

Document downloaded from:

<http://hdl.handle.net/10251/63158>

This paper must be cited as:

Ruiz Martinez, A.; Serralta Sevilla, J.; Romero Gil, I.; Seco Torrecillas, A.; Ferrer, J. (2015). Effect of intracellular P content on phosphate removal in *Scenedesmus* sp. Experimental study and kinetic expression. *Bioresource Technology*. 175:325-332. doi:10.1016/j.biortech.2014.10.081.



The final publication is available at

<http://dx.doi.org/10.1016/j.biortech.2014.10.081>

Copyright Elsevier

Additional Information

1 **Effect of intracellular P content on phosphate removal in**
2 ***Scenedesmus* sp. Experimental study and kinetic expression**

3

4 Ruiz-Martínez, A.*^a, Serralta, J.^a, Romero, I.^a, Seco, A.^b, and Ferrer, J.^a

5 ^aInstituto de Ingeniería del Agua y Medio Ambiente, IIAMA, Universitat Politècnica de
6 Valencia, Camino de Vera s/n, 46022 Valencia, Spain (e-mail: anruima1@upv.es,
7 jserralt@hma.upv.es, inrogi@dihma.upv.es, jferrer@hma.upv.es)

8

9 ^bDepartament d'Enginyeria Química, Escola Tècnica Superior d'Enginyeria, Universitat de
10 València, Avinguda de la Universitat s/n. 46100 Burjassot, Valencia, Spain (email:
11 aurora.seco@uv.es)

12

13 *Corresponding author. Tel. +34 963 877 000 ext. 76176; Fax +34 963 877 618, e-mail address:

14 anruima1@upv.es

15

16 **ABSTRACT**

17 The present work determines the effect of phosphorus content on phosphate uptake rate
18 in a mixed culture of Chlorophyceae in which the genus *Scenedesmus* dominates.
19 Phosphate uptake rate was determined in eighteen laboratory batch experiments, with
20 samples taken from a progressively more P-starved culture in which a minimum P
21 content of 0.11% (w/w) was achieved. The results obtained showed that the higher the
22 internal biomass P content, the lower the phosphate removal rate. The highest specific
23 phosphate removal rate was $6.5 \text{ mgPO}_4\text{-P} \cdot \text{gTSS}^{-1} \cdot \text{h}^{-1}$. Microalgae with a P content
24 around 1% (w/w) attained 10% of this highest removal rate, whereas those with a P
25 content of 0.6% (w/w) presented 50% of the maximum removal rate. Different kinetic
26 expressions were used to reproduce the experimental data. Best simulation results for
27 the phosphate uptake process were obtained combining Steele equation and Hill
28 function to represent the effect of light and intracellular phosphorus content,
29 respectively.

30 **Keywords**

31 Intracellular phosphorus content; microalgae; modeling; phosphate uptake; wastewater.

32

33

34

35 **1. INTRODUCTION**

36 Large amounts of phosphate are one of the causes of eutrophication in aquatic
37 environments, together with other inorganic nutrients like ammonium, nitrite or nitrate.
38 Several treatments for phosphate removal from wastewater can be applied, such as
39 chemical precipitation or biological phosphorus removal by means of polyphosphate
40 accumulating organisms and other bacteria present in activated sludge systems.
41 However, in the last decades, the use of microalgae for inorganic pollutant removal has
42 raised increasing attention.

43 Microalgae are photosynthetic microorganisms which use light energy and CO₂ for
44 growth, and whose ability to remove inorganic nutrients from different wastewaters has
45 been widely reported (De Alva et al. 2013, Gentili 2014, Ruiz-Marin et al. 2010, Samorí
46 et al. 2013, Van den Ende et al. 2014). On the other hand, microalgae are a renewable
47 energy source, since they can be transformed into biogas, biodiesel, biocrude,
48 biohydrogen and others (Razzak et al. 2013). Additionally, the recovery of inorganic
49 nutrients from wastewaters in an organic form converts microalgae also into valuable
50 fertilizers. The combination of these advantages makes microalgae an attractive option
51 for wastewater treatment.

52 Phosphorus is an essential component in microalgae: according to the Redfield ratio it
53 represents the 0.87% of its dry weight (Redfield 1958). However, in practice, microalgal
54 P content varies, due to diverse mechanisms of adaptation to the medium. Reynolds
55 (2006) estimated the minimum phosphorus cell quota to be around 0.2-0.4% of ash-free
56 biomass, although some species show a minimum value which is an order of magnitude
57 smaller. In fact, Wu et al. (2013) determined a minimal P content or *subsistence quota*
58 of 0.016% by fitting real data to a growth model for *Scenedesmus* sp. LX1. Minimal

59 intracellular phosphorus concentrations are achieved when microalgae grow under P-
60 starving conditions, as in the work by Markou (2012), who measured a minimum of
61 0.185%. On the other hand, when luxury phosphorus uptake takes place, microalgal P
62 content can rise up to values like 3.85% as measured by Powell et al. (2009). The main
63 phosphorus storage bodies in microalgae are polyphosphates, which are unbranched
64 chains of PO_4^- groups linked together by oxygen bridges. The amount of polyphosphate
65 present in the cells depends on different factors, such as the available phosphate in the
66 medium, light or temperature (Powell et al. 2008).

67 In the wastewater treatment field, mathematical models constitute useful tools for
68 process and equipment design, WWTP construction and upgrade or water quality
69 prediction. It is thus essential to have available models that describe in quantitative
70 terms the observed microalgal behavior in the context of nutrient removal.

71 Most models found in literature for phosphate uptake from the medium use Michaelis-
72 Menten kinetics (1):

$$73 \quad \frac{dS_{PO_4}}{dt} = \left(\frac{dS_{PO_4}}{dt} \right)_{max} \frac{S_{PO_4}}{k_S + S_{PO_4}} \quad (1)$$

74 where S_{PO_4} represents phosphate concentration in the medium and k_S is the
75 halfsaturation constant for phosphate uptake. However, this model cannot reproduce the
76 observed phenomenon of enhanced phosphate uptake rate due to internal phosphorus
77 deficiency. Michaelis-Menten uptake kinetics is often combined with Droop equation
78 for growth rate (Bougaran et al. 2010, Kwon et al. 2013):

$$79 \quad \mu = \mu_{max} \cdot \left(1 - \frac{q_{min}}{q} \right) \quad (2)$$

80 Where μ_{max} (d^{-1}) is the maximum specific growth rate, q is the internal microalgae P
 81 content (quota) ($mgP \cdot gTSS^{-1}$) and q_{min} ($mgP \cdot gTSS^{-1}$) is the minimum internal nutrient
 82 quota for microalgal growth.

83 However, in these models the internal cell quota does not affect phosphate uptake rate.
 84 Some authors have developed model extensions to take into account the influence of
 85 internal phosphorus content in the maximum phosphate uptake rate:

86 Klausmeier and Litchman (2004) defined the maximum phosphate uptake rate as a
 87 function of the cells internal P quota with the following term (3):

$$88 \left(\frac{dS_{PO_4}}{dt} \right)_{max} = \frac{\left(\frac{dS_{PO_4}}{dt} \right)_{max} \cdot k_{inh} - c \cdot (q - q_{min})}{q - q_{min} + k_{inh}} \quad (3)$$

89 Where k_{inh} ($mgP \cdot mgTSS^{-1}$) and c (dimensionless) are parameters to model the uptake
 90 inhibition.

91 Bougaran (2010) used eq. 4 for modeling the down-regulation in the uptake rate of an
 92 external nutrient by its own internal quota:

$$93 \frac{dS_{PO_4}}{dt} = \left(\frac{dS_{PO_4}}{dt} \right)_{max} \cdot \frac{q_{max} - q}{q_{max} - q_{min}} \quad (4)$$

94 where q_{max} ($mgP \cdot mgTSS^{-1}$) represents the hypothetical maximum value for P quota.

95 Other authors have proposed more complex models for phosphate assimilation: John
 96 and Flynn (2000) included 3 phosphorus pools within the cell, and Yao et al. (2011)
 97 took into account surface adsorption and desorption, together with the P-pool size and P
 98 stress level. The measurements needed for the calibration of these models are also of
 99 increased complexity.

100 It is the aim of this work to study the influence of the intracellular P content on the
101 phosphate uptake rate from the medium and to evaluate different kinetic expressions to
102 find the best one for predicting phosphate removal rates at different biomass
103 compositions.

104 To this aim, algae adapted to grow in P-sufficient medium were progressively deprived
105 from phosphorus, so that the cells P content gradually decreased. Different samples
106 from the resulting culture were used to seed 18 different batch experiments where
107 phosphate was added and its removal rate was measured. Equations found in literature
108 were used to fit the obtained data with moderately good results. A new expression was
109 developed which improved for the present culture of *Scenedesmus* sp. the accuracy of
110 model predictions. Light influence was also taken into account in all cases.

111 **2. MATERIALS AND METHODS**

112 **2.1. Microorganisms**

113 Microalgae were isolated from the walls of the secondary clarifier in the Carraixet
114 WWTP (Valencia, Spain) and maintained in a 7 L laboratory semicontinuous reactor
115 using the effluent of a submerged anaerobic membrane bioreactor (SAnMBR, described
116 in Giménez et al. 2011) as growth medium. This effluent displays a variable N/P ratio
117 and has proved to sustain algal growth (Ruiz-Martinez et al. 2012). The biomass in the
118 laboratory reactor formed a stable ecosystem where the dominant microalgae belonged
119 to the Chlorococcal order, of which >99% to the *Scenedesmus* genus.

120 **2.2. Experimental setup and operation**

121 **2.2.1. Semicontinuous reactor**

122 The 7 L laboratory reactor consisted of a cylindrical methacrylate tank, which was kept
123 at a constant temperature of 28°C and under continuous illumination of $156 \pm 17 \mu\text{E m}^{-2}$
124 s^{-1} . pH was regulated at 7.5 with pure CO₂ injections (for a more detailed reactor
125 description see Ruiz-Martinez et al. 2012). Cellular retention time was 4 days. During
126 the study, an artificial P-free medium was used for microalgae growth instead of the one
127 described in section 2.1, which had been previously used for culture maintenance. Thus,
128 the internal microalgae P content started to decrease, since the culture was not supplied
129 with any phosphorus during the whole study, which lasted 45 days. One liter of the
130 artificial medium was composed of 135 mg (NH₄)₂SO₄, 150 mg CaCO₃, 400 mg
131 CaCl₂·H₂O, 400 mg Na₂SeO₃·5H₂O, 350 mg MgSO₄·7H₂O, 54 mg (NH₄)₆Mo₇O₂·4H₂O,
132 30 mg ZnCl₂, 30 mg HBO₃, 30 mg NiCl₂·6H₂O, 18 mg CuCl₂·2H₂O, 12 mg K₂SO₄, 1.2
133 mg FeCl₃·4H₂O, 1.2 mg CoCl₂·6H₂O, 0.6 mg EDTA and 0.3 mg MnCl₂·4H₂O.

134 **2.2.2. Batch reactor**

135 The batch experiments were carried out in a 2 L cylindrical glass reactor equipped with
136 electronic sensors in order to obtain on-line temperature and pH measurements. The
137 reactors were placed inside a climatic chamber with air temperature control set to 20°C.
138 Due to the constant illumination the temperature reached 28°C. The probes were
139 connected to a multiparametric analyzer (CONSORT C832, Belgium), which was in
140 turn connected to a PC for data monitoring and storage. Data sampling was conducted
141 every 60 s. A fine bubble diffuser was mounted at the bottom of each reactor in order to
142 mix the algal culture by injecting compressed air. 8 vertical fluorescent lamps (Sylvania

143 GroLux, 18 W) continuously illuminated the reactor from a distance of 8 cm from all
144 sides. Photosynthetically active radiation (PAR) of $180 \pm 21 \mu\text{E m}^{-2} \text{s}^{-1}$ was measured at
145 the reactor surface.

146 **2.2.3. Batch experiments**

147 Different samples taken from the semicontinuous reactor were used to seed 18 batch
148 experiments along the experimental period of 45 days. Each batch experiment started
149 with the transfer of 1.9 L of the culture from the semicontinuous reactor into the batch
150 reactor. Phosphate in the form of KH_2PO_4 was then supplied, and phosphate
151 concentration in the medium was regularly measured in order to determine its uptake
152 rate. Additionally, nitrite, nitrate and ammonium concentrations were also determined,
153 as well as total suspended solids (TSS), volatile suspended solids (VSS) and total
154 phosphorus concentration. The batch experiments lasted between 4 and 26 hours,
155 according to the observed phosphate uptake rate. To avoid phosphate precipitation and
156 free ammonia stripping, pH value in all the experiments was maintained around 7.5 by
157 pure (99.9%) CO_2 injection from a pressurized cylinder.

158 **2.3. Analytical Methods**

159 Nutrient removal was evaluated by measuring inorganic nitrogen and phosphate levels
160 in the samples taken from the reactors. Ammonium ($\text{NH}_4\text{-N}$), nitrite ($\text{NO}_2\text{-N}$), nitrate
161 ($\text{NO}_3\text{-N}$) and phosphate ($\text{PO}_4\text{-P}$) were determined according to Standard Methods
162 (APHA 2005) (4500-NH₃-G, 4500-NO₂-B, 4500-NO₃-H, and 4500-P-F respectively)
163 in a Smartchem 200 automatic analyzer (Westco Scientific Instruments, Westco). The
164 acid peroxodisulphate digestion method (APHA 2005) was used for total phosphorus

165 (TP) measurements. The phosphorus in the algae biomass (total suspended phosphorus,
166 TSP) was calculated as the difference between total phosphorus and orthophosphate
167 concentration. TSS and VSS were determined according to Standard Methods (APHA
168 2005). All reported results were obtained from the previous analyses conducted in
169 duplicate.

170 3. RESULTS AND DISCUSSION

171 3.1. Biological phosphate removal

172 The pH control system was activated in all the experiments immediately after seeding,
173 which means that CO₂ was automatically injected whenever pH value exceeded 7.5.

174 This pH control assured that neither free ammonia stripping nor inorganic salts
175 precipitation took place. Thus, all conclusions drawn from this study are based on the
176 assumption that ammonium and phosphate removal are solely due to biological uptake.

177 Phosphate was added into each batch culture after seeding, and the first sample was
178 taken after mixing (ca. 20 s). Initial phosphate values reached $18 \pm 1.3 \text{ mgPO}_4\text{-P}\cdot\text{l}^{-1}$ in all
179 cases. Table 1 shows the initial biomass P content and TSS concentration for each batch
180 experiment.

181 The initial biomass P content in the batch experiments show a general decreasing trend
182 since the microalgae used in each experiment were taken from the culture in the
183 semicontinuous reactor, fed with a P-free medium (table 1). The study was prolonged
184 until the analytical value for biomass P content went below 0.2%, as this is, according
185 to Reynolds 2006, a general minimum P content value for cell survival. The lowest P
186 content that the microalgae in the culture finally reached was 0.11%. The polyphosphate
187 concentration in the microalgae at this stage was assumed to be almost nonexistent, and
188 P content was assumed to be almost completely structural phosphorus.

189 The initial total suspended solids in the last six batch experiments is clearly higher than
190 in the others (table 1), due to a period of 10 days (between batch experiments number
191 12 and 13) when no purge was extracted from the reactor. This procedure caused an
192 increase in the TSS of the culture, which allowed the study of the phosphate uptake rate

193 over a wider range of initial biomass concentration. Data from a wider range of TSS
194 was used to take into account the selfshading effect of the microalgae in the kinetic
195 expression proposed. Variable TSS concentration makes the available light for
196 photosynthesis variable even at constant external illumination rates.

197 Fig. 1 shows the phosphate concentration evolution in the medium for the 18 batch
198 experiments. It can be observed that phosphate concentrations can be fitted to a straight
199 line in all cases, being the slope of this line the phosphate removal rate ($\text{mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$).
200 It can be observed, for all batch experiments, that during the first hours after
201 phosphate addition its uptake rate is constant.

202 Since the lowest phosphate concentration reached was $8\text{ mgP}\cdot\text{l}^{-1}$ (at the end of batch
203 experiment 17) it can be stated that phosphate removal rate is constant for phosphate
204 values between 8 and $18\text{ mgP}\cdot\text{l}^{-1}$. This fact indicates that, should a Michaelis-Menten
205 kinetics be applied to model the influence of phosphate concentration in the medium on
206 phosphate uptake rate, the halfsaturation constant used would be in any case well below
207 $8\text{ mgP}\cdot\text{l}^{-1}$. On the other hand, high phosphate concentration in the medium at the end of
208 all batch experiments indicates that no phosphorus limitation occurred at any point of
209 the experiment.

210 The smallest phosphate uptake rates were measured in the first batch experiments, when
211 microalgae P content presented the highest values (fig. 1). The majority of literature
212 values on microalgal phosphate uptake rate under balanced conditions are similar or
213 lower than the values obtained for these first experiments: Dickinson et al. (2013)
214 reported a phosphate uptake rate of $0.104\text{ mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$ for *Scenedesmus* sp.,
215 Aravantinou et al. (2013) reported for *Chlorococcum* a value of $0.0475\text{ mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$,

216 and Aslan and Kapdan (2006) reported a value of $0.083 \text{ mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$ for *Chlorella*
217 sp.

218 In contrast, phosphate uptake rates for the last batch experiments (with P-starved cells)
219 reach much higher values than those observed in the first batch experiments, reaching a
220 maximum of $2.9 \text{ mg}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$. This value is not far from the one obtained in a previous
221 work (Ruiz-Martinez et al. 2014), where a phosphate uptake rate of $2 \text{ mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$
222 was achieved.

223 Therefore, the general trend is to find higher phosphate removal rates in those cultures
224 where microalgae have a smaller P content, although some exceptions can be found to
225 this observation. Since these exceptions are due to the different TSS concentration in
226 the batch cultures and its corresponding selfshading effect, phosphate uptake rates
227 should be compared using specific values ($\text{mgPO}_4\text{-P}\cdot\text{gTSS}^{-1}\cdot\text{h}^{-1}$). To this aim, in fig. 2,
228 the phosphate specific uptake rate has been represented versus the biomass P content at
229 the beginning of each batch experiment.

230 The lower specific removal rates were observed in those batch experiments in which
231 biomass presented a higher P content (fig. 2). It can be appreciated that when the culture
232 P content was above 1% (w/w), the specific phosphate removal rate was less than 10%
233 of the maximum removal rate achieved. The region around 0.5% P content is the
234 concentration at which phosphorus cellular content reduced phosphate uptake to half of
235 its highest value. The batch experiments with initial P content below 0.40% (empty dots
236 in the graph) are an exception to the general tendency of faster phosphate uptake rate
237 with smaller biomass P content. These batch experiments are those carried out at higher
238 initial TSS content. Thus, the light available for the microorganisms in these last
239 experiments was smaller than in the other experiments due to the markedly higher

240 suspended solids concentration, which resulted in higher selfshading levels. Therefore,
241 taking the light influence into account in the modeling process proves to be necessary.

242 This study shows an enhancement of phosphate uptake rate (regulated by light
243 availability) with decreasing biomass P content through the successive batch
244 experiments. Since the phosphate concentration in the medium was the same at the
245 beginning of all batch experiments, this observation suggests that not only the external
246 phosphate level, but also the *internal* biomass phosphorus concentration that the
247 microalgae are able to achieve influences the phosphate uptake rate. Therefore, the
248 biomass P content (relatively easily known by analyzing its composition) proves to be
249 an important indicator of the possible nutrient uptake rate for a given species.

250 **3.2. Biomass production and composition**

251 Biomass yield on phosphorus (Y_P , mass of generated biomass divided over the mass of
252 phosphorus taken up) varied along the batch experiments. The maximum Y_P value (120
253 $\text{mgTSS} \cdot \text{mgPO}_4\text{-P}^{-1}$) was measured for the batch with the higher initial P content, and
254 very low Y_P values (2-3 $\text{mgTSS} \cdot \text{mgPO}_4\text{-P}^{-1}$) correspond to P-starved cells (fig. 3).
255 Actually, these low values account only for the absorbed phosphate mass (mg PO_4) and
256 suggest no new biomass formation. Low biomass production in the cases of low initial P
257 content is explained directly by the lack of this essential nutrient and also by the
258 hindered N uptake: a smaller initial P content reduces the nitrogen uptake velocity
259 (Ruiz-Martinez et al. 2014), that being one of the causes for eventual lower biomass
260 formation.

261 The observations of this study suggest that, when the P-stress is relieved, the microalgae
262 first take up high amounts of phosphate from the medium at an increased rate, which is

263 higher the greater the P deficiency is. On the other hand, the slighter the P deficiency is,
264 the higher the rate at which biomass is generated.

265 The highest value for final biomass P content was 2.33%, which indicates that the
266 biomass capacity to take up phosphate from the medium is probably not exhausted at
267 that point. As reviewed in section 1, compositions of up to 3.85% P have been reported
268 before. Therefore, it could be assumed that (through a process of luxury uptake) in a
269 longer batch, final P content and final biomass concentrations could reach higher values.

270 **3.3. Modeling the phosphate uptake process**

271 The aim of this section is to establish a mathematical expression for modeling the
272 phosphate uptake process by microalgae. The structure of this expression will consist of
273 a maximum phosphate uptake rate multiplied by different terms (eq. 5). Each of these
274 terms includes the effect of a different factor in the phosphate uptake rate: A Monod
275 term models the effect of phosphate concentration, the Steele function (Steele 1977)
276 was chosen to model the light influence and a term τ_{XPP} will be established to model
277 the influence of the intracellular P content of the microalgae:

$$278 \quad \frac{dS_{PO_4}}{dt} = \left(\frac{dS_{PO_4}}{dt} \right)_{max} \cdot \frac{S_{PO_4}}{k_S + S_{PO_4}} \cdot \frac{I}{k_i} \cdot \exp\left(1 - \frac{I}{k_i}\right) \cdot \tau_{XPP} \quad (5)$$

279 where k_i is the optimal light intensity ($\mu E \cdot m^{-2} \cdot s^{-1}$) and I is a weighted average light
280 intensity ($\mu E \cdot m^{-2} \cdot s^{-1}$) which takes into account the reactor's geometry and the self-
281 shading factor of the microalgae. I is calculated dividing the reactor into discrete
282 concentric sections and applying Lambert-Beer's Law (eq. 6) for calculating a uniform
283 light for each section.

$$284 \quad I = I_0 \cdot \exp(-a \cdot TSS \cdot z) \quad (6)$$

285 where I_0 is the incident light intensity on the reactor surface ($\mu\text{E}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$), z (m) is the
 286 distance from the reactor surface, TSS are expressed in $\text{mgTSS}\cdot\text{l}^{-1}$ and a is the
 287 microalgal selfshading factor ($\text{m}^2\cdot\text{gTSS}^{-1}$), for which a value of 0.0758 was used in this
 288 study, based on Ketheesan and Nirmalakhandan 2004.

289 Other factors which were constant during the experiments, such as ammonium
 290 concentration, temperature, salinity or pH of the medium, have not been taken into
 291 account in the kinetic expression.

292 Since phosphate concentration in the medium was the same at the beginning of each
 293 batch experiment, the Monod phosphate term had a constant value. On the other hand,
 294 since initial phosphate concentration was high ($18\text{ mgP}\cdot\text{l}^{-1}$) compared with usual k_s
 295 values found in literature for *Scenedesmus* sp. ($0.037\text{-}0.124\text{ mgP}\cdot\text{l}^{-1}$ in Reynolds 2006,
 296 $0.0353\text{ mgP}\cdot\text{l}^{-1}$ in Rouzic and Bertru 1997), the Monod phosphate term did not have any
 297 regulating effect over the maximum uptake rate: its value was thus close to one in all
 298 cases. This term will be hereafter considered as constant, and included with

299 $\left(\frac{dS_{PO_4}}{dt}\right)_{max}$ into a single parameter K_{Max} . Expression (5) then becomes:

$$300 \quad \frac{dS_{PO_4}}{dt} = K_{Max} \cdot \frac{I}{k_i} \cdot \exp\left(1 - \frac{I}{k_i}\right) \cdot \tau_{XPP} \quad (\text{mgP}\cdot\text{mgTSS}^{-1}\cdot\text{h}^{-1}) \quad (7)$$

301 **3.3.1. Intracellular P content**

302 The term τ_{XPP} is meant to reproduce the effect of the biomass intracellular P content on
 303 the phosphate uptake rate. Initially, two expressions found in literature and presented in
 304 section 1 were used to reproduce the obtained data: that of Klausmeier and Litchman
 305 2004 (eq. 3), and that of Bougaran et al. 2010 (eq. 4). The combination of them with

306 equation (6) and (7) gives the following two expressions for modeling the phosphate
307 uptake rate (eq. 8 and eq. 9, respectively):

$$308 \quad \frac{dS_{PO_4}}{dt} = \frac{K_{Max} \cdot k_{inh} - c \cdot (q - q_{min})}{q - q_{min} + k_{inh}} \cdot \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i} \cdot \exp\left(1 - \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i}\right) \quad (8)$$

309 and

$$310 \quad \frac{dS_{PO_4}}{dt} = K_{Max} \cdot \frac{q_{max} - q}{q_{max} - q_{min}} \cdot \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i} \cdot \exp\left(1 - \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i}\right) \quad (9)$$

311 Model parameters were determined using the Solver program in Microsoft® Excel
312 2007 software for minimizing the residual sum of squared errors between the
313 experimental data and the model predictions. However, some restrictions had to be
314 applied in parameters q_{max} and q_{min} due to their biological significance. The values
315 obtained for model parameters are shown in table 2. Fig. 4a shows predicted phosphate
316 uptake rates using both expressions, represented against intracellular P content, together
317 with the experimental values. Both model predictions are also represented in fig. 4b
318 against the experimental values. Statistical analysis was carried out using SPSS 16.1,
319 which showed, for eq. 8 a Pearson correlation coefficient of 0.929 (P-value < 0.01) and
320 for eq. 9 a Pearson correlation coefficient of 0.581 (P-value < 0.05).

321

322 The phosphate uptake rate prediction is therefore acceptable using eq. 8 and quite poor
 323 using eq. 9. On the other hand, eq. 8 makes it necessary to calibrate 4 parameters, one
 324 more than eq. 9.

325 Based on these results, and on the observation of the data obtained as represented in fig.
 326 2, where a fast change in phosphate uptake rate is observed around a certain biomass P
 327 content (0.4 – 0.6 %), Hill equation was proposed for modeling the influence of
 328 intracellular stored phosphorus on the phosphate uptake rate. The resulting full equation
 329 that describes phosphate uptake from the medium is therefore:

$$330 \quad \frac{dS_{PO_4}}{dt} = K_{Max} \cdot \frac{k_{XPP}^n}{k_{XPP}^n + \left(\frac{X_{PP}}{X_{Alg}}\right)^n} \cdot \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i} \cdot \exp\left(1 - \frac{I_0 \cdot \exp(-a \cdot TSS \cdot z)}{k_i}\right) \quad (10)$$

331 being X_{PP}/X_{Alg} the intracellular stored polyphosphate, expressed in $\text{gP} \cdot \text{g TSS}^{-1}$, k_{XPP}
 332 ($\text{gP} \cdot \text{gTSS}^{-1}$) the ratio of X_{PP}/X_{Alg} that leads to a 50% reduction of the maximal uptake
 333 rate (50% effect concentration) and n the regulation coefficient or Hill number. Hill
 334 equation is of a similar nature to the sigmoidal functions used by John and Flynn (2000)
 335 and Flynn (2005) to describe internal P pools dynamics or by Yao et al. (2011) to model
 336 phosphate uptake from the medium. Originally used in enzymology, Hill allosteric
 337 regulation model has previously shown to successfully reproduce the influence of
 338 intracellular P content on the ammonium uptake rate (Ruiz-Martinez et al. 2014). De la
 339 Hoz Siegler et al. (2011) studied its use for N uptake, in order to reproduce his
 340 observations of growth uncoupled from nitrogen uptake and the consequent
 341 accumulation of intracellular nitrogen compounds. Hill equation showed the best fit
 342 among the studied models. However, he concluded that a simpler model like Michaelis-
 343 Menten should be chosen in exchange of a slightly worse fit.

344 In this study, the intracellular stored polyphosphate was calculated as the difference
 345 between the total suspended phosphorus (measured) and the P content of the microalgal
 346 structure (constitutional or structural phosphorus, not polyphosphate), which was
 347 considered a constant of the model, $i_{P_{Alg}}$ ($\text{gP} \cdot \text{gTSS}^{-1}$). For $i_{P_{Alg}}$ a value of 0.1% (0.001
 348 $\text{gP} \cdot \text{gTSS}^{-1}$) was set, which is below the phosphorus total composition at the end of the
 349 experiment (0.0011 $\text{gP} \cdot \text{gTSS}^{-1}$). It is assumed that at the final point there is nearly no
 350 polyphosphate in the cells.

351 A local sensitivity analysis of eq. (10) was performed, setting the initial parameters
 352 values based on previous experience and literature. Sensitivity was calculated as
 353 described in Marsili-Libelli et al. 2001:

$$354 \quad S_{P_j} = \frac{\Delta x}{\Delta P_j} \cdot \frac{P_{j_{nom}}}{x_{nom}}$$

355 Where S_{P_j} is the sensitivity of parameter P_j with respect to the state variable x , which
 356 was, in this case, the average calculated specific phosphate uptake rate. $P_{j_{nom}}$ is the
 357 parameter nominal value and x_{nom} is the model response when the nominal parameters
 358 are used. The applied parameter variation (ΔP_j) to obtain the test values with which to
 359 calculate Δx was $\pm 20\%$ of $P_{j_{nom}}$.

360 The sensitivity analysis gives information about the impact of the parameters into the
 361 response of the model. The results indicate that the biggest influence is exerted by
 362 parameter K_{Max} , followed by k_{XPP} and k_i . Hill number, n , bears the least significance.
 363 This result is however dependent on the initial value of k_{XPP} , due to the shape of Hill
 364 function when represented against X_{PP}/X_{Alg} for different k_{XPP} values. This function
 365 takes values close to zero or close to one for most of the spectrum, and values between
 366 zero and one for a narrow range of X_{PP}/X_{Alg} . How abrupt that change is depends on Hill

367 number, n , so it is logical that the influence of this parameter is only detected in a local
368 sensitivity analysis when the initial values are close to the point where the change takes
369 place. Therefore, if a sensitivity analysis was performed in specific points of the P
370 content spectrum (for example, only the first batch experiments, or only the last batch
371 experiments), the results might be different, since the sensitivity analysis was performed
372 on the average phosphate uptake calculated for all batch experiments.

373 Model parameters were determined using the Solver program in Microsoft® Excel
374 2007 software for minimizing the residual sum of squared errors between the
375 experimental data and the model predictions. The best fit obtained for the parameters is
376 shown in table 3.

377 The proposed model accurately reproduces the experimental data (figs. 5a and 5b).
378 Pearson correlation coefficient (P-value < 0.01) was 0.971. These results clearly
379 improve those obtained with eq. 9. The advantages with respect to eq. 8 are two: a better
380 fit and one parameter less which needs to be calibrated.

381 Literature k_i values vary in a wide range between 20 and 500 $W \cdot m^{-2}$ (Broekhuizen et al.
382 2012 and Reichert et al. 2001, respectively), in which the value obtained in this study of
383 $180 \mu mol \cdot m^{-2} \cdot s^{-1}$ would be included. Regarding k_{XPP} , 0.5% is the value for P content
384 around which phosphate uptake rate is 50% of its maximum. The value obtained for
385 maximum phosphate uptake is $8 mgP \cdot gTSS^{-1} \cdot h^{-1}$, which is also in agreement with the
386 fact that the highest obtained value in the experiment was $6.90 mgP \cdot gTSS^{-1} \cdot h^{-1}$, being
387 Monod and Hill term for that batch experiment almost one and the light influence term
388 0.85.

389 **4. CONCLUSIONS**

390 A *Scenedesmus* sp. culture was progressively deprived from phosphorus and, as a
391 consequence, phosphate uptake rate rose. Equations found in literature reproduce the
392 obtained data moderately good. A new expression was proposed, which includes a
393 Steele term for modeling the light influence and Hill equation for modeling the
394 influence of the biomass phosphorus content. The presented model improved the
395 accuracy obtained and decreased the number of parameters needed. It can be used for
396 phosphate removal rate prediction based on the microalgal composition, and thus it
397 represents a useful tool for designing and simulating wastewater treatment systems
398 using microalgal cultures.

399 **ACKNOWLEDGEMENTS**

400 This research work has been supported by the Spanish Ministry of Economy and
401 Competitiveness (MINECO, CTM2011-28595-C02-01/02) jointly with the European
402 Regional Development Fund (ERDF) which are gratefully acknowledged.

403

404 **REFERENCES**

- 405 [1] APHA, 2005. Standard methods for the examination of water and wastewater,
406 20th ed., American Public Health Association, Washington, DC.
- 407 [2] Aravantinou, A.F., Theodorakopoulos, M.A., Manariotis, I.D., 2013. Selection
408 of microalgae for wastewater treatment and potential lipids production.
409 *Bioresour Technol* 147, 130-134.
- 410 [3] Aslan, S., Kapdan, I.K., 2006. Batch kinetics of nitrogen and phosphorus
411 removal from synthetic wastewater by algae. *Ecol Eng* 28, 64-70.
- 412 [4] Bougaran, G., Bernard, O., Sciandra, A., 2010. Modeling continuous cultures of
413 microalgae colimited by nitrogen and phosphorus. *J Theor Biol* 265, 443-454.
- 414 [5] Broekhuizen, N., Park, J. B. K., McBride, G. B., Craggs, R. J., 2012.
415 Modification, calibration and verification of the IWA River Water Quality
416 Model to simulate a pilot-scale high rate algal pond. *Water Res.* 46(9) 2911-26.
- 417 [6] De Alva, M.S., Luna-Pabello, V.M., Cadena, E., Ortíz, E., 2013. Green
418 microalga *Scenedesmus acutus* grown on municipal wastewater to couple
419 nutrient removal with lipid accumulation for biodiesel production. *Bioresour*
420 *Technol* 14B6, 744-748.
- 421 [7] De la Hoz Siegler, H., Ben-Zvi, A., Burrell, R.E., McCaffrey, W.C., 2011. The
422 dynamics of heterotrophic algal cultures. *Bioresour Technol* 102, 5764–5774.
- 423 [8] Dickinson, K.E., Whitney, C.G., McGinn, P.J. (2013) Nutrient remediation rates
424 in municipal wastewater and their effect on biochemical composition of the
425 microalga *Scenedesmus* sp. *AMDD. Algal Research* 2 (2) 127-134.
- 426 [9] Flynn, K.J., 2005. Modelling marine phytoplankton growth under eutrophic
427 conditions. *J Sea Res* 54, 92 – 103.

- 428 [10] Gentili, F.G., 2014. Microalgal biomass and lipid production in mixed
429 municipal, dairy, pulp and paper wastewater together with added flue gases.
430 *Bioresour Technol* 169, 27-32.
- 431 [11] Giménez, J.B., Robles, A., Carretero, L., Duran, F., Ruano, M.V., Gatti,
432 M.N., Ribes, J., Ferrer, J., Seco, A., 2011. Experimental study of the anaerobic
433 urban wastewater treatment in a submerged hollow-fibre membrane bioreactor at
434 pilot scale. *Bioresour Technol* 102, 8799-8806.
- 435 [12] Gotham, I.J., Rhee, G.Y., 1981. Comparative kinetic studies of
436 phosphate-limited growth and phosphate uptake in phytoplankton in continuous
437 culture. *J. Phycol.* 17, 257-265.
- 438 [13] John, E.H., Flynn, K.J., 2000. Modelling phosphate transport and
439 assimilation in microalgae; how much complexity is warranted? *Ecol Model*
440 125, 145-157.
- 441 [14] Ketheesan, B., Nirmalakhandan, N., 2004. Modeling microalgal growth
442 in an airlift-driven raceway reactor. *Bioresour Technol* 136, 689–696.
- 443 [15] Klausmeier, C.A., Litchman, E., 2004. Phytoplankton growth and
444 stoichiometry under multiple nutrient limitation. *Limnol Oceanogr* 49, 1463-
445 1470.
- 446 [16] Kwon, H.K., Oh, S.K., Yang, H-S, 2013. Growth and uptake kinetics of
447 nitrate and phosphate by benthic microalgae for phytoremediation of eutrophic
448 coastal sediments. *Bioresource Technology* 129, 387–395.
- 449 [17] Lehman, J., Botkin, D., Likens, G., 1975. The assumptions and rationales
450 of a computer model of phytoplankton population dynamics. *Limnol Oceanogr*
451 20 (3), 343-364.

- 452 [18] Markou, G., 2012. Alteration of the biomass composition of *Arthrospira*
453 (*Spirulina*) *platensis* under various amounts of limited phosphorus. *Bioresour*
454 *Technol* 116, 533-535.
- 455 [19] Marsili-Libelli, S., Ratini, P., Spagni, A. & Bortone, G., 2001.
456 Implementation, study and calibration of a modified ASM2d for the simulation
457 of SBR processes. *Water Sci Technol*, 43(3), 69-76.
- 458 [20] Powell, N., Shilton, A., Pratt, S., Chisti, Y., 2008. Factors influencing
459 luxury uptake of phosphorus by microalgae in waste stabilization ponds.
460 *Environ Sci Technol* 42 (16), 5958-5962.
- 461 [21] Powell, N., Shilton, A., Chisti, Y., Pratt, S., 2009. Towards a luxury
462 uptake process via microalgae – defining the polyphosphate dynamics. *Water*
463 *Res* 43 (17) 4207-4213.
- 464 [22] Razzak, S.A., Hossain, M.M., Lucky, R.A., Bassi, A.S., De Lasa, H.,
465 2013. Integrated CO₂ capture, wastewater treatment and biofuel production by
466 microalgae culturing – A review. *Renew sust Energ Rev* 27, 622-653.
- 467 [23] Redfield, A., 1958. The biological control of chemical factors in the
468 environment. *Am Sci* 46, 205-221.
- 469 [24] Reichert, P., Borchardt, D., Henze, M., Rauch, W., Shanahan, P.,
470 Somlyódy, L., Vanrolleghem, P., 2001. River Water Quality Model no. 1
471 (RWQM1):II. Biochemical process equations. *Water Sci Technol* 43 (5) 11-30.
- 472 [25] Reynolds, C. S., 2006. Ecology of phytoplankton, Cambridge University
473 Press, New York.
- 474 [26] Rouzic, B., Bertru, G., 1997. Phytoplankton community growth in
475 enrichment bioassays: possible role of the nutrient intracellular pools. *Acta ecol*
476 18 (2), 121-133.

- 477 [27] Ruiz-Marin, A., Mendoza-Espinosa, L.G., Stephenson, T., 2010. Growth
478 and nutrient removal in free and immobilized green algae in batch and semi-
479 continuous cultures treating real wastewater. *Bioresour Technol* 101, 58-64.
- 480 [28] Ruiz-Martinez, A., Martin Garcia, N., Romero, I., Seco, A., Ferrer, J.,
481 2012. Microalgae cultivation in wastewater: Nutrient removal from anaerobic
482 membrane bioreactor effluent. *Bioresour Technol* 126, 247-253.
- 483 [29] Ruiz-Martinez, A., Serralta, J., Pachés, M., Seco, A., Ferrer, J., 2014.
484 Mixed microalgae culture for ammonium removal in the absence of phosphorus:
485 Effect of phosphorus supplementation and process modeling. *Process Biochem.*
486 *In press*
- 487 [30] Samorí, G., Samorí, C., Guerrini, F., Pistocchi, R., 2013. Growth and
488 nitrogen removal capacity of *Desmodesmus communis* and of a natural
489 microalgae consortium in a batch culture system in view of urban wastewater
490 treatment: Part I. *Water Res.* 47, 791-801.
- 491 [31] Steele, J.H., 1977. In: Lapidus, L., Amundson, N.R. (Eds.), *Microbial*
492 *Kinetics and Dynamics in Chemical Reactor Theory*. Prentice-Hall, Englewood
493 Cliffs, NJ, pp. 405 – 483.
- 494 [32] Van den Ende, S., Carré, E., Cocaud, E., Beelen, V., Boon, N.,
495 Vervaeren, H., 2014. Treatment of industrial wastewaters by microalgal
496 bacterial flocs in sequencing batch reactors. *Bioresour Technol* 161, 245-254.
- 497 [33] Wu, Y.H., Yu, Y., Hu, H.Y., 2013. Potential biomass yield per
498 phosphorus and lipid accumulation property of seven microalgal species.
499 *Bioresour Technol* 130, 599-602.

500 [34] Yao, B., Xi, B., Hu, C., Huo, S., Su, J., Liu, H., 2011. A model and
501 experimental study of phosphate uptake kinetics in algae: considering Surface
502 adsorption and P-Stress. *J Environ Sci* 23 (2), 189-198.
503
504

505 **FIGURE LEGENDS**

506 Fig. 1: a-h) Phosphate concentration in the medium during the batch experiments. Initial
507 values can be fitted to a straight line in all cases, being the slope of this line the
508 phosphate removal rate ($\text{mgPO}_4\text{-P}\cdot\text{l}^{-1}\cdot\text{h}^{-1}$).

509 Fig. 2: Specific phosphate uptake rate of the *Scenedesmus* sp. culture plotted against
510 their intracellular P content. Empty dots correspond to the batch experiments with initial
511 P content below 0.40%. Suspended solids in the batch reactors were higher at that point
512 (last days of experiment).

513 Fig. 3: Dependence between biomass yield on phosphorus and initial polyphosphate
514 content of the cells.

515 Fig. 4: a) Experimental values of phosphate uptake rate together with model predictions,
516 using eq. 8 (empty squares) and eq. 9 (full squares); b) Parity chart for phosphate uptake
517 rate: rates according to eq. 8 (empty squares) and eq. 9 (full squares) versus
518 experimental values.

519 Fig. 5: a) calculated (eq. 10) and observed phosphate uptake rates plotted together vs
520 initial %P content; b) calculated phosphate uptake rates (eq. 10) plotted vs observed
521 phosphate uptake rates.

522

523 **TABLES**

524 Table 1: Initial %P for each batch, together with the measured initial biomass

525 concentration.

Batch experiment number	Day of experiment	Initial %P (mgP·mgTSS ⁻¹)	Initial TSS (mgTSS·l ⁻¹)
1	1	1.47%	486
2	2	1.25%	421
3	3	1.04%	360
4	7	0.90%	358
5	8	0.95%	414
6	9	1.29%	357
7	11	0.36%	285
8	14	0.51%	264
9	15	0.53%	262
10	17	0.76%	398
11	18	0.53%	321
12	19	0.26%	229
13	29	0.49%	552
14	30	0.57%	424
15	34	0.30%	552
16	35	0.26%	500
17	41	0.18%	655
18	45	0.11%	566

526

527

528 Table 2: Obtained parameters for eq. 8 and 9

	K_{\max} (mgP·mgTSS ⁻¹ ·h ⁻¹)	k_i (microE·m ⁻² ·s ⁻¹)	q_{\max} (mgP·mgTSS ⁻¹)	q_{\min} (mgP·mgTSS ⁻¹)	k_{inh} (mgP·mgTSS ⁻¹)	c
eq. 8 (Klausmeier)	0.01	139.4		0.10%	0.36%	0.00264
eq. 9 (Bougaran)	0.005	29.6	1.47%	0.10%		

529

530

531 Table 3: Parameter sensitivity for eq. 10 and best fit obtained

Parameter	Sensitivity	Best fit value
K_{Max} (mgP·h ⁻¹ ·mgTSS ⁻¹)	1	0.008
k_{XPP} (gP·gTSS ⁻¹)	0.733	0.51%
k_i (μE·m ⁻² ·s ⁻¹)	0.626	180
n	0.006	3.2

532