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Del Río García, A.I.; García-Albert, C.; Molina Puerto, J.; Fernández Sáez, J.; Bonastre Cano, J.A.; Cases Iborra, F.J. (2017). On the behavior of reduced graphene oxide based electrodes coated with dispersed platinum by alternate current methods in the electrochemical degradation of reactive dyes. *Chemosphere*. 183:242-251. doi:10.1016/j.chemosphere.2017.05.121.



The final publication is available at

<http://dx.doi.org/10.1016/j.chemosphere.2017.05.121>

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Additional Information

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3 ***reactive dyes***

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8
9 **Abstract**

10 The electrochemical behavior of different carbon-based electrodes with and without
11 nanoparticles of platinum electrochemically dispersed on their surface has been
12 studied. Among others, reduced graphene oxide based electrodes was used to
13 determine the best conditions for the decolorization/ degradation of the reactive dye
14 C.I. Reactive Orange 4 in sulfuric medium. Firstly, the electrochemical behavior was
15 evaluated by cyclic voltammetry. Secondly, different electrolyses were performed
16 using two cell configurations: cell with anodic and cathodic compartments separated
17 (divided configuration) and without any separation (undivided configuration). The best
18 results were obtained when reduced graphene oxide based anodes were used. The
19 degree of decolorization was monitored by spectroscopic methods and high
20 performance liquid chromatography. It was found that all of them followed pseudo-
21 first order kinetics. When reduced graphene oxide-based electrodes coated with
22 dispersed platinum by alternate current methods electrodes were used, the lowest
23 energy consumption and the higher decolorization kinetics rate were obtained.

1 Scanning Electronic Microscopy was used to observe the morphological surface
2 differences.

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4 *Keywords: reduced graphene oxide; dispersed platinum; alternate current methods; reactive dye; electrochemical treatment.*

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12 **1. Introduction**

13 In 2010 the Nobel Prize in Physics was granted to Andre Geim and Konstantin
14 Novoselov, not for the discovery of graphene, but for the “groundbreaking
15 experiments regarding the two-dimensional material, graphene” (Nobel Prize Official
16 Web, 2010), based on their study published in 2004 (Novoselov et al., 2004).

17 Graphene exhibits a theoretical surface area of $2630 \text{ m}^2 \text{ g}^{-1}$, which is much greater
18 than that of graphite ($\sim 10 \text{ m}^2 \text{ g}^{-1}$) and even that of carbon nanotubes ($1315 \text{ m}^2 \text{ g}^{-1}$)
19 (Pumera et al., 2009). Moreover, the electrical conductivity of graphene is excellent.

20 Several synthetic methods have been established to prepare graphene, but each one
21 of them, besides possessing different scalability, generates graphene with very
22 different characteristics, which strongly influences the resulting properties.

23 Electrochemical methods represent an interesting approach, since they can be easily

1 controlled, can be performed under ambient conditions, do not require toxic or
2 dangerous chemical agents (the only reactive used is the electron), and require only
3 simple instrumentation. In this case, the limitations of electrochemical methods are
4 that the electrode or sample where the reduction takes place must be conductive, be
5 electrochemically active and be in contact with the solution. In literature,
6 electrochemically reduced graphene oxide (RGO) has been obtained on different
7 electrode materials such as glassy carbon (Chen et al., 2011; Hilder et al., 2011;
8 Bonanni and Pumera, 2012), gold (Hilder et al., 2011; Bonanni and Pumera, 2012;
9 Sheng et al., 2012), indium tin oxide (ITO) (Hilder et al., 2011) or Pt (Bonanni and
10 Pumera, 2012).

11 Moreover, due to their high surface area, these electrodes can be used as a support
12 with anchoring sites for metal nanoparticles such as Pt nanoparticles, to produce
13 graphene-nanoparticle hybrids. This combination lead to materials which have
14 enhanced electrocatalytic activity and interesting properties for a variety of
15 applications as methanol oxidation in fuel cells (Zhang et al., 2013; Hsieh, et al., 2013),
16 counter electrodes for dye sensitized solar cells (Yeh et al., 2014), hydrogen gas
17 sensing (Shafiei et al., 2010), oxalic acid sensing (Chen et al., 2013), DNA detection (Yin
18 et al., 2012), among others. In the case of Pt, there is a great dependence of the
19 degradation of pollutants on the presence of chloride. The presence of a relatively small
20 amount of chloride ions seems to inhibit the oxygen evolution reaction (OER), causing
21 an increase of the anode potential. Therefore, there is a higher reactivity of oxychloro
22 compounds and the performance of Pt electrodes can be significantly improved in the
23 presence of NaCl.

1 Although the dispersion of Pt nanoparticles on graphene surface has been done mainly
2 using chemical methods, currently, electrochemical methods have arisen great interest
3 within the scientific community. As reported in recent studies carried out by our
4 research group (Molina et al., 2014), the synthesis of Pt nanoparticles on the surface of
5 reduced graphene oxide can be accomplished potentiostatically or using alternating
6 current methods such as electrochemical impedance spectroscopy (EIS) technique.
7 With the EIS synthesis technique, a lower effective synthesis time was required to
8 obtain an optimum coating of Pt nanoparticles (Molina et al., 2014).

9 Considering these previous results, the present work deals with two new approaches
10 in the environmental field. Firstly, the study of the electrochemical behavior of
11 different carbonaceous materials with different structures in solutions containing the
12 dye C.I. Reactive Orange 4, commercially known as Procion Orange MX2R (PMX2R).
13 The carbonaceous materials studied in this part are: glassy carbon (GC), GC with Pt
14 dispersed on its surface (GC-Pt), reduced graphene oxide deposited on a Pt support
15 (RGO) and reduced graphene oxide deposited on a Pt support with Pt dispersed on its
16 surface using a potentiostatic method (RGO-Pt/POT) and a current alternating method
17 (RGO-Pt/EIS). Secondly, considering the voltammetric results as an initial reference for
18 the efficiency of these electrodes, different electrolyses under different conditions
19 were performed to evaluate the degradation and decolorization of PMX2R. In this part,
20 RGO-Pt/POT and RGO-Pt/EIS were studied and later compared to other carbonaceous
21 materials. These materials were activated carbon textile (ACT) and activated carbon
22 textile with Pt dispersed on its surface (ACT-Pt), also studied in previously published
23 works (del Río et al., 2015). In all cases, special attention was paid to the influence of
24 the synthesis method.

1 The dye selected for these studies, PMX2R, it is a monofunctional reactive dye with a
2 1, 3, 5-triazinyl group as a functional group and an azo group as chromophore.
3 Reactive dyes are widely employed in the textile industry. However, during the dyeing
4 with reactive dyes, they undergo a secondary reaction consisting on their hydrolysis.
5 These dyes are not easily biodegradable and thus even after extensive treatment, color
6 from unexhausted reactive dyes may still remain in textile wastewater. For this reason,
7 this dye was chosen as a representative model of recalcitrant dyes.

8

9 **2. Experimental**

10

11 *2.1. Reagents and materials*

12 All reagents used were of analytical grade. For the synthesis: Monolayer graphene
13 oxide (GO) powders were acquired from Nanoinnova Technologies S.L. (Spain). Lithium
14 perchlorate (LiClO_4) was purchased from Merck. Pt wires (0.5 mm diameter, 99.99%
15 purity) were acquired from Engelhard-Clal. The area of the electrodes was controlled
16 with Teflon®.

17 For the characterisation: Sulphuric acid (H_2SO_4), CH_3OH (methanol) and $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$
18 (hexachloroplatinic acid hexahydrate) were purchased from Merck. Iron (III) sulfate
19 pentahydrate ($(\text{Fe}_2\text{SO}_4)_3 \cdot 5\text{H}_2\text{O}$) was used as received from Acrös Organics. C.I. Reactive
20 Orange 4 (PMX2R) was purchased from Zeneca. NaCl was from Fluka. When needed,
21 solutions were deoxygenated by bubbling nitrogen (N_2 premier X50S). Ultrapure water
22 was obtained from an Elix 3 Millipore-Milli-Q Advantage A10 system with a resistivity
23 near to 18.2 $\text{M}\Omega \cdot \text{cm}$.

24

1 *2.2. Solutions*

2 Voltammetric measurements were performed using the following solutions: 0.5 M

3 H₂SO₄ containing 3.9 g L⁻¹ PMX2R and 0.5 M H₂SO₄ as blank solution.

4 Electrolysis analyses were performed using 0.08 g L⁻¹ dye concentrations in 0.5 M

5 H₂SO₄, according to real concentrations in wastewaters (Zaharia and Suteu, 2012).

6 When adding NaCl to the solutions, the concentration was 0.3 g L⁻¹.

7
8 *2.3. Electrodes. Pretreatment and / or preparation*

9 Pt electrodes were pretreated with a flame treatment to clean their surface according

10 to the method developed by Clavilier (Clavilier, 1979). GC electrodes were also

11 pretreated by polishing the electrode with 1.0, 0.3 and 0.05 μm alumina slurry. For the

12 preparation of ACT electrodes, the company Carbongen S.A. (Spain) supplied a

13 hydrophilic activated carbon fabric (ref HST 1110). To discard the presence of

14 impurities on the surface of the fabric, a previous analysis (not included) by FTIR-ATR

15 was carried out. The ACT electrodes were prepared by cutting strips of 1 cm × 2 cm

16 area from the textile. To ensure a proper electric contact between the textile samples

17 and the 2 mm copper rods used as a support, they were glued (the tip was flattened to

18 improve the electrical contact) using CircuitWorks conductive epoxy resin by

19 Chemtronics. The resin was cured in an oven at 90 °C and wrapped with Teflon tape to

20 protect it from the solution. The dispersion of Pt on GC and ACT electrodes (to obtain

21 GC-Pt and ACT-Pt electrodes) was performed in 5 mM H₂PtCl₆·6H₂O and 0.5 M H₂SO₄

22 aqueous solution by CV from – 0.25 to + 0.4 V at 10 mV s⁻¹ during 20 scans with a

23 stainless steel (SS) as counter electrode (CE) and Ag/AgCl (3.5 M KCl) as the reference

1 electrode. The pretreatment for the CE of SS electrodes was described by del Río et al
2 (del Río et al., 2009a, 2009b).

3 For the deposition of RGO on the Pt support, GO was reduced on the surface of Pt by
4 CV. The solution used for the synthesis contained ultrapure water, 3 g L⁻¹ GO and 0.1 M
5 LiClO₄ (supporting electrolyte). A Pt wire was used as CE and working electrode (WE)
6 and Ag/AgCl (3.5 M KCl) was used as reference electrode. To perform the
7 electrochemical synthesis of RGO, the potential was cycled between +0.6 V and -1.4 V
8 at 50 mV s⁻¹ for 40 scans. The GO suspension tended to precipitate slowly, reason why
9 bubbling for 3 s with N₂ gas was applied when needed. After the synthesis, the
10 obtained electrodes were rinsed with water and characterized in 0.1 M LiClO₄ aqueous
11 solution to observe the characteristic capacitive electrochemical behavior of RGO.

12 In the electrochemical synthesis of Pt nanoparticles on RGO by the potentiostatic
13 method (from now on called RGO-Pt / POT) the WE was RGO and a Pt wire was used as
14 CE. The reference electrode used was Ag/AgCl (3.5 M KCl). The synthesis solution was
15 5 mM H₂PtCl₆ in 0.5 M H₂SO₄ at 0 V.

16 For the synthesis of Pt nanoparticles on RGO using alternating current methods (from
17 now on called RGO-Pt / EIS), the potential from which the measurement started was a
18 potential where Pt synthesis was negligible. This is why +0.4 V (vs. Ag/AgCl 3.5 M KCl)
19 was used. The frequency was 10 Hz and the applied amplitude was ±350 mV
20 (maximum allowed by the equipment). Thus, the potential range during the synthesis
21 varied from + 0.05 V to + 0.75 V.

22 After the synthesis, the electrodes were characterized by CV in 0.5 M H₂SO₄ to test
23 their characteristic voltammetric response.

1 Due to the high surface area of ACT and its textile morphology it is very difficult to
2 obtain a representative and reproducible voltammetric response of the species
3 present in the solution. Therefore, the voltammetric response of the dye is poorly
4 detected and overlaps with the ACT response in this medium. Therefore the use of GC
5 electrodes was considered for this characterization. One of the reasons is that it is easy
6 to obtain a reproducible surface after the previous pretreatment which, obviously,
7 allows control of the area. Furthermore, GC electrodes present an appropriate
8 separation between the potential for the oxygen and hydrogen evolution. Assuming
9 these differences between GC and ACT electrodes, the results obtained with GC were
10 only considered to evaluate the range of potentials for oxidation and reduction
11 processes, which were used as reference values in the potentiostatic electrolyses.

12 13 *2.4. Experimental facilities and equipment*

14 15 *2.4.1. Cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS)*

16 An Eco-Chemie Autolab PGSTAT302 potentiostat/galvanostat was used to perform
17 electrochemical measurements using these techniques. In all cases, a three-electrode
18 configuration was used with Ag/AgCl 3.5 M KCl as reference electrode and a scan rate
19 of 50 mV s⁻¹.

20 21 *2.4.2 Electrolyses*

22 The electrolyses were performed using two different configurations of electrochemical
23 cell (Fig. SM-1). The working conditions for the different experiments carried out are
24 included in table 1. To study oxidation or reduction separately, a divided H-type cell

1 (divided) was employed. A Nafion 117 (DuPont) cationic membrane was used to
2 separate the compartments. The studies were also carried out with an Eco-Chemie
3 Autolab PGSTAT302 potentiostat/galvanostat at room temperature and constant
4 agitation. When the reduction was performed using ACT as cathode, the anode was a
5 Pt wire. When the oxidation was studied, the anode was ACT-Pt and the cathode was
6 Pt. When the combination of these two processes was studied (oxido-reduction),
7 undivided cell was used (undivided) and the anode was ACT-Pt and the cathode was
8 ACT. In the case of the electrolyses using RGO-Pt electrodes, these were always the
9 anode. When studying only the oxidation, the cathode was a Pt wire. For the oxido-
10 reduction, the cathode was ACT. The reference electrode was Ag/AgCl (KCl 3.5M) in all
11 cases. Moreover, when the H-type cell was used, the non-studied compartment was
12 filled with 0.5 M H₂SO₄ and 0.3 g L⁻¹ NaCl. The working volume was 0.055 dm³ and
13 different samples were collected during the electrolyses. The intensity, the charge, the
14 potential difference and the electrode potential in blank solution compartment were
15 also measured.

17 *2.5. Analyses and instruments*

18 Chromatographic analyses were performed by means of High Performance Liquid
19 Chromatography (HPLC) with a Hitachi Elite Lachrom Chromatographic System
20 equipped with diode array detector. The chromatographic separations were
21 performed on a Lichrospher 100RP-18C column (5 µm packing). The method used is
22 that described by del Río et al (del Río et al. 2009b). The detection wavelength (λ_{det})
23 was set at 486 nm. UV-Visible spectra were also obtained with this system. This was
24 made possible by changing the column for a tubular piece (without any packing inside).

1 This allowed the sample to flow to the detector with low volume consumption. TOC
2 and TN measurements were performed using a Shimadzu TOC-VCSN analyzer based on
3 the combustion-infrared method. The instrument operated at 720 °C and 20 µL sample
4 injection with an air (free of CO₂) flow rate of 150 mL min⁻¹.

5 A Jeol JSM-6300 field emission scanning electron microscope was used to observe the
6 morphology of the samples. FESEM analyses were performed using an acceleration
7 voltage of 3 kV.

8 The FTIR-ATR spectra were recorded with a FTIR NICOLET 6700 spectrophotometer
9 equipped with an ATR device, in which the bottom of the surface prism (ZnSe) serves
10 as the cavity for aqueous samples. The subtraction of the background signal (aqueous
11 solution 0.5 M H₂SO₄) was required to obtain the spectra of the different samples. The
12 spectra were collected at 8 cm⁻¹ resolution as a result of an average of 400 scans.

13 2.6. Electrical Energy per order (EEO):

14 The calculus of EEO was chosen according to the report of Bolton et al (Bolton et al.,
15 2001), considering that the concentration of pollutants in all cases were low. This
16 parameter is defined as the electrical energy in kilowatt-hour (kWh) required to
17 degrade a contaminant by one of magnitude in a unit of volume (e.g. 1 m³) of
18 contaminated water or air. The corresponding equation (Eq. 1) is the following:

$$EEO = \frac{P \cdot t \cdot 10^3}{V \cdot \log\left(\frac{A_i}{A_f}\right)} \quad (1)$$

19

1 Where: P is the electric power (kW), t is the time of electrolysis (h), V is the volume
2 treated (m^3), A_i and A_f are the initial and final area of the chromatographic peak
3 associated to the pollutant of interest. In this case the factor of 10^3 converts L to m^3 .

4 In the present study, the values of the dye concentration (g L^{-1}) remaining in solution
5 after the electrolyses were difficult to measure since the percentages of dye
6 degradation were very high. However, the chromatographic peak associated with the
7 chromophore group of the dye (absorbing at 486 nm) could be considered. This is
8 because the area of the peak is directly proportional to the concentration of dye
9 whose chromophore group has not been degraded yet, as previously mentioned.
10 Therefore, the area of this peak was used in calculus instead of concentration.

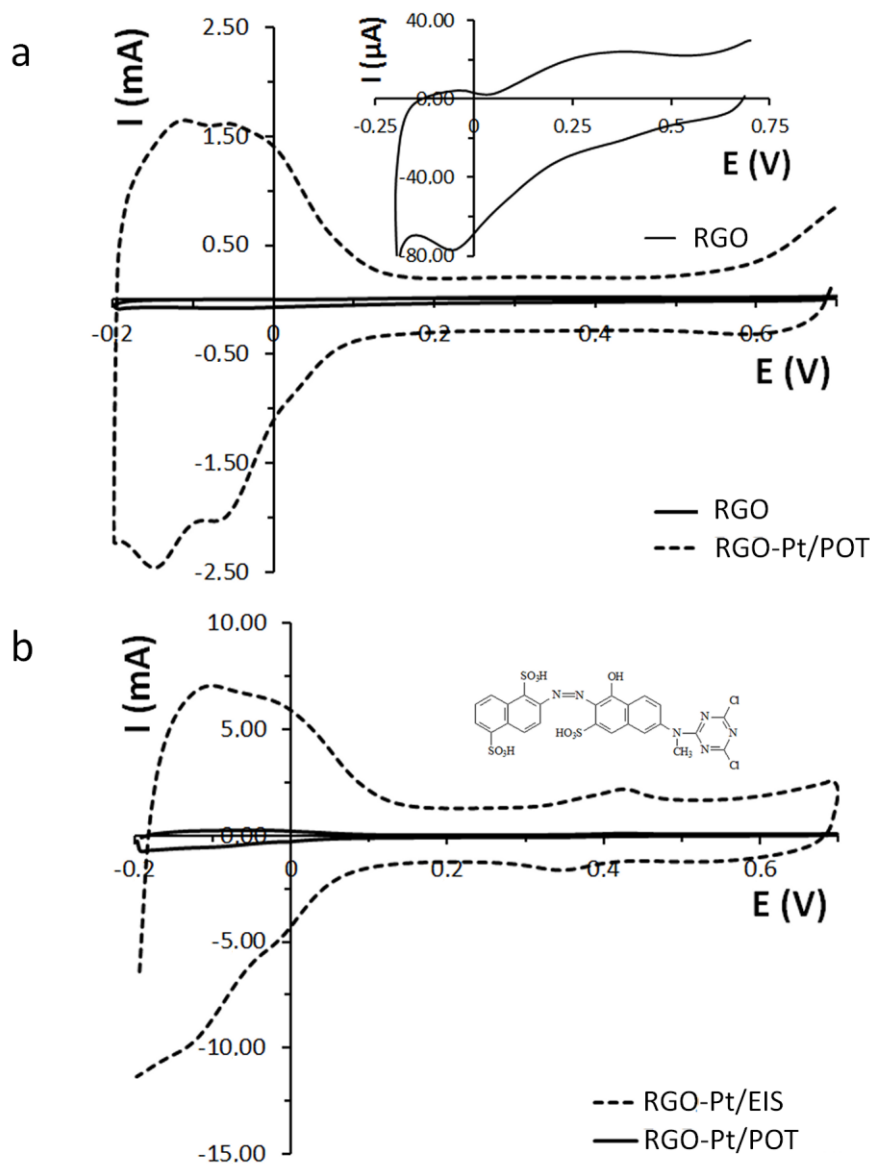
11 Even so, the area of the chromatographic peak associated with the dye was difficult to
12 measure in some cases due to the high percentages of decolorization obtained after 24
13 h of electrolysis and the detection limitations of the equipment. For this reason, a
14 percentage of decolorization of 80 % was considered as a reference value to calculate
15 the EEO consumption. At that point of the electrolysis all the solutions studied gave
16 chromatograms where the peak at 486 nm was still detected, although it is
17 considerably smaller than that of the initial solution. The values obtained have been
18 included in Table 1.

19 **3. Results and discussion**

20 *3.1. Voltammetric assays*

21 The electrochemical behavior of RGO, RGO-Pt/POT and RGO-Pt/EIS electrodes was
22 compared to observe the influence of the method used to disperse Pt on the RGO
23 surface. Fig. 1a shows the cyclic voltammograms of RGO and RGO-Pt/POT when cycling

1 between -0.2 V and + 0.7 V in 0.5 M H₂SO₄. As can be seen, the RGO-Pt/POT electrode
 2 showed the characteristic peaks of Pt in this medium. According to the figure inset in
 3 Fig. 1a, the electroactivity of RGO electrode was not relevant since the voltammetric
 4 charge was two orders of magnitude lower, showing the corresponding capacitive
 5 response of the RGO surface (Sheng et al., 2012). However, the oxidation and
 6 reduction processes of the underneath support of Pt could be observed probably due
 7 to a partial covering with RGO (Molina et al., 2014).



8

1 **Figure 1.** a) Cyclic voltammograms of RGO and RGO-Pt/POT as WE in 0.5 M H₂SO₄. Inset figure:
2 RGO as WE. b) Cyclic voltammograms of RGO-Pt/EIS and RGO-Pt/POT as WE in 0.5 M H₂SO₄
3 and 3.9 g L⁻¹ PMX2R. Inset figure: Chemical structure of C.I. Reactive Orange 4. Second scan in
4 all cases.

5 This work is mainly focused on the study of RGO-Pt/EIS. However, the study of RGO-
6 Pt/POT electrodes should be considered in order to evaluate the differences and their
7 efficiency. Fig. 1b shows their cyclic voltammograms in 0.5 M H₂SO₄ and 3.9 g L⁻¹ of
8 PMX2R. The RGO-Pt/EIS electrode presents a better electrochemical behavior due to a
9 high number of active sites in Pt covering. This is in accordance with previously
10 published studies (Molina et al., 2014).

11 To verify this enhancement of the dispersion of Pt nanoparticles by alternate current
12 methods and its influence in the voltammetric behavior of PMX2R, the voltammetric
13 profile of RGO-Pt/EIS electrodes were compared to Pt, GC and GC-Pt electrodes in a
14 0.5 M H₂SO₄ and 3.9 g g L⁻¹ of PMX2R (Fig. 2). Fig. 2a compares GC and GC-Pt
15 electrodes. When GC-Pt was used as WE, the voltammogram profile was similar of
16 bare Pt revealing an adequate covering of the GC surface with dispersed Pt. Apart from
17 the typical reversible peaks of the Pt surface, the oxidation and reduction peaks of the
18 dye were also observed. This can be seen when this profile is compared with the inset
19 figure of Fig. 2a that shows the GC and GC-Pt voltammograms obtained in 0.5 M H₂SO₄.
20 The GC-Pt electrode shows higher electroactivity than GC and the presence of Pt on its
21 surface is clearly evident according to the voltammetric profile.

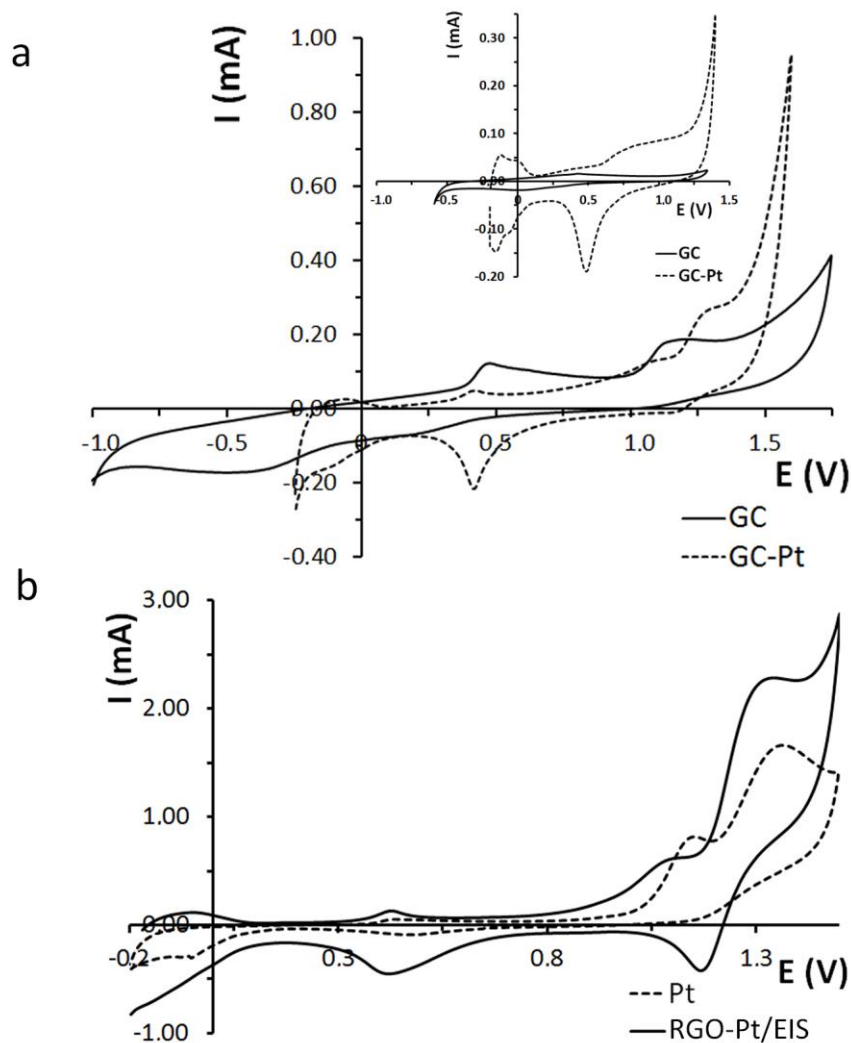


Figure 2. a) Cyclic voltammograms of GC and GC-Pt as WE in 0.5 M H₂SO₄ and 3.9 g L⁻¹ PMX2R. Scan rate: 50 mV s⁻¹. Inset: Cyclic voltammograms of GC-Pt and GC as WE in 0.5 M H₂SO₄ solution; scan rate: 10 mV s⁻¹. b) Cyclic voltammograms of Pt and RGO-Pt/EIS as WE in 0.5 M H₂SO₄ and 3.9 g L⁻¹ PMX2R solution; scan rate: 50 mV s⁻¹. Second scan in all cases.

Fig. 2b shows the voltammograms of Pt and RGO-Pt/EIS. Both voltammograms present a similar profile. The oxidation and reduction of bare Pt were observed at potential values lower than 0.1 V and higher than 0.5 V. At potential values between + 1.0 V and + 1.50 V, two oxidation peaks are observed. These are attributed to a double contribution of the oxidation of the electrode surface and the oxidation of the dye. The reduction peak observed in the reverse scan at 1.2 V is associated with the

1 corresponding reduction of the intermediates generated from the dye oxidation. The
2 reduction peak observed approximately at 0.5 V, corresponds to the reduction of Pt
3 oxides. It is worth noting that the charge associated with the electrochemical behavior
4 of RGO-Pt/EIS is significantly higher; indicating that this electrode is clearly more
5 electrocatalytic in these conditions. This can be explained by the higher surface area of
6 RGO. The higher charge of H adsorption (among other processes) on the Pt surface
7 implies a higher electrochemical surface area as result of the small size and uniform
8 dispersion of Pt (Molina et al., 2014). Therefore, more Pt nanoparticles are available to
9 catalyze the electrochemical reaction. In conclusion, the RGO-Pt/EIS electrode is more
10 electroactive than bare Pt with the great advantage that a lower quantity of Pt is
11 needed. Moreover, it is important to highlight that the electroactivity of RGO-Pt/EIS is
12 one order of magnitude higher than in case of using GC or GC-Pt, independently of the
13 presence or absence of dye in solution. In addition to this, it should be noted that GC,
14 GC-Pt and Pt electrodes were chosen as WE in voltammetric assays in order to
15 establish the adequate potentials to carry out the electrolyses where ACT was used as
16 cathode and ACT-Pt and RGO-Pt were used as anodes. Considering their voltammetric
17 behavior in a 0.5 M H₂SO₄ solution containing 3.9 g L⁻¹ PMX2R, it was found that the
18 oxidation of the dye takes place at + 1.3 V approximately. The potential needed for the
19 corresponding reduction was located between - 0.1 V (for GC-Pt and Pt) and - 0.4 V
20 (for GC). With the purpose of ensuring the oxidation and reduction processes during
21 the electrolyses, potentials were slightly modified applying cathodic and anodic
22 overpotentials. Therefore, the potentials applied for reduction and oxidation were -
23 0.35 V and + 1.50 V, respectively.

1 Since the electrolyses performed in this work were done with solutions containing 0.3
2 g L⁻¹ NaCl, the voltammetric characterization of RGO-Pt/EIS was also studied in this
3 media (Figure not shown). The cyclic voltammogram presented the same profile as in
4 the absence of chloride (Fig. 2-b). However, since chloride ions play an important role
5 in the oxidation, an appreciable difference in the voltammetric charge was observed
6 when chloride is in solution (Trasatti, 1987).

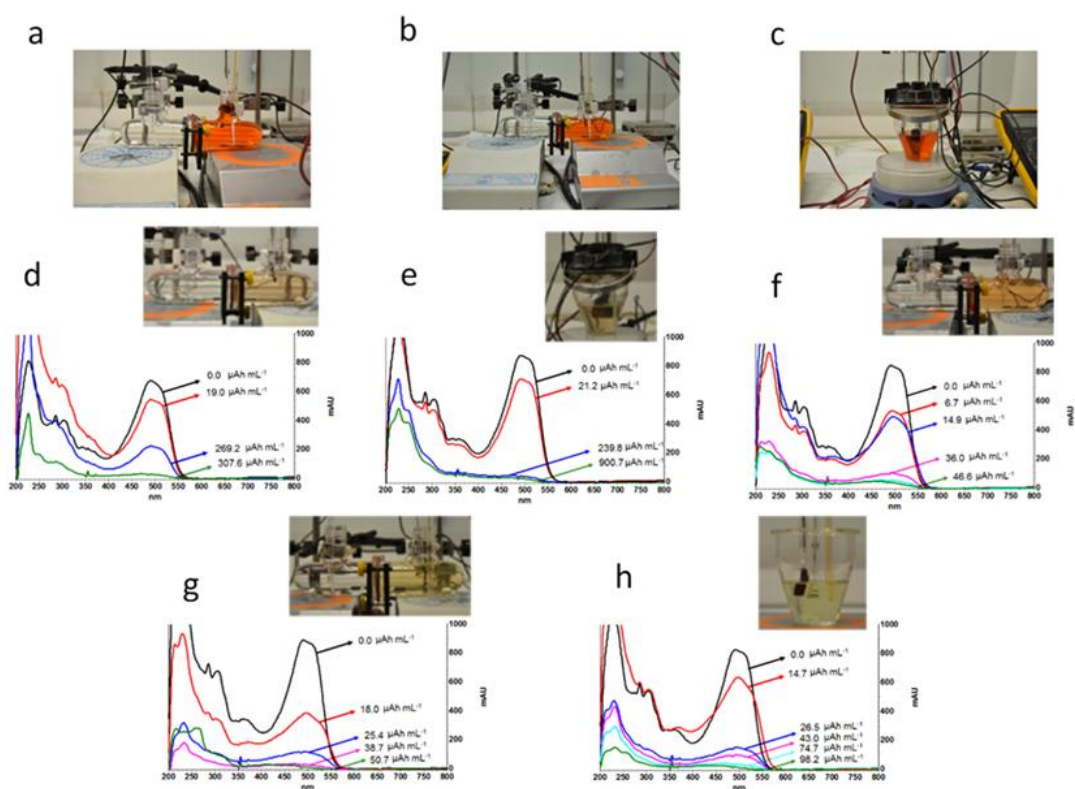
7 The voltammetric characterization in 0.5 M H₂SO₄ of different RGO-Pt/EIS electrodes
8 obtained at different frequencies has been previously published by our investigation
9 group (Molina et al., 2014; Fig. 8a). According to that study, the most appropriate
10 frequency for the synthesis of Pt on the RGO surface was 10 Hz (the reason why this
11 frequency was chosen for this study). Comparing the voltammogram of RGO-Pt/EIS (at
12 10 Hz) obtained in 0.5 M H₂SO₄ (Molina et al., 2014; Fig. 8a) and the voltammograms of
13 RGO-Pt/EIS (also at 10 Hz) obtained in 0.5 M H₂SO₄ and 3.9 g L⁻¹ PMX2R (Fig. 2b of the
14 present paper,) a considerable diminution of the voltammetric charge was observed in
15 the presence of PMX2R. This can be explained by a partial blockade of the surface due
16 to the dye and/or the intermediates generated and could explain the slight shift
17 observed for the peak associated with the reduction of Pt oxides (Molina et al., 2014;
18 Fig. 8a). Additionally, it is interesting to compare the voltammetric charge when RGO-
19 Pt/EIS was used as WE (Fig. 2b) and when GC and GC-Pt were used as WE (Fig. 2a) in a
20 0.5 M H₂SO₄ solution and 3.9 g L⁻¹ PMX2R. It was found that cyclic voltammograms
21 using GC and GC-Pt as WE presented a voltammetric charge one order of magnitude
22 lower than in case of using RGO-Pt/EIS.

23

3.2 Electrolyses

3.2.1. Spectroscopic results

Fig. 3 shows the UV-Vis evolution spectra for the processes where a satisfactory decolorization was obtained. Fig. 3b and c (experiments 1 and 2) show that no decolorization was obtained in oxidation and oxido-reduction with ACT-Pt as anode. The spectra of the final samples correspond to 24 h, except Fig. 3g and h (only 4 hours) because of the faster decolorization.



8

9 **Figure 3.** UV-Vis evolutions of 0.08 g L^{-1} PMX2R in $0.5 \text{ M H}_2\text{SO}_4$. a) Initial solution. b) Experiment number 1. c) Experiment number 2. d) Experiment number 3. e) Experiment number 4. f) Experiment number 5. g) Experiment number 6. h) Experiment number 7. Inset images: solution after the electrolyses.

1 The main bands studied were:

- 2
- 3 • The band at 486 nm, associated with the long conjugated π system linked by
- 4
- 5 the azo group and, therefore, to the decolourization obtained (Silverstein et al.,
- 6
- 7 1991; Lucas and Peres, 2006) as observed in Fig. 3d to h (experiments 3 to 7).
- 8
- 9 The inset image of Fig. 3f shows some color in the final solution suggesting that
- 10
- 11 more than 24 hours are needed for a complete degradation of these bonds.
- 12
- 13 • The bands at 230 nm and 310 nm, corresponding to $\pi \rightarrow \pi^*$ transitions of
- 14
- 15 benzenic and naphthalenic rings, respectively (Yang, 1987; Feng et al., 2000;
- 16
- 17 Galindo et al., 2000; Stylidi et al., 2004). Fig. 3d to h (experiments 3 to 7) show
- 18
- 19 a diminution of these bands indicating a loss of aromaticity, although some
- 20
- 21 benzenic compounds remain in solution (the band at 230 nm does not
- 22
- 23 disappear completely).
- 24
- 25 • The band at 350 nm, derived from $\pi - \pi^*$ transition between π system of
- 26
- 27 naphthalenic ring, the $-\text{SO}_3$ groups and the π^* system of the $-\text{N}=\text{N}-$ group
- 28
- 29 (Galindo et al., 2000; Cheninia et al., 2011). As shown in Fig. 3d to h
- 30
- 31 (experiments 3 to 7), naphthalene structures were degraded to give benzenic
- 32
- 33 compounds.
- 34
- 35 • The band at 280 nm, corresponding to the triazinic group (Silverstein et al.,
- 36
- 37 1991). As observed in Fig. 3d to h (experiments 3 to 7), this structure was
- 38
- 39 completely degraded.
- 40
- 41 • The band at 245 nm, corresponding to the $\text{Ar-NH-NH-Ar}'$ structure (Feng et al.,
- 42
- 43 2000; Qing, 1989). The appearance of this band was only observed in Fig. 3d
- 44
- 45 (experiment 3).
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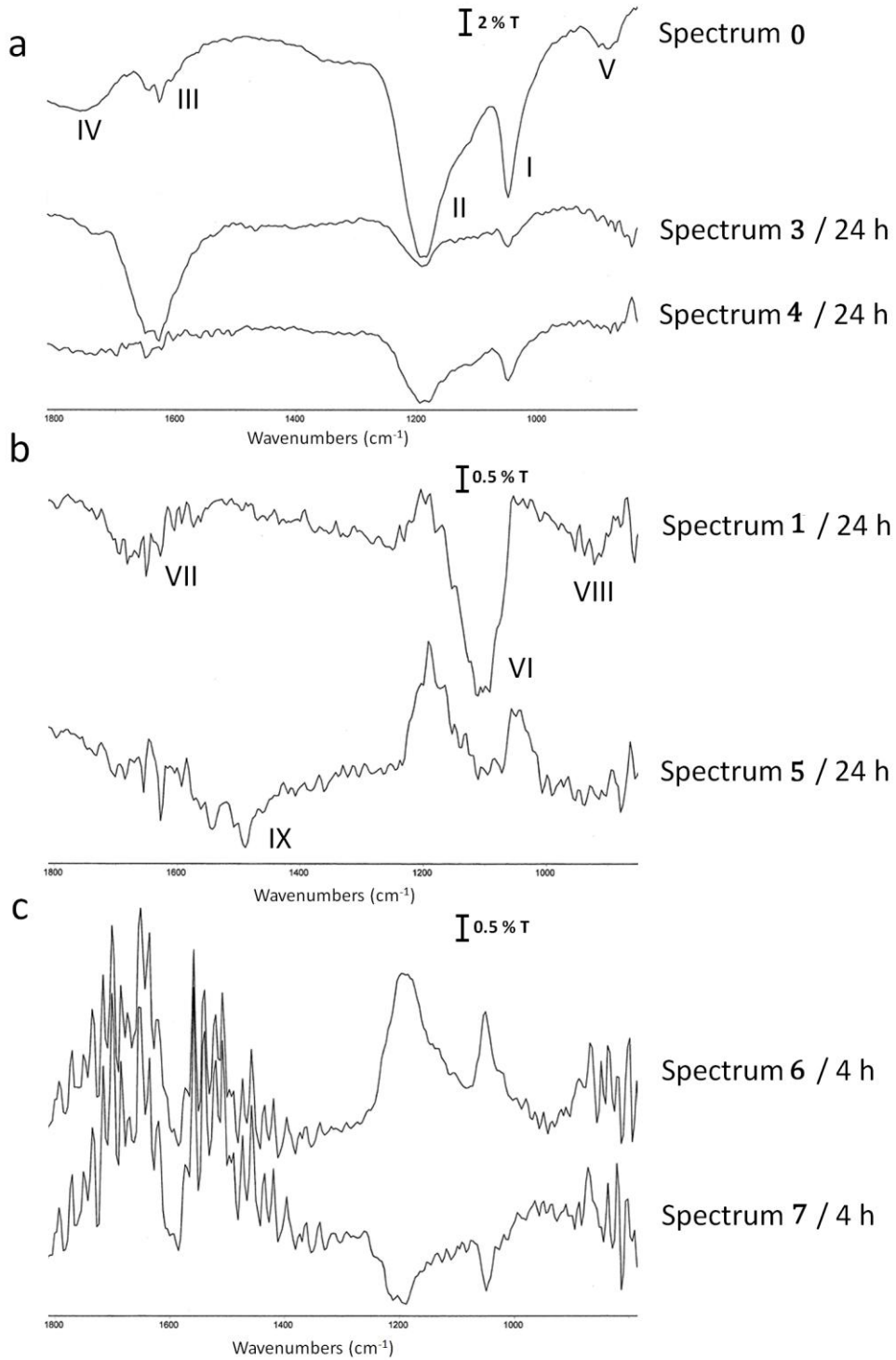
- 1 • The band at 260 nm, associated to oxidized benzene compounds (Feng et al.,
2 2000). Fig. 3e to h (experiments 4 to 7) demonstrate the presence of these
3 compounds in solution even after the treatment.

4 The FTIR-ATR spectra of the samples obtained after the different electrolyses are
5 shown in Fig. 4. The main bands of the original dye (spectrum 0) are:

- 6 • Bands at 1050 cm^{-1} (I) and 1192 cm^{-1} (II), ascribed to $-\text{SO}_3$ symmetric and
7 asymmetric stretching vibrations and naphthalene ring deformation
8 (Snehalatha et al., 2008). These bands diminish considerably after the
9 reduction with ACT as cathode (spectrum 3) indicating the structural
10 modifications in the naphthalene groups commented in Fig. 3d and the partial
11 elimination of the $-\text{SO}_3$ groups. After the oxido-reduction with ACT as cathode
12 and ACT-Pt as anode (spectrum 4), the diminution of these bands corroborates
13 the results mentioned in Fig. 3e. The decrease of the band II suggests the
14 oxidation of $-\text{SO}_3$ groups, as indicated in Fig. 3e (band at 260 nm). After the
15 oxidation using ACT-Pt as anode and Pt as cathode (spectrum 1), bands I and II
16 were not observed.

- 17 • The band at 1637 cm^{-1} (III), probably corresponding to the imine group (C=N-)
18 of the tautomeric form of PMX2R [30] or to the C-C stretching mode of the
19 naphthalene ring. In spectrum 3 this band appears wider and more intense.
20 This could be related to the bending of the amine N-H bond (Socrates, 1997).
21 This is in accordance with the bands at 245 nm observed in Fig. 3d. In spectrum
22 4 this band practically disappears due to the partial degradation of the
23 aromatic and chromophore structures. This was also observed in spectrum 1.

- The bands at 1750 cm^{-1} (IV) and 886 cm^{-1} (V), presumably associated with the dichlorotriazine ring (Navarro et al., 1995; Socrates, 1997; Spectral Database for Organic Compounds; Carneiro et al., 2003). In all cases, these bands were not observed confirming the degradation of this group.

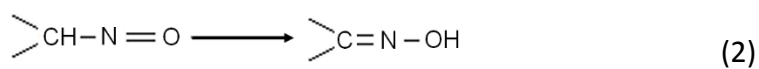


5

1 **Figure 4.** FTIR-ATR spectra of final samples. a) Spectrum 0: initial solution. Spectrum 3:
2 Experiment number 3. Spectrum 4: Experiment number 4. b) Spectrum 1: Experiment number
3 1. Spectrum 5: Experiment number 5 c) Spectrum 6: Experiment number 6. Spectrum 7:
4 Experiment number 7.

5 In addition to this, new bands appeared:

- 6 • Bands at 1106 cm^{-1} and 1660 cm^{-1} (spectrum 1, VI and VII, respectively),
7 attributed to hydroxyl and carbonyl groups (Carneiro et al., 2003). The band at
8 1660 cm^{-1} could be also assigned to C=N stretching vibration. This band and the
9 weak band at 930 cm^{-1} (VIII, N-O stretching vibration), could indicate the
10 presence of nitro compounds and oximes (Eq. 2) (Socrates, 1997):



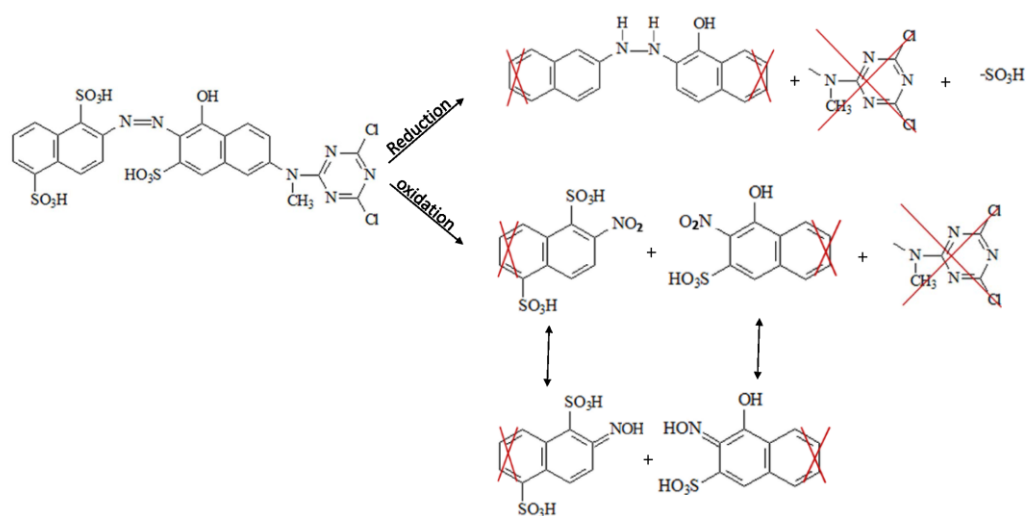
11
12
13 However, no decolorization was obtained during the oxidation with ACT-Pt as
14 anode maybe because of the appearance of other chromophore structures or a
15 contribution of the band III overlapped with band VII.

16 After the oxidation and oxido-reduction with RGO-Pt (spectra 5 to 7) all these
17 bands diminished indicating a severe degradation.

- 18 • The band centered at 1526 cm^{-1} (IX), probably associated with the asymmetric
19 NO_2 stretching vibration (spectrum 5) (Socrates, 1997).

20
21 In samples collected after oxidation and after oxido-reduction with RGO-Pt/EIS
22 (spectra 6 and 7) none of the bands mentioned above were observable after 24 h of

1 electrolysis. For this reason, the FTIR-ATR spectra shown correspond to samples of
 2 solution treated for 4 h.
 3 From these results, Fig. 5 show the reaction mechanisms proposed for electro-
 4 reduction and electro-oxidation.



5
 6 **Figure 5.** Oxidation and reduction reaction mechanisms.

7 3.2.2. Kinetics results

8 Decolorization during the electrolyses was also monitored by means of HPLC
 9 technique. With this purpose, the evolution of the dye concentration while passed
 10 charge (Q) increased was measured according to the chromatographic area of the peak
 11 associated with the dye when the detector wavelength was set at 486 nm. This was
 12 possible considering that the dye concentration is directly related to the
 13 chromatographic area. Table 1 shows a compilation of the kinetics results obtained
 14 from the linear regression analysis for the plots $\ln(A_t/A_0)$ vs. Q ($\mu\text{Ah mL}^{-1}$) where A_0
 15 and A_t are the area of the dye chromatographic peak (at 486 nm) of the initial sample

1 and the area of a sample taken at t time after electrolysis began, respectively. Table 1
 2 shows, too, the Q needed to obtain a complete decolorization (assuming a decrease in
 3 dye concentration of 99 per cent as complete decolorization). All the decolorization
 4 processes studied in this work agreed with pseudo-first order kinetics. As can be seen,
 5 the ACT electrodes (experience numbers 3-4) presented the slower decolorization rate
 6 (see k values in Table 1), independently of the electrochemical cell configuration. In
 7 fact, the value of Q necessary to obtain a complete decolorization is 500 – 550 $\mu\text{Ah mL}^{-1}$
 8 ¹ in both cases.

9 **Table 1.** Kinetics analyses obtained for all the electrolyses: decolorization kinetics rate ($\mu\text{A}^{-1} \text{h}^{-1}$
 10 mL), specific charge ($\mu\text{Ah mL}^{-1}$) for a complete decolorization (99 per cent), percentage of
 11 decolorization after 24 h of electrolysis and electrical energy per order (kWh m^{-3})
 12 corresponding to an 80 per cent decolorization.

Experiment number/WE	Cell configuration	WE potential (V)	Electrolyte	k ($\text{mL } \mu\text{A}^{-1} \text{h}^{-1}$)	$Q_{\text{decol 99 \%}}$ ($\mu\text{Ah mL}^{-1}$)	% decol 24 h	$EEO_{\text{decol 80\%}}$ (kWh m^{-3})
1/ACT-Pt	Divided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	-	-	-	-
2/ACT-Pt	Undivided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	-	-	-	-
3/ACT	Divided	-0.35	0.5 M H ₂ SO ₄	0.0086	535.80 (t > 24 h)	92.88	0.0239
4/ACT	Undivided	-0.35	0.5 M H ₂ SO ₄	0.0116	511.80 (t ≈ 16 h)	100.00	0.0316
5/RGO-Pt/POT	Divided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	0.0589	77.35 (t > 24 h)	93.81	0.0415
6/RGO-Pt/EIS	Divided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	0.1800	26.08 (t ≈ 1 h)	100.00	0.0127
7/RGO-Pt/EIS	Undivided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	0.0608	79.46 (t ≈ 2.8 h)	100.00	0.0564

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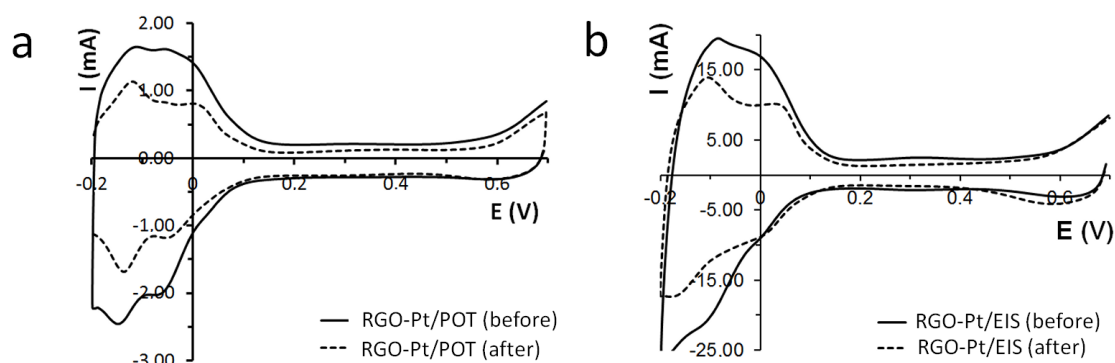
2 In the case of RGO-Pt electrodes, the oxidation was more effective when the anode
3 was RGO-Pt/EIS. Actually, the decolorization rate was three times higher than the rate
4 of RGO-Pt/POT electrodes. Moreover, on an equal basis, the electrolyses carried out
5 with RGO-Pt/EIS needed only $26.08 \mu\text{Ah mL}^{-1}$ for a complete decolorization. This
6 means that no more than 1 hour is required for a complete decolorization (this agrees
7 with the spectroscopic results, see Fig. 3) while the value of Q required with RGO-
8 Pt/POT electrodes is three times higher and more than 24 hours are needed.

9 In the oxido-reduction process with RGO-Pt/EIS as anode, the decolorization rate was
10 lower compared with that obtained after the oxidation with the same electrode.
11 Moreover, a higher electrolysis time and charge were required to obtain a complete
12 decolorization.

13 *3.2.3. Electrodes stability*

14 These results show indisputable evidences that the best results were obtained with
15 RGO anodes with platinum dispersed using alternating current method (RGO-Pt/EIS).
16 However, different reasons such as economy, adaptability, availability of the working
17 space, etc. imply to choose the most appropriate combination. Consequently, the
18 stability of RGO-Pt/POT and RGO-Pt/EIS electrodes in divided and undivided
19 configurations were respectively evaluated. Fig. 6 shows the voltammograms
20 registered in 0.5 M H_2SO_4 before and after the electrolyses. Dispersed Pt is still present
21 on the surface of RGO although a small reduction of the number of active sites was
22 detected in both cases. The voltammetric charge obtained with RGO-Pt/POT as WE

1 was one order of magnitude lower, indicating a higher electroactivity of the RGO-
2 Pt/EIS electrode, even after the electrolysis.



3
4 **Figure 6.** Voltammograms of a) RGO-Pt/POT and b) RGO-Pt/EIS in a 0.5 M H₂SO₄ before and
5 after the electrolysis.

6 Moreover, the separation between anodic and cathodic peaks of the voltammograms
7 of RGO-Pt/EIS (previously used in the electrolysis of PMX2R) registered in 0.5 M H₂SO₄
8 and 0.01 M Fe₂(SO₄)₃ was 0.085 V, slightly lower than in the case of RGO-Pt/POT (0.092
9 V) indicating faster electron transfer kinetics (figures not shown).

10 Fig. SM-2 shows the micrographs corresponding to the coating of a RGO-Pt/EIS anode
11 after performing the electrolysis. As can be seen in Fig. SM-2a, the surface of the
12 electrode showed a very packed coating of dispersed Pt. This reveals a small
13 nanoparticle size and a uniform covering of the RGO surface. After the electrolysis (Fig.
14 SM-2b, the covering showed some cracks although this does not represent a significant
15 influence on the reversibility and the electrocatalytic properties.

16 3.2.4. Operating costs. Electrical Energy per Order (EEO)

17 Apart from the kinetics analysis, one of the most important parameters affecting the
18 performance of an electrochemical system is the evaluation of the operating costs.

1 With this purpose in mind, the electrical energy consumption per order (EEO) was
2 calculated in all cases. The values obtained have been included in Table 1.

3 From the results in Table 1, the use of RGO-Pt/EIS for the oxidation (divided,
4 experience number 6) required the lowest EEO (kWh m^{-3}). This fact, together with the
5 kinetics results, shows that these are the best conditions to carry out an efficient
6 electrolysis of the PMX2R solution. In addition to this, the trend in EEO values obtained
7 with RGO-Pt electrodes is consistent with the trend of the kinetics results. This means
8 that the higher decolorization rate, the less electrical energy required. However, the
9 use of undivided cell configuration with RGO-Pt/EIS (experience number 7) increased
10 the value of EEO by 77 per cent.

11 Previous results reported by our research group demonstrated that the RGO-Pt
12 electrode with higher electroactive coating of nanoparticles of Pt was the one obtained
13 by EIS (Molina et al., 2014). Scanning electron microscopy (SEM) provided clear
14 evidence about the coatings obtained in every case. The micrographs revealed that the
15 coating of RGO-Pt/POT electrodes is composed of Pt nanoparticles that are highly
16 ordered and formed as a result of a two-dimensional growth. The size of nanoparticles
17 was found to be very small (Molina et al., 2014; Fig. 6c and d). In the case of RGO-
18 Pt/EIS electrodes, the coating showed three-dimensional growth giving a globular-like
19 structure (Molina et al., 2014; Fig. 6c and d). As a consequence, a greater quantity of Pt
20 nanoparticles is deposited on the RGO surface by EIS and, therefore, a more
21 electroactive coating was obtained.

1 4. Conclusions

2 Based on the voltammetric results, the dispersion of Pt on RGO using alternating
3 current method improves significantly the electroactivity of these electrodes since
4 there is a higher number of active sites on their surface in comparison with RGO-
5 Pt/POT electrodes.

6 It was also found that the degree of decolorization is highly influenced by the cell
7 configuration. The most efficient configuration was the one where anodic and cathodic
8 compartments were separated (divided), which means that there is no relevant
9 synergy between oxidation and later reduction of the dye and intermediates.
10 Moreover, a complete decolorization was obtained in all cases except after the
11 oxidation and the oxido-reduction of C.I. Reactive Orange 4 with ACT-Pt as anode at
12 constant potential of + 1.50 V; although FTIR-ATR studies revealed certain oxidation
13 degree. The rest of the processes showed complete decolorization according to a
14 pseudo-first order kinetics. Spectroscopic results revealed that the hydrogenation of
15 the azo bond is the most probable cause of the decolorization after the reduction with
16 ACT as cathode while the decolorization achieved in the rest of the processes was
17 related to the breakage of the azo bond. Furthermore, the elimination of the triazinic
18 group was shown. The degradation implied a partial elimination of the naphthalene
19 rings to give smaller benzenic compounds that remained in solution and were not
20 eliminated. The best results were obtained when RGO-Pt/EIS electrodes were used
21 with a divided cell, since a complete decolorization was accomplished after 1 h with
22 the lowest electrical energy consumption.

23

1 **Acknowledgements**

2 The authors wish to thank the Spanish Agencia Estatal de Investigación (AEI) and European
3 Union (FEDER funds) for the financial support (contract MAT2016-77742-C2-1-P). A.I. del Río is
4 grateful to the Spanish Ministerio de Ciencia y Tecnología for her FPI fellowship. J. Molina is
5 grateful to the Conselleria d'Educació, Formació i Ocupació (Generalitat Valenciana) for the
6 Programa VALi+D Postdoctoral Fellowship (APOSTD/2013/056). C. García is grateful to the
7 Conselleria d'Educació, Formació i Ocupació (Generalitat Valenciana) for her Gerónimo Forteza
8 fellowship. The authors wish to acknowledge to Chemviron Carbon who kindly donated the
9 265 ZORFLEX® activated carbon fabric.

10

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Table 1

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Experiment number/WE	Cell configuration	WE potential (V)	Electrolyte	k (mL $\mu\text{A}^{-1} \text{h}^{-1}$)	$Q_{\text{decol } 99\%}$ ($\mu\text{Ah mL}^{-1}$)	% decol 24 h	$\text{EEO}_{\text{decol } 80\%}$ (kWh m^{-3})
1/ACT-Pt	Divided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	-	-	-	-
2/ACT-Pt	Undivided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	-	-	-	-
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7/RGO-Pt/EIS	Undivided	1.50	0.5 M H ₂ SO ₄ + 0.3 g L ⁻¹ NaCl	0.0608	79.46 (t \approx 2.8 h)	100.00	0.0564

Figure 1
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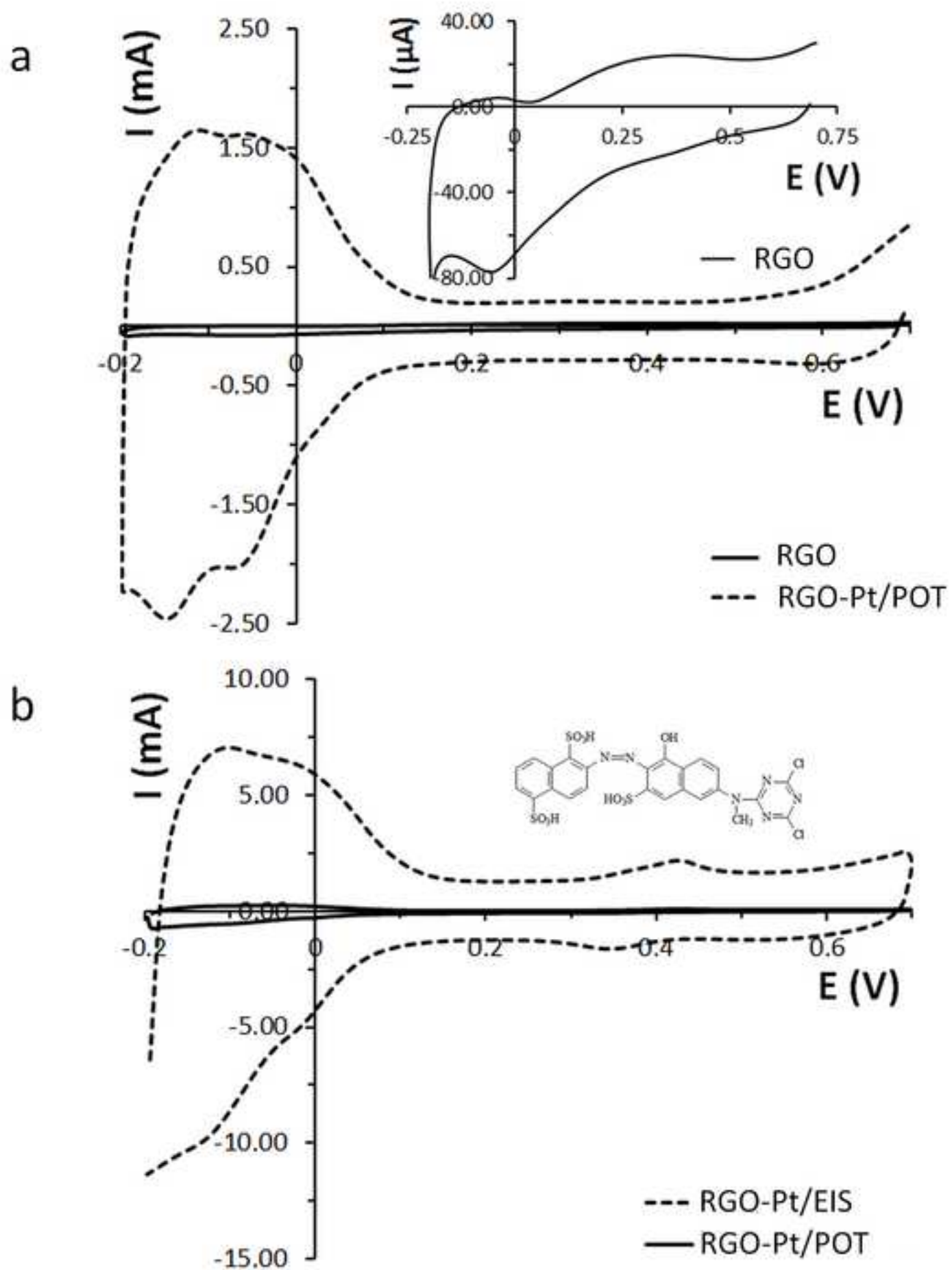


Figure 2

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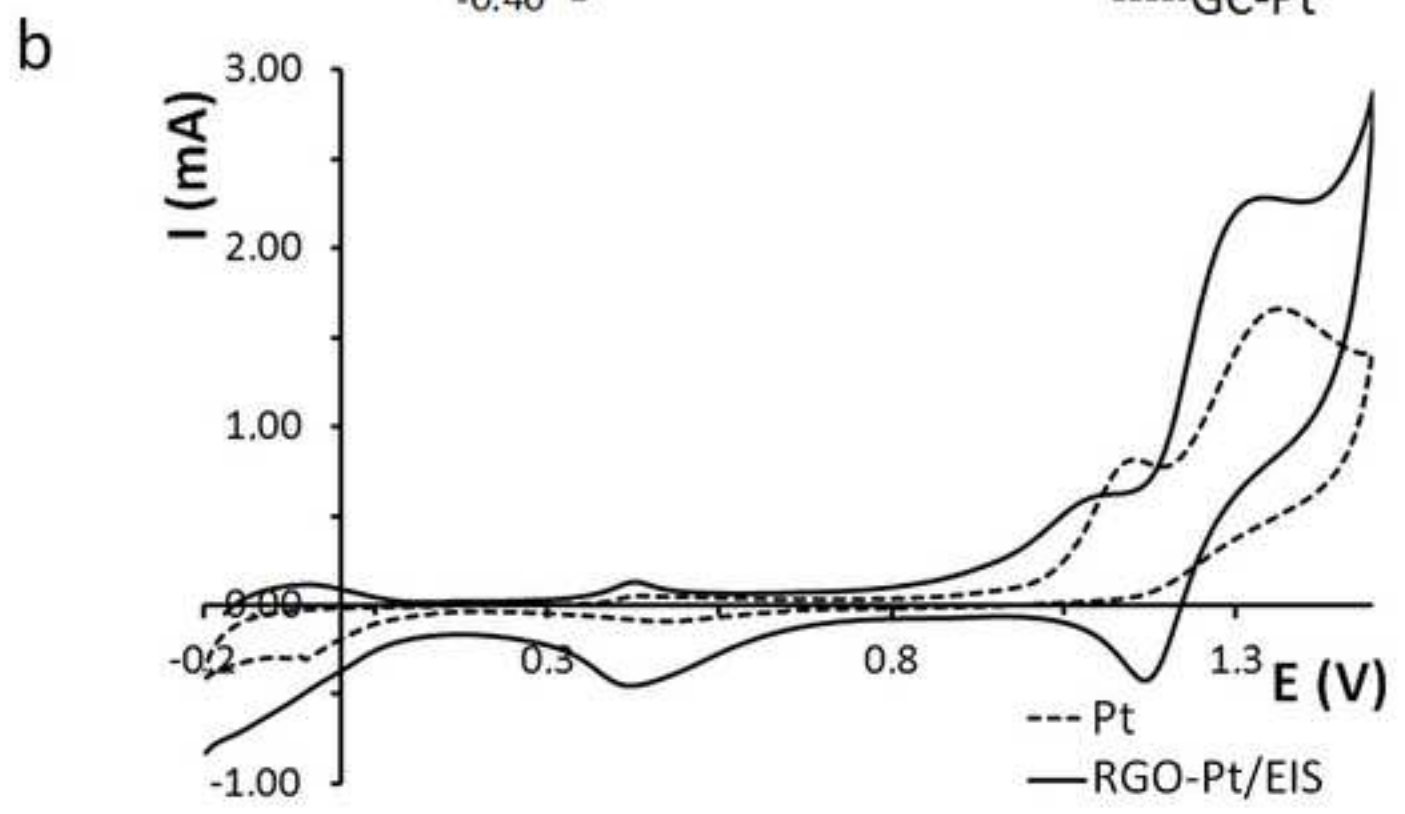
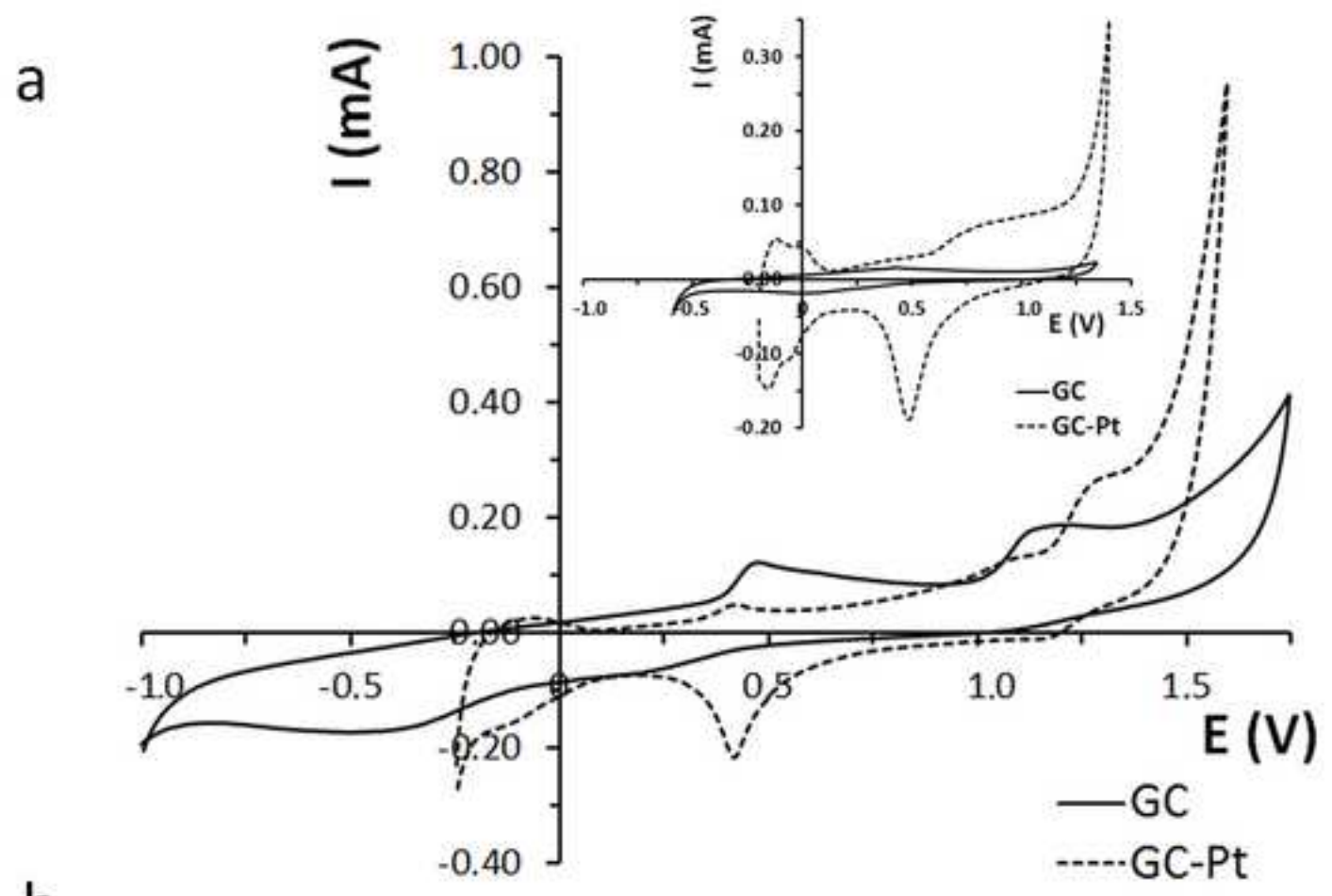


Figure 3
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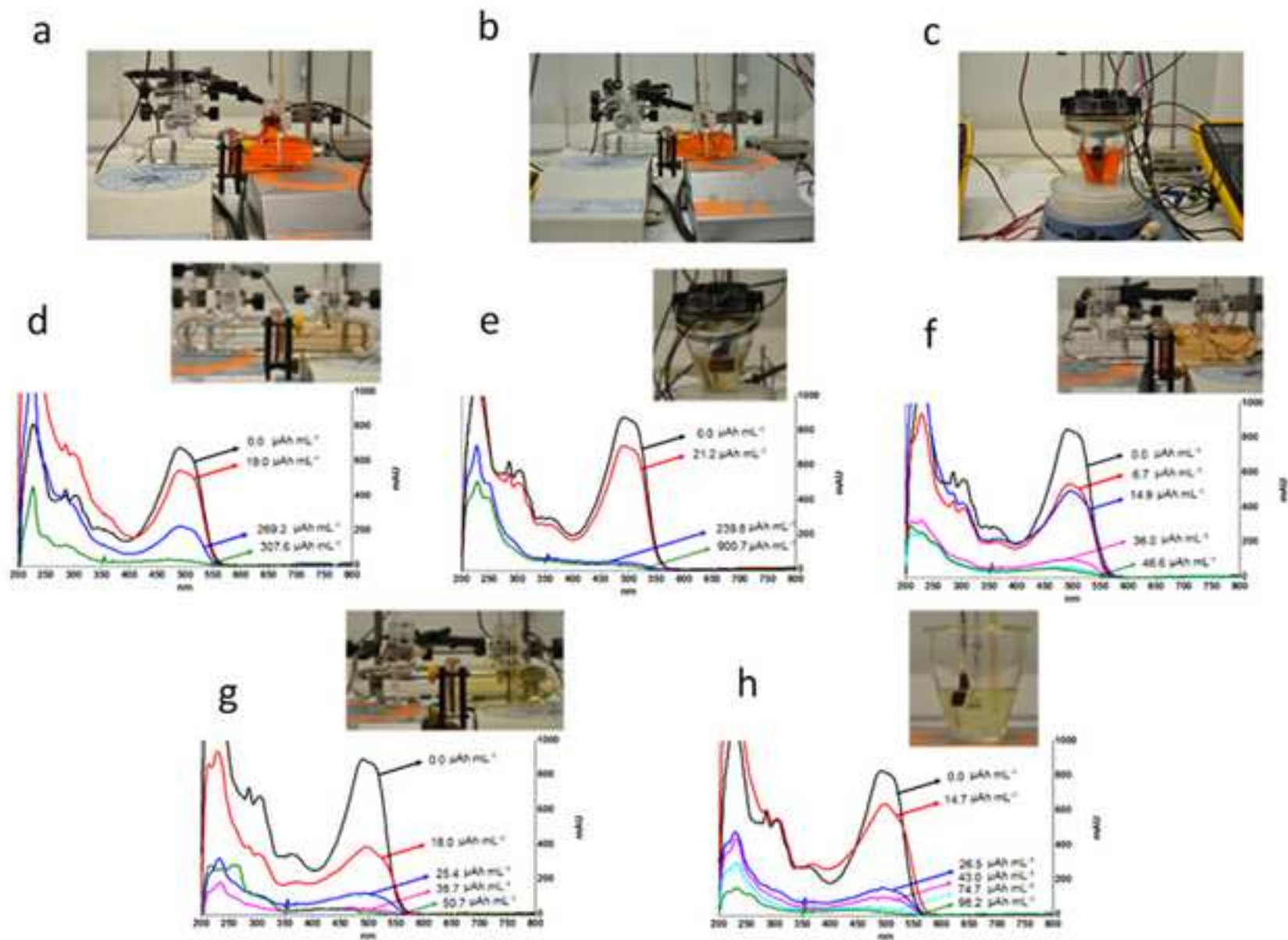


Figure 4

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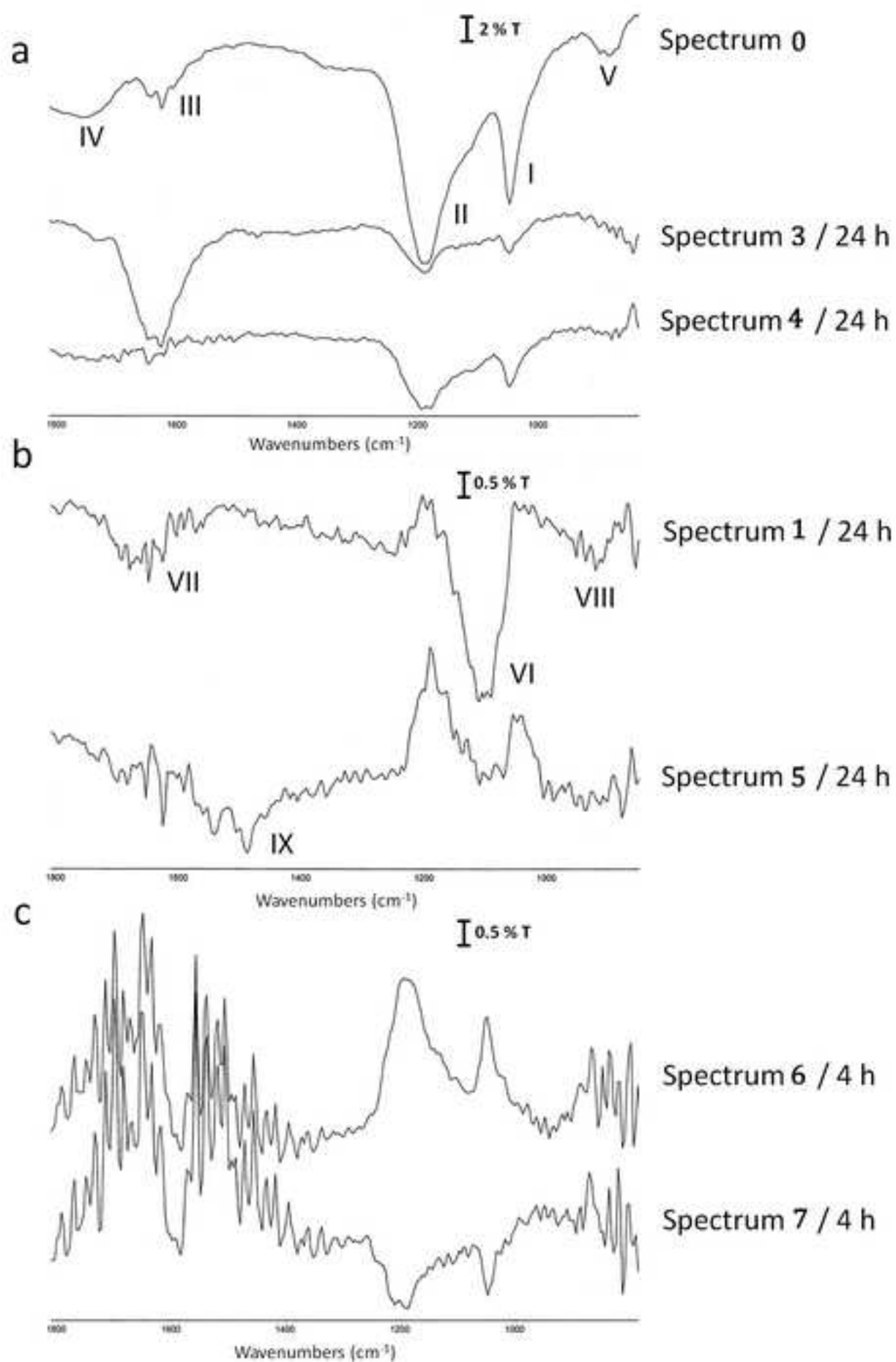


Figure 5
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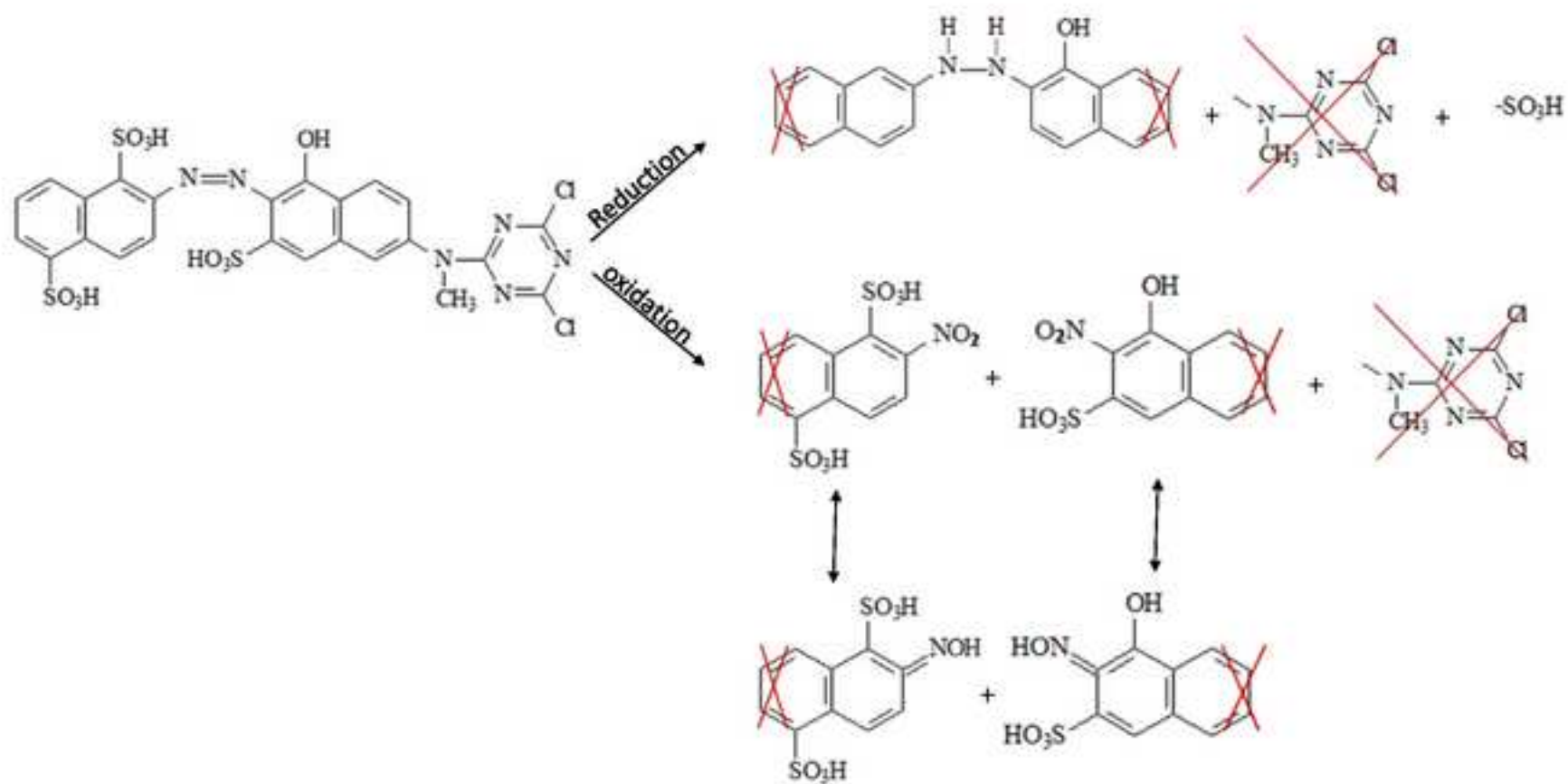


Figure 6
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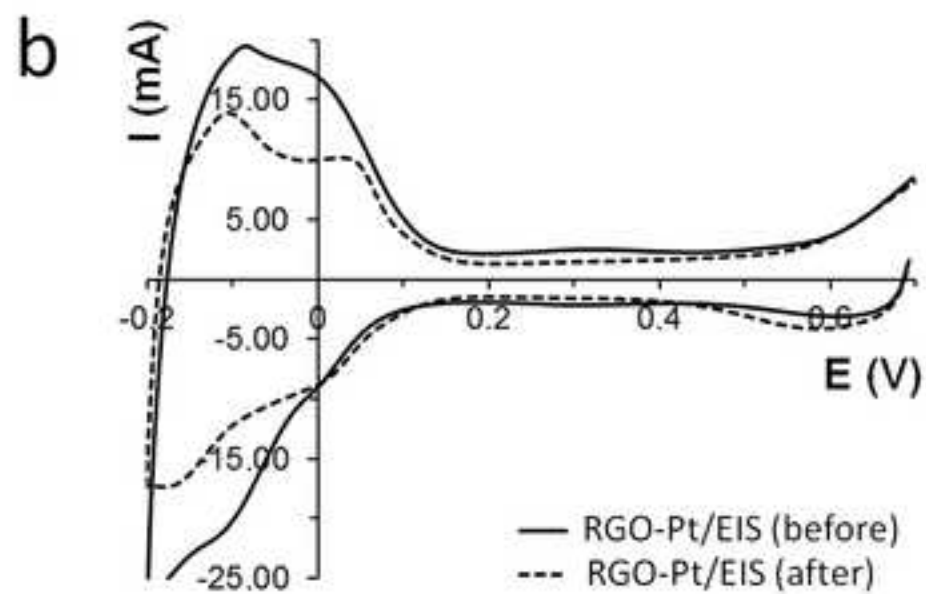
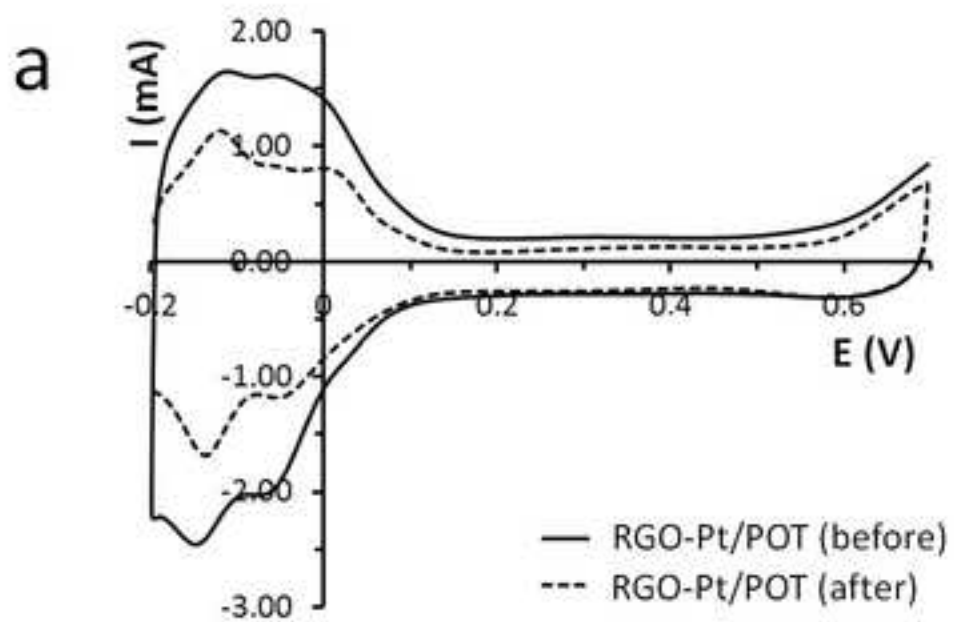


Figure SM-1

[Click here to download Supplementary Material: Fig SM-1 revised.tif](#)

Figure SM-2

[Click here to download Supplementary Material: Fig SM-2 revised.tif](#)

Table captions

Table 1. Kinetics analyses obtained for all the electrolyses: decolorization kinetics rate ($\mu\text{A}^{-1} \text{h}^{-1} \text{mL}$), specific charge ($\mu\text{Ah mL}^{-1}$) for a complete decolorization (99 per cent), percentage of decolorization after 24 h of electrolysis and electrical energy per order (kWh m^{-3}) corresponding to an 80 per cent decolorization.

Figure Captions

Figure 1. Figure 1. a) Cyclic voltammograms of RGO and RGO-Pt/POT as WE in 0.5 M H_2SO_4 . Inset figure: RGO as WE. b) Cyclic voltammograms of RGO-Pt/EIS and RGO-Pt/POT as WE in 0.5 M H_2SO_4 and 3.9 g L^{-1} PMX2R. Inset figure: Chemical structure of C.I. Reactive Orange 4. Second scan in all cases.

Figure 2. a) Cyclic voltammograms of GC and GC-Pt as WE in 0.5 M H_2SO_4 and 3.9 g L^{-1} PMX2R. Scan rate: 50 mV s^{-1} . Inset: Cyclic voltammograms of GC-Pt and GC as WE in 0.5 M H_2SO_4 solution; scan rate: 10 mV s^{-1} . b) Cyclic voltammograms of Pt and RGO-Pt/EIS as WE in 0.5 M H_2SO_4 and 3.9 g L^{-1} PMX2R solution; scan rate: 50 mV s^{-1} . Second scan in all cases.

Figure 3. UV-Vis evolutions of 0.08 g L^{-1} PMX2R in 0.5 M H_2SO_4 . a) Initial solution. b) Experiment number 1. c) Experiment number 2. d) Experiment number 3. e) Experiment number 4. f) Experiment number 5. g) Experiment number 6. h) Experiment number 7. Inset images: solution after the electrolyses.

Figure 4. FTIR-ATR spectra of final samples. a) Spectrum 0: initial solution. Spectrum 3: Experiment number 3. Spectrum 4: Experiment number 4. b) Spectrum 1: Experiment number 1. Spectrum 5: Experiment number 5 c) Spectrum 6: Experiment number 6. Spectrum 7: Experiment number 7.

Figure 5. Oxidation and reduction reaction mechanisms.

Figure 6. Voltammograms of a) RGO-Pt/POT and b) RGO-Pt/EIS in a 0.5 M H₂SO₄ before and after the electrolysis.

SUPPLEMENTARY MATERIAL

Figure SM-1. Images of the two configuration of the electrolyses cells: a) divided b) undivided.

Figure SM-2. a) FESEM micrograph of a freshly obtained RGO-Pt/EIS electrode. b) FESEM micrograph of RGO-Pt/EIS anode after the electrolysis of a PMX2R solution and 0.3 g L⁻¹ NaCl. Anodic potential: + 1.50 V.

