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Additional Information

Conversion of methanol to olefins: Stabilization of nanosized SAPO-34 by hydrothermal treatment

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Abstract

Nano-SAPO-34 zeolite catalyst (20 nm crystal size) has been stabilized by hydrothermal treatment. After steamed at high temperatures (T≥550°C), its textural properties and high lifetime during the reaction of methanol to olefins (MTO) are preserved, despite the decrease in acidity, even after months of contact with moisture. The stabilization effect is attributed to the migration of silicon to larger silicon islands in which the contribution of silicon on the edge is lower after steaming. Stabilization is not successful by a thermal treatment in air in the absence of water. Steaming at temperature >400°C is required for achieving hydrothermal stabilization. A stability test for SAPO-34 in MTO reaction is proposed.

Keywords

Methanol conversion, SAPO-34, deactivation, hydrothermal stabilization, nanocrystal.

1. Introduction

Nowadays, the high industrial demand for ethylene and propylene has renewed the interest on the reaction of methanol to olefins (MTO). In fact, more than 20 units are expected to operate in China in the next 2-3 years with an overall olefin capacity of more than 11 million Ton/year [1]. The feed methanol is obtained from reaction of synthesis gas on appropriate catalysts, being the synthesis gas obtained by gasification of coal or biomass and by steam-reforming of natural gas. The increasing amount of gas reserves due to the upcoming of shale gas have led to cheaper methane [2] and are expected to affect the market of methanol, renewing the interest for the MTO process [3]. If propylene is desired the catalyst used is based on high silica ZSM-5 (MTP process), which has a lifetime of 650 h in between the regeneration steps [4]. Another possibility is to use a catalyst based on silicoaluminophosphate SAPO-34 that can yield different C2=/C3= ratios depending on reaction conditions [5-7]. However, the latter catalyst has a much shorter lifetime than ZSM-5 due to the extension of coking reactions inside the cages of the CHA structure, and a continuous catalyst regeneration

process is required. Lifetime of SAPO-34 can be extended by using mesoporous SAPO-34 [8-12], by decreasing the size of the crystal [13-18] or by including metal oxides in the catalyst composition [19]. Smaller crystallites of SAPO-34 were achieved recently by heating the synthesis gel in a microwave apparatus [20, 21]. In this way, crystallites of 20nm sizes were obtained, and the resultant SAPO-34 presented much longer lifetimes than standard SAPO-34 samples. However, due to the small size of crystallites and the high external surface area, the material was very sensitive to hydrolysis by moisture at room conditions and suffered complete hydrolysis after months of storage. This behavior was already reported in the literature for more conventional SAPO-34 samples [22-25]. Briend et al. [22] related the lack of long-term stability to the presence of silicon islands, favored by the use of morpholine as template. Other authors [23, 26] showed that the structural deterioration can be prevented if after removing the template the acid sites are covered with ammonia.

In the present work we started from the hypothesis that it could be possible to increase the stability of SAPO-34 samples by performing a controlled hydrolysis of a part of the silicon, in an analogous way as it occurs with high aluminum zeolites that can be stabilized by controlled partial dealumination [27]. Therefore, we will present here the effect of the hydrothermal treatment at different temperatures on the long-term stability of nano and standard SAPO-34 materials. We will show how by an appropriate steaming temperature, nano-SAPO-34 becomes stabilized towards moisture. In addition, we will show that hydrothermal stability tests for SAPO-34, which are normally performed at very high temperatures (800°C) [1, 28, 29], should also include stability tests at reaction temperatures close to the reaction temperature used for MTO, to better ascertain the viability of this type of catalyst for the mentioned catalytic process.

2. Experimental.

2.1 Synthesis of materials

Nano-SAPO-34 was synthesized by microwave heating following the methodology of Lin et al. [13] and reported previously [21] by using TEAOH as the structure directing agent (SDA). The composition of the synthesis gel was 1 Al(OPri)₃ : 2 H₃PO₄ : 2 TEAOH : 0.3 SiO₂ : 30 H₂O : Al(OPri)₃. The crystallization was conducted in a microwave oven (Milestone ETHOS-D) with pre-programmed heating profiles at 180°C for 1hour. Then, the solid product was recovered by filtration washed with water and ethanol for 3 times and dried overnight at 50°C. The as-synthesized material was

calcined at 550°C in air for 6h to remove the SDA. A conventional sample of SAPO-34 was synthesized following hydrothermal method, with a mixture of morpholine and TEAOH 1:1 mol/mol as SDA being the composition of the gel $1 \text{ Al}_2\text{O}_3 : 1.06 \text{ P}_2\text{O}_5 : 1.08 \text{ SiO}_2 : 2.09\text{SDA} : 66 \text{ H}_2\text{O}$. The solution was introduced into Teflon-line autoclave and heated at 200°C for 24h. Then, the sample was treated following the same procedure to remove the SDA. This sample will be called standard-SAPO-34.

2.2 Characterization.

BET surface area, micropore volume and pore volume distribution were determined by N₂ adsorption and desorption in an ASAP2000. Crystallinity was measured by X-ray powder diffraction (XRD) with a Panalytical CUBIX diffract meter with monochromatic CuK α 1,2 radiation (λ =1.5406, 1.5444 Å; K α 2 / K α 1 intensity ratio=0.5). Chemical composition was analyzed by inductively coupled plasma atomic absorption spectroscopy (ICP-OES) using a Varian 715-ES apparatus. Acidity was measured by NH₃-TPD experiments carried out in a Micromeritics 2900 following the procedure reported earlier[17]. The MAS NMR spectra were recorded with a Bruker AV400 spectrometer. ²⁹Si MAS NMR spectra were at 79.459 MHz with a 60° pulse length of 4µs and 60s repetition time, spinning the sample at 5kHz. Deconvolution of ²⁹Si NMR bands corresponding to different Si environments was performed with Origin Pro 9.0 software with Gaussian shapes of constant width. ²⁷Al MAS NMR spectra were recorded at 104.218 MHz with a spinning rate of 10 kHz at a 90° pulse length of 0.5 µs with 1 s repetition time. ³¹P MAS NMR spectra were recorded at 161.9 MHz with a spinning rate of 10 kHz and at a 90° pulse length of 5 µs with 20s repetition time. ²⁹Si, ²⁷Al and ³¹P chemical shifts are reported relative to tetramethylsilane, Al(H₂O)₆, and H₃PO₄ respectively.

2.3 Catalytic experiments

50 mg of sample (0.2-0.4 mm) were mixed with 2 g quartz (Fluka) and placed in a quartz reactor. Methanol was fed by saturating N₂ (19mL/min) at 25°C, being the space velocity WHSV=7 h⁻¹. The catalyst was first activated with a nitrogen flow of 80 ml/min for 1 h at 540°C, and then the temperature was decreased to reaction conditions (400°C). Analysis of products was done each 5 min with an online gas chromatograph (BRUKER 450GC, with a 50m PONA and Al₂O₃-Plot capillary columns at 37°C of oven temperature, and two FID detectors). After reaction, the catalyst was regenerated

at 540°C in 80ml of air for 3h and the reaction was repeated again. Conversion and selectivities were calculated in carbon basis being methanol and dimethylether considered as feed.

3. Results and discussion

3.1 Crystallinity and acidity of SAPO-34 samples.

The XRD patterns of the calcined parent nano-SAPO-34 and steamed at different temperatures are shown in Fig.1. The broad shape and low intensity of the XRD of the parent material is characteristic of the small size of the crystals [21], which is around 20 nm (see Fig. 2). After steaming at temperatures of 550°C and 600°C, the diffraction patterns are still similar to that of nano-SAPO-34 suggesting that the structure of these samples is maintained. At 700°C a slight decrease in the intensity of the peaks is observed. However, the sample steamed at 400°C presents amorphous XRD pattern. In agreement with the XRD results, adsorption of nitrogen (Table 1) shows that the nano-SAPO-34 steamed at 400°C loses the microporosity while those steamed at higher temperatures preserve most of the textural properties with an optimum in microporosity for the sample steamed at 600°C. Even more important is the observation that for samples steamed at T≥550°C and exposed to moisture during days at room temperature, their crystallinity and micropore volume are preserved (Table 1 and Fig. 3), while non steamed template-free nano-SAPO-34 is negatively affected when exposed to moisture at room temperature. On the other hand, standard-SAPO-34 with larger cubic crystallites of around 500 nm is much less affected by steaming, with a smaller decrease in the BET surface after steaming at low (400) and high (700°C) temperatures.

When the acidity of the samples was measured by TPD of ammonia (Table 1 and Figure 4) the results indicate that, in general, steaming reduces the acidity of the samples when compared to the parent sample. This decrease is stronger in the case of the steaming at 700°C, while the samples steamed at 550 and 600°C present very similar acidity. When comparing the shape of the TPD desorption curves, it can be seen that all samples present a main component with a maximum in the range from 314 to 381°C, and a shoulder ca. 230°C (Fig. 3). The peak at higher temperature of desorption corresponds mainly to Brönsted acidity and the differences in the temperature of the maxima are better related to the amount of acid sites than to differences in acidity strength. The shoulder at low temperatures corresponds to physisorption of ammonia

and not to adsorption on catalytically active sites [30]. From the amounts of adsorbed ammonia given in Table 1, it can be seen that the decrease in acidity is proportionally larger than the decrease in micropore volume when increasing steaming temperatures (see Fig. 4). The results suggest that the hydrolysis of the acid sites when steaming do not necessarily imply a loss of crystallinity, i.e., a partial collapse of the structure but, as it occurs during a controlled steam dealumination process for high Al content zeolites in which silicon is reinserted in the framework, in the case of SAPO-34 can occur a migration of phosphorus to fill up some of the nests left by silicon. Let's investigate now by solid NMR the physicochemical transformations occurring in SAPO-34 upon steaming.

3.2 Solid NMR characterization.

The ²⁷Al MAS NMR spectra of nano-SAPO-34 given in Fig. 5 show an intense peak at 36 ppm and other two signals at -11 and 14 ppm for calcined nano-SAPO-34, that correspond to tetrahedrally coordinated aluminum in local structures of Al(PO)₄, and octa and pentacoordinated aluminum, respectively. After exposing the calcined sample to moisture at room temperature at increasing times, the octahedral Al signal at -14 ppm continuously increases, indicating hydration of the Al(PO)₄ species [24, 31]. Meanwhile, the signal of tetrahedral aluminum is shifted to 41 ppm, due to the distortion of the structure by interaction with water [32]. The ²⁷Al MAS NMR spectra of nano-SAPO-34 sample steamed at 700°C presents band intensities which are independent of the time of exposure and only a slight increase of octahedral aluminum is observed, indicating an increasing hydration effect with time.

The hydration effect is also evidenced through the ³¹P NMR spectra. Nano-SAPO-34 exhibits an asymmetrical signal at -30 ppm corresponding to tetrahedral P(OAl)₄. After 21 days of hydration, another signal at -16 ppm appears, which can be attributed to P(OAl)_x(H₂O)_y formed by P atoms coordinated with water [24, 26, 33]. After steaming the fresh nano-SAPO-34 sample at 700°C, the shoulder at -16 ppm appears, and slightly increases after long contact with moisture. This result correlates well with the increase in the signal of Al NMR at -14 ppm assigned to the hydration of the Al(PO)₄ species.

The ²⁹Si MAS NMR spectra give further information, and clear differences are observed with the hydrated-parent and steamed samples (Figure 5 and Table 2). The different silicon species of nano-SAPO-34 have been described elsewhere [21]. This

sample shows a large amount of silicon in silicon islands, Si3Al, Si2Al, Si1Al and SiOAl, which corresponds to the -95,-100, -,105 and -110 ppm bands respectively, and isolated silicon which is related to the band at -89 ppm. The fresh nano-SAPO-34 sample was shown to hydrolyze in contact with moisture by transforming silicon at the edge of the silicon islands (-95 ppm) into defective sites at -78-85 ppm. As we will see later this has an effect in activity, selectivity and deactivation of the catalyst during the reaction of methanol to olefins. However, when the fresh calcined sample is steamed, the population of isolated silicon Si4Al decreases which is in agreement with the reduction in acidity shown by TPD of ammonia. At the same time, the signals corresponding to silicon within silicon islands, especially SiOAl at -110 ppm, increases together with a reduction of silicon on the edge (Si3Al at -95) with no raise in defects (-78 to -85 ppm). In addition, the distribution of silicon species is not importantly affected when the steamed samples are contacted with moisture at room temperature. The above described effects are qualitatively similar for the sample steamed at 600 and 700°C, being the decrease of isolated silicon Si4Al species higher for the sample steamed at 700°C.

The results obtained here are in line with those previously reported for SAPO-34 and other SAPO's [31, 34, 35], in the sense that when they were thermally treated at high temperatures in the absence of added steam, part of silicon migrates to silicon islands while phosphorus healed the framework vacancies with no formation of defects. However, we have seen clear differences in the population of the different Si species and an impact on stability when the samples were steamed. The question then is what is the effect of steaming on the framework composition and its implication on stability to moisture, acidity, activity and selectivity for MTO.

Wilson and Barger [7, 36] studied the effect of hydrothermal treatment on the activity and selectivity of SAPO-34 and they observed no degradation of the structure and a longer lifetime. Recently, Aramburo et al. [25] reported no difference with the purely thermally treated samples [31, 34, 35], i.e., a reduction in acidity with migration of silicon species to silicon islands. However, in an earlier contribution Park et al. [37] showed that SAPO-34 thermally treated at 750°C loses more crystallinity after reaction with water than the fresh sample indicating that only thermal treatment does not stabilize SAPO-34 samples. If our original hypothesis on the positive effect of water on the mobility of silicon and phosphorus through the framework of SAPO-34, in a similar way as it occurs with aluminum and silicon during ultrastabilization without generation

of defects in zeolites, was possible in SAPO-34, a controlled steaming of the SAPO should stabilize towards the negative effect of moisture at room conditions on crystallinity. In this case, steam at high temperatures should facilitate the formation of larger silicon islands together with an easier reallocation of phosphorus occupying the vacancies left by silicon. This hypothesis is supported by a smaller amount of silicon species on the edge of the silicon islands found in steamed samples, as deduced from silicon NMR with an increase in the signals of silicon islands upon steaming. Theoretical calculations on the role of steaming on clusters of isomorphous zeolite SSZ-13 and SAPO-34 [38] also to support our hypothesis on the effect of steaming on SAPO-34 stability.

In summary, we can say that steaming produces a decrease of isolated Si species and its migration to silicon islands which grow in size, as suggested by the decrease of silicon species at the edge of silicon islands. The effect of steaming on lowering the amount of Si at the border of Si islands can explain the lower extension of hydrolysis in the steamed samples upon exposure to moisture at room temperature. This, in turn, would be responsible for the higher stability of the steamed samples.

- 3.3 Catalytic activity.
- 3.3.1 Influence of stabilization on catalyst activity and lifetime.

The activity of calcined and steamed nano-SAPO-34 is shown in Fig. 7. The experiments were performed at WHSV=7h⁻¹ and 400°C of reaction temperature. Nano-SAPO-34 samples steamed at 550, 600 and 700°C present a lifetime close to fresh nano-SAPO-34, though clear differences appear in the slope or the time at which catalyst deactivation starts to be observed. Here we have fitted the experimental data to the kinetic model developed by Janssens [39]. This model is able to separate the contribution of activity (K) from the deactivation rate (a) on ZSM-5 and was also successfully applied to SAPO-34 [21]. By doing that, the effect of steaming temperature is clearly visible. Indeed, the results in Table 3 indicate that activity (K) decreases when increasing the steaming temperature and that decrease correlates well with the decrease of acidity measured by TPD of ammonia. On the other hand, the rate of deactivation, which is also a measure of the catalyst half lifetime, is maintained despite the decrease of overall acidity due to steaming. Therefore, steaming decreases the activity of the catalyst while deactivation rate does not increase. However, the most important observation is that the samples steamed at temperatures ≥550°C present a similar

activity and lifetime after days, and even months, of contact with moisture at room temperature. This result would be consistent with the preservation of micropore volume and acidity of steamed samples observed upon exposure to moisture for long periods of time. The long-term stability must be related to the decrease of silicon at the edge of silicon islands due to both, migration of silicon and merging of small to larger islands in which the contribution of edges is less important. In addition, the decrease of Si species at the edge (Si3Al) is also responsible for the longer lifetime of the remaining acid sites since those sites have been considered strongly acid [40-42] and thus, more prone to deactivation by coking.

When the micropore volume of steamed samples of nano-SAPO-34 was plotted versus the temperature of steaming, it appears that an optimum steaming temperature may exist between 600 and 700°C. In fact, at lower steaming temperatures samples are hydrolyzed as shown by BET measurements, while at higher temperatures the decrease in acidity produced is larger with the correspondent loss of activity observed (Fig. 4).

Finally, a sample of nano-SAPO-34 which was only thermally treated in air at 750°C was also tested when fresh and after being in contact with moisture at increasing times. It can be clearly seen in Figure 8 that despite the high initial lifetime of the fresh thermally treated sample, this strongly decreases when contacted with moisture. This result is in clear contrast what it occurs with the samples steamed at T≥550°C that retain their microporosity, acidity and activity upon exposure to moisture.

3.3.2 Influence of stabilization on catalyst selectivity

Selectivity at constant conversion of the steamed samples is shown in Fig. 9. Notice that in the case of MTO it is mandatory to compare the selectivities at the same level of conversion. By doing that, the effect of thermodynamic equilibrium among olefins at high methanol conversion, can be isolated from the true selectivity of the hydrocarbon pool in SAPO-34. In fact, it was shown recently [21] that as the hydrocarbon pool forms through the catalytic bed, its selectivity is modified by further secondary reaction on the fresh portion of the catalyst, approaching thermodynamic equilibrium and masking therefore the selectivity obtained.

When comparing different selectivities of steamed samples at constant conversion it can be seen that $C_2^{=}/C_3^{=}$ ratio decreases after steaming when compared with calcined nano-SAPO-34, being the decrease more marked at 700°C of steaming temperature (Fig. 10). More specifically, the results show an effective decrease of the

selectivity to ethylene, while the distribution among the other olefins is not affected. This effect on the selectivity of ethylene must be related to the decrease in the strength of the acid sites due to the formation of larger silicon islands and the consequent decrease in the density of silicon species located at the edge, when compared with the calcined parent sample, as it is supported by ²⁹Si NMR results (Table 2).

Previously, when the parent nano-SAPO-34 (20 nm) was compared with a standard SAPO-34 of similar total acidity and much larger crystal size (500nm), nano-SAPO-34 presented much higher C_2 =/ C_3 = ratio [17], indicating that this ratio is not controlled by a faster diffusion of ethylene vs. propylene [5, 43, 44] but it would support the fact that with a higher acid strength, the olefin selectivity is produced through aromatic intermediates by the side-chain methylation mechanism [45]. If this is so, then a SAPO-34 with higher acid strength should yield more ethene since the formation from a hexa or tetramethylbenzene reaction center is less energetically favoured [46]. In our case, after steaming of nano-SAPO-34, the C_2 =/ C_3 = ratio also decreases when compared with the parent sample, in line with a decrease in the distribution of silicon species at the edge of silicon islands. We can conclude from the experimental data that selectivity is governed by silicon distribution, (which has been modified by steaming) and not by shape selectivity effects, due to preferential diffusion of ethene or deactivation by coke.

3.3.3 Methodology suggested for performing SAPO-34 stability tests.

In addition, the results presented in this contribution help to define which are the best conditions to perform a SAPO-34 stability test that simulates a long period of a working catalyst with many cycles of reactions and regeneration, both in the presence of water. This has been done for other petrochemical process using zeolites in the catalyst inventory as it is the case of Fluid Catalytic Cracking. In this case, steaming at temperatures of 750°C or higher and high partial pressures of water are used for simulating an equilibrium catalyst. However, this kind of hydrothermal stability test does not seem suitable for SAPO-34 since the mechanism of dealumination for zeolites is different from the desilication on silicoaluminophosphates [38]. In fact, while steaming at high temperature generates wide dealumination in ZSM-5 crystals with severe loss of acidity [47-49], in the case of standard SAPO-34, both, textural and acidity properties are preserved (see Table 1 and ref. [25]). Moreover, if the SAPO-34 sample presents high mesoporosity, as it is the case of the nano-SAPO-34 sample, steaming at 400°C strongly affects the stability. Our results indicate that SAPO-34

samples, especially if they are of hierarchical nature, should be submitted to hydrothermal stability test at low temperature, similar to the reaction temperature of methanol to olefins in order to evaluate their properties as potential MTO catalyst. Then, if required, they can be stabilized by steaming at 600-700°C.

4. Conclusions

Nano-SAPO-34 has been stabilized towards contact with moisture by steaming at T≥550°C. The stabilization effect is attributed to the migration of silicon to larger silicon islands in which the overall contribution of Si species on the edge of silicon islands has been reduced. The role of steam at high temperature is to facilitate the migration of silicon while the vacancies are healed by phosphorus. In the absence of steam, thermally treated nano-SAPO-34 is not stabilized and its lifetime decreases after contact with moisture. At low temperature of steaming the structure of nano-SAPO-34 collapses due to the hydrolysis of Si-O-Al bonds. Suitable hydrothermal stability tests for nanosized or mesoporous SAPO-34 samples should include steaming at temperatures close to the temperature of the reaction of methanol and, if required, stabilization by steaming at T≥550°C should be performed.

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Table 1. Textural properties of nano-SAPO-34 and standard-SAPO-34 samples fresh and steamed at different temperatures after days of exposure to moisture.

Sample	Steaming temperature	Days with moisture at	BET (m ² g ⁻¹)	t-plot S _{ext}	V _{micro} (cm ³ /g)	V _{meso} (cm ³ /g)	Acidity (mmol
	(°C)	r.t.	(III g)	(m^2/g)	(cm/g)	(cm/g)	$NH_3 g^{-1}$
Nano- SAPO-34	fresh	1	646	231	0.20	0.21	1.03
	fresh	14	616	224	0.19	0.20	0.86
	fresh	42	561	223	0.18	0.20	-
	fresh	107	536	223	0.15	0.20	-
	400	1	120	57	0.03	0.15	-
	550	1	534	177	0.17	0.21	0.74
	550	7	534	176	0.18	0.21	-
	550	14	538	179	0.18	0.21	-
	600	1	575	172	0.20	0.20	0.77
	600	12	574	173	0.20	0.20	-
	600	23	581	180	0.20	0.21	-
	700	1	490	143	0.17	0.18	0.43
	700	50	488	160	0.16	0.19	-
	700	65	491	144	0.17	0.19	-
Standard- SAPO-34	fresh	5	460	63	0.19	0.11	1.01
	fresh	29	463	62	0.19	0.11	0.97
	fresh	44	463	64	0.19	0.11	0.95
	400	1	432	41	0.19	0.10	0.83
	700	1	443	40	0.20	0.10	0.73

Table 2 Distribution of silicon species by deconvolution of different ²⁹Si MAS NMR signal of samples of nano-SAPO-34 fresh and steamed at 600 or 700°C followed by exposure to moisture (days) at room temperature.

G'1' '	ppm	Fresh	Fresh	St-700	St-700	St-700	St-600	St-600	St-600
Silicon species			(23d)	(8d)	(75d)	(90d)	(1d)	(7d)	(21d)
Defects	-78-85	5.1	14.3	13.9	11.5	7.9	7.4	3.5	1.5
Si4Al	-89	16.3	18.7	12.2	12.9	12.8	16.1	9.4	8.5
Si3Al1Si	-95	25.6	17.2	14.6	15.2	14.9	16.9	16.2	16.7
Si2Al2Si	-100	18.9	18.8	19.8	19.7	17.0	17.7	16.6	16.8
Si1Al3Si	-105	13.7	13.6	16.9	17.3	16.8	15.9	18.4	19.3
Si4Si	-110	20.4	17.4	22.6	23.4	30.6	26.1	35.9	37.2
Si in silicon islands	-100 to -110	53	49.8	59.3	60.4	64.4	59.7	70.9	73.3

Table 3. Kinetic parameters, halflifetime (t_{0.5}), breakthrough time (t_{0.8}), and methanol conversion capacity of nano and standard-SAPO-34 samples obtained by fitting of Janssen's kinetic model.

Sample	Days of	k (mol/gh)	a	t _{0.5}	t _{0.8}	Methanol
	exposure		(g/mmol)	(min)	(min)	conversion
	to moisture					capacity
Nano SAPO-34	1	9.98	5.6	147	76.7	$\frac{(g_{\text{metanol}}/g_{\text{catalyst}})}{15.9}$
Nailo SAI O-34	1	7.76	5.0	147	70.7	13.7
	28	6.82	3.6	231	70.0	25.1
Nano SAPO-34	7	5.51	5.5	149	20.4	16.2
St. 700°C	53	5.47	6.3	131	17.2	14.2
	62	6.86	5.9	138	42.3	15.0
Nano SAPO-34	1	5.94	5.3	155	31.1	16.9
St. 600°C	12	7.00	5.8	142	45.7	15.4
	22	8.85	6.8	120	55.5	13.0
Nano SAPO-34	1	9.08	5.5	149	71.2	16.2
St. 550°C	7	7.70	4.9	167	63.8	18.1
	14	7.23	4.9	166	56.9	18.1

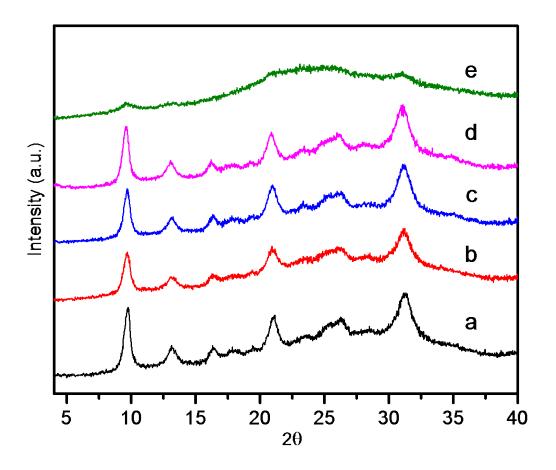
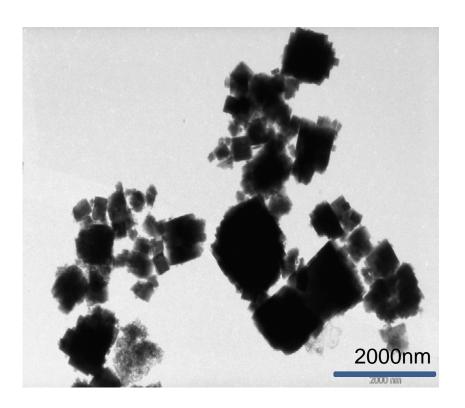


Figure 1. XRD patterns of nano-SAPO-34 (a) as calcined, and after steaming at (b)700°C, (c)600°C, (d)550°C, (e)400°C.



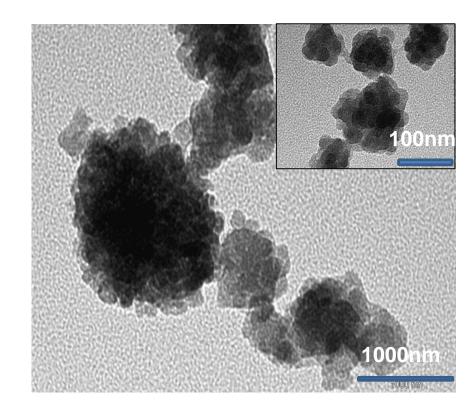


Figure 2. TEM pictures of standard and nano-SAPO-34.

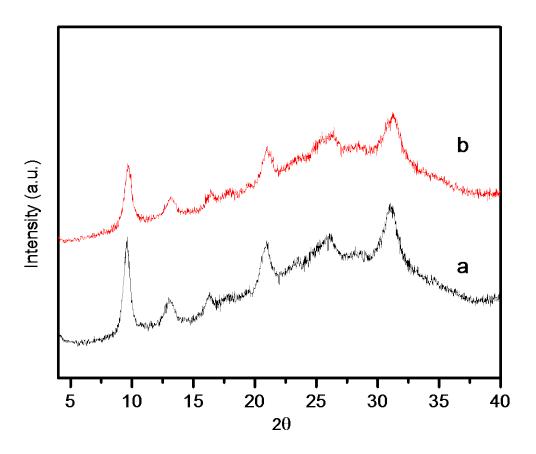


Figure 3. XRD patterns of nano-SAPO-34 steamed at 700°C after contact with moisture for (a) 1day (b)67 days.

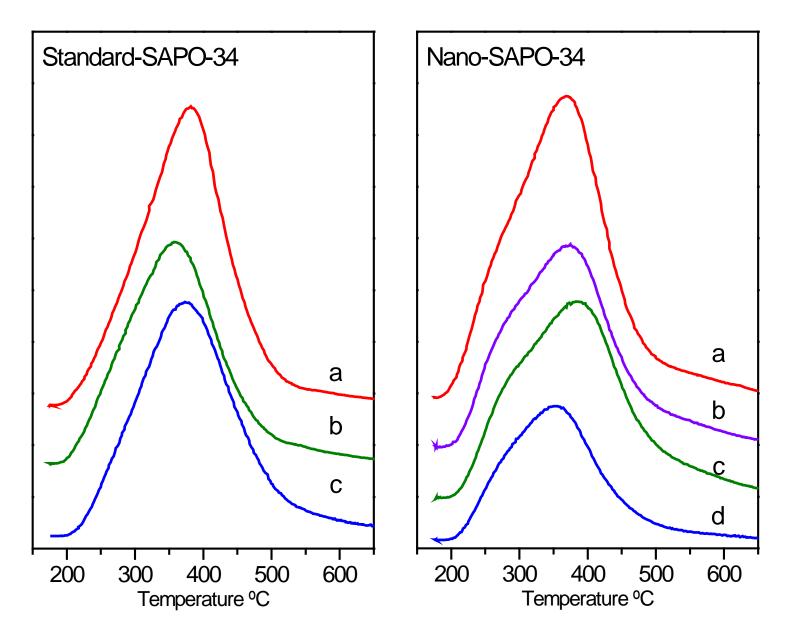


Figure 4. NH_3 -TPD of standard-SAPO-34 (a)fresh, (b)steamed at 400°C, (c)steamed at 700°C; and nano-SAPO-34 (a)fresh, and steamed at (b)550, (c)600 and (d)700°C.

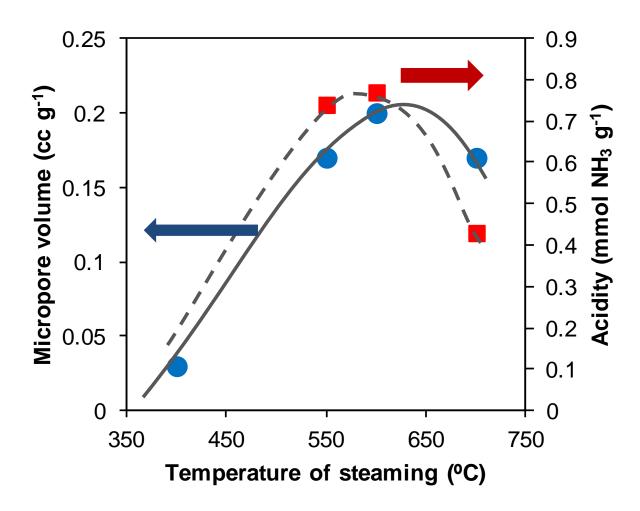


Figure 5. Micropore volume (circles) and acidity (squares) of nano-SAPO-34 samples steamed at different temperatures.

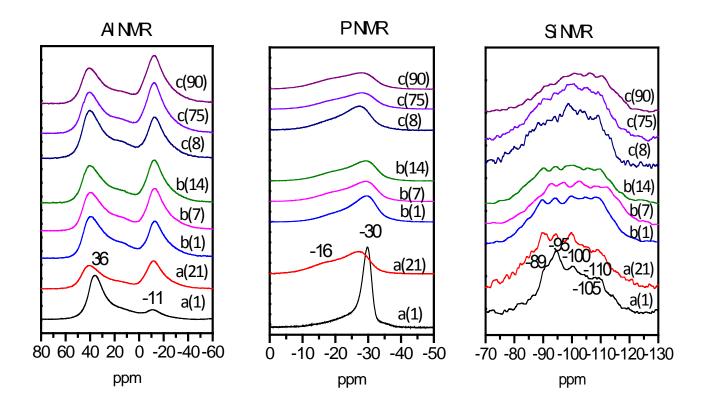


Figure 6. ²⁷Al, ³¹P and ²⁹Si MAS NMR of nano-SAPO-34 samples (a)fresh and steamed at (b)600 or (c)700°C followed by exposure to moisture at room temperature for () days.

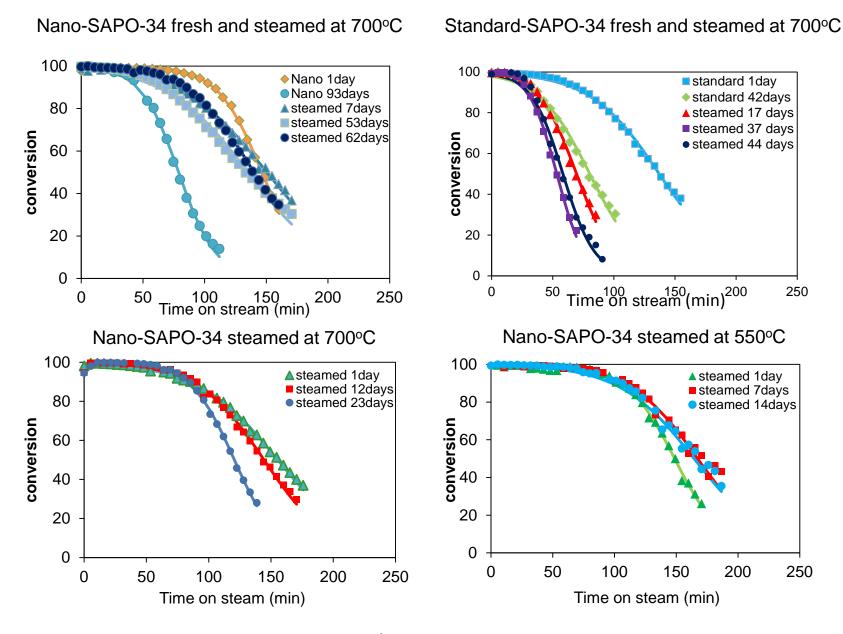


Figure 7. Conversion of methanol at 400°C and WHSV: 7 h⁻¹ on nano-SAPO-34 and standard-SAPO-34 samples fresh, after steaming at different temperatures and subsequent exposure to moisture. Lines correspond to the fitting following Janssens's kinetic model.

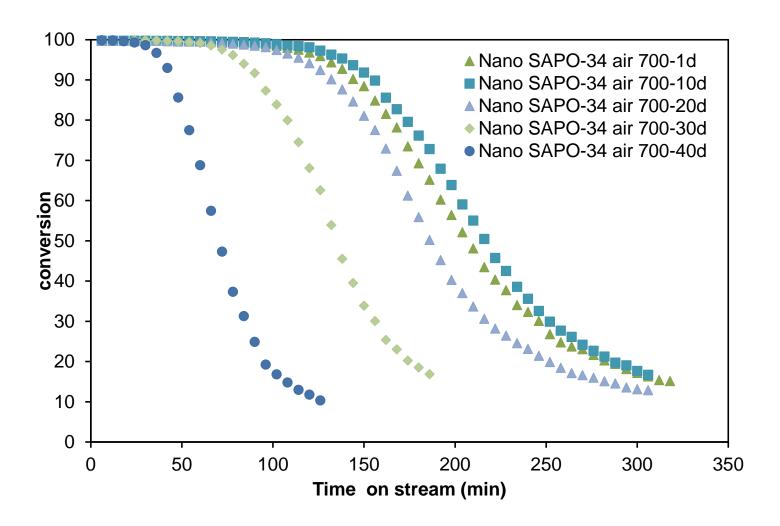


Figure 8. Conversion of methanol at 400°C and WHSV: 7 h⁻¹ on nano-SAPO-34 thermally treated in air at 700°C for 5h fresh and after contact with moisture at room temperature up to 40 days.

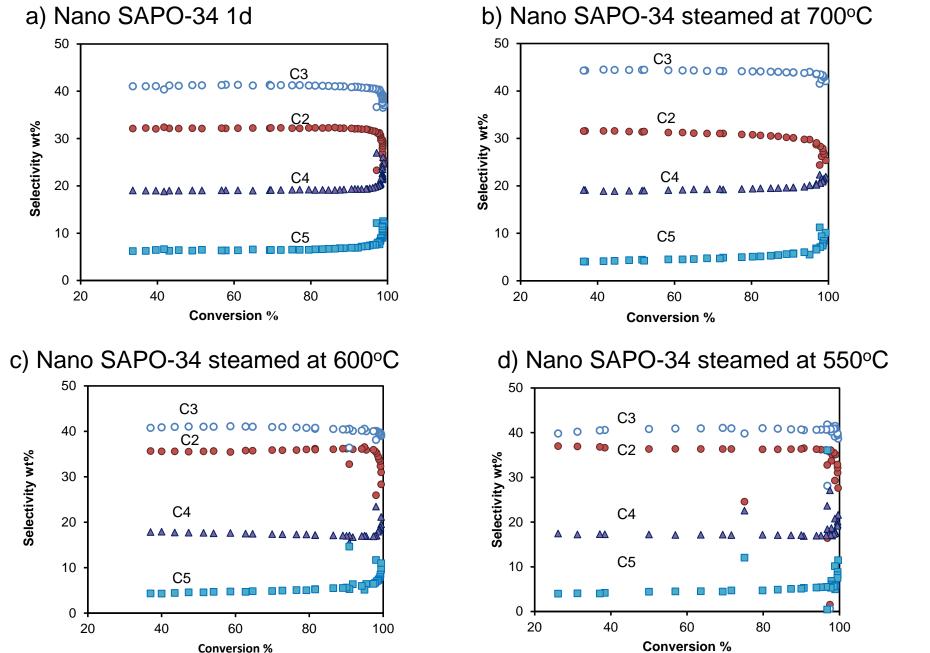


Figure 9. Selectivities to C2, C3, C4 and C5+ hydrocarbons in the conversion of methanol on nano-SAPO-34 fresh and steamed at 550, 600 and 700°C.

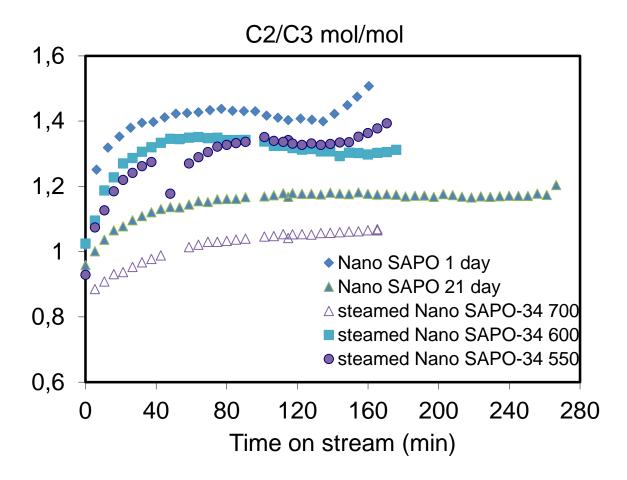


Fig. 10. C2/C3 ratio of products in the conversion of methanol at 400° C and WHSV = 7 h^{-1} on nano-SAPO-34 fresh and after steaming at 550, 600 and 700°C.