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**RESISTANT MALTODEXTRIN'S EFFECT ON THE  
PHYSICOCHEMICAL AND STRUCTURE PROPERTIES OF  
SPRAY DRIED ORANGE JUICE POWDERS**

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Keywords:	resistant maltodextrin, colour, microstructure, spray drying, orange juice

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Manuscripts

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3 1 **RESISTANT MALTODEXTRIN'S EFFECT ON THE PHYSICOCHEMICAL AND**  
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5 2 **STRUCTURE PROPERTIES OF SPRAY DRIED ORANGE JUICE POWDERS**  
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3 25 **Abstract:**  
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5  
6 26 Resistant maltodextrin (RMD), derived from the heat treatment of corn starch, is a  
7  
8 27 water-soluble fermentable functional fibre. Its benefits include being a satiating  
9  
10 28 prebiotic, reducer of glucose and triglycerides in the blood, and promoter of good gut  
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12  
13 29 health. Despite its functionality, there is still further need for investigations of its use as  
14  
15 30 a food formulating ingredient and their physicochemical property changes. This study  
16  
17 31 aimed to evaluate the effect of RMD addition on the physicochemical and structural  
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19 32 properties of spray dried orange juice powders. The physicochemical properties  
20  
21 33 evaluated were water content, hygroscopicity, bulk density, porosity, water solubility,  
22  
23 34 water absorption index, colour, and microstructure. We found RMD addition  
24  
25 35 improved the orange juice spray dried powder productivity. Samples with RMD were  
26  
27 36 more porous and less hygroscopic, and they presented low water content;  
28  
29 37 physicochemical properties desirable for powders. Therefore, to reach a compromise  
30  
31 38 between powders' functionality and physicochemical property changes, especially  
32  
33 39 colour, the addition of 5 RMD% is recommended.  
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45 42 **Keywords:** resistant maltodextrin; colour; microstructure; spray drying; orange juice  
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12  
13 53 The authors declare no conflict of interest.

14  
15  
16 54 *Availability of data and material*

17  
18 55 Not applicable

19  
20  
21 56 *Code availability*

22  
23 57 Not applicable

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25  
26 58 *Author Contributions*

27  
28  
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30  
31 60 investigation, M.I and P.G-S.; resources, P.G-S.; data curation, M.I. and P.G-S.;

32  
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34  
35 62 M; supervision, J.M-M.; project administration, P.G-S.; funding acquisition, P.G-S. and

36  
37 63 J. M-M. All authors have read and agreed to the published version of the manuscript.

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## 66 1. Introduction

67 Fruits have historically been considered rich sources of essential dietary micronutrients  
68 and fibres. Moreover, they have been recognised as important sources for an array of  
69 phytochemicals that individually, or in combination, may benefit health [1]. Frequent  
70 consumption of fruits and vegetables is associated with a lowered risk of cancer, heart  
71 disease, hypertension, and stroke [2-4]. Among fruits, citrus juice is an important  
72 dietary source of bioactive compounds, whose beneficial health effects are ascribed to  
73 its high content of vitamins, phenols, and carotenoids [5-7].

74 Powdered fruit products may be an alternative to increase fruit consumption in  
75 response to the increased demand for ready-to-eat foodstuffs. The benefits of handling,  
76 packing, and transport of the fruit powder are the product's high stability and the ease  
77 of its final consumption. Powdered fruit products are sugar-rich foods, thus present  
78 structural problems like stickiness, caking, and collapse [8]. One way to prevent this is  
79 the addition of biopolymers of high-molecular-weight [9]. Biopolymers, such as gums,  
80 maltodextrins, proteins, starches, and natural fibre have been used as drying carriers to  
81 obtain stable powder fruits products [10-13]. However, the addition of biopolymers  
82 may cause effects in other properties, such as changes in porosity, colour, or  
83 microstructure of the final product [14].

84 Resistant maltodextrin (RMD), derived from heat treatment of corn starch, is a water-  
85 soluble fermentable functional fibre. Other authors have shown its important benefits  
86 such as being a satiating prebiotic [15, 16], reducer of glucose and triglycerides in the  
87 blood [17, 18], and promoter of good gut health [19]. Despite its functionality, there is  
88 still a need for further investigations on its use as a food formulation ingredient and  
89 their physicochemical property changes.

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2  
3 90 Spray drying (SD) is a well-established and widely used method for transforming  
4  
5 91 liquid food products into powder form. The process of SD comprises transforming a  
6  
7 92 product from fluid to a solid powdered state, through the dispersion of the product  
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9  
10 93 droplets inside a chamber where it contacts hot air [20]. Spray dried powders are more  
11  
12  
13 94 economical to produce than other processes, such as freeze drying [21]. SD has many  
14  
15 95 applications, particularly in the food, pharmaceutical, and agrochemical industries [22–  
16  
17  
18 96 25]. However, drying fruit pulps or juices, such as sugar-rich foods, using SD is  
19  
20 97 difficult as sticky products are produced, causing high operational costs and low  
21  
22  
23 98 product yield. To complete the process economically and with technical viability, it is  
24  
25 99 necessary to add carrying agents [13, 26].

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28 100 This study aimed to evaluate the effect of RMD addition on the physicochemical and  
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30 101 structural properties of spray dried orange juice powders. Thus, to help promote fruit  
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33 102 consumption in a useful format, with functional fibre.

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## 36 37 104 **2. Materials and Methods**

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### 40 41 106 *2.1. Raw material*

42  
43 107 This study was conducted with freshly squeezed orange juice supplied by Refresco  
44  
45 108 Iberia S.A.U. (València, Spain). Resistant maltodextrin (RMD; Fibersol-2) was  
46  
47 109 purchased from ADM/Matsutani, LLC (Decatur, IL, USA).

48  
49 110

### 50 51 111 *2.2. Preparation of the feed mixture and spray drying (SD) conditions*

52  
53 112 Freshly squeezed orange juice was mixed with RMD, reaching RMD (2.5, 5, and 7.5%).  
54  
55 113 The mixture was stirred for 30 min until homogeneous. After, the °Brix was measured

1  
2  
3 114 with a refractometer at 20 °C (PAL-BX/RI, Atago, Japan), it was fed into a Büchi B-290  
4  
5 115 (Switzerland) mini spray dryer with the following operating conditions: aspirator rate  
6  
7  
8 116 90% (35 m<sup>3</sup>/h); atomisation air rotameter 40 mm (473 L/h) with a co-current flow; pump  
9  
10 117 rate 30% (9 mL/min), drying air inlet temperature was 150 °C, and the outlet  
11  
12  
13 118 temperature was registered. After the experiment was completed and when the air  
14  
15 119 inlet temperature fell below 50 °C, the samples were collected from the product  
16  
17  
18 120 collection vessel.

19  
20 121 For comparing physicochemical properties of spray dried samples to juice powder  
21  
22  
23 122 without RMD, freshly squeezed orange juice was freeze dried. A juice layer (0.5 cm  
24  
25 123 thick) was placed on a standardised aluminium plate (15 cm diameter and 5 cm height)  
26  
27  
28 124 and frozen at -45 °C for 24 h. After, the sample was dried in a Lioalfa-6 Lyophiliser  
29  
30 125 (Telstar, Spain) at 2,600 Pa at -56.6 °C for 48 h. This sample was the control.  
31  
32

33 126

### 34 35 127 2.3. Product yield, drying ratio, and productivity

36  
37  
38 128 Product yield ( $Y_p$ ) was defined as the ratio of the mass of solutes present in the  
39  
40 129 powder obtained at the end of each SD period, to the mass of solutes present in the  
41  
42 130 mixture prior to SD [27]. The SD drying ratio and productivity were calculated  
43  
44  
45 131 according to Cai and Corke [28] with slight modification. The drying ratio was  
46  
47 132 calculated using equation (1) (powder solid content/feed solid content).

$$48 \text{ Drying ratio} = \frac{(X_w^i + 1)}{(X_w^f + 1)} \quad (1)$$

49  
50  
51 133 Where  $X_w^i$  is the mixture feed moisture (dry basis) and  $X_w^f$  is the powder moisture (dry  
52  
53  
54 134 basis). The productivity was calculated using equation (2).  
55  
56  
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$$\text{Productivity (g/h)} = \frac{\text{Feed rate (g/h)}}{\text{Drying ratio}} \quad (2)$$

135

136 *2.4. Physicochemical analysis*

137 All the analyses on samples, described in this section, were conducted in triplicate.

## 138 2.4.1. Water content

139 The water mass fractions (g/100g) in freshly squeezed orange juice, mixtures with  
140 RMD, and obtained powders were obtained by vacuum drying the samples in a  
141 vacuum oven (Vaciotem, J.P. Selecta, Spain) at  $70 \pm 1$  °C under a pressure of < 100  
142 mmHg until achieving constant weight (AOAC, 2000).

143

## 144 2.4.2. Soluble solid content

145 The soluble solid mass fractions in freshly squeezed orange juice and mixtures with  
146 RMD ( $x_s$ ) were determined by measuring the °Brix in a previously homogenised  
147 sample with a portable digital refractometer PAL-BX/RI, at 20 °C (Atago, Japan).

148

## 149 2.4.3. Hygroscopicity

150 To measure hygroscopicity [28], samples (about 1 g in a Petri dish) of each powder  
151 were placed at 25 °C in an airtight plastic container containing a Na<sub>2</sub>SO<sub>4</sub> saturated  
152 solution (81% RH) at the bottom. After 1, 3, and 7 days, each sample was weighed and  
153 hygroscopicity was expressed as g of water gained per 100 g dry solids.

154

## 155 2.4.4. Bulk density and porosity

1  
2  
3 156 The porosity ( $\epsilon$ ), percentage of air volume related to the total volume, was calculated  
4  
5  
6 157 from the true ( $\rho$ ) and bulk ( $\rho_b$ ) densities according to equation 3.

$$\epsilon = \frac{(\rho - \rho_b)}{\rho} \quad (3)$$

7  
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10  
11 158 The true density of powders was determined using a helium pycnometer (AccPyc 1330,  
12  
13  
14 159 Micromeritics, Norcross, USA) and the bulk density by the ratio mass to volume of the  
15  
16  
17 160 tapped samples according Agudelo et al. [10].  
18

19 161

#### 20 21 162 2.4.5. Water solubility index (WSI) and water absorption index (WAI)

22  
23  
24 163 The WSI and WAI were determined using the method of Singh and Smith [30]. A 2.5 g  
25  
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27 164 sample was dispersed in 25 g of distilled water, using a rod to manually break up any  
28  
29  
30 165 lumps. After stirring for 30 min using a magnetic stirrer, the dispersions were rinsed in  
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32  
33 166 to tared 50 mL centrifuge tubes, made up to 32.5 g and centrifuged at 3,000 g for 10  
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36 167 min. The supernatant was decanted for determination of its dissolved solid content and  
37  
38  
39 168 the sediment was weighed. WSI and WAI were calculated according to equations 4 and  
40  
41 169 5, respectively.

$$\text{WSI (\%)} = \left( \frac{\text{weight of dissolved solids in supernatant}}{\text{weight of dry solids}} \right) \times 100 \quad (4)$$

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$$\text{WAI} = \frac{\text{weight of sediment}}{\text{weight of dry solids}} \quad (5)$$

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#### 52 53 172 2.4.6. Colour measurement

54  
55  
56 173 The colour of the powder samples was measured using a Konica Minolta CM-700d  
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59 174 colorimeter (Konica Minolta CM-700d/600d series, Tokyo, Japan) with standard D65  
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3 175 illuminate and 10° visual angle. The powder was placed in a circular aluminium  
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5 176 sample holder of 17.7 mm in diameter and 9.53 mm in height. A reflectance glass (CR-  
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8 177 A51, Minolta Camera, Japan) was placed between the sample and colorimeter lens. The  
9  
10 178 measurement window was 6 mm in diameter. The results were expressed using  
11  
12  
13 179 CIELab system [31]. Chroma; C\* (saturation), hue angle; h\*, and the total colour  
14  
15 180 difference ( $\Delta E$ ) taken orange juice freeze dried powder without RMD as reference were  
16  
17  
18 181 also calculated.  
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20  
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### 22 23 183 *2.5. Powder morphology*

24  
25 184 Morphology and surface microstructures of control and spray dried orange juice  
26  
27  
28 185 powder with different RMD concentrations were examined using a Zeiss Ultra55 Field  
29  
30 186 Emission Scanning Electron Microscope (FESEM; Carl Zeiss AG, Germany) with the  
31  
32  
33 187 Secondary Electron Detector (ETSE). The powder was fixed on a carbon adhesive tape  
34  
35 188 and was platinum coated before analysis. Images were taken at an accelerating voltage  
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38 189 of 1 kV and WD 3.5 mm. To examine the microstructure of samples, the electron mode  
39  
40 190 was used under  $\times 100$  magnifications; to avoid charging a sample micrograph was  
41  
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43 191 taken after platinum coating. Three representative location areas were imaged for each  
44  
45 192 sample, and at least 12 images at different magnifications were obtained to assure the  
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47  
48 193 FESEM imaging results were representative.

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### 51 52 195 *2.6. Statistical analysis*

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55 196 Analysis of variance (ANOVA), with a confidence level of 95% ( $p < 0.05$ ), using  
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58 197 Statgraphics (Centurion XVII Software, version 17.2.04) was applied to evaluate the  
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3 198 differences among samples. A correlation analysis among all parameters studied, with  
4  
5 199 a 95% significance level, was achieved (Centurion XVII Software, version 17.2.04).  
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### 201 **3. Results and Discussion**

12 202 Freshly squeezed orange juice presented a soluble solid mass fraction mean value (and  
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14  
15 203 standard deviation) 0.130 (0.002)  $g_{\text{soluble solid}}/g_{\text{product}}$ . After mixing with 2.5, 5, and 7.5%  
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17 204 resistant maltodextrin (RMD) this changed to 0.153 (0.002), 0.172 (0.003), and 0.198  
18  
19 205 (0.002)  $g_{\text{soluble solid}}/g_{\text{product}}$  respectively.  
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#### 207 *3.1. Spray drying (SD) parameters*

28 208 Orange juice contains sugars and organic acids [32] which make the SD process  
29  
30 209 difficult, mainly due to the basic physical characteristics of the low molecular weight  
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32  
33 210 sugars. Moreover, organic acids, such as tartaric, malic, and citric acid, also contributes  
34  
35 211 to the problem of stickiness in the powder [22]. Therefore, it is extremely difficult to  
36  
37 212 obtain powder at the exit of the dryer in samples without adding high-molecular-  
38  
39 213 weight solutes, thus large deposits are formed on the main chamber and cyclone walls  
40  
41 214 of spray driers.  
42  
43  
44

45 215 Table 1 shows mean values and standard deviation of outlet temperature, product  
46  
47 216 yield, drying ratio, productivity, and water content of spray dried samples with 2.5, 5,  
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49 217 and 7.5% RMD. As seen, higher RMD concentrations give higher outlet temperatures  
50  
51 218 and using different RMD % affected the outlet temperature significantly ( $p < 0.05$ ).  
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53 219 Further, the sample product yield increased with RMD %, however, the differences  
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55 220 among samples are not significant ( $p > 0.05$ ). The drying ratio decreased significantly  
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3 221 ( $p < 0.05$ ) when the RMD % increased, whereas the productivity increased significantly  
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5 222 ( $p < 0.05$ ) when RMD % increased. Several authors have reported that an increase in  
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8 223 the maltodextrin content results in an increase of the recovery of feed solids in the  
9  
10 224 product [10, 33, 34]. Water content of orange juice powder exhibited an inverse  
11  
12  
13 225 relationship with increasing RMD %, which was also reported by other authors  
14  
15 226 working with maltodextrins or gum arabic [20, 25, 28, 35].  
16  
17

18 227

### 20 228 *3.2. Physicochemical properties of obtained powders.*

22 229 Water content, hygroscopicity, bulk density, porosity, water solubility, water  
23  
24 230 absorption, colour, and structure of powders are important physicochemical properties  
25  
26  
27 231 to evaluate the suitability of orange juices powders.

28  
29 232 Food powders with lower hygroscopicity and water content are considered good  
30  
31 233 powdered products. Goula and Adamopoulos [35] suggested that adding maltodextrin  
32  
33 234 decreased powder hygroscopicity. Figure 1 shows the evolution of hygroscopicity of  
34  
35 235 each orange juice powder along the assay time. All samples increased their  
36  
37 236 hygroscopicity gradually during the assay time. After 7 d, hygroscopicity of orange  
38  
39 237 juice powder was significantly ( $p < 0.05$ ) lower than the other samples when the RMD  
40  
41 238 concentration was 5 or 7.5%. The lower hygroscopicity of orange juice powders when  
42  
43 239 the RMD was added could be related to the less hygroscopic nature of maltodextrin.  
44  
45 240 Other authors have reported similar observations [20, 25, 28, 35].  
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48  
49 241 Figure 2 shows the bulk density and porosity of each orange juice powder. Comparing  
50  
51 242 with the control, orange juice powders with 2.5 or 5% RMD were more similar than  
52  
53 243 sample powder with 7.5% RMD. There was a significant ( $p < 0.05$ ) increase of porosity  
54  
55 244 and decrease of bulk density due to RMD concentration in powders. Porosity plays an  
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3 245 important role in the agglomerate strength of dried foods [36]. Furthermore, a greater  
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5 246 porosity (and lower bulk density) corresponds to a freer flowing powder with a greater  
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8 247 air volume distributed among particles plus is more soluble [36, 37]. Other studies  
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11 248 showed a similar trend as porosity increases when solutes with high-molecular-weight  
12  
13 249 were added [10, 11].

14  
15 250 Figure 3 shows the water absorption index (WAI) and water solubility index (WSI) of  
16  
17  
18 251 each orange juice powder. The WAI indicates the amount of water immobilised by the  
19  
20  
21 252 samples [38], whereas the WSI is related to the amount of soluble solids present in the  
22  
23 253 product as a function of the solubilisation of starches, sugars, proteins, fibres, and  
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25 254 maltodextrin [39]. Observed in Figure 3, the highest difference was between the control  
26  
27  
28 255 and spray dried samples, since the different processes (freeze and spray dried) affected  
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30  
31 256 the indexes significantly ( $p < 0.05$ ). Besides, WAI and WSI of the orange juice powders  
32  
33 257 were satisfactory because most of the solid elements in the powder obtained under the  
34  
35 258 experimental conditions were easily soluble in water. The spray dried sample's WAI  
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37  
38 259 decreased significantly ( $p < 0.05$ ) when higher RMD % was used. However, WSI did  
39  
40  
41 260 not show significant differences ( $p > 0.05$ ) when adding RMD. Furthermore, spray  
42  
43 261 dried samples presented higher WSI than the control (freeze dried sample).

44  
45 262 Table 2 shows Pearson correlation coefficients among the  $x_w$ , WAI, WSI,  $\rho_b$ ,  $\varepsilon$  and  $Hg_{7d}$   
46  
47  
48 263 of orange juice spray dried powders. There were positive and significant ( $p < 0.05$ )  
49  
50  
51 264 correlations between  $x_w$ , WAI, and  $\rho_b$ . However, there was negative and significant ( $p <$   
52  
53 265  $0.05$ ) correlation between  $x_w$  and  $\varepsilon$ . Samples with higher water content presented higher  
54  
55 266 amounts of water immobilised and bulk density and lower free flowing powders.  
56  
57  
58 267 Likewise, WAI showed significant positive and negative correlations ( $p < 0.05$ ) with  $\rho_b$   
59  
60 268 and  $\varepsilon$  respectively. Further, powders with higher WAI are prone to agglomeration.

1  
2  
3 269 Colour coordinates of samples are shown in Table 3. The control showed L\* and b\* was  
4  
5 270 like the spray dried sample with 2.5% RMD, however, a\* was nearer to the spray dried  
6  
7 271 sample with 5% RMD, while C\* and h\* were nearer with 7.5% RMD. Table 3 shows  
8  
9 272 there was a significant ( $p < 0.05$ ) effect of on colour coordinates with RMD addition.  
10  
11 273 Colour of spray dried samples with RMD showed significant differences among  
12  
13 274 studied % (2.5, 5 and 7.5). Powder with 2.5 % RMD presented the lowest L\* and the  
14  
15 275 highest a\* and b\*. When RMD concentration increased in spray dried samples, L\* and  
16  
17 276 h\* increased while a\*, b\*, and C\* decreased. This trend was also observed in other  
18  
19 277 studies in grapefruit powders with gum arabic [10, 11]. Total colour differences  
20  
21 278 between spray dried samples, and the control were higher than 3 units. Therefore, they  
22  
23 279 are perceptible by human eye, which only distinguishes colour difference if  $\Delta E^*$  is  
24  
25 280 larger than 3 [40]. Total colour differences were higher when RMD concentration  
26  
27 281 increased. Furthermore, there were significant ( $p < 0.05$ ) differences among spray dried  
28  
29 282 samples. The highest colour differences were observed in powders with 7.5 % RMD.  
30  
31 283 Figure 4 shows the appearance of the studied samples. In concordance with colour  
32  
33 284 coordinates, orange juice spray dried with 7.5% RMD was more whitish. Powders with  
34  
35 285 2.5 % RMD was redder than the rest, as can be observed in Table 3 (a\* colour  
36  
37 286 coordinate). The control's appearance was like the orange juice spray dried with 2.5 or  
38  
39 287 5% RMD. Therefore, all samples could be suitable in relation with colour and  
40  
41 288 appearance of powders.  
42  
43 289 Figure 5 shows FESEM micrographs of control and spray dried orange juice powders  
44  
45 290 with 2.5, 5, and 7.5% RMD. Spray dried orange powder has a spherical or oval shape  
46  
47 291 and smooth surfaced particles, typical of SD samples as shown by other authors in  
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49 292 mangos [41] and lychees [42]. Powdered particles presented a continuous wall and the

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2  
3 293 absence of surface cracks. Furthermore, when increasing RMD % in orange juice,  
4  
5 294 powdered particles are smaller with a higher particle density, observed in the analysed  
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7  
8 295 field. This is likely related to more free flowing powders, because samples with 7.5%  
9  
10 296 RMD were more porous (Figure 2). Moreover, in a concordance to Bazaria and Kumar  
11  
12  
13 297 [43], increasing the solids content in the liquid to be spray dried leads to a smoother  
14  
15 298 particle surface. The average particle size obtained from micrographs of the powders  
16  
17  
18 299 was between 48 to 117  $\mu\text{m}$ . Particle size mean values (and standard deviation) of the  
19  
20 300 control was 98 (3)  $\mu\text{m}$ ; whereas spray dried samples were 117 (9), 77 (9), and 48 (8)  $\mu\text{m}$   
21  
22  
23 301 for 2.5, 5, and 7.5% RMD, respectively. Therefore, the effect of RMD % on particle size  
24  
25 302 is clear in spray dried samples; where an increase in % RMD provoked smaller  
26  
27  
28 303 particles size. These results are consistent with the findings of Tze et al. [44], studying  
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30 304 maltodextrin % in spray dried pitaya fruit powders.  
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### 34 306 **3. Conclusions**

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37 307 Resistant maltodextrin (RMD) added in orange juice to give powders by spray drying  
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39 308 improved the productivity of the drying process. When RMD concentration increased  
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42 309 in powders porosity and luminosity increased where the water content, bulk density,  
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45 310 water absorption index, hygroscopicity, particle size, and redness decreased. Thus,  
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48 311 samples with RMD were more porous and less hygroscopic, and presented low water  
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50 312 content. These physicochemical properties are desirable for powders. However, high %  
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53 313 RMD (7.5) showed high value of total colour differences. Therefore, to reach a  
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55 314 compromise between the functionality of the powders indicated by other authors and  
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58 315 the possible changes of their physicochemical properties, especially colour, the  
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60 316 addition of 5% RMD is recommended. Consequently, the adequate physicochemical



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3 317 properties of the powdered product obtained from orange juice are maintained to a  
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5 318 greater extent.

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10 320 **Acknowledgements:**

11  
12 321 The authors thank Refresco Iberia S.A.U. for supplying the freshly squeezed orange  
13 322 juice.

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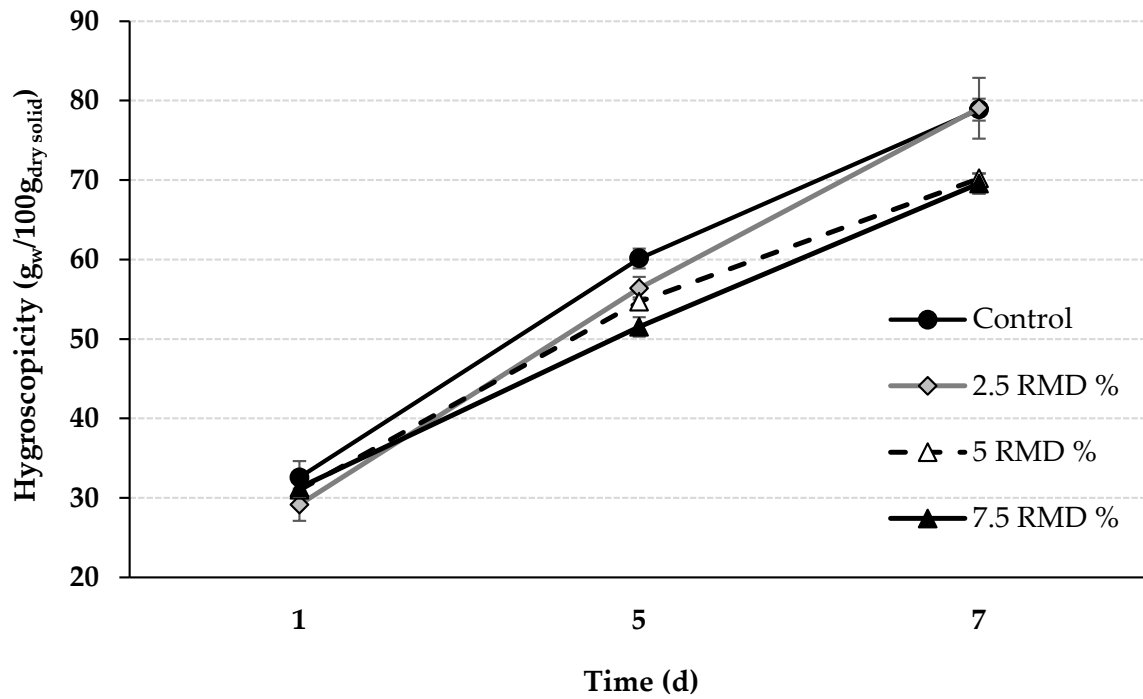
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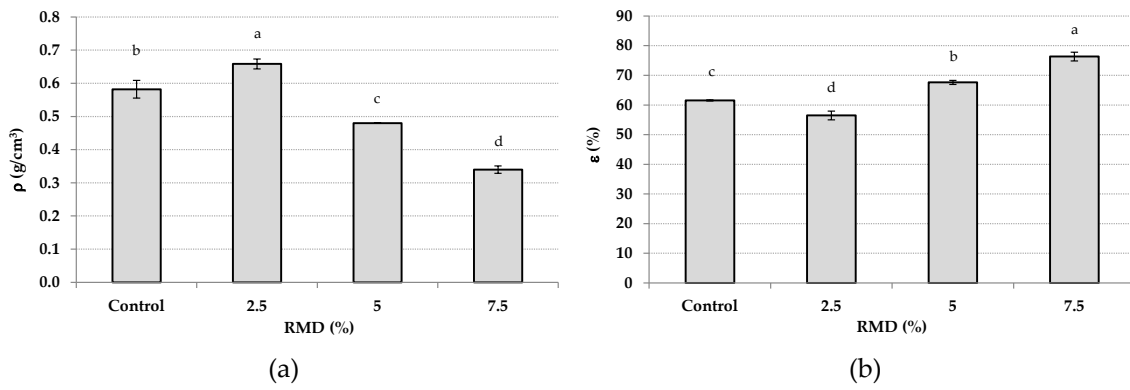
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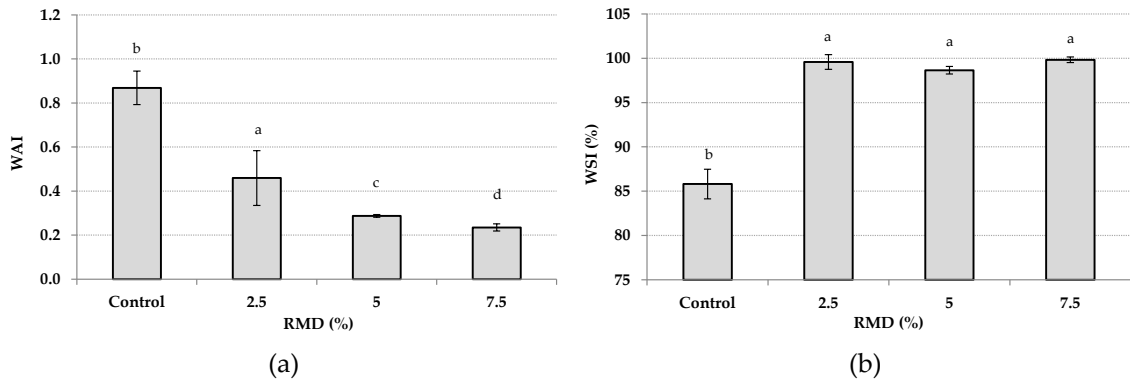
**Figure 1.** Evolution of hygroscopicity (mean and standard deviation) of each orange juice powder along the assay time.



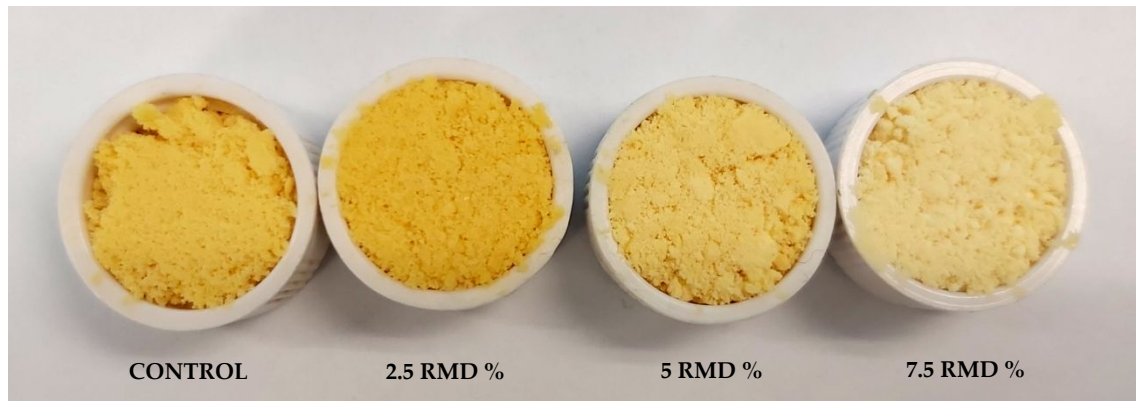
**Figure 2.** Mean values and standard deviation of (a) bulk density and (b) porosity. Letters indicate homogeneous groups established using the ANOVA ( $p < 0.05$ ) for each parameter analysed.

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**Figure 3.** Mean values and standard deviation of (a) water absorption index and (b) water solubility index. Letters indicate homogeneous groups established by the ANOVA ( $p < 0.05$ ) for each parameter analysed.



**Figure 4.** Appearance of studied orange juice powder samples.

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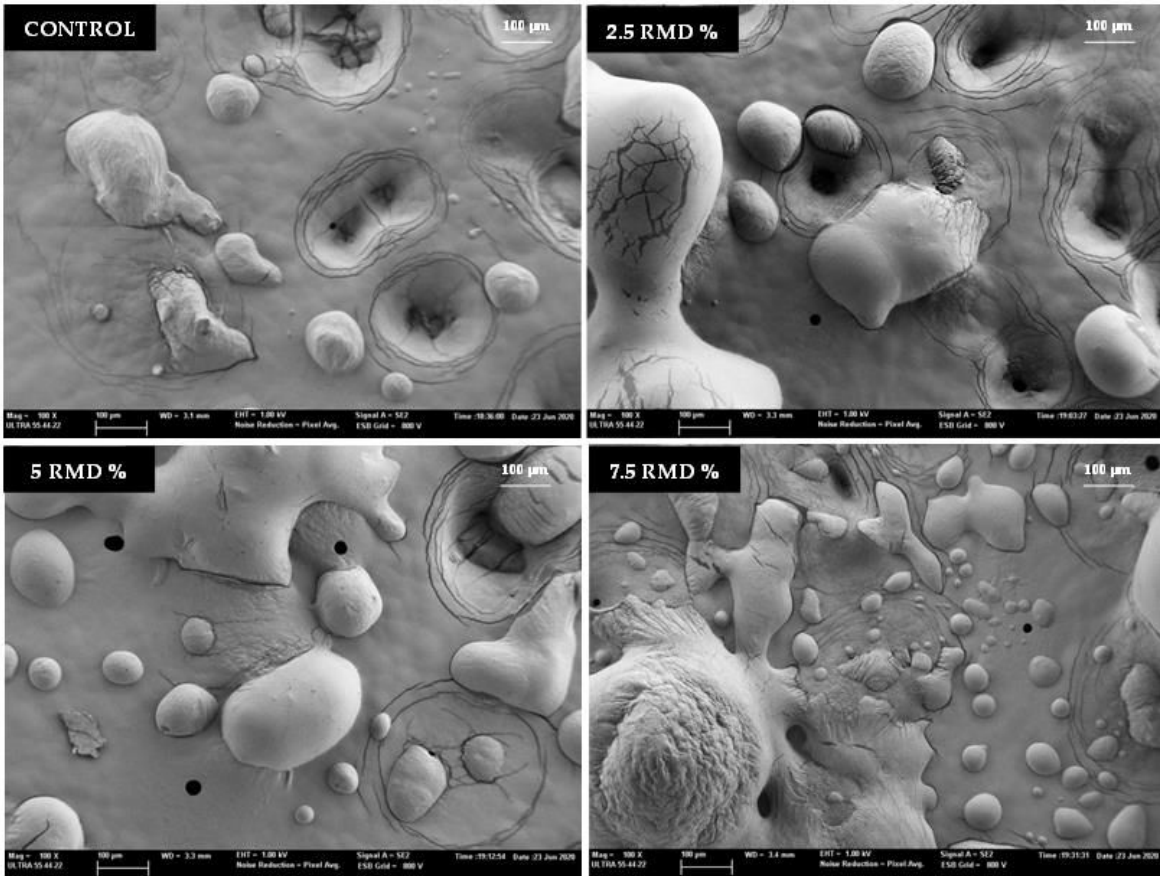


Figure 5. FESEM micrographs at 100 magnifications of studied samples.

**Table 1.** Outlet temperature, product yield, drying ratio, productivity, and water content ( $x_w$ ) mean values (and standard deviation) of spray dried powders.

Parameter	% of RMD		
	2.5	5	7.5
Outlet temperature (°C)	86.5 (1.2) <sup>c</sup>	91.0 (0.6) <sup>b</sup>	94.3 (0.8) <sup>a</sup>
Product yield (g <sub>solutes in the powder</sub> /100 g <sub>solutes in the mixture</sub> )	44.0 (0.3) <sup>a</sup>	44.8 (0.6) <sup>a</sup>	44.9 (0.2) <sup>a</sup>
Drying ratio	5.935 (0.015) <sup>a</sup>	5.363 (0.012) <sup>b</sup>	4.895 (0.003) <sup>c</sup>
Productivity (g/h)	99.86 (0.06) <sup>c</sup>	114.80 (0.09) <sup>b</sup>	126.9 (0.5) <sup>a</sup>
$x_w$ (g <sub>water</sub> /g <sub>product</sub> )	0.0952 (0.0003) <sup>a</sup>	0.0751 (0.0012) <sup>b</sup>	0.0512 (0.0012) <sup>c</sup>

Letters indicate homogeneous groups established by the ANOVA ( $p < 0.05$ ) within rows.

**Table 2.** Pearson correlation coefficients among studied parameters of orange juice powders.

	<b>WAI</b>	<b>WSI</b>	<b><math>\rho_b</math></b>	<b><math>\varepsilon</math></b>	<b>Hg<sub>7d</sub></b>
<b><math>x_w</math></b>	0.8341*	-0.2006	0.9907*	-0.9828*	-0.7634
<b>WAI</b>		-0.1587	0.8377*	-0.8844*	0.5662
<b>WSI</b>			-0.0700	0.1453	0.4626
<b><math>\rho_b</math></b>				-0.9863*	0.8370*
<b><math>\varepsilon</math></b>					-0.7665

\* Correlation is significant at the 0.05 level.

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**Table 3.** Mean values (and standard deviations) of colour coordinates ( $L^*$ ,  $a^*$ ,  $b^*$ ,  $C^*$ , and  $h^*$ ) and total colour differences ( $\Delta E$ ) of orange juice powders.

	<b>Control</b>	<b>2.5% RMD</b>	<b>5% RMD</b>	<b>7.5% RMD</b>
<b><math>L^*</math></b>	79.9 (0.8) <sup>c</sup>	78.4 (0.7) <sup>d</sup>	83.0 (0.6) <sup>b</sup>	87.1 (0.4) <sup>a</sup>
<b><math>a^*</math></b>	4.40 (0.13) <sup>b</sup>	6.8 (0.4) <sup>a</sup>	3.7 (0.3) <sup>c</sup>	1.113 (0.108) <sup>d</sup>
<b><math>b^*</math></b>	45.7 (0.2) <sup>b</sup>	50.9 (0.7) <sup>a</sup>	40.5 (0.5) <sup>c</sup>	31.7 (0.6) <sup>d</sup>
<b><math>C^*</math></b>	21.7 (1.4) <sup>d</sup>	51.3 (0.8) <sup>a</sup>	40.7 (0.5) <sup>b</sup>	31.7 (0.6) <sup>c</sup>
<b><math>h^*</math></b>	87.5 (0.8) <sup>a</sup>	82.4 (0.4) <sup>c</sup>	84.8 (0.4) <sup>b</sup>	88.0 (0.2) <sup>a</sup>
<b><math>\Delta E</math></b>		5.8 (0.9) <sup>b</sup>	6.3 (0.7) <sup>b</sup>	16.3 (0.7) <sup>a</sup>

The same letter in superscript within row indicates homogeneous groups established by ANOVA ( $p < 0.05$ ).

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