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Additional Information

<u>1</u>	PROTECTIVE EFFECT OF CHITOSAN ON ACRYLAMIDE FORMATION IN MODI		
<u>2</u>	AND BATTER SYSTEMS		
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<u>8</u> Abstract

9 In recent years high contents of acrylamide, a potentially carcinogenic substance, have been 10 found in a wide range of fried and baked foods. For this reason, the health authorities together 11 with the food industry have carried out research to find ways to minimize the presence of 12 acrylamide during food processing. The addition of chitosan may be an excellent alternative for <u>13</u> achieving this goal because due to their richness in amino groups, they would interfere with the <u>14</u> Maillard reaction that unleashes the formation of acrylamide. The main aims of this study were <u>15</u> to analyze the addition of different concentrations of chitosan in model systems as a new way of <u>16</u> mitigating generation of acrylamide during frying processes, while evaluating the influence of <u>17</u> pH, reducing sugars (glucose and fructose) present in the system and frying temperature, and to determine the functionality of adding chitosan in fried batter systems. The results showed that <u>18</u> <u>19</u> chitosan is capable of inhibiting the formation of acrylamide in model systems and in fried 20 batters. In model systems, a reduction in acrylamide ranging from 49 to 85 % was achieved for <u>21</u> 1% of chitosan, the maximum inhibition taking place in asparagine-fructose model systems and <u>22</u> the lowest in asparagine-glucose model systems. In fried batter, acrylamide was mitigated by 59 \pm 6 % with a chitosan concentration of 0.27% in batter formulations. Double concentrations of 23 24 chitosan (0.54 %) did not considerably improve the inhibition capacity.

<u>25</u>

26 Keywords: Acrylamide, Chitosan, Model systems, Batter systems

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<u>28</u> 1. Introduction

29 It is well-known that food processing can improve nutrition, quality and safety. However, 30 toxic substances such as acrylamide can sometimes be formed through the interaction of 31 food compounds, from natural and added ingredient. According to some epidemiological 32 studies, acrylamide is potentially carcinogenic compound for humans (IARC, 1994), not 33 only due to its consumption, but also to its role as a precursor in the development of other 34 compounds during hepatic metabolism such as glycidamide (Blank, 2005). Acrylamide is 35 mainly used in industrial processes used to make paper, dyes, plastics and treating drinking 36 water. However, it can also be present in small amounts in food packaging, some adhesives 37 and cigarette smoke (Rudel, Ackerman, Attfield, & Brody, 2014). Acrylamide was also found to be formed in some starchy foods, especially potato products, during high-<u>38</u> 39 temperature cooking and under low moisture conditions, such as frying, baking and roasting, 40 formation being lower in protein-rich foods (Tareke, Rydberg, Karlsson, Eriksson, & Tornqvist, 2002). Acrylamide is formed during Maillard reactions, and mainly between the 41 42 reaction of asparagine and reducing sugars at high temperatures (Mottram, Wedzicha, & 43 Dodson, 2002; Stadler et al., 2002; Becalski, Lau, Lewis, & Seaman, 2003). Several studies <u>44</u> have proven the importance of temperature, time, levels of precursors, pH, nature of the 45 matrix, etc. on acrylamide formation in food. Consequently, a wide range of strategies have 46 been developed in the last decade to reduce the final content of acrylamide in model systems and foods processed at high temperatures. Some strategies based on controlling processing <u>47</u> 48 conditions such as time and temperature (Tareke et al., 2002), as well as frying in low <u>49</u> pressure conditions or novel frying techniques, such as, microwave or air frying have achieved a significant inhibition of acrylamide formation (Troncoso & Pedreschi, 2009; 50 <u>51</u> Barutcu, Sahin, & Sumnu, 2009; Sansano, Juan-Borrás, Escriche, Andrés, & Heredia, 2015). 52 It is also advantageous to apply treatments before frying, such as blanching, or soaking the <u>53</u> food products in acids, vitamins, cations or amino acids in order to reduce acrylamide
<u>54</u> precursors, and to interfere with and modify Maillard reactions triggering acrylamide
<u>55</u> formation (Pedreschi, Kaack, & Granby, 2004, Jung, Choi, & Ju, 2003, Zeng et al., 2009,
<u>56</u> Gökmen & Şenyuva, 2007, Rydberg et al., 2003).

Hydrocolloids are hydrophilic polymers that modify the functional properties of food <u>57</u> 58 systems, such as thickening, gelling and emulsifying properties (Saha & Bhattacharya, 59 2010). Some studies have tested the use of hydrocolloids to control moisture diffusion and 60 consequently, oil absorption during frying. Lower contents of fat were obtained when including hydrocolloids such as soy protein isolate, whey protein isolate, methylcellulose <u>61</u> 62 and hydroxypropyl methylcellulose as an edible film coating before frying (Albert & Mittal, <u>63</u> 2002; Balasubramaniam, Chinnan, Mallikarjunan, & Phillips, 1997) or, what seems to be most effective, introducing them as an ingredient in batter formulation (Holownia, Chinnan, 64 65 Erickson, & Mallikarjunan, 2000; Sanz, Salvador, & Fiszman, 2004). Zeng et al. (2010) tested some hydrocolloids (agar, alginic acid, carrageenan, carob gum, gelatin, hydroxyprpyl 66 <u>67</u> distarch phosphate, pectin and xanthan gum) in acrylamide formation in model and real <u>68</u> systems. They found positive results mainly for pectin and alginic acid, but these hydrocolloids did not significantly change the water content of the fried potatoes strips. <u>69</u> 70 Therefore, they are unlikely to modulate the formation of acrylamide due to their property of 71 water retention. These authors suggested that the formation of surface coatings might also 72 modulate heat transfer from the surrounding oil to the product.

Among the different hydrocolloids, chitosan, a polycationic polymer and waste product from the sea food processing industry, is an abundant natural resource that has, as yet, not been fully utilized. The advantages of this polymer include availability, low cost, high biocompatibility, biodegradability and ease of chemical modification. Chitosan has many applications in several sectors because of its multiple properties: it is not digestible by

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humans, so it is considered to be a dietary fiber; which binds lipids and helps in reducing <u>78</u> 79 cholesterol (Muzzarelli, 1996), and it is protective, fungistatic and antibacterial (El Ghaouth, Arul, Ponnapalam, & Boulet, 1991; Tsai & Su, 1999). Moreover, chitosan is a molecule 80 81 which is rich in amino groups, this being the main characteristic leading to our hypothesis: amino groups of chitosan would compete with amino groups of asparagine to bind to 82 83 carbonyl group of reducing sugars and thus, would modulate acrylamide generation 84 (Lindsay & Jang, 2005). If this hypothesis is confirmed chitosan would be proven to have 85 another function: protecting against acrylamide formation. The main purpose of this study was to analyze the addition of chitosan as a way to mitigate the generation of acrylamide 86 87 during frying processes in model systems and fried batter systems. The effect of pH of the <u>88</u> reaction, the type of reducing sugars (glucose and/or fructose) present in the model system 89 and the temperature were also evaluated.

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<u>91</u> 2. Materials and methods

<u>92</u> 2.1. Chemicals and consumables

<u>93</u> Asparagine, glucose and fructose were purchased from Sigma-Adrich Company (St. Louis, MO, USA). Chitosan (Poly (D-glucosamine)*Deacetylated chitin) was also <u>94</u> 95 purchased from Sigma- Adrich (St. Louis, MO, USA). Chitosan was used in coarse 96 ground flakes and powder, presented a deacetylation degree superior to 75% with a high <u>97</u> molecular weight (lot: MKBH5816V). Formic acid, acetonitrile and magnesium sulfate 98 were purchased from VWR-Prolabo (Fontenay-sous-Bois, France), methanol and <u>99</u> hexane were obtained from Panreac (Barcelona, Spain). Acrylamide standard (> 99%) 100 was purchased from Merk (Darmstadt, Germany), sodium chloride was obtained from <u>101</u> Scharlab (Barcelona, Spain) and Primary secondary amine (PSA) was purchased from 102 Supelco (Bellefonte, USA). Double distilled water was prepared for chromatographic

use (Milli-Q, Millipore Corp., Bedford, MA). All chemicals used were analytical grade, 103 104 and those used for chromatographic analysis were HPLC grade. To test the effect of 105 chitosan in a real system, a commercial formulation was used (Yolanda, Murcia, Spain). 106 This formulation consists of wheat and rise flours, an acidity regulator (E-334), bulking 107 agent (E-500ii) and coloring (E-160b). Moisture and ash contents (11.5% and 1.8%, 108 respectively) were measured using AACC methods (1995), protein and fat contents <u>109</u> (10.0% and 1.4%, respectively) were supplied by manufacturers, and particle size (78.0 110 µm) was analyzed with the Mastersizer 2000 (Malvern Instruments, Germany) coupled 111 with the Scirocco 2000 module for dry measurement.

<u>112</u> 2.2. Preparation of reaction mixtures for pyrolysis

<u>113</u> In order to confirm our hypothesis, we carried out chemical model reactions following <u>114</u> the method proposed by Gökmen and Şenyuva (2007) with some minor modifications. 115 The reaction was carried out using a 25mL threaded Pyrex tube which contained 5 µmol of asparagine and 5 µmol of reducing sugars, and 100 µl of acid lactic solution on <u>116</u> 117 which chitosan was previously dissolved at 0, 0,5 or 1%. Eighteen different model systems were formulated depending on the type of sugar used: glucose, fructose or an 118 119 equimolecular mixture of both; the pH (4 and 5) and the concentration of chitosan (0, <u>120</u> 0.5 and 1%).

<u>121</u> The samples were placed in an oil bath previously preheated at the two temperatures
 <u>122</u> tested (150 and 180°C) and the total heating time for the samples was 30 minutes. After
 <u>123</u> the reaction time, the tubes were immediately cooled in an ice-water bath for 5 minutes.

<u>124</u> 2.3. Preparation of batters systems for frying

<u>125</u> Batter formulations consisted of the commercial formulation with chitosan solutions (at

<u>126</u> 0, 0.5 and 1%) at pH=4 with 2.5% of salt in a water-to-dry-mix proportion of 1.2/1. The

<u>127</u> final chitosan contents in the formulations were 0, 0.27 and 0.54% respectively. Batter

128 samples were kept for at least 30 minutes at room temperature before frying. The frying 129 step was carried out in a commercial deep-fat fryer with a capacity of 2 L (model: FM 6720 Ideal 2000 Professional, Solac) at 180 \pm 2°C. Samples (11.5 \pm 0.1g) were placed in 130 131 an aluminum cylindrical instrument and then introduced in the fryer in order to obtain homogenous ring shaped fried samples (height: 11±1mm; outer diameter= 65mm±2 and 132 133 inner diameter= 25 ± 1 mm). Triplicate samples (n = 3) were fried for 2, 4 and 7 minutes <u>134</u> for the three formulations tested. The excess oil was removed with paper on both sides <u>135</u> for 20 seconds after taking the samples out of the fryer.

<u>136</u> 2.4. Analysis of acrylamide

<u>137</u> 2.4.1. *Extraction of acrylamide from pyrolysates (model systems)*

138Two mL of Mili-Q water were added to the pyrolisates obtained and tubes were agitated139in a vortex for 1 minute. The tube content was filtered (0.22 μ m Nylon filters) and140transferred to a vial for the following acrylamide content determination, studied in141triplicate (n=3).

<u>142</u> 2.4.2. Extraction of acrylamide from the fried batter systems

143 The acrylamide content was determined by means of dispersive solid phase extraction 144 (QuEChERS) according to Mastovska and Lehotay (2006) with some modifications. <u>145</u> The standard addition was used rather than the traditional calibration curve in order to remove the matrix effect, fortifying at five different levels (10, 20, 50, 100 and 300 µg <u>146</u> <u>147</u> kg^{-1}), with six replicates for each level (n=6). Fried batter systems were subjected to a previous acrylamide extraction as follows: three samples were ground in a blender and a 148 <u>149</u> sub-sample (1 g) was placed in a 50mL Falcon tube, following which 5 mL of n-hexane 150 were added. The tube was shaken in a vortex for 30 seconds, after which10 ml bidistilled water, 10 mL acetonitrile, 4 g MgSO4 and 0.5 g NaCl were added and stirred <u>151</u> in the vortex for one minute. The suspension was then centrifuged at 2026 RCF 152

(Centronic BL II (Selecta, Spain)) for 5 minutes, following which the hexane layer
(upper phase) was discarded. 1mL of the acetonitrile phase, containing the acrylamide,
was then transferred to a 2 mL polypropylene tube containing 50 mg PSA and 150 mg
MgSO4, and stirred for 30 seconds. The homogenate was centrifuged at 2697 RCF
(Labofuge 200 (Heraeus, Germany)) for 1 minute and the supernatant was transferred to
a vial for acrylamide analysis.

159 2.4.3. LC/MS/MS analysis

160 The acrylamide analysis was performed with an Agilent 1200 Series HPLC system coupled to an Agilent 6410 triple quadrupole mass spectrometer (Agilent Technologies <u>161</u> <u>162</u> Inc., CA, USA) with an electrospray type ionization source. The column used in this study was a Zorbax Eclipse XDB C-18 (2.1mmx50mm, 1.8µm). The mobile phase used <u>163</u> 164 consisted of 2.5% methanol/ 97.5% of 0.1% formic acid (A) and methanol (B). The <u>165</u> elution gradient was as follows: 0-3 min 100% of A; 3.1-3.5 min 70% A; 3.6 min 100% 166 A, with 1 min post-time to equilibrate the column. The column oven temperature was <u>167</u> set at 30°C, the flow was maintained at 0.4 mL/minute and the injection volume was <u>168</u> 10µL. The electrospray was operated in positive ion mode. The conditions used in the ionization source were: 350°C at 12 L/min for the drying gas (N₂), a nebulizer pressure <u>169</u> 170 of 40 psi and a capillary voltage of 4000 V. Identification and quantification of 171 acrylamide in the samples was performed using the multiple reaction monitoring mode <u>172</u> (MRM), and the ion m/z 72 > 27 and m/z 72 > 55.2 were studied respectively.

<u>173</u> 2.5. Water content determination

<u>174</u> Water content was analyzed by vacuum drying at 60°C until constant weight was<u>175</u> achieved (20.103, AOAC, 1980).

<u>176</u> 2.6. Statistical analysis

<u>177</u>	Statistical analysis of variance (ANOVA) was performed by Statgraphics Centurion to
<u>178</u>	estimate the effect of process variables (pH, reaction temperature and time, reducing
<u>179</u>	sugars and chitosan content) on the obtained results. Evaluations were based on 95 and
<u>180</u>	99% significance levels.

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182

183 3. Results and discussion

<u>184</u> *3.1. Effect of chitosan on acrylamide formation in model systems*

The acrylamide content generated in model systems formulated with glucose, fructose and 185 186 the equimolecular mixture of both sugars are shown in Figure 1. In all cases the higher the <u>187</u> percentage of chitosan, the lesser the amount of acrylamide produced. Temperature was an 188 important factor, considering that at 150°C the acrylamide content grows gradually with 189 heating time, but at 180°C, after 10-15 minutes the amount of acrylamide generally reaches 190 the maximum value and starts to decrease lightly with treatment time, likely due to <u>191</u> polymerization (Stadler et al., 2004). The statistical analysis revealed that except pH, all the <u>192</u> factors considered in this study (type of reducing sugars present in the system, the reaction <u>193</u> time, the % of chitosan and the temperature) have a significant influence on acrylamide 194 formation (Table 1). As the pH was not a significant factor, Figure 1 only includes results at 195 pH 4. According to the F-Ratio values, the temperature and the percentage of chitosan are <u>196</u> the most significant factors, as well as the interaction between them. Time is also a 197 significant element, as has been proven in many studies, as well as the temperature and their <u>198</u> interaction (Gertz & Klostermann, 2002).

<u>199</u> The potential of generating acrylamide from suitable precursors has mainly been attributed
 <u>200</u> to the concentration of asparagine, which directly provides the backbone of the acrylamide
 <u>201</u> molecule. However, there is some indication in literature that the type of sugar, or in general

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the carbonyl compound, may significantly affect the final amount of acrylamide generated
 through the Maillard reaction. Some authors have speculated on the role of physical
 properties of precursors and suggested that the melting point of sugars is a possible
 parameter to consider (Stadler et al., 2004).

In figure 2, differences in acrylamide content depending on the type of reducing sugar in the system can be appreciated. Higher amounts of acrylamide were produced with fructose than with glucose. Other authors have stated that mixtures with fructose generate acrylamide earlier, meaning at a lower temperature, than those containing glucose (at about 125 and 140°C, respectively), which means the final content of acrylamide was higher with fructose than with glucose (Robert et al., 2004).

Figure 3 shows the inhibitory effect of chitosan on acrylamide formation. In fact, adding <u>212</u> 213 0.5% of chitosan led to an inhibition of acrylamide formation (according to the control) of <u>214</u> 52% and 65% at 180 and 150°C respectively, and 1% of chitosan, 75% and 76% at 180 and 215 150°C respectively. The influence of the temperature on acrylamide formation is well known <u>216</u> but when the interaction between the temperature and the concentration of chitosan was <u>217</u> analyzed, it can be observed that chitosan drastically reduces the influence of temperature on the acrylamide formation. This seems to indicate that there is likely to be a reaction of <u>218</u> 219 chitosan with reducing sugars at temperatures below acrylamide formation temperatures. In 220 spite of the small concentration of chitosan, the resulting inhibitory effect was significant, <u>221</u> ranging between 40% and 84% (results not shown) depending on the reducing sugar and the 222 treatment temperature. The protective effect of chitosan is very high as compared to the <u>223</u> results reported by Zeng et al., (2010), who used other hydrocolloids in model systems and in which at the concentration of 1% none of the hydrocolloids showed a significant 224 <u>225</u> inhibition of the formation of acrylamide, although around 60% was achieved when 2% of 226 alginic acid and pectin were tested.

227 3.2. Effect of chitosan on acrylamide formation in fried batter systems

228 As evidenced in the model systems, the effect of chitosan on acrylamide inhibition was observed in real systems. The results showed that the concentration of chitosan was again 229 230 the most significant factor followed by the frying time (F-ratio: 44.38 and 33.43, 231 respectively) and their interaction (chitosan %-frying time). The ability of chitosan to 232 compete with asparagine to bind to reducing sugars was quite significant even at low 233 concentration and no significant differences are found between using 0.27 or 0.54% of 234 chitosan at 2 and 4 minutes (Figure 4). At 7 minutes, which is above the optimum frying time, the reduction in acrylamide formation was dependent on the percentage of chitosan, 235 <u>236</u> being more effective at 0.54 than 0.27%. It is generally known that water content is a key <u>237</u> factor that has to be considerate in fried products in terms of acrylamide formation. Chitosan, 238 as a hydrocolloid, joins water, but water content of fried samples was not a significant 239 variable in acrylamide formation in this study. Chitosan did not significantly modified water 240 content of fried samples (p-value= 0.9725), but, as was expected, frying time was a significant factor (p-value=0.0000, F-ratio=60.99). Values of percentage of moisture content 241 <u>242</u> at 2, 4 and 7 minutes were 20 ± 2^a , 17 ± 2^b , 5.8 ± 1.9^c for control samples; 21 ± 3^a , 16.3 ± 0.6^b , $4.5\pm1.8^{\circ}$ when 0.27% of chitosan was added, and $22\pm2^{\circ}$, $16\pm2^{\circ}$, $4.4\pm0.2^{\circ}$ for 0.54% of <u>243</u> 244 chitosan.

Figure 5 shows that at similar heating times, $85\pm9\%$ of reduction was the highest inhibitory rate found in model systems when 1% of chitosan was present in the medium. In fried batter systems the inhibition rate reached by adding chitosan to batter formulation was about $60\pm7\%$ regardless of the percentage of chitosan tested (0.27 and 0.54%). These are excellent results as compared to other hydrocolloids tested in real foods, i.e., the maximum inhibitory rate reported by Zeng et al. (2010) that tested the addition of different hydrocolloids to the formulation of a cracker, was 43% when 5% of pectin was incorporated to the formula.

<u>252</u> **4.** Conclusion

253 Adding small amounts of chitosan in model and fried batter systems has been proven to be a 254 new way to mitigate the generation of acrylamide. In fried batters, 0.27% of chitosan was 255 capable of reducing the content of acrylamide in the final product by 59% and in model <u>256</u> systems, the reduction depended largely on the reducing sugar tested, but to an even greater 257 extent, on the percentage of chitosan, especially when fructose was present in the medium 258 (up to 85%). The proposed mechanism of acrylamide reduction is based on the richness of 259 amino groups of chitosan, which compete with asparagine amino groups to bind carbonyls (e.g. reducing sugars), the first stage of acrylamide formation. For this reason, chitosan has a 260 <u>261</u> high potential to provide consumers with healthy food products (lower acrylamide content) <u>262</u> if it is incorporated into batters on a commercial scale.

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 <u>352</u> Inhibition of acrylamide formation by vitamins in model reactions and fried potato
 <u>353</u> strips. *Food Chemistry*, *116*(1), 34–39.
- <u>354</u>
- <u>355</u>

- 356 **Table 1.** Multifactor ANOVA for Acrylamide content (mg/Kg) of main effects and their
- <u>357</u> interactions in model systems.

MAIN EFFECTS	<u>Df</u>	F-Ratio
рН	1	0.13 (NS)
Reducing Sugar	2	54.86**
Time (min)	5	175.00**
Chitosan (%)	2	618.45**
Temperature (°C)	1	624.55**
INTERACTIONS	<u>Df</u>	F-Ratio
pH- Reducing sugar	2	6.01**
pH- Time	5	4.18**
pH-Chitosan	2	4.43*
pH- Temperature	1	1.39 (NS)
Reducing sugar-Time	10	5.26**
Reducing sugar-Chitosan	4	17.61**
Reducing sugar-Temperature	2	2.56 (NS)
Time- Chitosan	10	29.79**
Time -Temperature	5	41.27**
Chitosan-temperature	2	77.67**

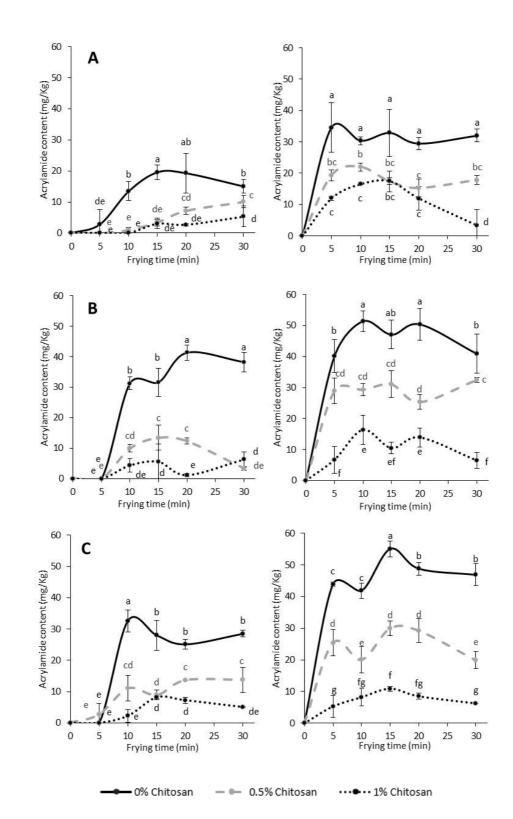
**Statistical significance \geq 99% (p-value ≤ 0.01); *Statistical significance \geq 95% (p-value ≤ 0.05); NS (not statistical significance, p-value > 0.05). Df: degrees of freedom

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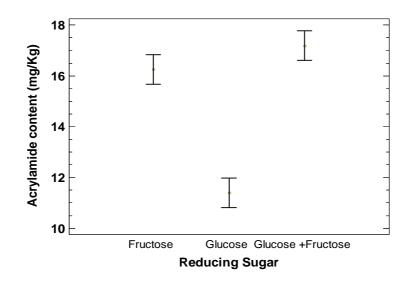
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Figure 1. Average acrylamide content (mg/Kg) generated in model systems with 0, 0.5 and 1% of chitosan, pH 4 at 150°C (left) and 180°C (right) after 5, 10, 15, 20 and 30 minutes of frying. (A) asparagine-glucose; (B) asparagine-fructose; (C) asparagine-glucose-fructose. Error bars represent standard deviations (n=3). Homogeneous groups are represented by the same letter.

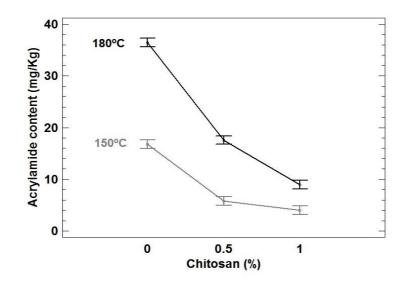


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370 Figure 2. Influence of the type of reducing sugars tested on acrylamide formation (mg/Kg) in model

<u>371</u> systems. Error bars represent 95% LSD (Least significance difference).

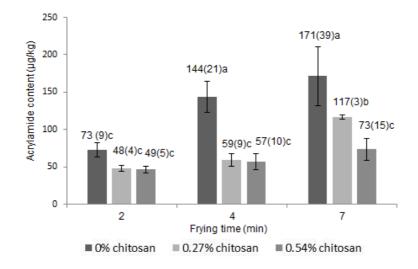
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374 Figure 3. Influence of process temperature (150 and 180°C) and chitosan content (0, 0.5 and 1%) on
375 acrylamide formation (mg/Kg) in model systems. Error bars represent 95% LSD (Least significance
376 difference).

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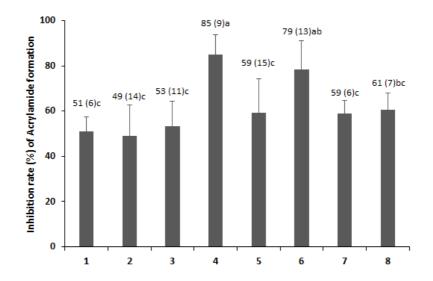


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380 Figure 4. Acrylamide content (mean and standard deviation) in fried batter systems with 0, 0.27 and

- <u>381</u> 0.54% of chitosan at 2, 4 and 7 minutes. Homogeneous groups are represented by the same letter.
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386 Figure 5. Inhibitory effect of chitosan (%) (mean and standard deviation (n=3)) on acrylamide
387 formation in model systems (after 5 minutes of reaction time) and fried batter systems (after 4
388 minutes of frying) at 180°C. X-axis legend: (1) (2) asparagine-glucose and 0.5 or 1% of chitosan; (3)
389 (4) asparagine-fructose and 0.5 or 1% of chitosan; (5) (6) asparagine-glucose-fructose and 0.5 or 1%
of chitosan; (7) (8) fried batters with 0.27 or 0.54% of chitosan. Homogeneous groups are
391 represented by the same letter.

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