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Additional Information

SHORT COMMUNICATION

Fluid flow and radiative nonlinear heat transfer over a stretching sheet

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Abstract   In the present paper, we endeavor to perform a numerical analysis in connection with the boundary layer flow induced in a quiescent fluid by a continuous sheet stretching with velocity u_w $(x) \sim x^{1/3}$ with heat transfer. The effects of thermal radiation using the nonlinear Rosseland approximation are investigated. We search for similarity solutions and reduce the problem to a couple of ordinary differential equations containing three dimensionless parameters: the radiation parameter N_R, the temperature ratio parameter θ_w and the Prandtl number Pr. The computational results for velocity, temperature and heat transfer characteristics are presented in both graphical and tabular forms.

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1. Introduction

In contrast to the well-known Blasius flow problem (see, for instance, Cortell, 2005), and ref. therein) which involves laminar viscous boundary layer fluid flow above a fixed flat plate, the flow of a viscoelastic fluid over a rigid plate moving steadily in an otherwise quiescent fluid is sometimes referred to as Sakiadis flow (see Sakiadis, 1961) after the pioneering work of that researcher. Ahmad and Al-Barakati (2009) obtained an approximate analytical solution of the Blasius problem. Sakiadis flow's studies were recently dealt by Sadeghy et al.

(2005) in their work on boundary layer of an upper-convected Maxwell fluid flow where the role played by fluid's elasticity in the flow characteristics was analyzed.

When the difference between the sheet and the ambient temperature is large the thermal radiation effects become important, and also at high operating temperature the presence of thermal radiation alters the thermal boundary layer structure and the rate of heat transfer also results altered. In such industrial processes knowledge of radiative heat transfer becomes relevant. Abo-Eldahab and Azzam Gamal El-Din (2005) gave examples like nuclear power plants, gas turbines, satellites, etc. Viskanta and Grosh (1962) studied boundary layer flow in thermal radiation absorbing and emitting media by using the Rosseland approximation (Rosseland, 1931). Numerical results for hydro-magnetic mixed convection flow over a permeable non-isothermal wedge were reported by Prasad et al. (2013). Hossain et al. (1999) studied thermal radiation's effects using the Rosseland diffusion approximation on natural convection flow of an optically thick viscous

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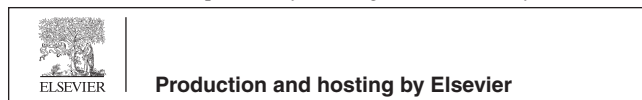
Nomenclature

c_P	Specific heat of the fluid at constant pressure J kg^{-1} K^{-1}
$\frac{d}{d\eta}$	Derivative with respect to η
f	Dimensionless stream function
k^*	Rosseland mean absorption coefficient m^{-1}
k	Fluid thermal conductivity W m^{-1} K^{-1}
L	Characteristic length m
N_R	Radiation parameter
Pr	Prandtl number
q_r	Component of radiative heat flux in y direction W m^{-2}
T	temperature K
u, v	Velocity components along x and y directions, respectively m s^{-1}

x, y	Cartesian coordinates along the plate and normal to it, respectively. m

Greek symbols

α	Thermal diffusivity m^2 s^{-1}
η	Dimensionless similarity variable
θ	Dimensionless temperature
μ	Absolute viscosity kg m^{-1} s^{-1}
υ	Kinematic viscosity m^2 s^{-1}
ρ	Density kg m^{-3}
σ^*	Stefan-Boltzmann constant W m^{-2} K^{-4}

Subscripts

w, ∞	Conditions at the surface and within the free stream, respectively

Superscript

prime	Derivative with respect to η

incompressible flow past a uniformly heated vertical porous surface with constant suction, and further, Hossain et al. (2001) analyzed the effect of variable viscosity on this type of flow. On the other hand, Raptis and Perdikis (1998) used a linearized form of the aforesaid Rosseland approximation in view to analyze the steady flow of a visco-elastic fluid past an unmoving surface. These simplifications permit an easier analysis, and many investigations (see, for instance, Cortell, 2008a,2011a; Abdul Hakeem et al., 2013) have been carried out in the recent past that deal with thermal studies by applying the cited linearized form, which is derived by assuming sufficiently small temperature differences within the flow that may assure to express T^4 as a linear function of temperature. Studies about motion and mass transfer with chemically reactive species in a porous space were recently undertaken by Cortell (2007a, 2007b). Moreover, treatments to the radiative heating for flows generated by linear/nonlinear stretching sheets enclosing magneto-hydrodynamics, non-Newtonian fluids, porous media, etc. constitute analytical or numerical attempts which have been made in the recent past (Arpaci, 1968; Cortell 2008b, 2011b, 2012a, 2012b; Turkyilmazoglu, 2011; Misra and Sinha, 2013). The problem of steady micropolar fluid flow past a stretching surface has been devised by many authors (see, for instance, Ishak, 2010; Hsiao, 2010) and even, very recently, unsteady fluid flow with (Hsiao, 2012) or without (Bachok et al., 2011) thermal radiation effects has also been analyzed.

One of the objectives of the present paper is to extend the investigation of Cortell (2008c) to analyze the Sakiadis flow generated by a sheet stretched with a velocity which is assumed to be proportional to the $x^{1/3}$ quantity, x being the distance from the slit. We also assume appropriate boundary conditions for the energy equation that may assure the existence of similarity solutions (i.e., constant temperature at the surface) when radiative nonlinear heat transfer is studied. Very recently, Rahman and Eltayeb (2013), Pantokratoras and Fang (2013) used the Rosseland diffusion approximation in studying radiative nonlinear heat transfer in different geometries. Unlike the linearized Rosseland approximation which is derived by assuming sufficiently small temperature differences between the plate and the ambient fluid, when use is made of

the nonlinear Rosseland diffusion approximation one can obtain results for both small and large differences between T_w (constant surface temperature) and T_∞ (the constant ambient fluid temperature). It is also known that the inclusion of nonlinear radiative effects in the energy equation had led to a highly nonlinearity in the governing equations (see El-Hakim and Rashad, 2007).

The fluid is at rest and the motion is created by the surface whose velocity varies nonlinearly with the distance x from a fixed point and the sheet is held at a temperature higher than the temperature T_∞ of the ambient fluid. For the stated problem and to our knowledge, the presented data on thermal analysis have not been considered before.

This paper aims to find similarity numerical solutions for problem above-mentioned. In Section 2 we shall examine the analysis of the flow and its mechanical characteristics. Heat transfer of a viscous fluid over a nonlinear stretching sheet in the presence of thermal radiation will be analyzed in Sections 3–4 by means of the nonlinear Rosseland diffusion approximation. The paper ends with its conclusions in Section 5.

2. Flow analysis

Let us consider the flow of an incompressible viscous fluid past a flat sheet coinciding with the plane $y = 0$, the flow being confined to $y > 0$. Two equal and opposite forces are applied along the x-axis so that the wall is stretched keeping the origin fixed. The fluid is assumed to be a gray, absorbing-emitting but non-scattering medium. Use is made of usual notation and then we can express the basic equations describing the conservation of mass and momentum in the boundary layer as

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = \upsilon\frac{\partial^2 u}{\partial y^2}, \tag{2}$$

where (x, y) denotes the Cartesian coordinates along the sheet and normal to it, u and v are the velocity components of the fluid in the x and y directions, respectively, and $\upsilon(= \frac{\mu}{\rho})$ is the

kinematic viscosity; ρ is the fluid density and μ is the absolute viscosity.

The mass and momentum Eqs. (1) and (2) must be solved subject to the boundary conditions

$$u_w(x) = \frac{\upsilon}{L^{\frac{1}{3}}} x^{\frac{1}{3}}, \quad v = 0 \; at \; y = 0, u \to 0 \; as \; y \to \infty. \tag{3}$$

where L is a characteristic length.

Now we introduce the following non-dimensional variables.

$$\eta = y \frac{x^{\frac{-1}{3}}}{L^{\frac{2}{3}}}, u = \frac{\upsilon}{L^{\frac{1}{3}}} x^{\frac{1}{3}} f'(\eta), \; v = -\frac{\upsilon}{L^{\frac{1}{3}}} x^{\frac{-1}{3}} \frac{[2f - \eta f']}{3}, \tag{4}$$

It is clear that u and v satisfy the equation of continuity (i.e., Eq. (1)). Introducing these new variables in Eq. (2) we get

$$3 \frac{d^3 f}{d\eta^3} + 2f \frac{d^2 f}{d\eta^2} - \left(\frac{df}{d\eta}\right)^2 = 0, \tag{5}$$

where $\frac{d}{d\eta}$ denotes differentiation with respect to the independent similarity variable η and f is the dimensionless stream function. The boundary conditions (3) can now be written as

$$f = 0, \; f' = 1 \; at \; \eta = 0, \; f' \to 0 \; as \; \eta \to \infty. \tag{6}$$

The numerical complete solution to the problem (5–6) is depicted in Fig. 1. It was already solved by Cortell (2008c) numerically by employing a Runge-Kutta algorithm for high order initial value problems (see Cortell, 1993). Based on that numerical solution, we have $f''(0) = -0.677647$ and we will utilize this numerical result in the following. Further, it is observed from Fig. 1 that the velocity component u decreases in the boundary layer with increase of η.

3. Heat transfer analysis

By using usual boundary layer approximations, the equation of the energy for temperature T in the presence of thermal radiation is given by

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} - \frac{1}{\rho c_P} \frac{\partial q_r}{\partial y} \tag{7}$$

where α is the thermal diffusivity, c_P is the specific heat of the fluid at constant pressure and q_r is the radiative heat flux in y direction.

Using the Rosseland approximation for radiation (Rosseland, 1931), the radiative heat flux is simplified as

$$q_r = -\frac{4\sigma^*}{3k^*} \frac{\partial T^4}{\partial y}, \tag{8}$$

where σ^* and k^* are the Stefan-Boltzmann constant and the mean absorption coefficient, respectively.

At this stage, it is necessary to note that for a boundary layer flow over a horizontal flat plate (see Pantokratoras and Fang, 2013), from Eq. (8) we get

$$q_r = -\frac{16\sigma^*}{3k^*} T^3 \frac{dT}{dy}, \tag{9}$$

where T is the temperature across the boundary layer. We have supposed T as x-independent, and in view to Eq. (9), Eq. (7) reduces to

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{d}{dy} \left[(\alpha + \frac{16\sigma^* T^3}{3\rho c_P k^*}) \frac{dT}{dy} \right]. \tag{10}$$

where $\alpha = \frac{k}{\rho c_P}$, k being the thermal conductivity. From the above equation it is seen that the effect of radiation is to enhance the variable thermal diffusivity, which is now T-dependent.

The boundary conditions are

$$T = T_w \; at \; y = 0; \quad T \to T_\infty \; as \; y \to \infty \tag{11}$$

with $T_w \rangle T_\infty$, and T_∞ is the fluid temperature far away from the surface, T_w is the temperature at the wall.

By defining the non dimensional temperature $\theta(\eta)$ as

$$\theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty} \tag{12}$$

we obtain $T = T_\infty(1 + (\theta_w - 1)\theta)$, with $\theta_w = \frac{T_w}{T_\infty}$, $\theta_w \rangle 1$) being the temperature ratio parameter.

Taking into account the above we get

$$-\frac{\partial q_r}{\partial y} = \frac{16\sigma^* T_\infty^3}{3k^*} \cdot \frac{x^{\frac{-2}{3}}}{L^{\frac{4}{3}}} (T_w - T_\infty) \cdot \frac{\partial}{\partial \eta} \left[[1 + \theta(\theta_w - 1)]^3 . \theta' \right] \tag{13}$$

Substituting Eqs. (4) and (13) into Eq. (7) and after some algebra one can write

$$-\frac{2\upsilon}{3} f\theta' = \frac{k}{\rho c_P} \theta'' + \frac{16\sigma^* T_\infty^3}{3\rho c_P k^*} \cdot \frac{\partial}{\partial \eta} [[1 + \theta(\theta_w - 1)]^3 . \theta'] \tag{14}$$

and further the final energy equation can be expressed as

$$\frac{4}{3N_R} \cdot \frac{d}{d\eta} [(1 + \theta(\theta_w - 1))^3 \theta'] + \theta'' = -\frac{2}{3} \Pr f\theta'. \tag{15}$$
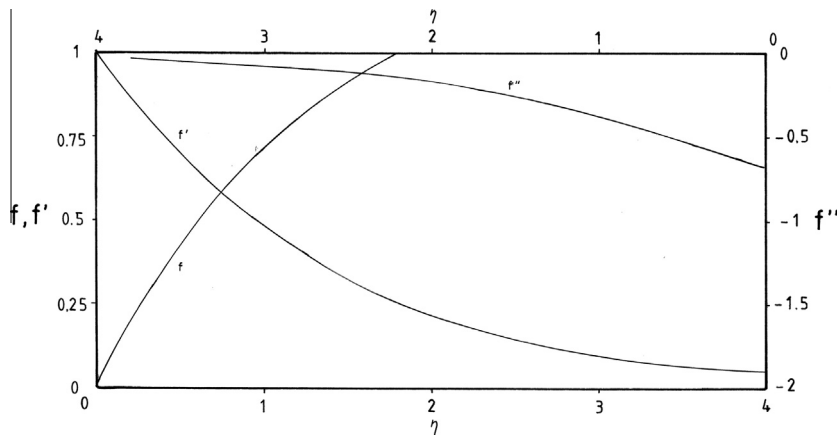

Figure 1 Plot of the functions f, f' and f'' for problem (5 and 6)

In the above equation $\Pr(= \frac{v}{\alpha})$ is the Prandtl number, both $\frac{d}{d\eta}$ and the prime denote differentiation with respect to η and $N_R = \frac{k^*k}{4\sigma^*T_\infty^3}$ is the radiation parameter.

The boundary conditions for $\theta(\eta)$ can now be expressed as

$$\theta = 1 \ at \ \eta = 0, \ \theta \to 0 \ as \ \eta \to \infty \tag{16}$$

Taking into account the thermal radiation, we can express the surface heat flux as:

$$q_w = -k\left(\frac{\partial T}{\partial y}\right)_w + (q_r)_w$$
$$= -\frac{k(T_w - T_\infty)}{L}\left(\frac{x}{L}\right)^{-\frac{1}{3}}\left[1 + \frac{4\theta_w^3}{3N_R}\right]\theta'(0). \tag{17}$$

with $\theta_w \rangle 1$. $N_R \to \infty$ implies no thermal radiation's effects, and then Eqs. (15) and (17) reduce to

$$\theta'' + \frac{2}{3}\Pr f\theta' = 0; \ q_w = -k\frac{T_w - T_\infty}{L}\left(\frac{x}{L}\right)^{\frac{-1}{3}}.\theta'(0), \tag{18}$$

which coincide with Eqs. (17) and (20) in Cortell, 2008c putting there $m = 0$ and $E_c = 0$ (i.e., constant surface temperature and without viscous dissipation) along with $k_0 = 1$ (no thermal radiation's effects).

4. Results and discussion

Without a break, we begin now the development of the procedure for completing the numerical solution for $\theta(\eta)$. There is no any analytical solution for the momentum transfer problem and, accordingly, one had to use numerical techniques. It is clear that $f''(0) = -0.677647$ (Cortell, 2008c) in that problem. Hence, the present numerical analysis extends the most recent thermal study of Cortell, 2008c to the case of nonlinear Rosseland approximation for thermal radiation, and with its use we will obtain numerical values of $\theta'(0)$ (i.e., temperature-gradient at the wall) in order to show the influences of the dimensionless parameters Pr, θ_w and N_R onto the heat transfer characteristics and temperature distributions. Since the flow problem is uncoupled from the thermal problem, changes in the values of Pr, θ_w and N_R will not affect the fluid velocity. For this reason, both the function f and its derivatives are identical in the complete problem (flow and heat transfer). In view of the above discussions, use will be made of $f''(0) = -0.677647$

(Cortell, 2008c) and, with this result, we shall solve numerically the momentum and heat transfer problems. The best approximate for solving Eqs. (5), (6), (15–16) that can be used is the Runge-Kutta fourth order numerical method with shooting procedure (see White, 1991). Many other results are obtained throughout this work, and hence a selected set of results is presented graphically in Figs. 2–4 in order to analyze the distinct physical aspects of the problem. The effects of Prandtl number Pr on temperature profiles are depicted in Fig. 2 at $\theta_w = 1.5$ and $N_R = 1$. From this figure one can immediately observe that the thermal boundary layer thicknesses decrease drastically with an increase in Pr and, as a consequence, an increase (in absolute sense) in the wall temperature gradient occurs. Low Prandtl number Pr indicates fluids with large thermal conductivity and this produces thicker thermal boundary layer structures than that for high Pr number.

Fig. 3 illustrates the effect of temperature ratio parameter θ_w on $\theta(\eta)$ curves. It should be noticed that increasing the temperature ratio parameter θ_w increases the thermal state of the fluid, resulting in increases in temperature profiles. However, as the thermal radiation parameter N_R increases, it is observed from Fig. 4 that the temperature profiles decrease and then the thermal boundary layer thicknesses shrink.

As was already pointed out by Rahman and Eltayeb (2013) when use is made of the nonlinear Rosseland approximation to take into account thermal radiations effect a point of inflection appeared on temperature profiles. In this paper, making use of our numerical approach, we find out the full set of η_∞ (i.e., the extent of our integration domain), $\theta(\eta)$, and $\theta'(\eta)$ results, and for each studied case, we will be able to give the location of the aforesaid point onto temperature distributions.

In Table 1 we display some numerical results of $\theta(\eta)$ and $\theta'(\eta)$ when Pr = 3; $\theta_w = 1.5$ and $N_R = 1$.. The computed values displayed in Table 1 indicate that the point of inflection for the $\theta(\eta)$ curve is located at $\eta = 0.84$ when $|\theta'(\eta)|$ reaches its maximum value in the interval $[0, \eta_\infty]$. For each set of fixed values of the three dimensionless parameters entering the problem, it is clear that an only missed value at $\eta = 0$ is guessed in our numerical approach, that is, the temperature-gradient at the wall $\theta'(0)$. The suitable guess value is chosen and the integration for heat transfer problem, Eqs. (15), (16), is carried out as an initial value problem by the Runge-Kutta shooting method of fourth order. For each numerical solution $\theta(\eta)$ the value
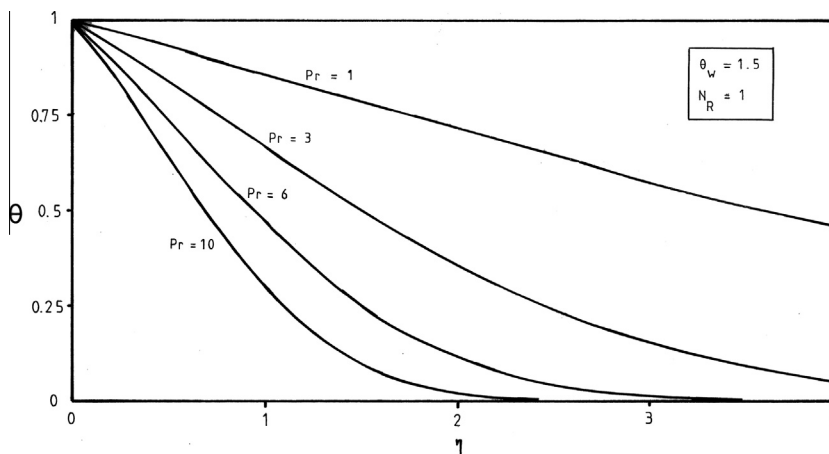

Figure 2 Effects of Prandtl number Pr on temperature profiles at $\theta_w = 1.5$ and $N_R = 1$.
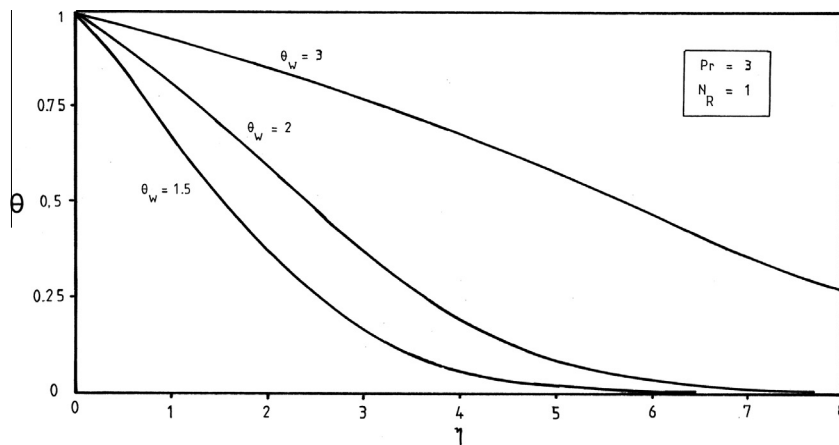
Figure 3   Effects of the temperature ratio parameter θ_w on temperature profiles at Pr $= 3$ and $N_R = 1$..
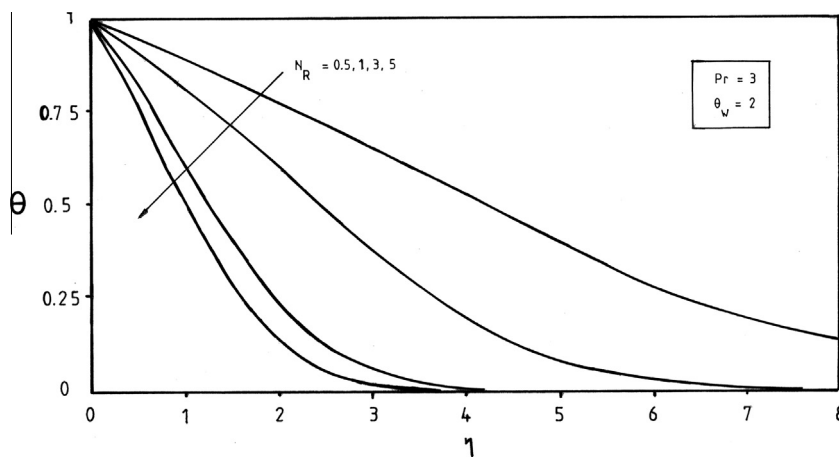

Figure 4   Effects of the thermal radiation parameter N_R on temperature profiles at Pr $= 3$ and $\theta_w = 2$.

Table 1   Some numerical results for $\theta(\eta)$ and $\theta'(\eta)$ with $\Delta\eta = 0.02$ when Pr $= 3$; $\theta_w = 1.5$ and $N_R = 1$.

η	$\theta(\eta)$	$-\theta'(\eta)$
0	1	0.304279
0.2	0.93773	0.317966
0.4	0.87303	0.328431
0.6	0.80659	0.335256
0.8	0.73919	0.338071
0.82	0.73243	0.338119
0.84	0.72567	0.338125
0.86	0.71891	0.338087
1	0.67165	0.336591
3	0.15644	0.145608
5	0.01999	0.021663
10	0.00015	0.000086

of $\theta'(0)$ is iteratively estimated under the simultaneous assumptions $\theta(\infty) \to 0$ and $|\theta'(\infty)| \to 0$ (see Table 1 in which temperature and temperature gradient profiles tend to zero at infinity simultaneously in an asymptotical fashion). Due to the fact no heat fluxes should exist outside the thermal boundary layer we

need here to adopt the extra boundary condition $\frac{d\theta}{d\eta} \to 0$ as $\eta \to \infty$, and in this manner we circumvent possible unphysical behaviors of the solution. The latter was already established in the literature for related problems (see Van Gorder and Vajravelu, 2010). Also, in accord with Van Gorder and Vajravelu (2010), we also adopted the extra boundary condition $\frac{d^2f}{d\eta^2} \to 0$ as $\eta \to \infty$ in Cortell (2008c) with a view to obtain $f''(0) = -0.677647$ numerically; however, the aforementioned numerical treatment has been used in our studies since early 1990s (see, for example, Cortell, 1994). On the other hand, during the last years, numerous comparisons between our own numerical data and results obtained by means of several numerical procedures were presented in the open literature (note, for instance, the recently published numerical data by Rohni et al. (2012)). In Rohni et al. (2012) a completion for the shrinking sheet case but without thermal radiation effects of the Cortell's paper (Cortell, 2012a) was carried out. Regarding existence and uniqueness of the solution, which we do not analyze in this short communication, boundary conditions (Van Gorder, 2010) and even additional terms in the energy equation (i.e., dissipative term) (Turkyilmazoglu and Pop, 2013) play an important role in these types of nonlinear boundary value problems.

Table 2 Flow and heat transfer characteristics for several values of the parameters entering the problem.

$-f''(0)$		Pr	θ_w	N_R	$-\theta'(0)$
0.677647	Cortell (2008c)	1	1.5	1	0.131636
		3			0.304279
		6			0.478746
		10			0.652147
		3	1.5	1	0.304279
			2		0.169978
			3		0.064057
		3	2	0.5	0.100474
				1	0.169978
				3	0.335764
				5	0.434466

Finally, the values of the wall temperature gradient $[-\theta'(0)]$ as a function of all the parameters of the thermal boundary layer treated in this work have been tabulated in Table 2. It is apparent from this table that the effect of Prandtl number Pr on $[-\theta'(0)]$ is such that the $|\theta'(0)|$ value increases sharply with an increase in Pr and hence produces an increase in the heat transfer rate. As can be expected, the heat transfer rate $|\theta'(0)|$ also increases as N_R increases with all other parameter fixed, that is, an increase in the radiation parameter N_R will produce a decrease in the thermal boundary layer thickness, associated with the reduction in the temperature profiles. However, an augment in θ_w yields an augment in $\theta(\eta)$ and the rate of heat transfer tends to zero as the temperature ratio parameter θ_w increases (see Table 2).

5. Conclusions

The thermal radiation effects on flow influenced by a nonlinearly stretching sheet were studied numerically. The radiative heat flux term in the energy equation is introduced by means of the nonlinear Rosseland diffusion approximation. The effects of various physical parameters like Pr, θ_w and N_R on heat transfer phenomena have been studied. It should also be concluded that in contrast to the linear Rosseland diffusion approximation, when use is made of the nonlinear one, the problem is also governed by the newly temperature ratio parameter θ_w. Similarity solutions for the case of stretching materials which have a wide variety of technical and environmental applications were found for all the aforementioned dimensionless physical parameters. The results presented indicate quite clearly that θ_w, which is an indicator of the small/large temperature difference between the surface and the ambient fluid, has a relevant effect on heat transfer characteristics and temperature distributions within the flow region generated by an isothermal sheet stretched in a non-linear fashion. From the above numerical research, the following conclusions may be drawn:

1. An increasing Prandtl number Pr causes diminution in the thickness of the thermal boundary layer.
2. For fixed Pr and N_R, the rate of heat transfer $|\theta'(0)|$ extinguishes as the temperature ratio parameter θ_w increases.

3. From a qualitative point of view, the temperature ratio parameter θ_w and the thermal radiation parameter N_R have the opposite effect, that is, temperature increases with increasing θ_w, whereas N_R does the reverse.

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