0.84 (0.02)	0.0185 (0.0005)	1	9.8 (0.5)	147 (12)
FAM 28d	0.328 (0.014)	0.77 (0.06)	0.0291 (0.0018)	1	11.5 (1.8)	183 (28)