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Additional Information

1 **Chemical composition and temperature influence on the rheological behaviour of honeys**

2  
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5  
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12  
13  
14 **Abstract**

15  
16 The purpose of this work was to examine the viscoelastic properties of Spanish honeys with  
17 various sugar contents [fructose (32 - 42 g/100 g honey), glucose (24 - 35 g/100 g honey),  
18 sucrose (0.0 - 3.4 g/100 g honey)]; concentrations (79 – 83 °Brix) and moisture levels (16 - 19  
19 g/100 g honey) at different temperatures (5, 10, 15, 20, 25, 30 and 40°C). Honey showed  
20 Newtonian behaviour, presenting a highly viscous part (loss modulus was much greater than the  
21 elastic modulus). The loss modulus ( $G''$ ) and viscosity increased with moisture content and a  
22 decrease with temperature. Exponential and power law models were applied to fit loss modulus  
23 and viscosity data. Polynomial models were proposed to describe the combined effect of

24 temperature, fructose, glucose, sucrose content, other sugars, non-sugar substance and moisture  
25 content.

26

27

28 **Key words:** honey, viscosity, viscoelasticity, polynomial model

29

## 30 **INTRODUCTION**

31

32 Knowledge about the rheological behaviour of viscous food stuff is useful in: quality and process  
33 control, the calculation of energy requirements, and the selection of suitable processing  
34 equipment [1]. Recently, the influence of temperature on the flow behaviour of honey varieties  
35 has been studied [2-17] however there are few articles related to the effect of temperature on the  
36 viscoelastic behaviour of honeys [18]. In particular, little information is available on the  
37 viscoelastic properties of Spanish honeys with different botanical origins.

38

39 The purpose of this study was on one hand to observe the influence of temperature and total  
40 soluble content on viscosity and the loss modulus of different honeys, and on the other hand to  
41 obtain a polynomial model that could explain the behaviour of viscosity and the loss modulus as  
42 a function of the chemical composition (sugars, moisture, etc.) and temperature.

## 43 **MATERIALS AND METHODS**

44

### 45 **Materials**

46 11 different types of Spanish honey were used in this study. Before being used, they were  
47 warmed to 55°C to dissolve any crystals, and kept in flasks at 30°C to remove air bubbles that  
48 could interfere in rheological studies. This was done because rheological properties can be  
49 influenced by the presence of crystals and air bubbles [2, 19, 20].

50

### 51 **Moisture content**

52

53 The moisture content of the honey samples was obtained by measuring the refractive index at 20  
54 °C using a digital refractometer (3T Atago Abbe refractometer, Atago Co., Tokyo, Japan). The  
55 water content and °Brix concentration were determined based on a Chataway table [21]. Each  
56 measurement was taken in duplicate.

57

### 58 **Sugar determination**

59

60 Glucose, fructose and sucrose in honey samples were measured using a HPLC 10ADVP-  
61 SHIMADZU, with RI-detector, according to a method described by Bogdanov [21]. The linear  
62 regression factor of the calibration curves was higher than 0.9982 for all sugars. Sugars were  
63 quantified by comparison of the peak area obtained with those of standard sugars. The results for  
64 each sugar were expressed as g/100g. Values of parameters were expressed as the mean and  
65 standard deviation to a confidence interval of 95% for the mean.

66

### 67 **Viscoelastic measurement**

68 The dynamic rheological properties of honey samples were obtained with a RheoStress 1  
69 rheometer (Thermo Haake, Germany) at different temperatures (5, 10, 15, 20, 25, 30 and 40°C),  
70 using a parallel plate system (Ø 60 mm) at a gap of 500 µm. A batch of each composition was  
71 prepared and at least two measurements were performed on each batch, using a fresh sample for  
72 each measurement. After loading the sample, a waiting period of 5 min was used to allow the  
73 sample to recover itself and to reach the desired temperature. In order to determine the linear  
74 viscoelastic region, stress sweeps were run at 1 Hz first. Then, the frequency sweeps were  
75 performed over the range  $\omega=0.62\text{--}62.83\text{Hz}$  at 1 Pa stress. The 1 Pa stress was in the linear  
76 viscoelastic region. Rheowin Job software (v. 2.93, Haake) was used to obtain the experimental  
77 data and to calculate storage (or elastic) modulus ( $G'$ ), loss (viscous) modulus ( $G''$ ), and  
78 complex viscosity ( $\eta^*$ ).

79

## 80 **Statistical analysis**

81

82 The variables were weighted with the inverse of the standard deviation of all objects in order to  
83 compensate for the different scales of the variables. The proposed models have been made up  
84 using SPSS trial version, Excel 2007, Statgraphics trial version and Design Expert trial version.

85 To verify the suitability of the models, the mean relative deviation modulus  $D$  (eq. 1) was  
86 calculated:

$$87 \quad D = \frac{100}{n} \sum_{i=1}^n \left| \frac{A_{\text{exp}} - A_{\text{pred}}}{A_{\text{exp}}} \right| \quad (1)$$

## 88 **RESULTS AND DISCUSSIONS**

89

90 Physicochemical parameters of honey are summarised in Table 1. The moisture content ranged  
91 between 15.60-19.10 g/100 g and met the threshold requirement of moisture content required by  
92 the Codex Alimentarius (max. 20g/100 g) [22]. Sugars represent the main components of any  
93 type of honey. Reducing sugars (invert sugar), mainly fructose and glucose, are the major  
94 constituents of honey but small quantities of sucrose are also present [23].The actual proportion  
95 of fructose to glucose, in any particular honey, depends largely on the source of the nectar [7-  
96 9].The total content of glucose and fructose was over 60 g/100 g of honey, in accordance with  
97 the 2001/110/CE Directive. The fructose/glucose ratio was calculated for all samples. This ratio  
98 gives information about the crystallization state of honey, when fructose is higher than glucose  
99 honey is fluid. In all the cases this ratio was higher than 1 (Table 1), which was confirmed by the  
100 crystallization state of the mentioned honey sample; all the honeys were in a liquid state. For the  
101 rheological characterization of honey the F/G ratio must be higher than 1, if not the rheological  
102 parameters could not be determined due to crystallization of the honey.

103  
104 Figure 1 presents a typical rheogram of a honey sample in a 0.10–10 Hz frequency domain at 5-  
105 40 °C; it shows the changes in storage modulus ( $G'$ ) and loss modulus  $G''$  with the frequency,  
106 while the viscosity is not influenced by the shear stress. All the samples analysed exhibited a  
107 Newtonian behaviour (fig. 1c). The rheological parameters ( $G'$ ,  $G''$ ,  $\eta$ ) increased with the  
108 increment of the frequency applied to the sample, showing that  $G''$  had a greater magnitude than  
109  $G'$ . All the viscoelastic parameters are positively influenced by the °Brix concentration. In  
110 general,  $G'$  is less important than  $G''$  due to its low value with respect to  $G''$  ( $G'' > G'$ ) as  
111 indicated by Doubly and Cavalier [24]. Therefore, the elastic behaviour of honey seems to be  
112 less important than its viscous behaviour, as noted by Yoo[18]. The rheological properties of

113 honey can also be affected by additional factors, such as sugars and other polymeric compounds  
114 in the honey [4, 8]. In particular, the sugar content (glucose and fructose) can greatly affect the  
115 rheological properties because these sugars have different rheological behaviours. The models  
116 used for predicting the loss modulus and viscosity (with respect to temperature, concentration),  
117 presented below, use the magnitude of the two parameters at 1 Hz.

118

### 119 **Viscosity modelling**

120

121 **Influence of Temperature:** The influence of temperature on honey viscosity is described by the  
122 Arrhenius model (equation 2):

123

$$124 \quad \eta = \eta_0 \cdot \exp\left[-\frac{E_a}{RT}\right] \quad (2)$$

125

126 where  $\eta_0$  is a constant, R is the gas constant [ $\text{kJ}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$ ], and  $E_a$  activation energy (is an  
127 energy barrier to flow) [ $\text{kJ}\cdot\text{mol}^{-1}$ ], T – absolute temperature [K]. The activation energies ( $E_a$ )  
128 values (tab.2), calculated by the Arrhenius model ranged between 90.78 – 100.28 kJ/mol. The  
129 magnitude of  $\eta$  influenced the activation energy magnitude.

130

131 **Effect of Concentration:** The increase of honey viscosity with soluble solid content (C, °Brix)  
132 can be described by power-law (eq. 3):

$$133 \quad \eta = \eta_1 C^{a_1} \quad (3)$$

134 and exponential models (eq.4) [24, 25]:

135 
$$\eta = \eta_2 \exp(a_2 C) \quad (4)$$

136 where  $\eta_1, \eta_2, a_1, a_2$  are constants, and C is the concentration in °Brix. In order to calculate the  
137 model constants, the viscosity data were fitted to equations 2-3 by non-linear regression. The  
138 resulting values of the constants are presented in table 3. The coefficients of regression ( $R^2$ ) are  
139 fairly similar, so the two models are suitable for describing the effect of the soluble solids on  
140 honey viscosity.

141

142 Taking into account the mean relative deviation, it seems that the exponential models are suitable  
143 for predicting the influence of the concentration on the magnitude of viscosity. For a given  
144 temperature, the activation energy for flow depends on the soluble solid content which can be  
145 described by several models [26]. Two models, similar to equations 5 and 6 were used.

146 
$$E_a = A_1 C^{B_1} \quad (5)$$

147 
$$E_a = A_2 \exp(B_2 C) \quad (6)$$

148 where  $A_1, A_2, B_1$  and  $B_2$  are constants. The  $E_a$  values and their respective concentrations were  
149 fitted to equations 5 and 6 by non-linear regression to determine the model parameters. The  
150 calculated parameters for these models are given in table 4. The coefficients of regression ( $R^2$ ) of  
151 the two models proposed above are the same. Computing the mean relative deviation (eq. 1) of  
152 the activation energies, it was observed that the exponential model was better than the power law  
153 model in describing the dependency of  $E_a$  on °Brix concentration.

154

155

156

157



158 **Combined effect of Temperature and Concentration**

159

160 For practical applications, it is useful to obtain an equation describing the combined effect of  
161 temperature and concentration on viscosity [27]. The combined influence of temperature and  
162 concentration on honey viscosity is represented in figure 2. The following models for viscosity  
163 (eq. 7 and 8) were investigated:

164 
$$\eta = \eta_3 \exp(E_1 C + E_a / RT) \quad (7)$$

165 
$$\eta = \eta_4 C^{E_2} \exp(E_a / RT) \quad (8)$$

166 The viscosity, concentration, and temperature data were fitted to these models by non-linear  
167 regression and the values of the model constants were determined. The values of these constants  
168 are summarised in Table 5. The viscosity predictions with temperature and °Brix concentration  
169 achieve coefficients of regression between 0.67 and 0.77. The mean relative deviation *D* certifies  
170 that the suitable model corresponds to eq. 7. Therefore, for the interval of °Brix concentrations  
171 and temperatures (T) were studied the following equation (equation 9) is proposed to evaluate  
172 honey viscosity:

173 
$$\eta = 7.14 \cdot 10^{-19} \cdot \exp(0.16 * C + 76406 / RT) \quad (\text{eq. 9})$$

174

175 **Polynomial modelling of viscosity**

176

177 The data model regarding the prediction of honey viscosity according to its chemical  
178 composition (fructose, glucose, sucrose, sugars (the difference between °Brix concentration –  
179 reported as dry matter – and the sum of fructose, glucose and sucrose), non-sugars components  
180 (the difference, reported to 100 g, between 100 g and the sum of moisture content and °Brix

181 concentration), moisture content and temperature was made using a 3<sup>rd</sup> grade polynomial  
 182 equation with seven variables. The measured and predicted values have been compared to check  
 183 the suitability of the model. The equation of the model is shown below (eq. 10):

$$184 \quad \eta_{pred} = b_0 + \sum_{i=0}^n b_i x_i + \sum_{i=1}^n b_{ii} x_i^2 + \sum_{i=1}^n b_{iii} x_i^3 + \sum_{i<j<k} b_{ijk} x_i x_j x_k + \sum_{i<j}^n b_{ij} x_i x_j + \sum_{i<j}^n b_{ij} x_i^2 x_j + \sum_{i<j}^n b_{ij} x_i x_j^2 \quad (10)$$

185  
 186 where  $\eta_{pred}$  is the loss modulus predicted,  $b_0$  is a constant that fixes the response at the central  
 187 point of the experiments,  $b_i$  – regression coefficient for the linear effect terms,  $b_{ij}$  – interaction  
 188 effect terms,  $b_{ii}$  – quadratic effect terms and  $b_{iii}$  – cubic effect terms. The operating region and  
 189 the levels of the design variables (key factors) are given in actual and coded values as shown in  
 190 Table 6. Based on the design variables (Table 6) a 3<sup>rd</sup> order polynomial equation with 7 variables  
 191 for viscosity was obtained as follows (eq.11):

$$192 \quad \log(\eta) = 2.15 - 1.07 \cdot X_1 - 1.11 \cdot X_2 - 0.85 \cdot X_3 - 0.70 \cdot X_4 - 0.55 \cdot X_5 \\
 193 \quad - 0.26 \cdot X_7 - 1.60 \cdot X_7^2 - 0.68 \cdot X_1 \cdot X_7 - 0.71 \cdot X_2 \cdot X_7 - 0.65 \cdot X_3 \cdot X_7 - 0.36 \cdot X_4 \cdot X_7 \\
 - 0.07 \cdot X_5 \cdot X_7 + 0.01 \cdot X_7^3 + 1.65 \cdot X_1 \cdot X_7^2 + 1.68 \cdot X_2 \cdot X_7^2 + 1.27 \cdot X_3 \cdot X_7^2 + 1.07 \cdot X_4 \cdot X_7^2 \\
 + 0.53 \cdot X_5 \cdot X_7^2 \quad (11)$$

194  
 195 The coefficient of regression of the proposed model represents 99.91% ( $R^2$ adjusted 99.84%). The  
 196 model is a significant one ( $P=0.001$ ). In figure 3 the measured and predicted values of viscosity  
 197 are plotted.

198  
 199 **Loss modulus modelling**

200

9

201 **Influence of Temperature:** The influence of temperature on honey loss modulus is described by  
202 the Arrhenius model (equation 12):

203

$$204 \quad G'' = G_0'' \cdot \exp\left[-\frac{E_a}{RT}\right] \quad (12)$$

205

206 where  $G_0''$  is a constant,  $R$  is the gas constant [ $\text{kJ}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$ ], and  $E_a$  activation energy ( it is an  
207 energy barrier to flowing) [ $\text{kJ}\cdot\text{mol}^{-1}$ ],  $T$  – absolute temperature [K].The activation energy ( $E_a$ )  
208 values (tab.7), calculated by the Arrhenius model ranged between 80.82 – 95.05 kJ/mol. The  
209 magnitude of  $G''$  influenced the activation energy magnitude. The activation energy is  
210 negatively correlated with moisture ( $r = - 0.85$ ).

211

### 212 **Effect of Concentration**

213

214 The increase of honey loss modulus with soluble solid content ( $C$ , °Brix) can be described by  
215 power-law (eq. 13):

$$216 \quad G'' = G_1'' C^{b_1''} \quad (13)$$

217 and exponential models (eq.14) [24, 25]:

$$218 \quad G'' = G_2'' \exp(b_2'' C) \quad (14)$$

219 where  $G_1''$ ,  $G_2''$ ,  $b_1''$ ,  $b_2''$  are constants, and  $C$  is the concentration in °Brix. In order to calculate the  
220 model constants, the loss modulus data were fitted to equations 13-14 by non-linear regression.  
221 The resulting values of the constants are presented in table 8. The coefficients of regression ( $R^2$ )

222 are fairly the same so the two models are suitable for describing the effect of the soluble solids  
223 on honey loss modulus.

224

225 Taking into account the mean relative deviation, it seems that the exponential models are suitable  
226 for predicting the influence of the concentration on the magnitude of loss modulus. For a given  
227 temperature, the activation energy for flow depends on soluble solid content which can be  
228 described by several models [26]. Two models similar to equations 15 and 16 were used.

$$229 \quad E_a = A_1'' C^{B_1''} \quad (15)$$

$$230 \quad E_a = A_2'' \exp(B_2'' C) \quad (16)$$

231 where  $A_1''$ ,  $A_2''$ ,  $B_1''$  and  $B_2''$  are constants. The  $E_a$  values and their respective concentrations were  
232 fitted to equations 15 and 16 by non-linear regression to determine the model parameters. The  
233 calculated parameters for these models are given in table 9. The coefficients of regression ( $R^2$ ) of  
234 the two models proposed above are the same. Computing the mean relative deviation (eq.1) of  
235 the activation energies, it was observed that the exponential model was better than the power law  
236 model in describing the dependency of  $E_a$  on °Brix concentration.

237

### 238 **Combined effect of Temperature and Concentration**

239

240 For practical applications, it is useful to obtain an equation describing the combined effect of  
241 temperature and concentration on honey loss modulus [27]. The combined influence of  
242 temperature and concentration on honey loss modulus is presented in figure 4. The following  
243 models for loss modulus (equations 17 and 18) were investigated:

244

245 
$$G'' = G_3'' \exp(E_1'' C + E_a / RT) \quad (17)$$

246 
$$G'' = G_4'' C^{E_2''} \exp(E_a / RT) \quad (18)$$

247

248 The loss modulus, concentration, and temperature data were fitted to these models by non-linear  
 249 regression and the values of the model constants were determined. The values of these constants  
 250 are summarised in Table 10. The loss modulus predictions with temperature and °Brix  
 251 concentration achieve coefficients of regression between 0.65 and 0.75. The mean relative  
 252 deviation  $D$  certifies that the suitable model corresponds to eq. 17. Therefore, for the interval of  
 253 °Brix concentrations and temperatures (T) studied, the following equation (eq. 19) is proposed to  
 254 evaluate the loss modulus ( $G''$ ) of honeys:

255

256 
$$G'' = 2.23 \cdot 10^{-10} \cdot \exp(0.19 * C + 71630 / RT) \quad (\text{eq. 19})$$

257

258 **Polynomial modelling of loss modulus**

259

260 The data model regarding the prediction of honey loss modulus ( $G''$ ) according to its chemical  
 261 composition (fructose, glucose, sucrose, sugars (the difference between °Brix concentration –  
 262 reported as dry matter – and the sum of fructose, glucose and sucrose), non-sugars components  
 263 (the difference, reported to 100 g, between 100 g and the sum of moisture content and °Brix  
 264 concentration), moisture content and temperature was made using a 3<sup>rd</sup> grade polynomial  
 265 equation with seven variables (according to table 6). The equation of the model is as follows (eq.  
 266 20):

267 
$$G''_{pred} = b_0 + \sum_{i=0}^n b_i x_i + \sum_{i=1}^n b_{ii} x_i^2 + \sum_{i=1}^n b_{iii} x_i^3 + \sum_{i<j<k} b_{ijk} x_i x_j x_k + \sum_{i<j} b_{ij} x_i x_j + \sum_{i<j} b_{ij} x_i^2 x_j + \sum_{i<j} b_{ij} x_i x_j^2 \quad (20)$$

268 where  $G''_{pred}$  is the loss modulus predicted,  $b_0$  is a constant that fixes the response at the central  
 269 point of the experiments,  $b_i$  – regression coefficient for the linear effect terms,  $b_{ij}$  – interaction  
 270 effect terms,  $b_{ii}$  – quadratic effect terms and  $b_{iii}$  – cubic effect terms. Based on the design  
 271 variables (Table 6) a 3<sup>rd</sup> order polynomial equation with 7 variables for loss modulus was  
 272 obtained as follows (eq. 21):

273 
$$\begin{aligned} \log(G'') = & -887.14 + 1498.77 \cdot X_1 + 1381.78 \cdot X_2 + 466.51 \cdot X_3 + 1714.68 \cdot X_4 + 27.09 \cdot X_5 \\ & + 476.13 \cdot X_6 + 2962.67 \cdot X_7 + 1.38 \cdot X_1^2 - 1.89 \cdot X_2^2 + 1.77 \cdot X_3^2 - 1.64 \cdot X_4^2 - 3.77 \cdot X_5^2 \\ & - 2075.60 \cdot X_7^2 - 4993.87 \cdot X_1 \cdot X_7 - 4604.92 \cdot X_2 \cdot X_7 - 1555.18 \cdot X_3 \cdot X_7 - 5714.61 \cdot X_4 \cdot X_7 \\ & - 91.68 \cdot X_5 \cdot X_7 + 0.07 \cdot X_7^3 - 3.21 \cdot X_1^2 \cdot X_7 + 3492.46 \cdot X_1 \cdot X_7^2 + 4.57 \cdot X_2^2 \cdot X_7 \\ & + 3221.87 \cdot X_2 \cdot X_7^2 - 4.11 \cdot X_3^2 \cdot X_7 + 1088.83 \cdot X_3 \cdot X_7^2 + 3.72 \cdot X_4^2 \cdot X_7 + 3998.68 \cdot X_4 \cdot X_7^2 \\ & + 8.90 \cdot X_5^2 \cdot X_7 + 66.75 \cdot X_5 \cdot X_7^2 + 1114.11 \cdot X_6 \cdot X_7^2 \end{aligned} \quad (21)$$

274  
 275 The coefficient of regression of the proposed model represents 99.71 ( $R^2$ adjusted 99.50). The  
 276 model is a significant one ( $P=0.001$ ). In figure 5 the measured and predicted values of loss  
 277 modulus are plotted.

278  
 279 **CONCLUSIONS**

280 Spanish honeys present a Newtonian behaviour, while from the viscoelastic point of view it  
 281 behaves like a liquid with loss modulus much greater than the elastic modulus in the domain of  
 282 the temperature used (5-40 °C). The viscosity, loss and modulus are influenced negatively by the  
 283 increasing of the temperature, and positively by °Brix concentration. The exponential models are  
 284 much suitable for predicting the influence of °Brix concentration on loss modulus and viscosity.  
 285 In the case of viscosity and loss modulus a model of the influence of temperature and °Brix

286 concentration was obtained. Based on the experimental design results, the cubic polynomial  
287 models with 7 variables were developed for predicting the loss modulus as a combination of  
288 design variables, namely fructose, glucose, sucrose, sugars, non-sugars, moisture content and  
289 temperature. The polynomial models were statistically validated by F-ratio test.

290

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356 Tab. 1. Physicochemical parameters of honey

Parameter	Value
	Mean (standard deviation)
Fructose (g/100 g honey)	36 (4)
Glucose (g/100 g honey)	30 (3)
Sucrose (g/100 g honey)	2 (1)
F/G	1.2 (0.1)
Sugars (g/100 g honey)	14 (4)
Moisture content (g/100 g honey)	18 (1)
Non-sugar substances (g/100 g honey)	1.69 (0.06)

357

358 Tab.2. Influence of temperature on honey viscosity

Sample	$\eta_0$ [mPa·s]	Ea [kJ/mol]	R2
H1	$9.26 \cdot 10^{-16}$	94.59	0.99
H2	$6.41 \cdot 10^{-15}$	92.10	0.99
H3	$9.98 \cdot 10^{-15}$	91.60	0.99
H4	$2.02 \cdot 10^{-15}$	92.41	0.99
H5	$1.43 \cdot 10^{-15}$	93.60	0.99
H6	$3.29 \cdot 10^{-15}$	98.56	0.98
H7	$7.56 \cdot 10^{-15}$	101.87	0.99
H8	$6.59 \cdot 10^{-15}$	93.08	0.99
H9	$9.73 \cdot 10^{-16}$	100.28	0.99
H10	$2.82 \cdot 10^{-15}$	90.78	0.99
H11	$1.57 \cdot 10^{-15}$	99.86	0.99

359

360 Tab.3. Effect of °Brix concentration (C) on the honey's viscosity at different temperature (T)

	Power law				Exponential model			
	$\eta_1$	$a_1$	$R^2$	D	$\eta_2$	$a_2$	$R^2$	D
5	$2 \cdot 10^{-11}$	60.12	0.98	6.28	$1 \cdot 10^{-24}$	0.74	0.98	5.90
10	$2 \cdot 10^{-11}$	60.96	0.98	6.97	$2 \cdot 10^{-25}$	0.75	0.98	5.52
15	$2 \cdot 10^{-96}$	50.84	0.98	4.13	$2 \cdot 10^{-21}$	0.63	0.98	4.09
20	$1 \cdot 10^{-91}$	48.18	0.98	3.75	$2 \cdot 10^{-20}$	0.59	0.98	3.45
25	$9 \cdot 10^{-91}$	47.59	0.98	2.06	$2 \cdot 10^{-20}$	0.59	0.98	2.02
30	$7 \cdot 10^{-86}$	44.93	0.99	3.51	$1 \cdot 10^{-19}$	0.55	0.99	3.32
40	$7 \cdot 10^{-89}$	46.27	0.97	1.48	$1 \cdot 10^{-20}$	0.57	0.98	0.95

<i>D</i> -mean				4.03				3.61
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362 Tab.4. Influence of the °Brix concentration on the viscosity's activation energy

Model	$\eta$			
	$A_i^*$	$B_i^*$	$R^2$	$D$
$E_a = A_1 \cdot C^{B_1}$	$1.01 \cdot 10^{-4}$	2.85	0.98	0.52
$E_a = A_2 \cdot \exp(B_2 C)$	5.39	$3.50 \cdot 10^{-3}$	0.98	0.54

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364 Tab.5. Combined effect of °Brix concentration and temperature on the honey's viscosity

Model	$\eta$ [mPa·s]	$E_i$	$E_a$	$R$	$D$
$\eta = \eta_3 \exp(E_1 C + E_a / RT)$	$7.14 \cdot 10^{-19}$	0.16	76.41	0.77	20.26
$\eta = \eta_4 C^{E_2} \exp(E_a / RT)$	$3.90 \cdot 10^{-14}$	-0.89	91.15	0.68	30.15

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366 Tab.6. Correspondence between actual and coded values of design variables

Design variables	Symbol	Actual values of coded levels	
		-1	+1
Fructose (g/100g)	$X_1$	31.50	42.47
Glucose (g/100g)	$X_2$	24.40	34.52
Sucrose (g/100g)	$X_3$	0.00	3.42
Sugars (g/100g)	$X_4$	3.26	15.82
Moisture content (g/100g)	$X_5$	15.60	19.10
Non-sugar substances (g/100g)	$X_6$	1.59	1.80
Temperature (°C)	$X_7$	5	40

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375 Tab.7. Influence of temperature on honey loss modulus

Sample	G''		
	Go'' [mPa]	E <sub>a</sub> [kJ/mol]	R <sup>2</sup>
H1	9.20·10 <sup>-14</sup>	89.00	0.99
H2	4.10·10 <sup>-14</sup>	84.99	0.99
H3	8.80·10 <sup>-14</sup>	83.24	0.99
H4	2.10·10 <sup>-14</sup>	86.86	0.99
H5	1.30·10 <sup>-14</sup>	88.09	0.99
H6	5.90·10 <sup>-15</sup>	92.15	0.99
H7	2.52·10 <sup>-14</sup>	95.05	0.99
H8	1.09·10 <sup>-13</sup>	87.73	0.99
H9	1.22·10 <sup>-12</sup>	80.82	0.99
H10	6.41·10 <sup>-14</sup>	89.76	0.99
H11	3.34·10 <sup>-14</sup>	93.02	0.99

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377 Tab.8. Effect of °Brix concentration (C) on the honey loss modulus at different temperature (T)

	Power law model $G'' = G_1'' C^{b_1''}$				Exponential model $G'' = G_2'' \cdot \exp(b_2'' C)$			
	G <sub>1</sub> '' [mPa]	b <sub>1</sub> ''	R <sup>2</sup>	D	G <sub>2</sub> '' [mPa]	b <sub>2</sub> ''	R <sup>2</sup>	D
<b>5</b>	3·10 <sup>-114</sup>	60.99	0.97	12.48	3·10 <sup>-24</sup>	0.75	0.97	12.90
<b>10</b>	2·10 <sup>-114</sup>	60.94	0.99	26.97	1·10 <sup>-24</sup>	0.75	0.99	23.52
<b>15</b>	1·10 <sup>-95</sup>	50.84	0.98	24.13	1·10 <sup>-20</sup>	0.62	0.98	26.69
<b>20</b>	9·10 <sup>-91</sup>	48.17	0.99	3.75	1·10 <sup>-19</sup>	0.59	0.99	3.45
<b>25</b>	8·10 <sup>-90</sup>	47.54	0.99	6.06	1·10 <sup>-19</sup>	0.58	0.99	5.40
<b>30</b>	5·10 <sup>-85</sup>	44.89	0.99	2.51	9·10 <sup>-19</sup>	0.55	0.99	3.32
<b>40</b>	5·10 <sup>-88</sup>	46.27	0.98	6.48	9·10 <sup>-20</sup>	0.57	0.98	3.95
<b>D - mean</b>				11.76				11.32

378

379 Tab.9. Influence of the °Brix concentration on the loss modulus's activation energy

Model	G''			
	A <sub>1</sub> ''	B <sub>1</sub> ''	R <sup>2</sup>	D
$E_a = A_1'' C^{B_1''}$	5·10 <sup>-6</sup>	3.78	0.94	3.41
$E_a = A_2'' \exp(B_2'' C)$	2.021	0.05	0.94	1.65

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381 Tab.10. Combined effect of °Brix concentration and temperature on the honey's loss modulus

Model	G <sub>i</sub> '' [mPa]	E <sub>i</sub> ''	E <sub>a</sub> (kJ/mol)	R <sup>2</sup>	D
$G'' = G_3'' \exp(E_1'' C + E_a / RT)$	2.23·10 <sup>-10</sup>	0.19	71.63	0.78	1723.40

$G'' = G_3'' \cdot C^{E_2} \exp(E_a / RT)$	$1.49 \cdot 10^{-12}$	-0.78	99.87	0.67	2893.30
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